

PERFORMANCE AND NO<sub>X</sub> MODELLING IN A  
DIRECT INJECTION STRATIFIED CHARGE ENGINE

by

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ABSTRACT

A model has been developed to predict the performance and NO<sub>X</sub> emission of the Texaco stratified charge engine. This complete engine cycle program starts from engine geometry, valve and fuel injection timing, fuel characteristics and operating conditions and includes the following phases: valve overlap, intake, compression, combustion, expansion and exhaust.

The fuel mixing process is described by a jet mixing model and the equations are solved in a cylindrical coordinate system with a non-uniform pressure field. The jet shape changes were calculated for the jet impingement effect against a solid wall. The air motion inside the cylinder is determined by a detailed model to specify the field for the fuel jet.

During combustion fuel jet is divided into many elements and the combustion process of each element is analyzed as a mixing process between the jet and surrounding air, entrainment into a flame front and subsequent combustion.

For heat transfer the walls of the combustion chamber are divided into five regions; intake valve, exhaust valve, cylinder head, cylinder wall and piston top. Each region is assumed to have a different temperature and different gas velocity.

Nitric oxide emissions are calculated by using the extended Zel'dovich kinetic scheme, with the steady state assumption for the N concentration and equilibrium values used for H, O, O<sub>2</sub> and OH concentrations.

The model computes combustion rates, heat transfer and NO<sub>X</sub> based on the same jet mixing assumptions without appeal to separate mixing processes at each stage.

Comparison of the model prediction with the available experimental data shows reasonably good agreement.

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## SYMBOLS

- A = heat transfer area  
Bore = cylinder bore diameter  
b = jet radius in free jet  
 $b_c$  = jet radius when contacting with wall  
 $c_p$  = specific heat at constant pressure  
E = internal energy  
H = specific enthalpy  
h = distance from cylinder head to piston top  
 $L_{cnr}$  = length of connecting rod  
M = mass  
N = engine speed  
Nu = Nusselt number  
P = pressure  
Q = heat transfer to system  
R = radial distance of jet location  
 $R_c$  = radius of piston cup  
Re = Reynolds number  
 $R_g$  = gas constant  
 $R_p$  = radius of piston  
 $R_{cr}$  = radius of crank  
s = distance along the jet trajectory  
 $S_e$  = plume surface area  
T = temperature  
u = jet velocity

$u_e$  = turbulent eddy entrainment velocity  
 $V$  = volume  
 $V_c$  = piston cup volume  
 $v_i$  = parallel component of cross flow to  $u$   
 $v_n$  = normal component of cross flow to  $u$   
 $v_r$  = radial component of jet (swirl) velocity  
 $v_z$  = vertical component of jet (swirl) velocity  
 $w$  = angular velocity of jet (swirl)  
 $W$  = work done by system  
 $X_f$  = mass fraction of fuel in jet  
 $Z$  = axial distance of jet location  
 $\alpha$  = entrainment parameter for the parallel flow  
 $\beta$  = entrainment parameter for the normal flow  
 $\rho$  = density  
 $\phi$  = equivalence ratio  
 $\theta$  = tangential component of jet location  
 $\theta_i$  = fuel injection timing  
 $\theta_j$  = jet contacting angle with wall (see Fig. 4)  
 $\theta_{cr}$  = crank angle (0 at top dead center)  
 $\lambda$  = Taylor microscale  
 $t_c$  = characteristic reaction time for the microscale

**Subscripts**

i = element number i  
in = inflow  
out = outflow  
e = entrained gas in the plume  
b = burned gas in the plume  
u = unburned gas in the plume  
 $\infty$  = the gas surrounding the jet

## I Introduction

The name, Texaco Controlled Combustion System (TCCS) is used to describe a spark ignited, direct injection, stratified charge engine. The combustion chamber is a deep cup in the piston; relatively higher air swirl is used. This engine may be thought of as a cross between the homogeneous charge, spark-ignition gasoline engine, and the heterogeneous charge, compression-ignition diesel engine. However, since combustion timing is controlled by fuel injection rates; the combustion process more nearly approximates that of an open chamber diesel engine. This engine concept appears to have the well controlled, soft combustion of the spark-ignition engine and, thereby, the lightweight structure of the gasoline engine. The TCCS concept also demonstrates excellent fuel economy, broad fuel tolerance, (multi-fuel capability) and relatively low emissions. The basic conceptual details behind the Texaco Controlled Combustion System are described below while additional hardware details can be found in the references on the TCCS engine (1-4).

### TCCS Engine Description

The Texaco Controlled Combustion System, as illustrated in Fig. 1, requires coordination of air swirl, fuel-injection and positive ignition. The high air swirl is obtained from a shrouded inlet valve and is amplified during compression by being forced into a deep narrow

combustion chamber. The combustion chamber is essentially a cup having a cylindrical upper section with toroidal bottom cast into the head of the piston. The diameter of the cup is approximately one half of the cylinder diameter.

The high pressure injection system is based on standard diesel practice and uses a special version of a standard Roosa Master Pencil Nozzle. The distinguishing feature of this nozzle is a special flat seat and a single-hole orifice instead of the more usual conical seating, multi-hole sac-tip design. Valve opening pressure is usually set at 1500-2000 psi. For full load, fuel injection duration corresponds approximately to the time for one air swirl and the overall fuel-air ratio is near stoichiometric. At lower loads, obtained by decreased fuel injection duration and quantity, the operation is lean of stoichiometric and over all air to fuel ratio approaches 100:1 at idle conditions.

The usual diesel engine problems of long ignition delay, high rates of pressure rise and high peak pressures with low cetane fuels are avoided in TCCS operation by providing a positive ignition source. The Texaco Ignition System (TTIS) is a high energy, multi-spark unit with controlled duration. The ignition is triggered near the start of injection and continues through part or all of the injection process. The problems of spontaneous ignition and octane requirement associated with conventional gasoline engines is eliminated with TCCS since the residence time of combustible fuel-air mixtures is extremely short.

The TCCS mode of operation thus results in unique characteristics;

high part-load thermal efficiency at lean mixtures and inherently low hydrocarbon and carbon monoxide emissions resulting from excess air operation and controlled combustion rates. In addition, with the high pressure injection system, a wide range of fuel volatility can be tolerated. High compression ratio and/or inlet super charging can be used to produce good operation and performance on low cost fuels. These characteristics, in addition to quick warm-up and excellent driveability are significant factors in achieving an automotive engine with good performance and low exhaust emissions.

The purpose of the research work to be described in the following pages has been to develop a model to predict the performance of the TCCS, stratified charge engine given the engine geometry, operating parameters and the fuel properties. Once the model is shown to be effective in predicting the performance and  $\text{NO}_x$ , it can then be used as a design tool. With the brief description of the geometry and the mode of operation of the engine given above, we will now proceed to a discussion of the model.

## II. Direct Injection Engine Simulation Model

### 1. Background

In the direct fuel injection engine, a distribution of temperature and equivalence ratio exists inside the combustion chamber. Since formation of  $\text{NO}_x$  is very much dependent on the local equivalence ratio and temperature, the key problem for this engine simulation is to define the spacial and temporal distribution of these parameters.

Early diesel engine combustion models include work by Lyn (6) and he developed an empirical calculation of the heat release rate by using triangles to simulate mixing and combustion of successive burned elements. Shahed, et. al. (7) integrated this idea with assumptions that have been widely used in spark ignition engine models (8,9) to compute  $\text{NO}_x$ . In this model, the fuel is assumed to mix with a stoichiometric amount of air before combustion and the mixed gas is divided into many packaged elements which are not mixing with each other. The temperature distribution inside the combustion chamber was explained by the different combustion time of each element. Bastress (34) took into consideration the distribution of equivalence ratio inside the combustion chamber, but this model is not based on physical mixing and combustion processes.

Following this work much effort was placed on developing physical arguments to compute the heat release rate proposed by Lyn. Shipinski (10), Whitehouse (11) and Bracco (12) have explained this delay by using fuel droplet evaporation models. But it is apparent that the combustion

process in direct injection engines cannot be predicted only by evaporation time.

Spray formation and mixing in engines was studied using continuum models by Adler (13) and Rife (14). Rife concludes that the motion of the fuel jet can be satisfactorily analyzed with such a model, but this model was not integrated into a combustion calculation.

Hiroyasu (15) made a complete heterogeneous mixture combustion model by assuming a simple cone shaped spray model and a more extensive jet mixing model, which included the effects of cross flow and jet tip shape, was developed by Chiu (16). These models do not include any adjustments of the fuel jet on the wall of the combustion.

Much of the work on heterogeneous combustion is based on gas turbine engine models. Stochastic techniques appear to be a powerful method (17, 18) for including the mixing phenomena in a statistical way. Further, the mixing rates have a physical basis. However, the models lack the geometric detail required for design and consequently have somewhat limited utility. In addition, these models require an enormous computing time in the case of reciprocating engines because of the way the combustion chamber air motion changes with crank angle. It is also possible that air motion inside the reciprocating engine is complicated enough to require more than a single mixing parameter.

In previous work, a model of the TCCS engine was developed by Jain (19). In our first extension of this model to compute  $\text{NO}_x$ , the

combustion chamber is divided into two areas; one a hot burned gas area, the other cold air. Each zone was considered to have uniform equivalence ratio and temperature.  $\text{NO}_x$  was calculated by using extended Zel'dovich equations. Values for the  $(\text{NO}_x)$  concentration obtained from this calculation are very low and this result was assumed to be due to the following reasons:

- a) During the rapid combustion process, fixed equivalence ratio (1.4) for the combustion zone was assumed.  $(\text{NO}_x)$  concentration and one way reaction rates decrease sharply as equivalence ratio goes above  $1.1 \sim 1.2$ .
- b) The model assumed temperature constant inside the plume thereby making the  $(\text{NO}_x)$  concentration even lower, when compared with the actual case where a temperature distribution is known to exist.

Consequently we focused our attention on a new model that would include the mixing process through appeal to the equations of motion for a turbulent jet.

## 2. The New Model

The model divides the complete engine cycle into the following periods:

- i) valve overlap period
- ii) intake period
- iii) compression period
- iv) combustion period
- v) expansion period
- vi) exhaust period

Also the engine cycle is divided into the following items based on physical phenomena:

- i) gas exchange
- ii) heat transfer
- iii) air motion inside the cylinder
- iv) fuel jet dynamics
- v) heat release
- vi) NO<sub>x</sub> formation
- vii) friction loss

The great benefit of this program is to be able to calculate the jet

dynamics coupled with the surrounding air motion, as a basis for calculation of the heat release rate, the  $\text{NO}_x$  formation and heat transfer between jet elements and combustion wall.

The computer program is based on the following assumptions;

- i) Temperatures in the cylinder are functions of time and location.
- ii) Pressures in the cylinder are functions of time only.
- iii) The charge is assumed homogeneous during intake, compression and exhaust process. (During combustion, the fuel jet is divided into 7-15 elements and each element has a different location and different equivalence ratio.)
- iv) The individual elements in the gas mixture are homogeneous but each has two different temperature zones, i.e., burned and unburned mixture. The unburned gas is composed of a low temperature mixture of air, non-reacting fuel and residual gases. The combustion zone is composed of high temperature unburned mixture and combustion products.
- v) There is mixing between jet elements and their environment, but no mixing between jet elements themselves.
- vi) Quasi-steady adiabatic and isentropic flow is assumed for mass flows past the valves.
- vii) The intake and exhaust manifolds are treated as infinite plenums having specified pressure and temperature histories, except during reversed flow past the intake valve, when plug flow is assumed to occur.

viii) Heat transfer is predicted with a model based on concepts introduced by Woschni(20) that have been extended to use local velocities in the combustion chamber.

ix) Thermodynamic characteristics of gas are based on a model proposed by Martin and Heywood(21).

x) Nitric oxide emissions are calculated by using the extended Zel'dovich kinetic scheme, with the steady state assumption for the N concentration and equilibrium values used for H, O, O<sub>2</sub>, and OH concentrations in the adiabatic core.

### 3. Systems and Thermodynamic Equations

The early complete engine cycle simulation by Borman(22) assumed that the combustion gas as one uniform mixed element. In our model air and fuel are divided into many elements and every element has the same set of system and thermodynamic equations. A schematic of our model is shown in Fig. 2. Every element is viewed as an open system. \*

i) State equation:

$$\begin{aligned} PV_i &= M_i R_{gi} T_i \\ \frac{\dot{P}}{P} + \frac{\dot{V}_i}{V_i} &= \frac{\dot{M}_i}{M_i} + \frac{\dot{T}_i}{T_i} \end{aligned} \quad (3-1)$$

$R_{gi} = R_{gi}(T_i, P, \phi_i)$  - constant during each computing interval

ii) Mass conservation:

$$\dot{M}_i = \dot{M}_{in_i} - \dot{M}_{out_i} \quad (3-2)$$

iii) Energy conservation for open system:

$$\dot{E}_i = \dot{Q}_i - \dot{W}_i + \dot{M}_{in_i} H_{in_i} - \dot{M}_{out_i} H_{out_i} \quad (3-3)$$

---

\*All symbols are defined on pages 10 and 11.

iv) Internal energy equations:

$$\begin{aligned} E_i &= M_i H_i - PV_i \\ \dot{E}_i &= \dot{M}_i H_i + M_i \dot{H}_i - \dot{P}V_i - P\dot{V}_i \end{aligned} \quad (3-4)$$

v) Work definition:

$$\dot{W}_i = \dot{P}V_i \quad (3-5)$$

vi) Enthalpy definition:

$$\dot{H}_i = C_{pi} \dot{T}_i$$

$$C_{pi} = C_{pi}(T_i, P, \phi_i) - \text{constant during each computing interval} \quad (3-6)$$

vii) Volume constraint:

$$\dot{V}_1 + \dot{V}_2 + \dots + \dot{V}_n = \dot{V} \quad (3-7)$$

viii) From geometry:

$$\begin{aligned} \dot{V} &= R_{cr} \times \sin\theta_{cr} + L_{cnr} \times \frac{(R_{cr}/L_{cnr})^2 \times \sin\theta_{cr} \times \cos\theta_{cr}}{\sqrt{1-(R_{cr} \times \sin\theta_{cr}/L_{cnr})^2}} \\ &\quad \times Bore^2 \times \frac{\pi}{4} \times \frac{d\theta_{cr}}{dt} \end{aligned} \quad (3-8)$$

Values of  $Q_i$ ,  $M_{in_i}$  and  $M_{out_i}$  are given from several subprograms in advance before these differential equations will be solved. Total number of unknowns is  $N$  elements  $\times$  6 values ( $E_i$ ,  $M_i$ ,  $H_i$ ,  $V_i$ ,  $W_i$  and  $T_i$ ) + 2 ( $P$  and  $V$ ). Since the total number of differential equations is  $N$  elements  $\times$  6(Eq.(1) ~ Eq.(6)) + (Eq. (17) and Eq. (8)), these differential equations can be solved.

In the computer program these differential equations are solved according to the following procedure:

We get  $V_i$  from Eq. (1) ~ Eq. (6)

$$\begin{aligned} \dot{V}_i &= \frac{V_i}{M_i C_p T_i} (Q_i + M_{in_i} H_{in_i} - M_{out_i} H_{out_i} - (M_{in_i} - M_{out_i}) H_i) \\ &\quad + \frac{M_{in_i} - M_{out_i}}{M_i} V_i + \left( \frac{V_i^2}{M_i C_p T_i} - \frac{V_i}{P} \right) P \end{aligned} \quad (3-9)$$

Substituting  $V_i$  in Eq. (7) by Eq. (9), we get

$$\dot{P} = (V - A)/B \quad (3-10)$$

where

$$\begin{aligned} A &= \sum_{i=1}^n \frac{V_i}{M_i C_p T_i} (Q_i + M_{in_i} H_{in_i} - M_{out_i} H_{out_i} - (M_{in_i} - M_{out_i}) H_i) \\ &\quad + \frac{M_{in_i} - M_{out_i}}{M_i} V_i \end{aligned} \quad (3-11)$$

$$B = \sum_{i=1}^n \left( \frac{v_i^2}{M_i C_p T_i} - \frac{v_i}{P_i} \right) \quad (3-12)$$

#### 4. Jet Model

From the study of diesel combustion in a rapid compression machine by Rife and Heywood(14), it can be concluded that the fuel jet breaks into droplets near the nozzle orifice and the relative velocity of droplets in the jet flow is small. This means the mixing between packaged jet elements themselves is not important and only mixing between jet elements and surrounding air is taken into consideration. From the characteristics lengths analysis by Jain(19) he concluded that most of the droplets can evaporate before reaching the spark plug. Thus the model that fuel ignition is initiated by the spark plug and heat release is controlled only by mixing is now justified.

The mixing model is based on the turbulent entrainment assumptions of Hoult and Weil(23). The rate of entrainment for turbulent plumes introduced by Hoult and Weil have been modified to include the effects of large density variations, as suggested by Ricou and Spalding(24) and Escudier(25).

For the application of these turbulent entrainment theories to reciprocal engines, three more new aspects were added to them.

- 1) The  $\text{NO}_x$  value is not determined only by the present gas characteristics, but also it is very much dependent on the previous histories of gas characteristics. For this purpose jet model is solved by using the packaging method in order to identify every jet element at any instant.
- 2) All the previous jet models were set in a two-dimensional cartesian coordinate system. However, a cylindrical coordinate system is much more appropriate for reciprocal engines. The most important difference between these two systems is that the pressure field is not constant any more in the cylindrical coordinate system, especially in high swirl ratio engines. Jet elements, thus, are affected by the surface forces from the non-uniform pressure field and these surface forces have the same magnitude but opposite direction of the centrifugal forces when the jet elements have the same density and angular velocity as the surrounding air.

- 3) Restrictions of the combustion wall were taken into account. The cross section geometry of the jet was assumed to be in the shape of a D (Fig. 4) when it is contacting with the wall with the same centerline position and cross section area of the cylindrical jet. This consideration proved to have a good advantage for determining jet trajectory and heat transfer rate between jet elements and the combustion wall.

Let us consider a jet element "1" into a quiescent atmosphere of

element "∞" in the absence of any chemical reaction (Fig. 3). Then, the general equations of the jet model reduce to the following.

i) Conservation of mass

when jet is not contacting with the wall

$$\frac{1}{dt} \cdot \frac{1}{ds} (\rho \pi b^2 u) = (\rho / \rho_\infty)^{1/2} \rho_\infty 2\pi b (\alpha |u - v_i| + \beta |v_n|) \quad (4-1)$$

when jet is contacting with the wall

$$\frac{1}{dt} \cdot \frac{1}{ds} (\rho \pi b^2 u) = (\rho / \rho_\infty)^{1/2} \rho_\infty 2\pi b_c (1 - \frac{\theta_j}{2\pi}) (\alpha |u - v_i| + \beta |v_n|) \quad (4-1)$$

$\theta_j$ : jet contacting angle with the wall (see Fig. 4)

$$\text{Max. of } \theta_j = \pi$$

ii) Conservation of angular momentum

$$\frac{d}{dt} (\rho \pi b^2 u R w_s) = R w_s \frac{d}{dt} (\rho \pi b^2 u) - \rho \pi b^2 u v_r w \quad (4-2)$$

$w_s$ : angular velocity of swirl

$\rho \pi b^2 u v_r w$ : coriolis force

iii) Conservation of radial direction momentum

$$\frac{d}{dt}(\rho \pi b^2 u v_r) = \rho \pi b^2 u R w^2 - \rho_\infty \pi b^2 u R w_s^2 + v_{R\infty} \frac{d}{dt}(\rho \pi b^2 u) \quad (4-3)$$

$\rho \pi b^2 u R w^2$ : centrifugal force

$\rho_\infty \pi b^2 u R w_s^2$ : force arising from pressure gradient swirling flow

iv) Conservation of vertical direction momentum

$$\frac{d}{dt}(\rho \pi b^2 u v_z) = v_{z\infty} \frac{d}{dt}(\rho \pi b^2 u) \quad (4-4)$$

v) From geometry

$$u \frac{du}{dt} = R_w^2 \frac{dw}{dt} + R w^2 \frac{dR}{dt} + v_r \frac{dv_r}{dt} + v_z \frac{dv_z}{dt} \quad (4-5)$$

$$\frac{dR}{dt} = v_r \quad (4-6)$$

vi) Conservation of fuel

$$\frac{d}{dt}(\rho \pi b^2 u X_f) = 0 \quad (4-7)$$

vii) Jet is in the combustion chamber

$$\text{Jet location } (R, \theta, Z) \leq \text{combustion chamber} \quad (4-8)$$

viii) For contacting angle  $\theta_j$

$$\pi b^2 = \pi b_c^2 \times \left(1 - \frac{\theta_j}{2\pi}\right) + \frac{b_c^2}{2} \sin \theta_j \quad (4-9)$$

## 5. Air Motion Surrounding the Jet

Calculation of gas velocity surrounding the jet is required to define the jet trajectory and mixing ratio between the jet and gas. A first order calculation was made by M. Martin(21). This model is limited to the regions close to the cylinder wall or piston by the assumptions and the model can be extended to the whole region inside the cylinder for our purpose. Since an exact solution including viscous effects is difficult and time-consuming, several assumptions are necessary for simplification of this model.

i) The combustion chamber is divided into three regions (Fig. 6);

Inside each region, axial velocity is uniform on the same horizontal plane, radial velocity and angular velocity is uniform on the same radius.

ii) In region (3) there is no radial velocity.

This assumption is necessary in order to avoid a large velocity discontinuity at the piston cup edge due to a large area discontinuity there.

iii) Boundary conditions.

Axial velocity = 0 at cylinder head,  
 radial velocity = 0 at cylindar wall,  
 and axial velocity is the same as piston at piston surface.

iv) Swirl at bottom center is solid body rotation.

v) Angular momentum is not conserved.

After precisely checking the pictures (26) of the rapid compression machine it was found that the swirl amplitude (the ratio of swirl at TDC to swirl at BDC) decreases when swirl magnitude goes up. Under normal Texaco engine operation (swirl ratio is  $3.65 \times \text{rpm}$  at BDC), this swirl decaying is about 10%. The following equation is used for estimating swirl decaying:

$$\frac{\text{swirl momentum decayed}}{\text{initial swirl momentum}} = C_{DE} \times w^2 \times \text{Time}$$

$C_{DE}$ : swirl decaying factor  $6.5 \times 10^{-6}$  for Texaco engine

w: angular velocity (rad/sec)

Time: time since intake valve closes (sec)

(1) Calculation of Radial Velocities (Fig. 6)

(a)  $R_c < r < R_p$ 

$$\frac{dM_2}{dt} = - \frac{dM_1}{dt} = 2\pi rh\rho \bar{v}_r \quad (5-1)$$

$$M_1 = \pi(R_p^2 - r^2) h\rho \quad (5-2)$$

$$M_2 = (\pi r^2 h + v_c)\rho \quad (5-3)$$

 $M_i$ : the mass in control volume i

t: time

 $\rho$ : density of the charge $v_c$ : piston cup volume

Combining (5-1), (5-2) and (5-3)

$$(\pi r^2 h + v_c)\rho' + \pi r^2 \rho h' = - \pi(R_p^2 - r^2) (h'\rho + \rho'h)$$

$$\rho' = -\left(\frac{h'}{K_1 + h}\right)\rho \quad (5-4)$$

when  $K_1 = \frac{V}{\pi R_p^2}$  (5-5)

Let  $X = \frac{h}{K_1}$  (5-6)

Then solving for  $\rho$  in terms of initial conditions at time  $t_0$  yields

$$\rho(t) = \rho(t_0) \left( \frac{x(t_0) + 1}{x(t) + 1} \right) \quad (5-7)$$

From Eq. (5-1) and (5-2) we have

$$\bar{v}_r = \frac{-\frac{dM_1}{dt}}{2\pi rh\rho} = \frac{-\pi(R_p^2 - r^2)(h'\rho + \rho'h)}{2\pi rh\rho}$$

Using (5-4) and letting

$$v_p = \frac{dh}{dt} = \text{piston velocity (upward velocity has negative sign)}$$

We find

$$\bar{v}_r(r, t) = -\left(\frac{r}{2K_1}\right)\left[\left(\frac{R_p^2}{r^2}\right) - 1\right] \frac{v_p(t)}{X(t)(1+X(t))} \quad (5-8)$$

(b)  $0 < r < R_c$

The radial velocity inside the piston cup is assumed to be zero.

$$\frac{dM_2}{dt} = -\frac{dM_1}{dt} = 2\pi rh\rho\bar{v}_r \quad (5-9)$$

$$k_2 = v_c / (\pi R_c^2) \quad (5-10)$$

$$M_1 = \pi(R_p^2 - r^2) h\rho + \pi(R_c^2 - r^2) k_2 \rho \quad (5-11)$$

$$M_2 = \pi(h + k_2)r^2 \rho \quad (5-12)$$

Combining (5-9), (5-11) and (5-12)

$$\pi(h + k_2)r^2 \rho' + \pi r^2 \rho h' = -\pi(R_p^2 - r^2)(h'\rho + h\rho')$$

$$-\pi(R_c^2 - r^2)k_2 \rho'$$

$$\rho' = -\left(\frac{h'}{k_1 + h}\right)\rho \quad (5-13)$$

From Eq. (5-9) and (5-12) we have

$$\bar{v}_r(r, t) = \left(\frac{r}{2k_1}\right) \frac{\left(\frac{k_2}{k_1} - 1\right)}{X(t)} \frac{v_p(t)}{(1 + X(t))} \quad (5-14)$$

## (2) Calculation of Axial Velocities

(a)  $0 < Z < h$

$$-\frac{dM_1}{dt} = \frac{dM_2}{dt} = \pi R_p^2 \bar{v}_z \rho \quad (5-15)$$

$$M_1 = \pi R_p^2 \rho Z \quad (5-16)$$

$$M_2 = \pi R_p^2 \rho (h-z) + v_c \rho \quad (5-17)$$

We assume

$$\bar{v}_{z1}(Z, t) = v_p Z/h \quad \text{for } R_c < r < R_p \quad (5-18)$$

From (5-15), (5-16), (5-17) and (5-18) we have

$$\bar{v}_{z2}(Z, t) = v_p Z/h \left\{ 1 - \left( \frac{R_p}{R_c} \right)^2 \frac{1}{(X(t) + 1)} \right\} \quad \text{for } 0 < r < R_c \quad (5-19)$$

(b)  $h < Z$

$$-\frac{dM_1}{dt} = \frac{dM_2}{dt} = \pi R_c^2 \bar{v}_z \rho \quad (5-20)$$

$$M_1 = \pi R_p^2 h + \pi R_c^2 (Z-h) \quad (5-21)$$

$$M_2 = \pi R_c^2 (k_2 - (Z-h)) \quad (5-22)$$

From (5-20), (5-21) and (5-22) we have

$$\bar{v}_z(Z, t) = \frac{k_1 - k_2 + Z}{k_1 + h} v_p \quad (5-23)$$

## (3) Calculation of Angular Velocity

The gas angular velocity inside the cylinder is assumed to be a solid body rotation.

From momentum equation

$$\begin{aligned}
 & \underbrace{\int_0^{R_p} \int_0^h \int_0^{2\pi} \rho w r^3 d\theta dz dr}_{\text{momentum in region (1)}} + \underbrace{\int_0^{R_c} \int_0^{k_2} \int_0^{2\pi} \rho w r^3 d\theta dz dr}_{\text{momentum in region (2)}} \\
 & = (1 - \text{DECAY}) \times \left[ \underbrace{\int_0^{R_p} \int_0^h \int_0^{2\pi} \rho_o w_o r^3 d\theta dz dr}_{\text{initial momentum}} + \underbrace{\int_0^{R_c} \int_0^{k_2} \int_0^{2\pi} \rho_o w_o r^3 d\theta dz dr} \right] \quad (5-24)
 \end{aligned}$$

DECAY: swirl decaying ratio

From Eq. (5-24)

$$\begin{aligned}
 w(t) &= (1 - \text{DECAY}) \times \frac{\rho_o}{\rho} \times \frac{\frac{k_2 R_c^4}{4} + \frac{h_o R_p^4}{4}}{\frac{k_2 R_c^4}{4} + h R_p^4} w_o \\
 &= (1 - \text{DECAY}) \times \frac{(h + k_1)}{(h_o + k_1)} \times \frac{\frac{k_2 R_c^4}{4} + \frac{h_o R_p^4}{4}}{\frac{k_2 R_c^4}{4} + h R_p^4} w_o \quad (5-25)
 \end{aligned}$$

Figure 7 and Fig. 8 are the calculation results using these assumptions. At -50 BTDC gas movement is dominated by the piston velocity and swirl. The radial velocity is almost negligible. At - 30 BTDC, the radial velocity begins to grow as the gas in the squish area is forced into the piston cup. At -10 BTDC, the piston is almost stopped and the radial velocity, especially at the edge of the piston cup, is very high. Squish effect can be computed from this study. This more detailed study in general confirms the basic conclusions of Martin but provides more detailed specification of the flows for jet mixing analysis.

## 6. Combustion Model

From the observation of pictures in the rapid compression machine it was found that the unburned gas mixture hitting the spark plug has a small plume first and this plume grows, entraining surrounding unburned gas mixture. The main flame can be seen a little bit downstream from the spark plug and this ignition delay time is about 0.7 - 0.8 msec at 2000 rpm. These phenomena are also verified by log P-log V diagrams shown in Marsh thesis(27). A mixing and chemical induction time seems to be associated with this delay and the order of magnitude is similar to the delay in a spark ignition engine.

To explain the combustion delay mentioned above, an analytical model for combustion reaction time was developed. In this model a fuel-air

element starts to burn when it hits the spark plug but the fuel in the jet element doesn't burn instantaneously because of finite flame speed and a typical induction period. In the early stages of combustion growth, this burning nucleus is so small that this stage can be treated as if there were no combustion. The schematic of this model applied to the TCCS engine is shown in Fig. 9.

### i) Entrainment of unburned mixture

The entrainment of the surrounding gas mixture into the burning nucleus has been treated with an analysis based on the work of Blizzard and Keck(28) which relates the turbulent eddy entrainment velocity to the engine speed.

The mass rate of entrainment of surrounding gas mixture can be given as

$$\frac{dM_e}{dt} = \sqrt{\rho_u \rho_b} * Se * U_e \quad (6-1)$$

where  $Se$  is plume surface area and  $U_e$  the turbulent eddy entrainment velocity. In the Blizzard and Keck model, the entrainment velocity is based on the velocity of the inlet jet. However, in the TCCS geometry, entrainment into the spark nucleus is dominated by the velocity of the fuel jet

$$U_e \approx 0.22u \quad (6-2)$$

ii) Combustion delay

Tabaczynski(29) computed a characteristic reaction time ( $\tau$ ) for a large eddy using a characteristic reaction time ( $\tau_c$ ) defined for an eddy of the order of the turbulent microscale. The rate of mass burned in an individual eddy is assumed to be proportional to the mass of unburned gas that exists in the plume

$$\frac{dM_b}{dt} = \frac{M_u}{\tau_c} = \frac{M_e - M_b}{\tau_c}$$

$M_e$ : entrained gas in the plume

$M_b$ : burned gas in the plume

$M_u$ : unburned gas in the plume

$\tau_c = \lambda / Se$  characteristic reaction time for the microscale

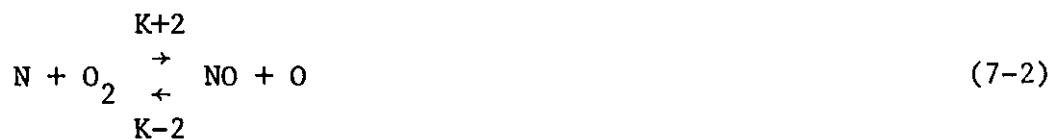
$\lambda$ : Taylor microscale

$$\lambda = 0.17 \times \frac{\text{intake valve lift}}{\text{compression ratio}} \quad (\text{Ref. (28) and (30)})$$

$Se$ : laminar flame speed (Ref. (28))

## 7. NO<sub>x</sub> Model

The NO<sub>x</sub> formation model is based on the same model as combustion mentioned before which is composed of unburned gas mixture outside flame front, burning zone and burned gas. But the temperatures of these zones are defined by only two typical temperatures: burned and unburned gas temperatures, by decoupling the burning zone into these two temperature zones. Figure 12 shows the mass histories of these zones during the period from the fuel injection to fully developed plume. As can be seen, the burning zone is very thin and disappears quickly, and this zone is proved not to have much effect on NO<sub>x</sub> amount by computer simulation. This model also calculates the transferred amount of NO<sub>x</sub> between elements by mixing. The NO formation model described by Lavoie, Heywood and Keck (32), and Komiya and Heywood (8) is used, i.e., NO formation is governed by the extended Zel'dovich mechanism:



The hydrocarbon oxidation reactions are fast relative to the NO formation process and a reasonable approximation is that the species O, O<sub>2</sub>, H, OH and N<sub>2</sub> are in equilibrium. A steady-state assumption is made for [N]. The rate of change of NO mass fraction {NO} due to chemical reaction;

$$\frac{d\{\text{NO}\}}{dt} = \frac{2M_{\text{NO}}}{\rho} \frac{(1 - (\{\text{NO}\}/\{\text{NO}\}_e)^2) R_1}{(1 + K\{\text{NO}\} / \{\text{NO}\}_e)} \quad (7-4)$$

{NO} = NO mass fraction

M<sub>NO</sub> = molecular weight of NO

$\rho$  = gas density

$$R_1 = K_{+1} (O)_e (N_2)_e = K_{-1} (N)_e (NO)_e$$

( )<sub>e</sub> = mole concentration in equilibrium

$$K = \frac{R_1}{R_2 + R_3} = \frac{K_{-1} (NO)_e}{K_{+2} (O_2)_e + K_{+3} (OH)_e}$$

## 8. Heat Transfer Model

Heat transfer calculation of the TCCS engine seems to require a more complicated model than that of the spark ignition engine, because the heterogeneous mixture causes a large temperature distribution inside the combustion chamber, and also heat transfer between the jet and piston top has an important effect on the early stage of combustion like the impingement effect. The wall inside the TCCS engine, thus, is divided into five regions as many diesel engines are so, i.e., piston top, cylinder wall, cylinder head, intake valve and exhaust valve (see Fig. 10). These temperatures are estimated as  $650^{\circ}\text{K}$ ,  $600^{\circ}\text{K}$ ,  $650^{\circ}\text{K}$ ,  $500^{\circ}\text{K}$  and  $700^{\circ}\text{K}$  respectively. Each wall of the combustion chamber is in contact with the hot, burned gas plume while the remaining are in contact with relatively cold unburned gas mixture.

All the necessary data for the heat transfer calculation like the heat transfer area of the jet elements and gas velocity at the wall are provided by the jet model calculation.

The conventional engine heat transfer correlations of Woschni(20) have been used to model the heat transfer process. The Nusselt number is expressed as;

$$\text{Nu} = 0.035 R_e^{0.8} \quad (8-1)$$

Using Woschni's relationships for gas velocities, density, viscosity and thermal conductivity, the convective heat transfer coefficient is expressed as;

$$\mu = 7014 B_{\text{ore}}^{-0.2} P^{0.8} G^{-0.53} [C_1 + 100C_2 \frac{V_T}{P_o V_o} (P - P_{is}) + C_3 v_s]^{0.8} \quad (8-2)$$

$$Q = \mu A (T - T_w) \quad (8-3)$$

$B_{\text{ore}}$ : bore

P: pressure

T: temperature

A: heat transfer area

N: engine speed

V: total volume

$v_s$ : swirl velocity

$P_o, T_o$  and  $V_o$ : pressure, temperature and volume when intake valve closes

$P_{is}$ : when compression and expansion are isentropic

Woschni used an average piston speed ( $\frac{SN}{30}$ ) as a gas velocity at the wall in his equations but the swirl velocity has a much higher magnitude than the piston speed for the Texaco engine and the swirl velocity term ( $v_s$ ) was added to them. Heat transfer is not assumed to occur between jet elements and air.

### III Comparison of Simulation Predictions with Experimental Data and Conclusions

Experimental works were performed on a TCCS engine by Marsh (27) and Fly (33). A 3-7/8" x 3-7/8" single cylinder engine designed by Texaco has been set up at the Sloan Automotive Laboratory at MIT to carry out experimental investigations on the TCCS, stratified charge concept. A brief description of the engine set up and cross-cut distillate fuel characteristics are given in Table 1-3. Additional details regarding the engine set up, data taking and data reduction can be found in their theses (27) (33).

The following comparisons of calculation results with experimental data were conducted while changing injection timing and equivalence ratio;

- i) Mass fraction burned (Figs. 15,16)
- ii) Cylinder pressure (Figs. 17,18)
- iii) NO versus injection timing (Fig. 19)
- iv) Volumetric efficiency, indicated mean effective pressure and peak pressure versus injection timing (Fig. 20)
- v) Exhaust temperature versus injection timing (Fig. 21)
- vi) NO concentration histories in each element (Fig. 23)  
(prediction only).
- vii) Swirl effects on indicated mean effective pressure and NO (Fig. 24)  
(prediction only).

As shown in these figures, every parameter except exhaust temperature was predicted accurately by this simulation model. The

major conclusions which have been drawn from this study are:

1. Ignition delays were calculated successfully by the travelling time from fuel nozzle to spark plug and induction time of unburned mixture to the burning zone.
2. The burning rate was accurately predicted by the jet mixing process based on turbulent entrainment assumptions.
3. Good agreement in cylinder pressure during compression and expansion process means that the heat transfer amount between gas and wall was accurately estimated by the model, which calculates the local gas velocities and jet contacting areas with the wall based on the Woschni correlations.
4.  $\text{NO}_x$  values were predicted within practical errors.  $\text{NO}_x$  concentration is very sensitive to the mixing process. The figure of  $\text{NO}_x$  concentration histories in each element shows that exhaust  $\text{NO}_x$  can be reduced drastically by rapid mixing after the spark plug.
5. The model predicted higher exhaust temperatures than actual data. Heat transfer calculations from gas to port seems to be necessary for precise exhaust temperature prediction.

6. Higher swirl ratio has a good effect on NO concentrations at high equivalence ratios due to the rapid cooling of burned gas. At low equivalence ratios, however, higher swirl ratio has an unfavorable effect on NO concentration due to the coincidence of higher gas temperatures and peak cylinder pressures.

7. Some more detailed calculation about air motion inside the cylinder is recommended to get more accurate NO prediction over wide range engine operations.

8. It is recommended that this model be applied for calculating another size engine performance to check this model validity.

## REFERENCES

1. Davis et. al., "Fuel Injection and Positive Ignition -- A Basis for Improved Efficiency and Economy" Paper 190A presented at SAE Summer Meeting, Chicago, June 1960.
2. Mitchell, et. al., "Design and Evaluation of a Stratified Charge Multifuel Military Engine," SAE Transactions, Vol. 77 (1968), Paper 680042.
3. Mitchell, et. al., "A Stratified Charge Multifuel Military Engine -- A Progress Report," SAE Paper 720051.
4. Alperstein, et. al., "Texaco's Stratified Charge Engine -- Multifuel, Efficient, Clean and Practical," SAE Paper 740563.
5. Canup, R.E., "The Texaco Ignition System -- A New Concept for Automotive Engines," SAE Paper 750347.
6. Lyn, W.T., "Study of the Burning Rate and Nature of Combustion in Diesel Engines," IX International Symposium on Combustion, 1962.
7. Shahed, S.M., et. al., "A Preliminary Model for the Formation of Nitric Oxide in Direct Injection Diesel Engines and It's Application in Parametric Studies," SAE Paper 730083.
8. Komiya, K and Heywood, J.B., "Predicting NO<sub>x</sub> Emissions and Effects of Exhaust Gas Recirculation in Spark-Ignition Engines," SAE Paper 730475.
9. Higgins, J., "Performance and Emission Parameter Study of a Conventional Spark Ignition Engine," MS Thesis, M.E., MIT, 1976.
10. Shipinski, J.H., et. al., "A Spray -- Droplet Model for Diesel Combustion," pp.28-35, Symposium on Diesel Engine Combustion, Institution of Mechanical Engineers, 1970.
11. Whitehouse, N.D., et. al., "A Simple Method for the Calculation of Heat Release Rates in Direct Engines Based on the Fuel Injection Rate," SAE Paper 710134.
12. Bracco, F.V., et.al., "Two Phase, Two-Dimensional, Unsteady Combustion in Internal Combustion Engines; Theoretical-Experimental Results," SAE Paper 760114.

13. Adler, D. and Lyn, W.T., "The Evaporation and Mixing of a Liquid Fuel Spray in a Diesel Engine Combustion," Institution of Mechanical Engineers, 1970.
14. Rife, J.M. and Heywood, J.B., "Photographic and Performance Studies of Diesel Combustion with a Rapid Compression Machine," SAE Paper 740948.
15. Hiroyasu, H., et. al., "Models for Combustion and Formation of Nitric Oxide and Soot in Direct Injection Diesel Engines," SAE Paper 760129.
16. Chiu, W.S., et. al., "A Transient Spray Mixing Model for Diesel Combustion," SAE Paper 760128.
17. Pompei, F., "The Role of Mixing in Burner Generated Carbon Monoxide and Nitric Oxide," MS Thesis, M.E., MIT 1972.
18. Flagan, R.C., "The Formation of Nitric Oxide from Organiz Nitrogen Contained in Fossil Fuels," PhD Thesis, M.E., MIT 1973.
19. Jain, B.C., et. al., "A Performance Model for the Texaco Controlled Combustion, Stratified Charge Engine," SAE Paper 760116.
20. Woschni, G., "A Universally Applicable Equation for the Instantaneous Heat Transfer Coefficient in the Internal Combustion Engine," Paper 670931 of SAE Transactions, 76, 30653083, 1968.
21. Martin, M.K., "Photographic Study of Stratified Combustion Using A Rapid Compression Machine," SM Thesis, MIT, 1975.
22. Borman, G.L., "Mathematical Simulation of Internal Combustion Engine Processes and Performance Including Comparisons with Experiment," PhD Dissertation, M.E., U. of Wisconsin, Madison, 1964.
23. Hoult, D.P. and Weil, W.C., "Turbulent Plume in a Laminar Cross Flow," Atmospheric Environment, Vol. 6, 1972, pp. 514-531.
24. Ricou, J.P. and Spalding, D.B., "Measurement of Entrainment by Axial Symmetric Turbulent Jets," J. Fluid Mech., 9, 21 (1961).
25. Escudier, M.P., "Aerodynamics of a Burning Turbulent Gas Jet in a Cross Flow," Combustion Science and Technology, April 1972.
26. Wong, V.W., "A Photographic and Performance study of Stratified Combustion Using a Rapid Compression Machine," pp. 68-70 and pp. 91-94, MS Thesis, M.E., MIT, 1976.

27. Marsh, G.D., "A Detailed Performance Comparison of Distillate Fuels in the Texaco Stratified Charge Engine," MS Thesis, M.E., MIT 1976.
28. Blizzard, N. and Keck, J.C., "Experimental and Theoretical Investigation of Turbulent Burning Model for Internal Combustion Engines," SAE Paper 740191.
29. Tabaczynski, R., et.al., "A Turbulent Entrainment Model for Spark-Ignition Engine Combustion," SAE Paper 770647.
30. Dent, J. and Salama, N., "The Measurement of the Turbulence Characteristics in an Internal Combustion Engine cylinder," SAE Paper 750886.
31. Beer, J.M. and Chigier, N.A., "Combustion Aerodynamics," John Willey and Sons, 1972.
32. Lavoie, G.A., et. al., "Experimental and Theoretical Study of Nitric Oxide Formation in Internal Combustion Engines," pp. 313-326 Combustion Science and Technology, Vol. 1, 1970.
33. Fly, G.W., "Parametric Study of the Impact of Mixing Rates on the Formation of NO<sub>x</sub> in a TCCS Engine," MS Thesis, M.E., MIT 1977.
34. Bastress, E.K., et.al., "Control of Nitrogen Oxide Emissions from Diesel Engines: A Theoretical Analysis," NREC Report No. 1160-1, June 8, 1971.
35. Bishop, I.N., "Effect of Design Variables on Friction and Economy," SAE Automotive Engineering Congress, Jan. 13-17, 1964.
36. Hires, S.D., et. al., "Performance and NO<sub>x</sub> Emissions Modeling of a Jet Ignition Prechamber Stratified Charge Engine," SAE Paper 760161.
37. JANAF Thermochemical Tables, National Bureau of Standards Publication NSRDS - NBS 37, 1971.

TABLE 1  
Engine Specifications

Dimensions			
bore		3.875	in.
stroke		3.875	in.
connecting rod		6.625	in.
clearance volume		4.570	in. <sup>3</sup>

Valve Timings			
	Opens	Closes	
inlet valve	10 BTCD (1) 0 (2)	55 ABDC (2) 45 (1)	
exhaust valve	55 BBDC (1) 45 (2)	10 ATDC (2) 0 (1)	

(1) at 0.006 in. valve lift

(2) valve face flush with head

TABLE 2  
Summary of Instrumentation

<u>Temperatures</u>		
Air Orifice Inlet	Water Outlet	Bearing Oil
Air Inlet	Exhaust	Fuel Inlet
Water Inlet	Crankcase Oil	Fuel Returns

Instrument - All Points

Chromel - Alumel Thermocouple  
 Omega DS - 500 Digital Readout  
 Resolution 1°F

Pressures

	Method	Resolution
Inlet Air	Water Manometer	.1 in.
Crankcase Vacuum	Water Manometer	.1 in.
Oil Pressure	Panel Gage	2 PSI
Exhaust	Mercury Manometer	.1 in.
Dynamometer Load	Mercury Manometer	.1 in.
Injection Line	Kistler 601 Piezoelectric transducer, Kistler 504E	30 PSI*
	Charge Amplifier	
Combustion Chamber	Kistler 609A Piezoelectric Transducer, Kistler 503D	.2 PSI**
	Charge Amplifier	

TABLE 3  
Summary of Fuel Properties

	Cross-cut Distillate
Molecular Wt.	~125
H:C Ratio	1.825
Specific Gravity	.80
Boiling Point °F	106-648
Lower Heating Value (Btu/lbm)	18038
Stoichiometric F/A Ratio	.0694
  FIA - %	
Aromatics	29.5
Olefins	3.0
Saturates	67.5
Octane No. RON	76.6
Cetane No.	28.3

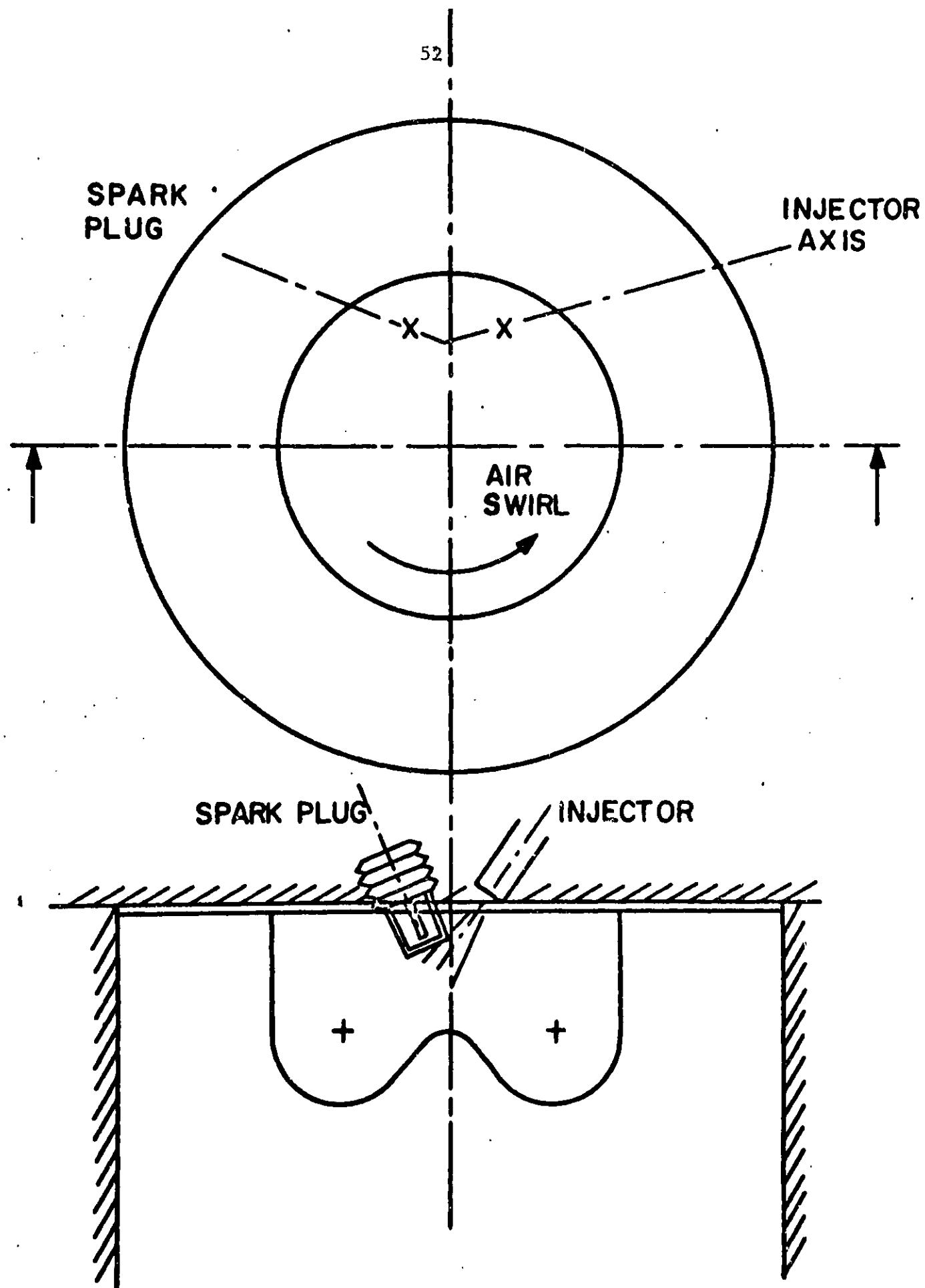


Fig. 1 TEXACO CONTROLLED COMBUSTION  
SYSTEM (SCHEMATIC)

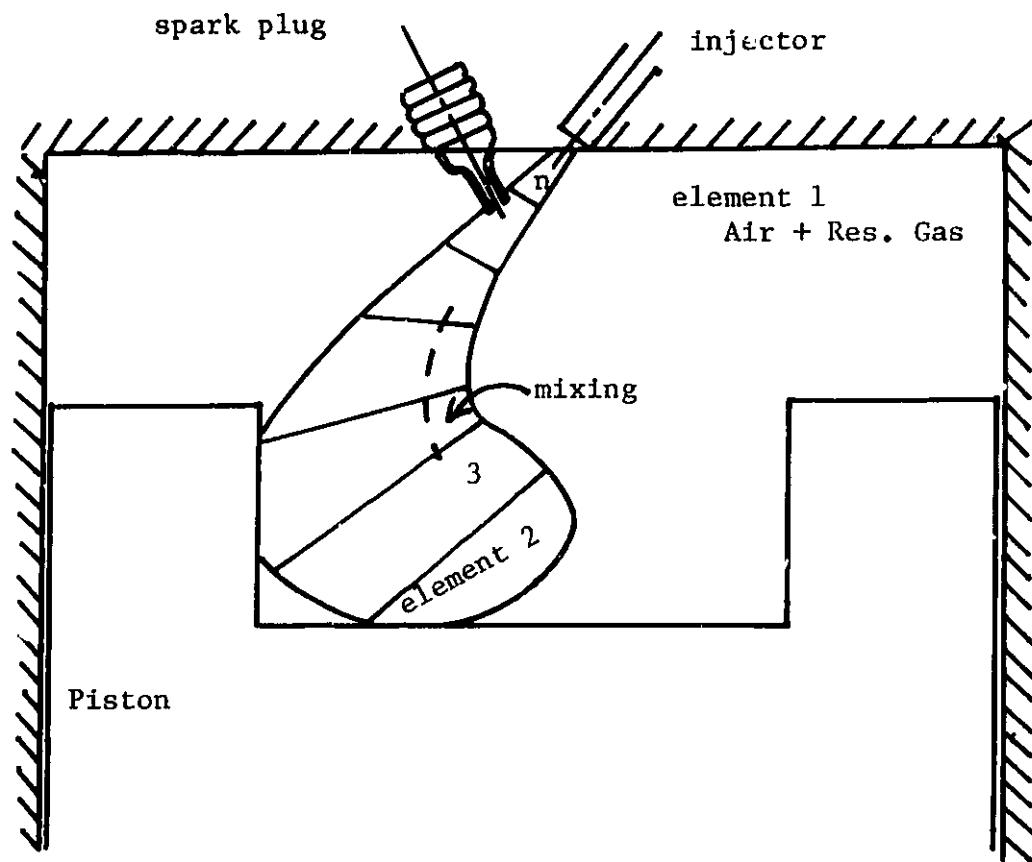
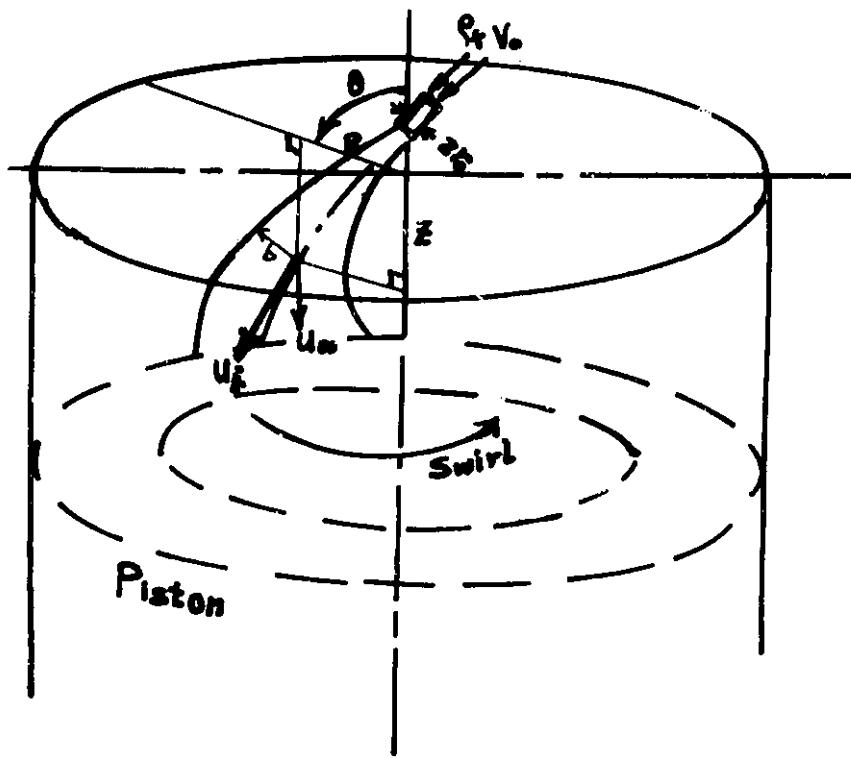


Fig. 2 System Model



$$\text{Jet Velocity } U_j = U_j(v_R, w, V_z)$$

$$\text{Air Velocity } U_\infty = U_\infty(v_{R\infty}, w_s, V_{z\infty})$$

Fig. 3 Jet Model with Swirl

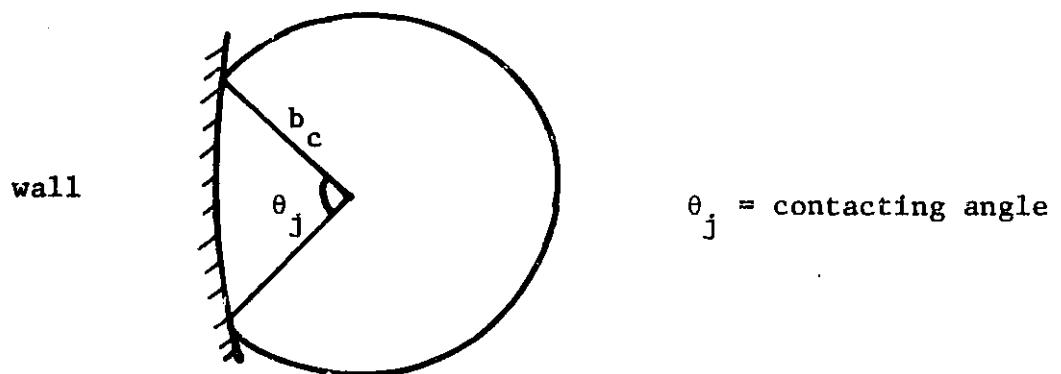
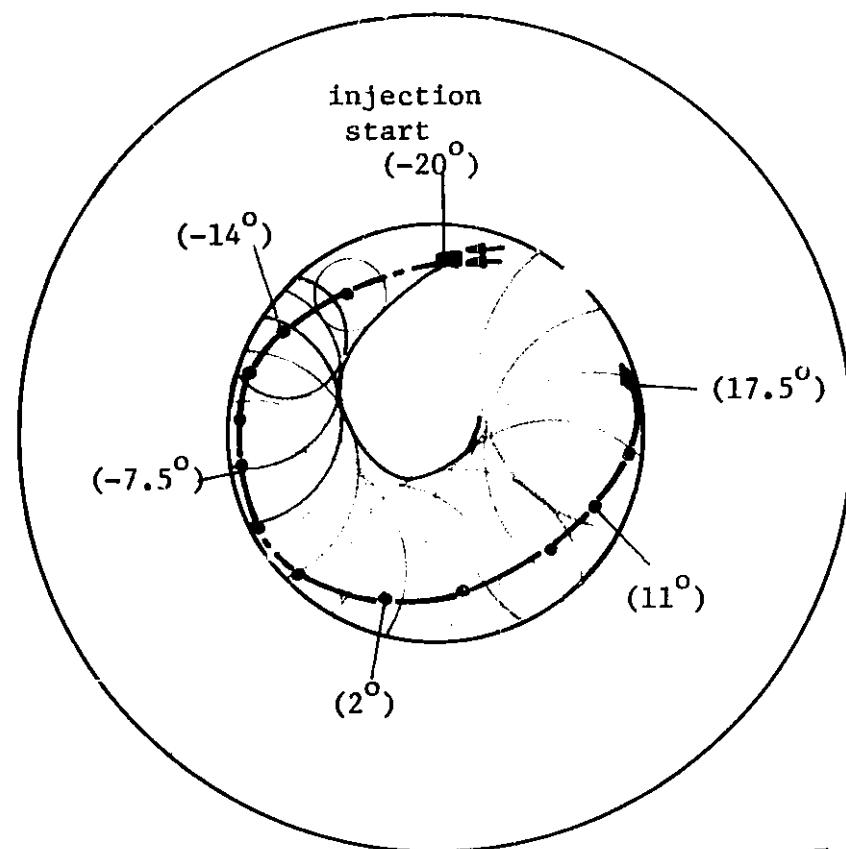
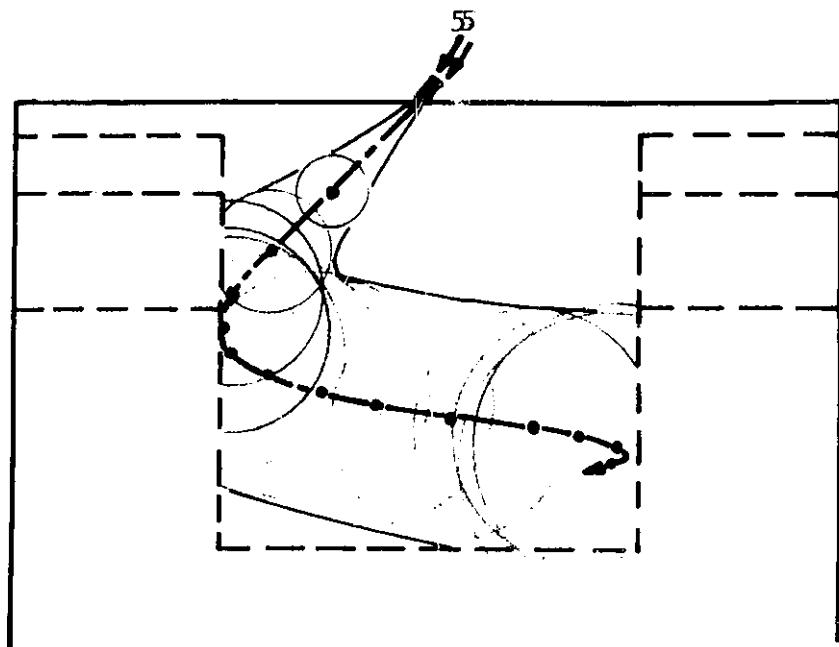


Fig. 4 Jet Cross Cw. Shape When Contacting with Wall



Engine Speed = 2000 rpm  
 Swirl Ratio =  $3.65 \times$  Engine Speed (at  
 $\phi = 0.545$

Fig. 5 Calculation Results of Jet Model  
(First Jet Element Trajectory)

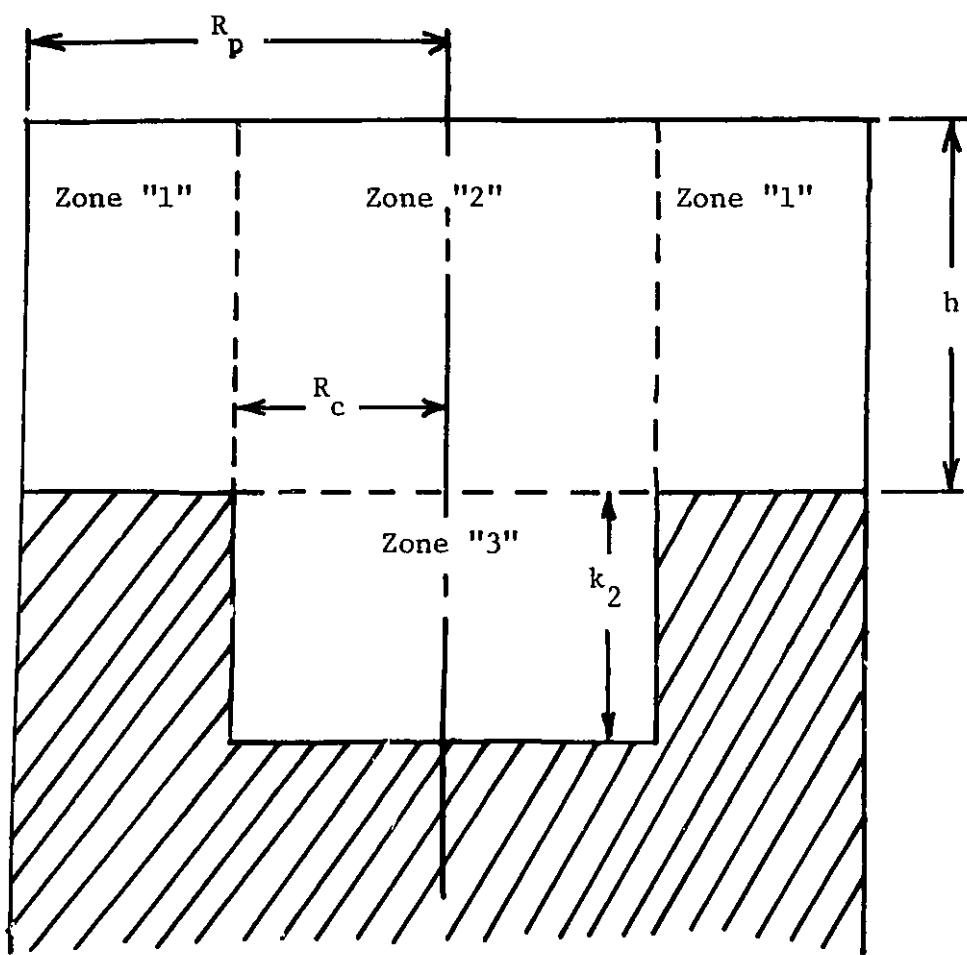
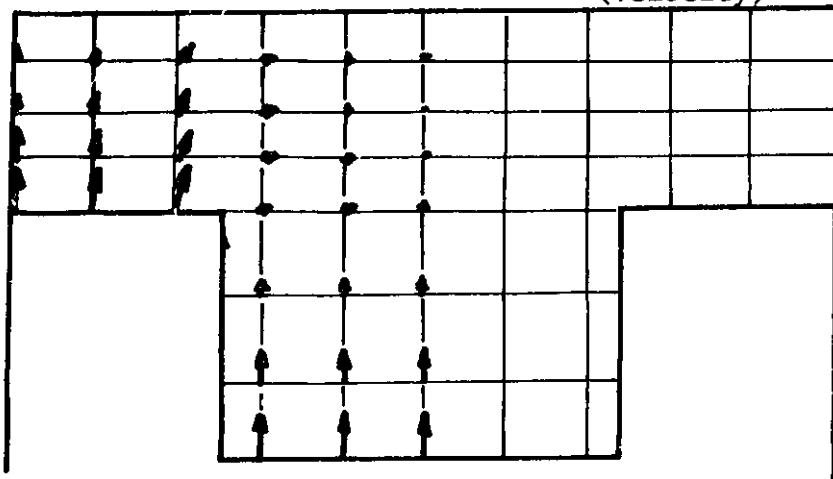


Fig. 6 Model of Air Motion Calculation

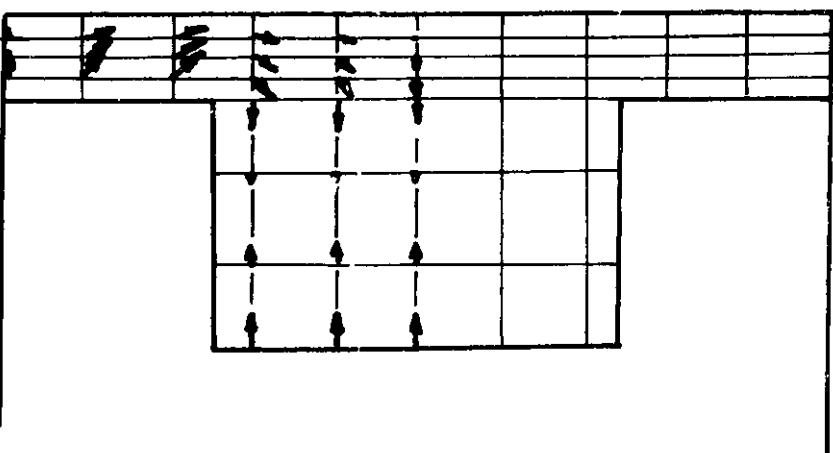
i) at  $-50^\circ$  before TDC

piston speed  
 $= 11.8 \text{ m/s}$



ii) at  $-30^\circ$  before TDC

piston speed  
 $= 8.1 \text{ m/s}$



iii) at  $-10^\circ$  before TDC

piston speed  
 $= 2.9 \text{ m/s}$

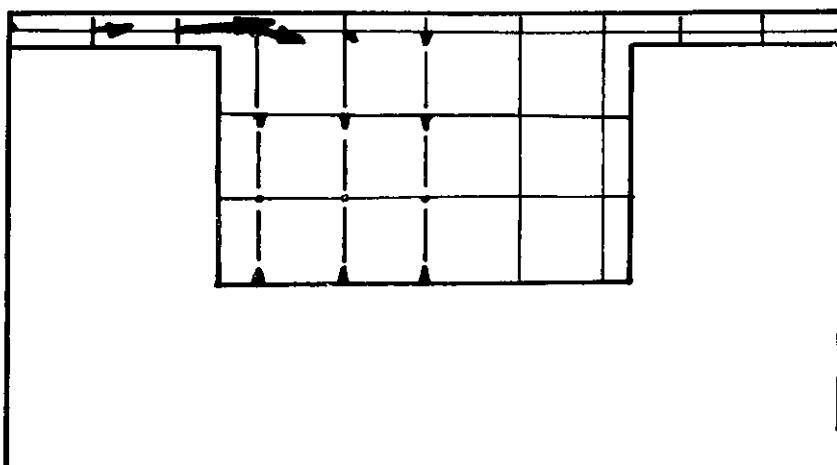


Fig. 7 Air Motion by Calculation

(Radial and Axial Components)

RPM = 2500 rpm

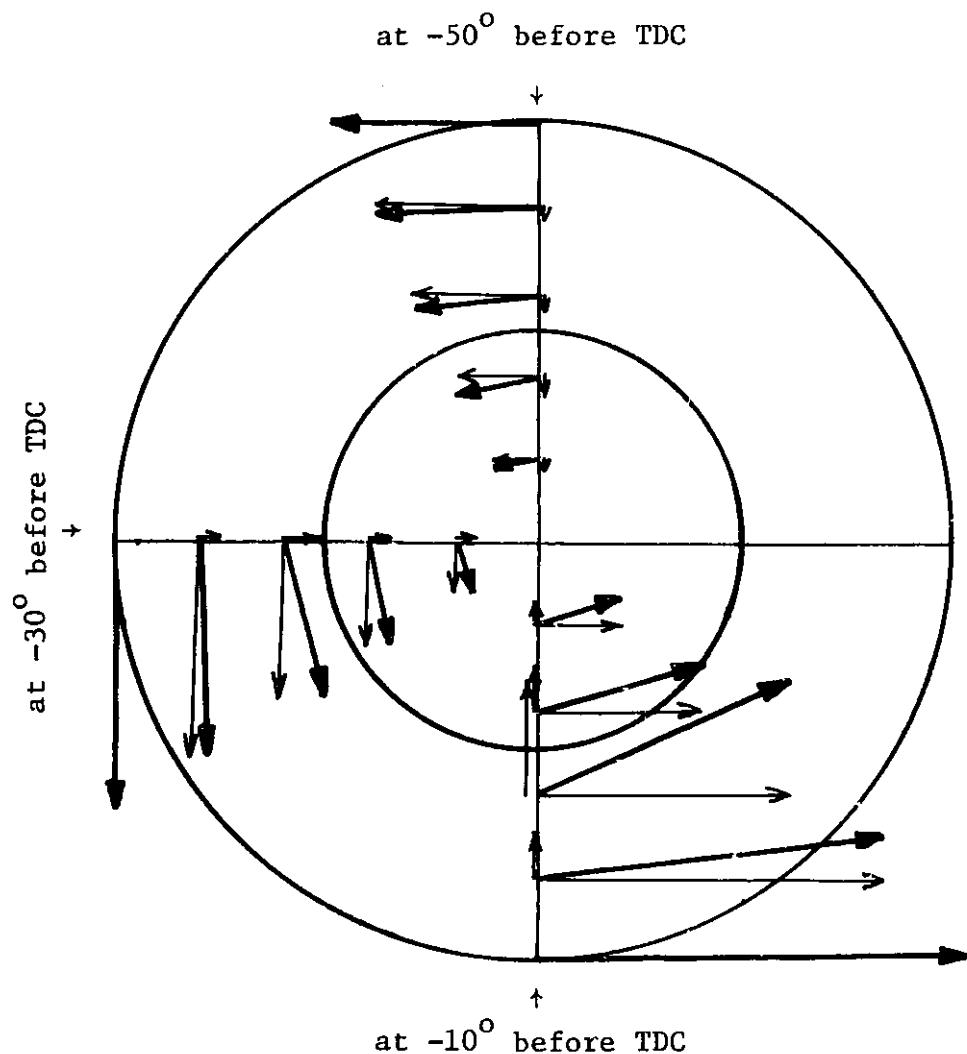
Scale 20m/s  $\rightarrow$  1 cm (velocity)

Fig. 8 Air Motion (Prediction)  
(Radial and Tangential Components)

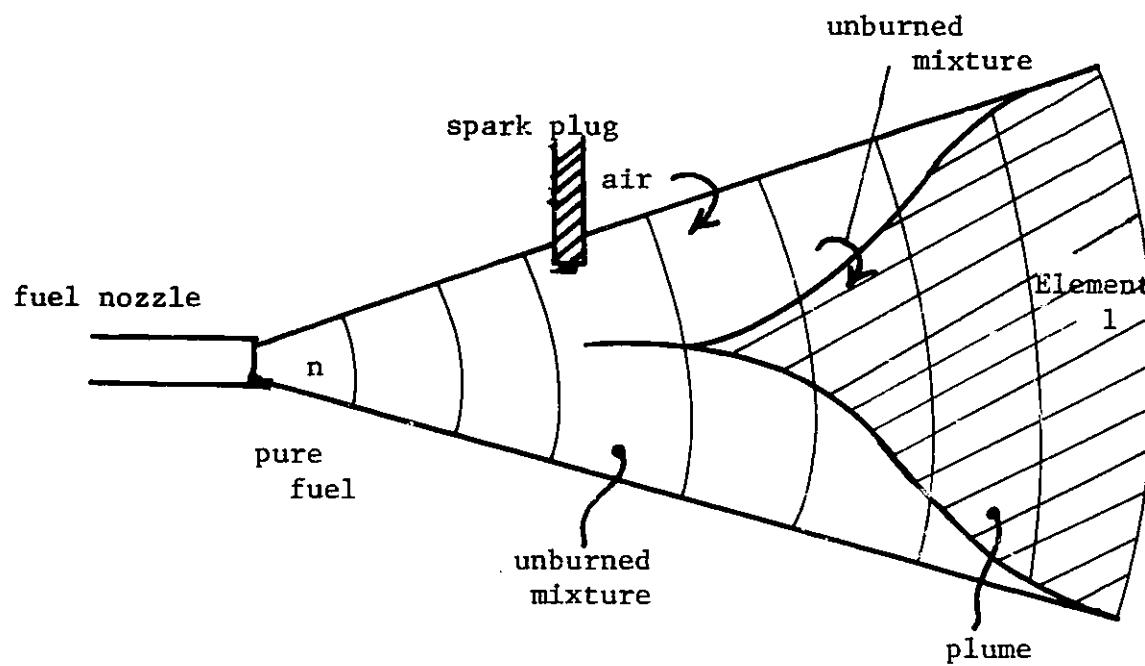


Fig. 9 The Schematic of Ignition Model

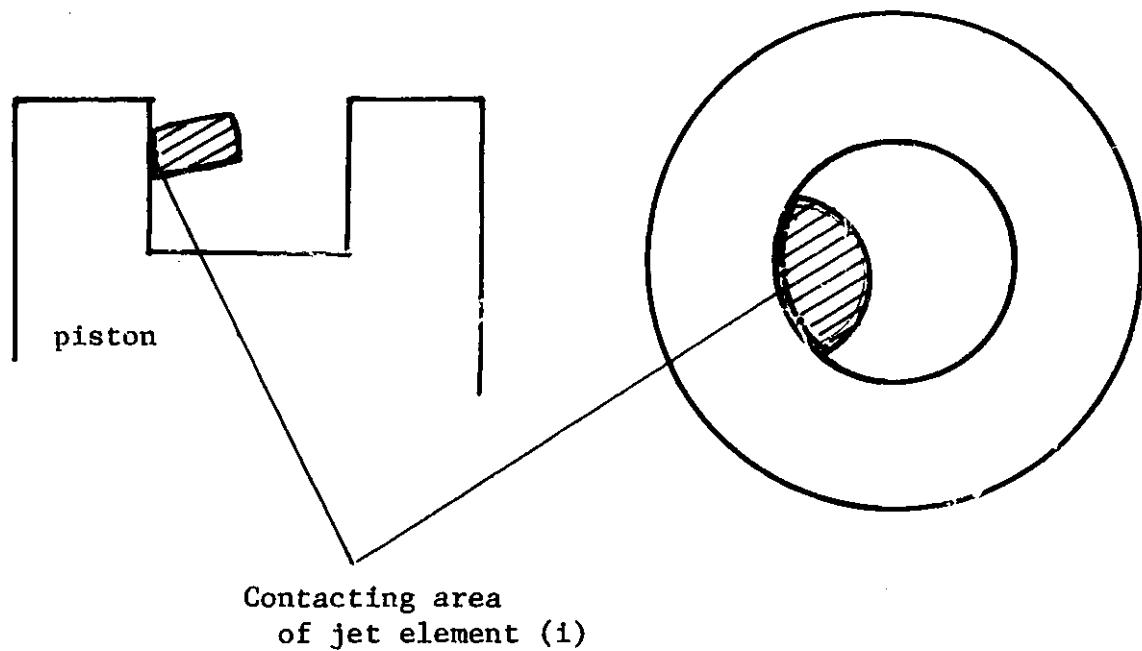
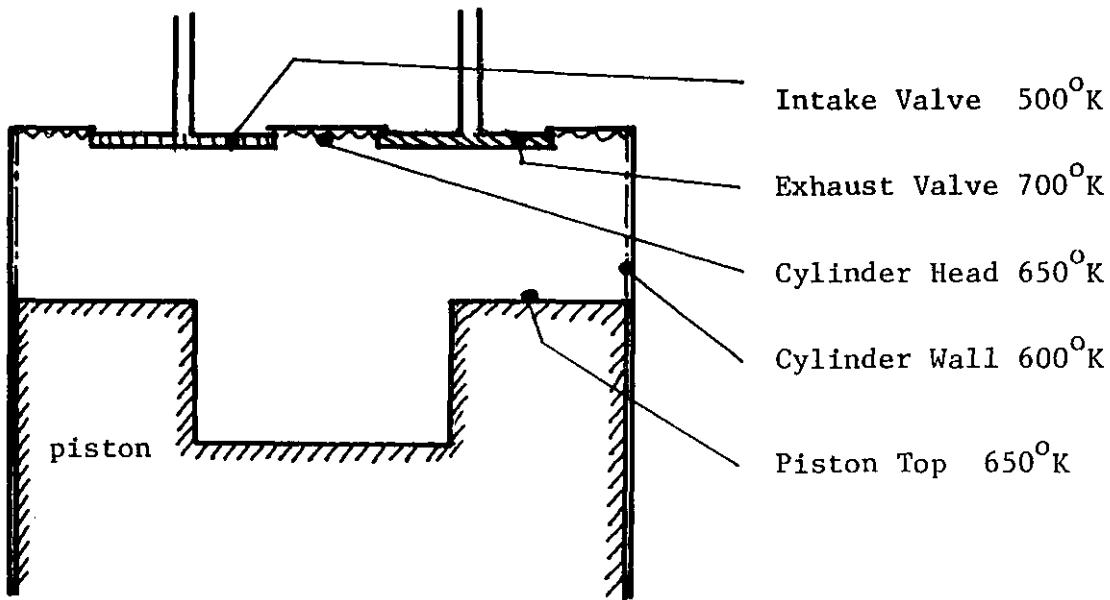


Fig. 10 Heat Transfer Model

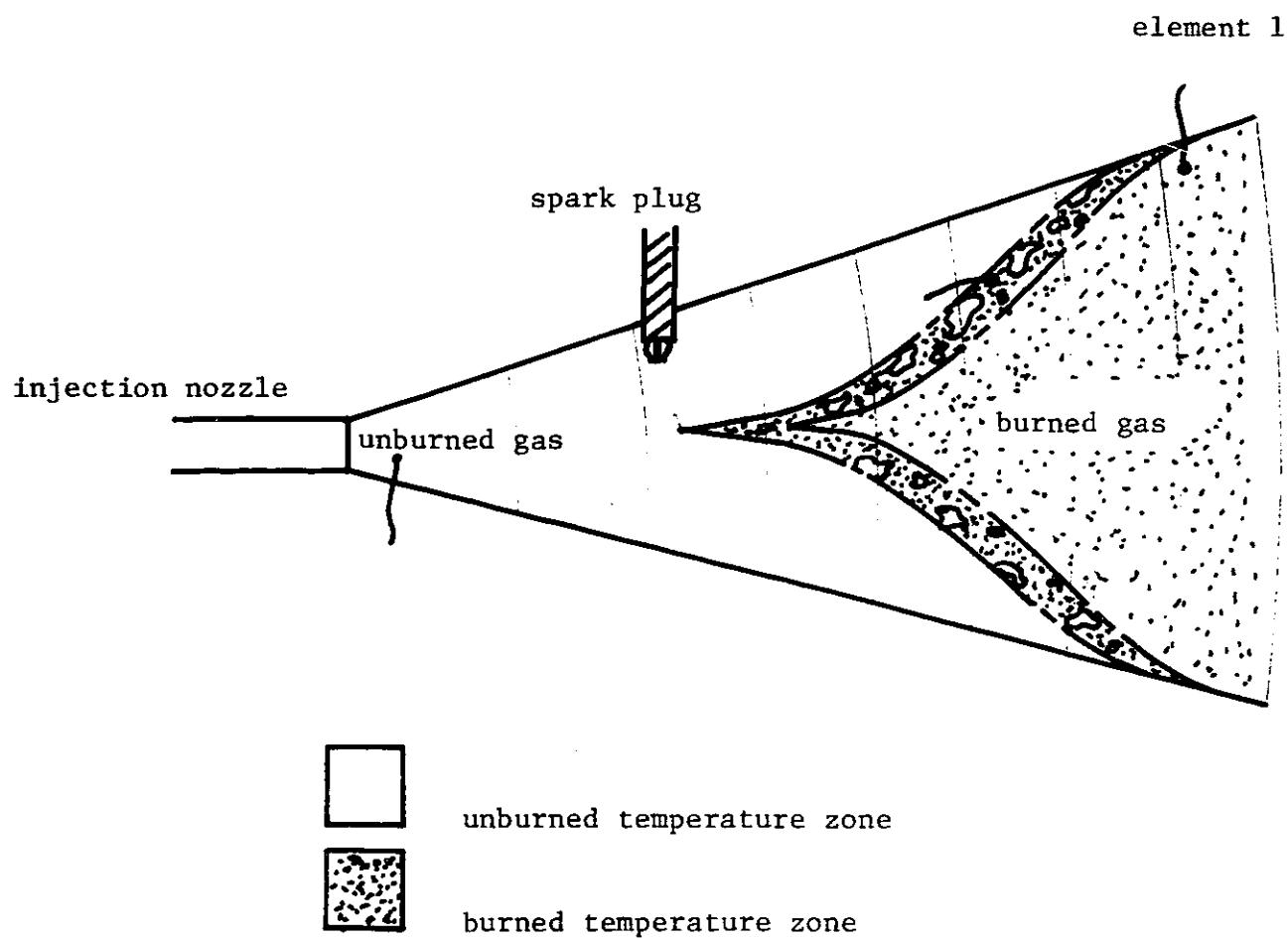


Fig. 11 The Schematic of NO<sub>x</sub> Model

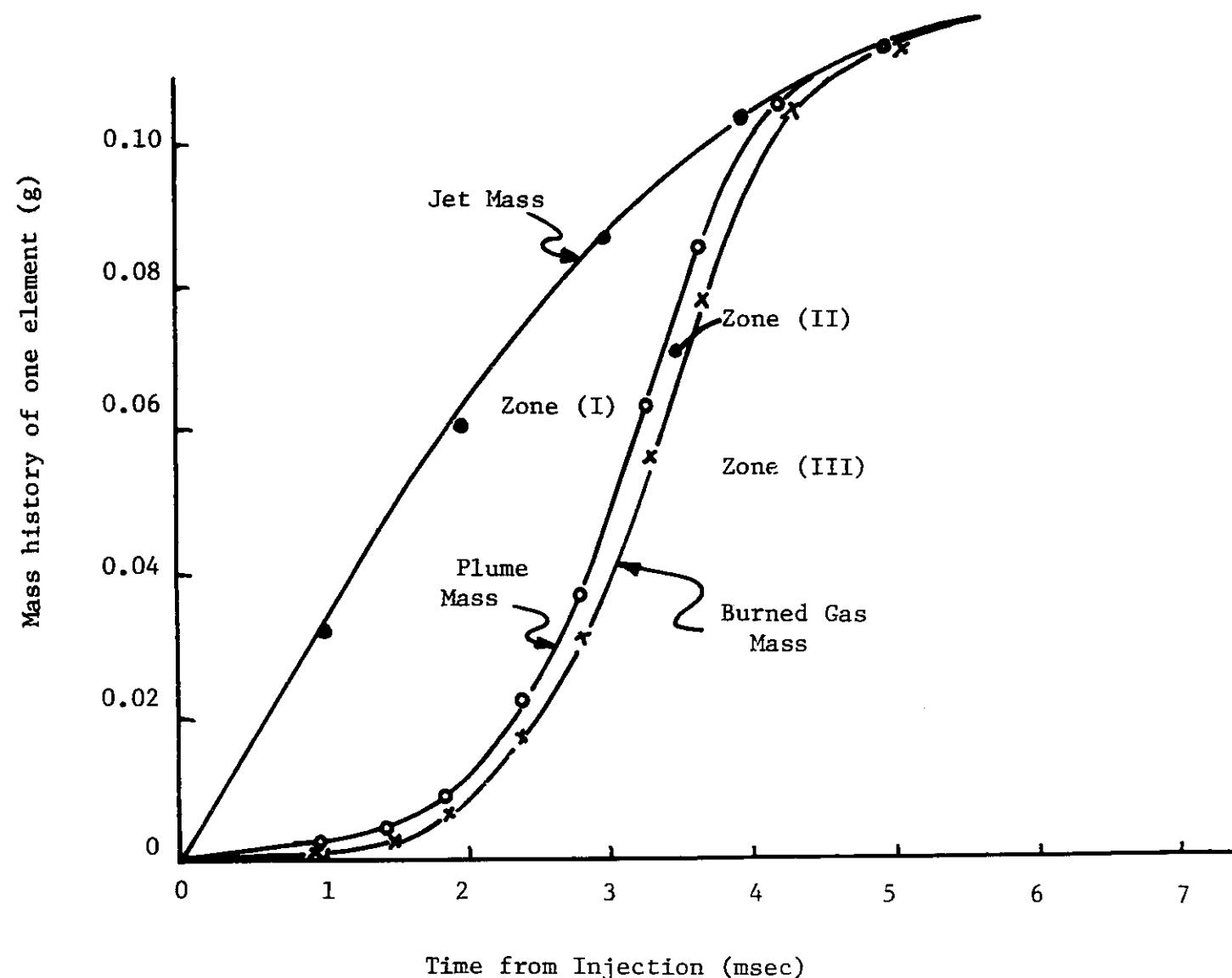


Fig. 12 Mass History of One Element (prediction)

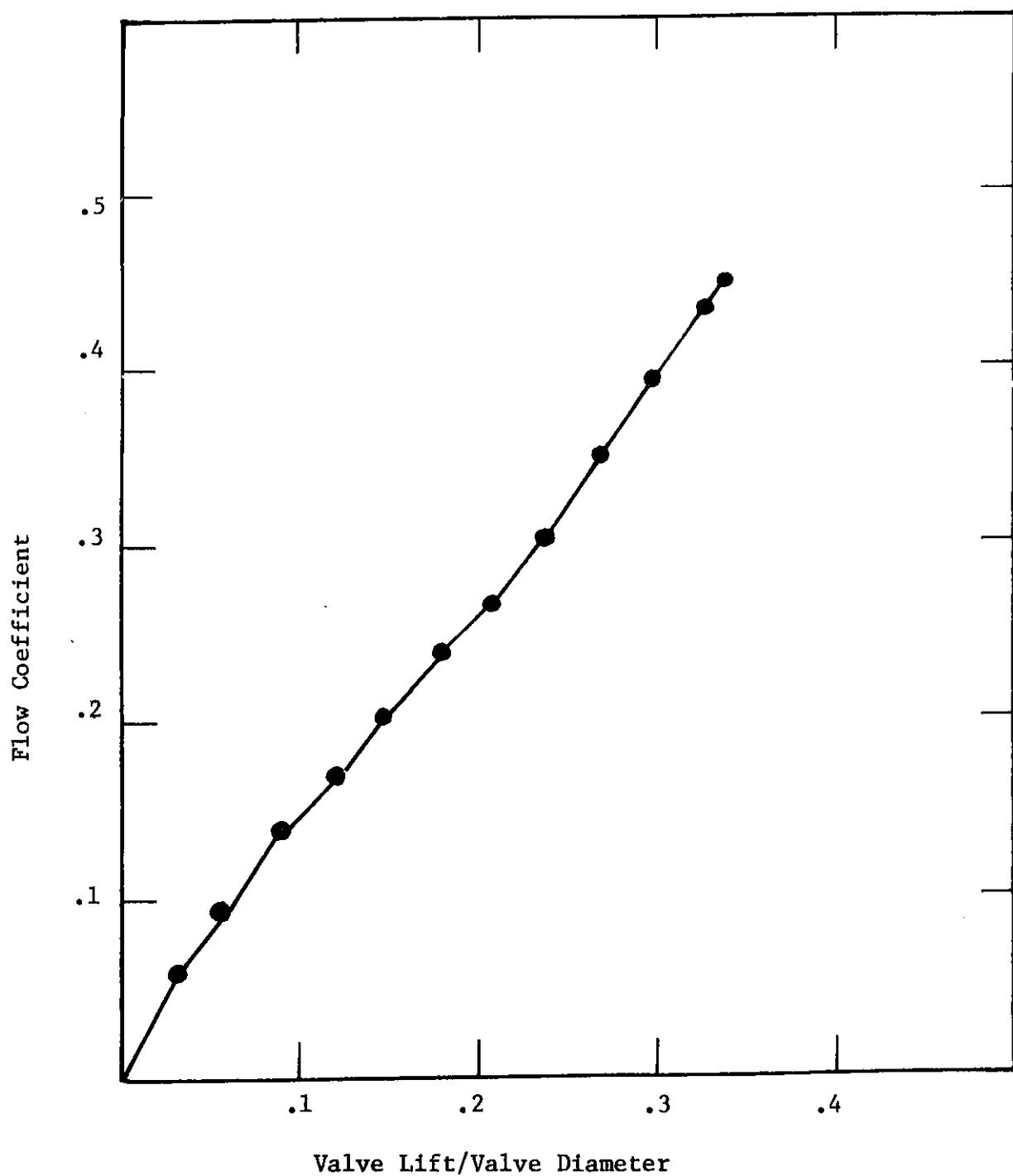


Fig. 13 Valve Flow Coefficient for the Intake Valve

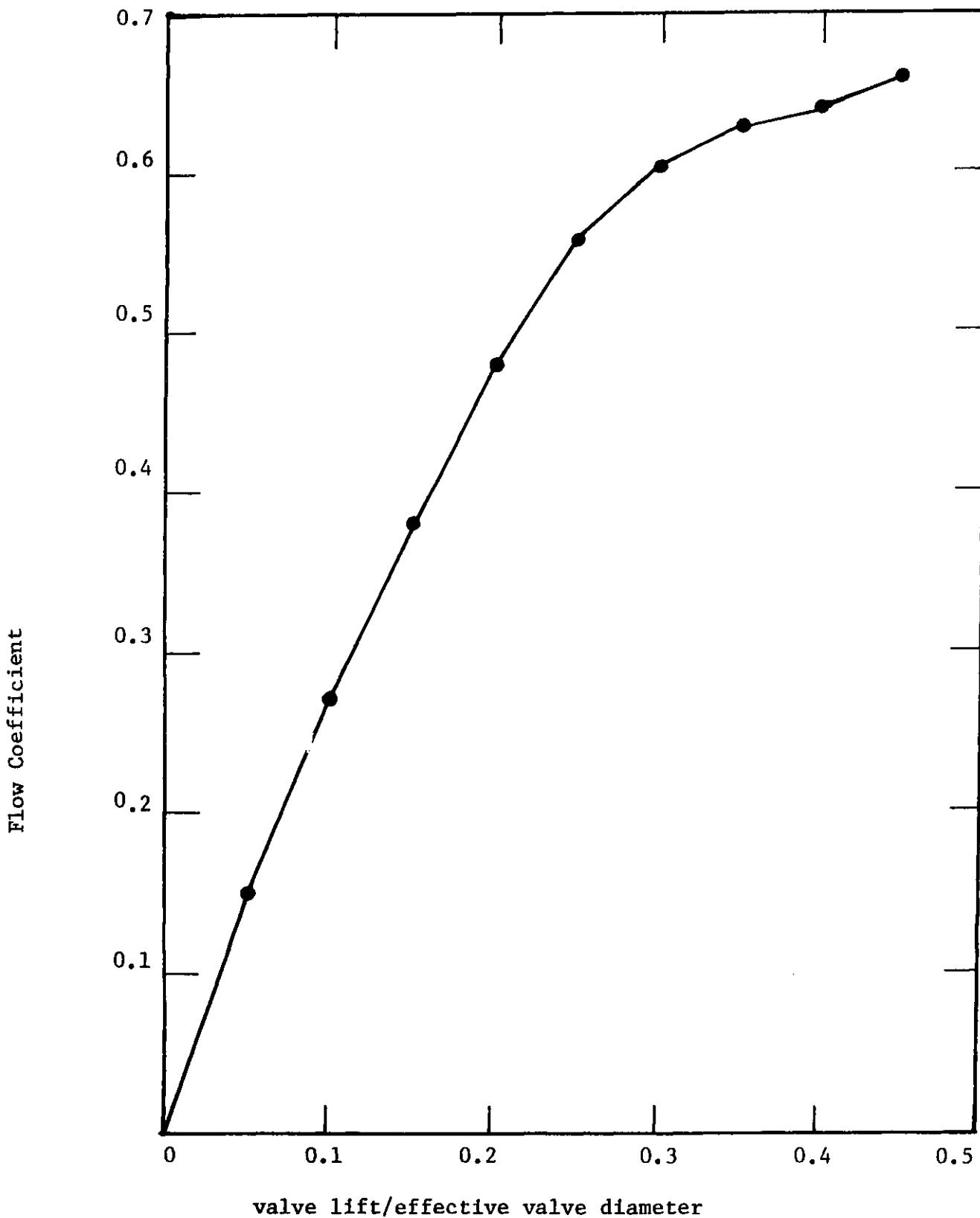


Fig. 14 Valve Flow Coefficient for the Exhaust Valve

Fig. 15 Normalized Mass Fraction

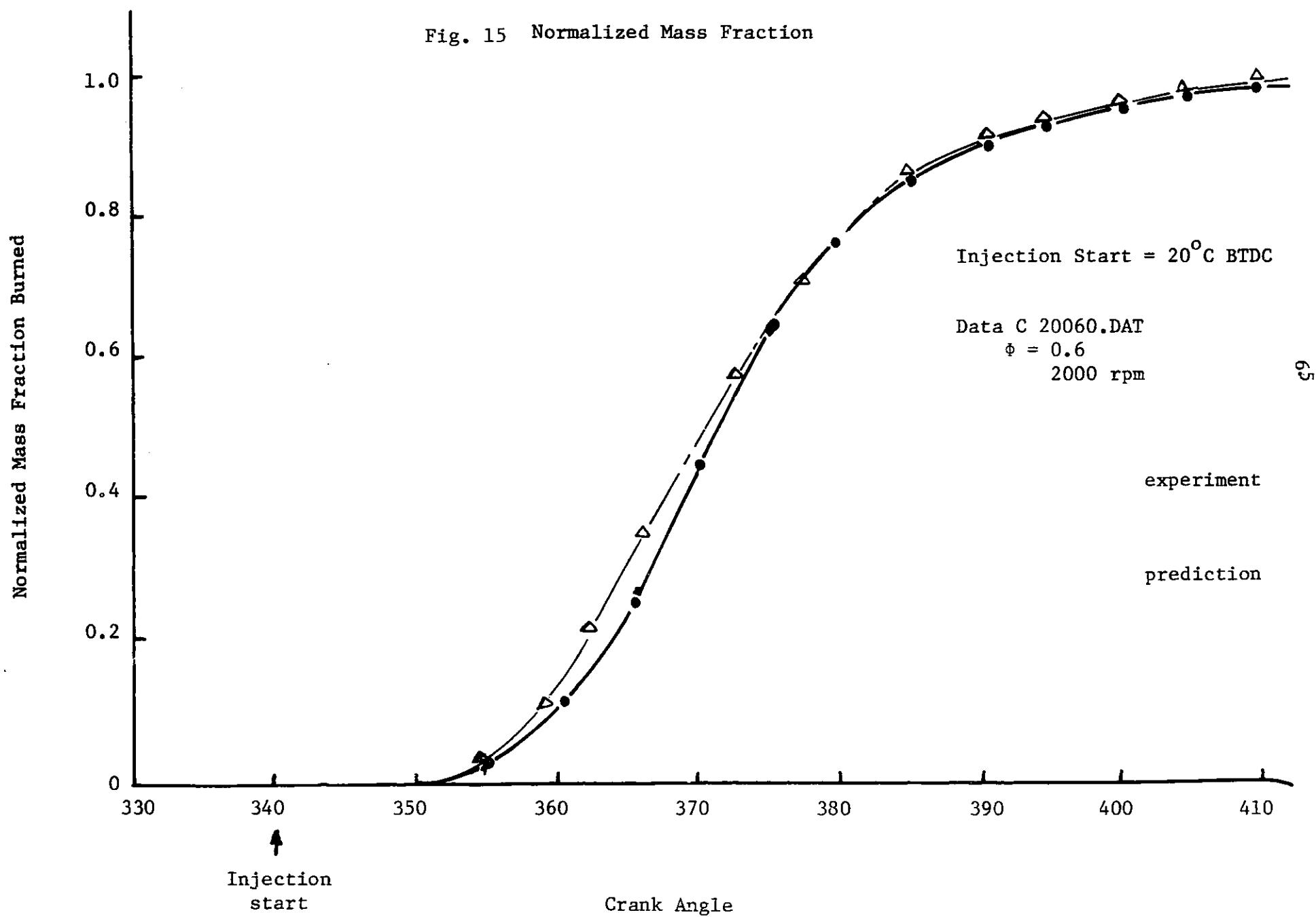
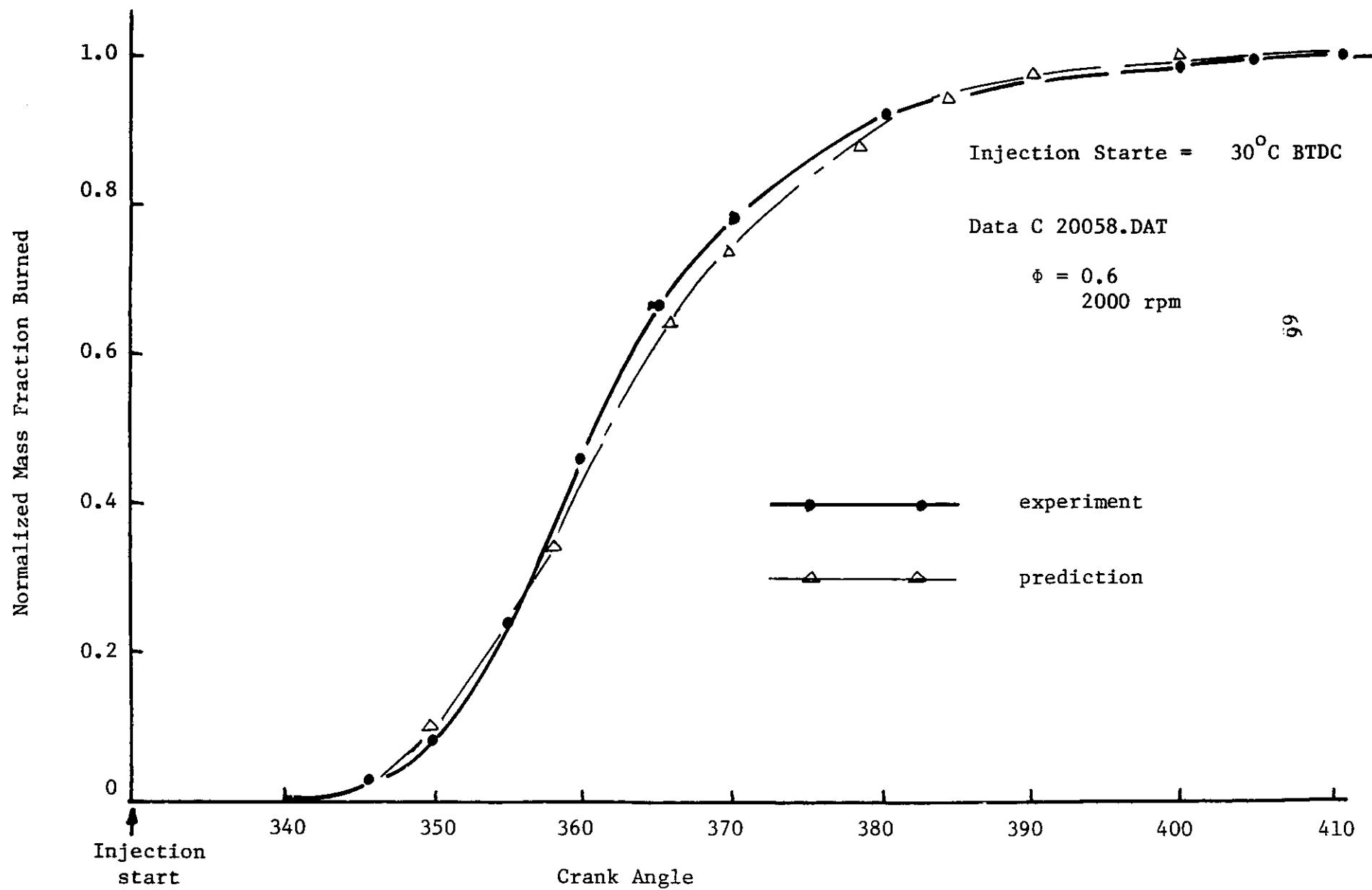


Fig. 16 Normalized Mass Fraction Burned



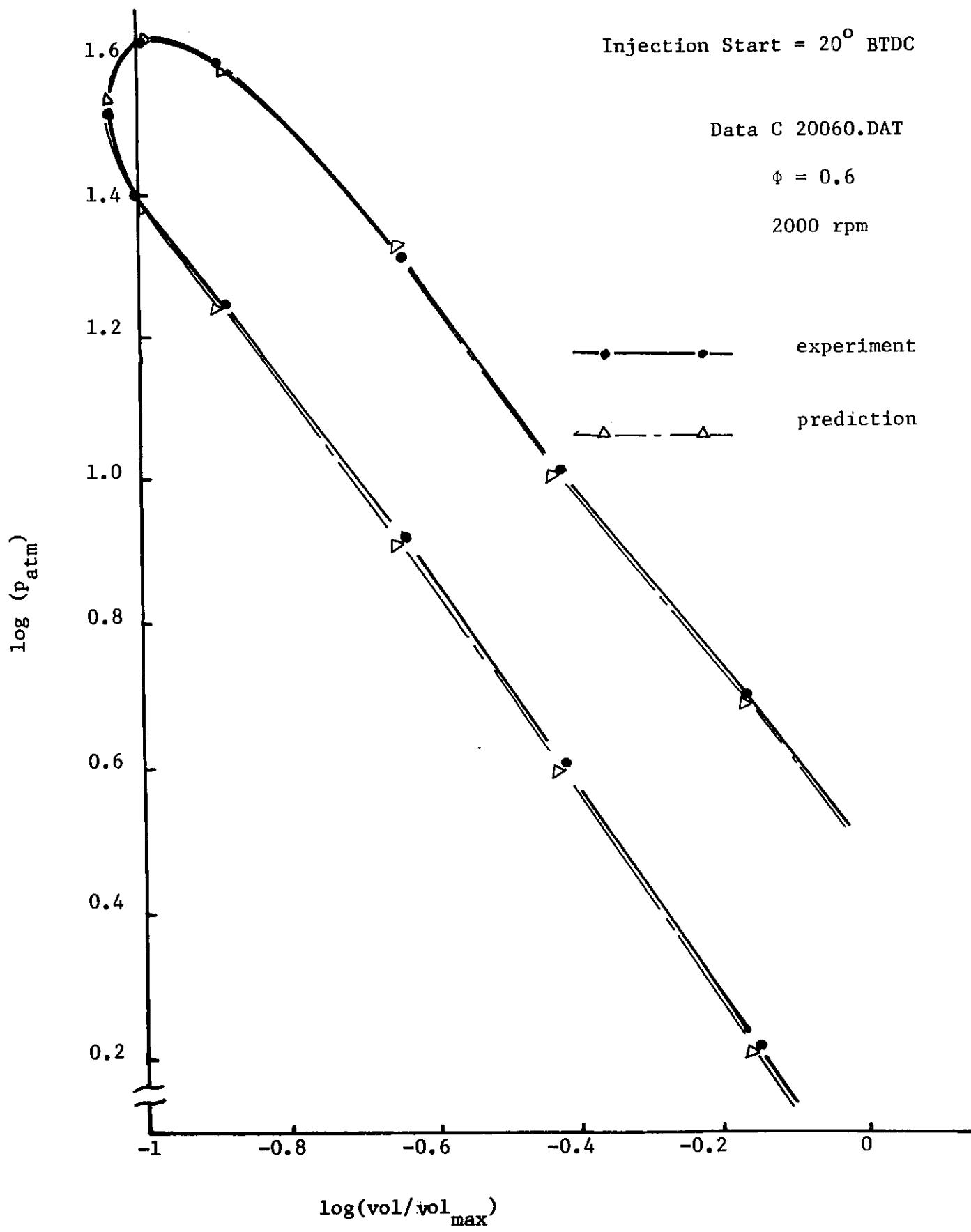


Fig. 17 log P - log V Diagram ( $\theta_i = -20^\circ$ )

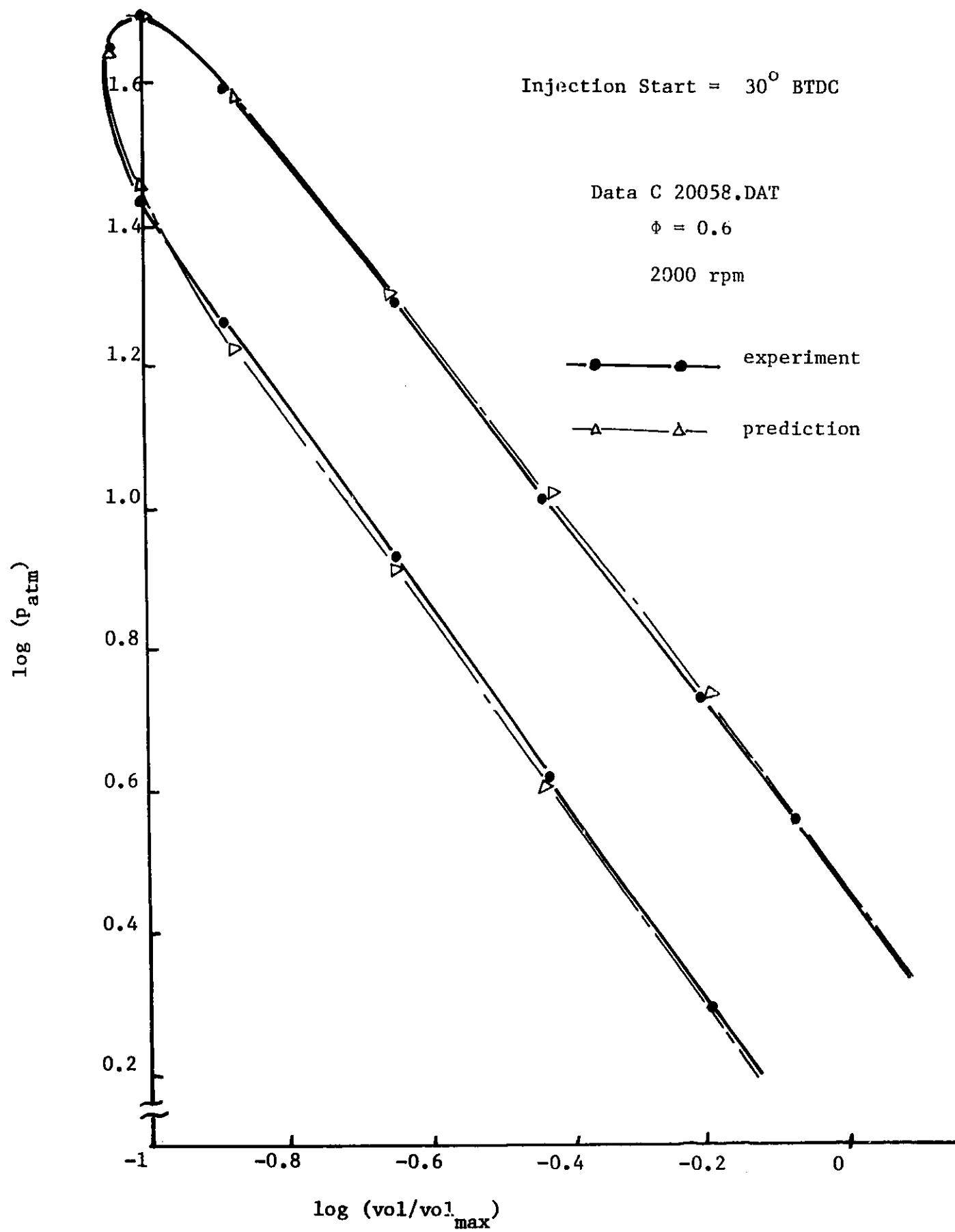


Fig. 18 log P - log V Diagram ( $\theta_1 = -30^{\circ}$ )

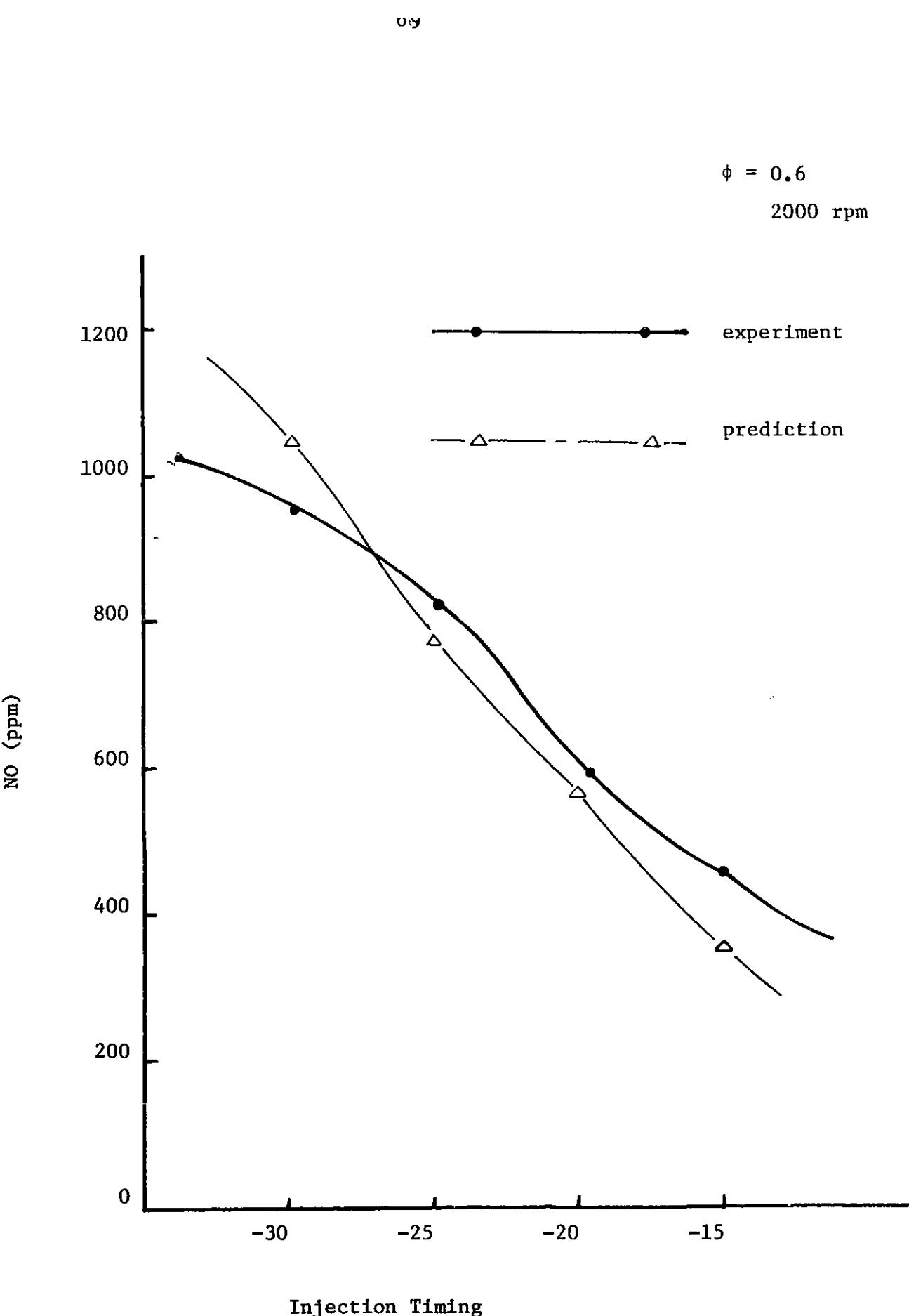


Fig. 19 Exhaust NO

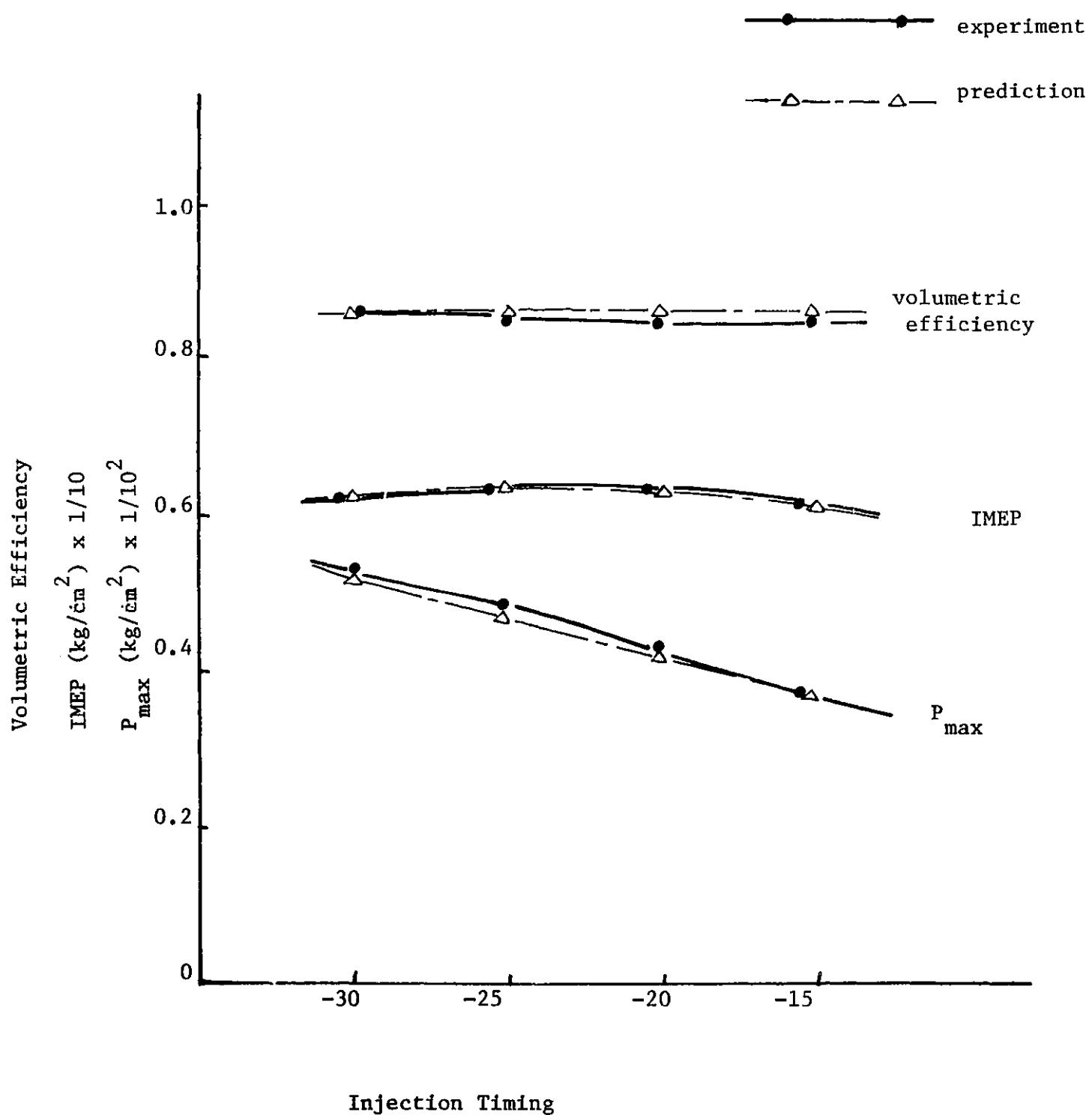


Fig. 20 Volumetric Efficiency, IMEP and  $P_{max}$

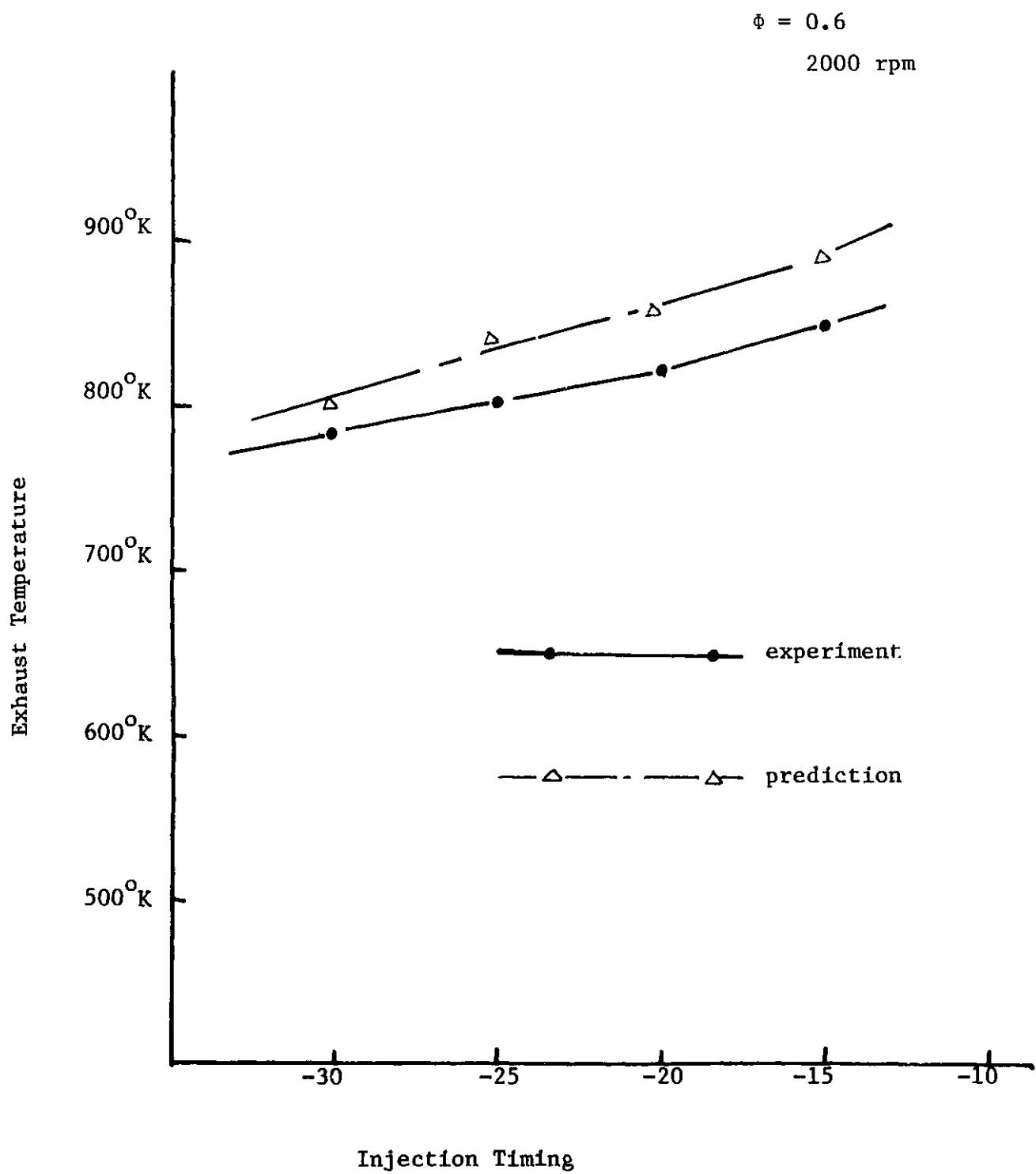


Fig. 21    Exhaust Temperature

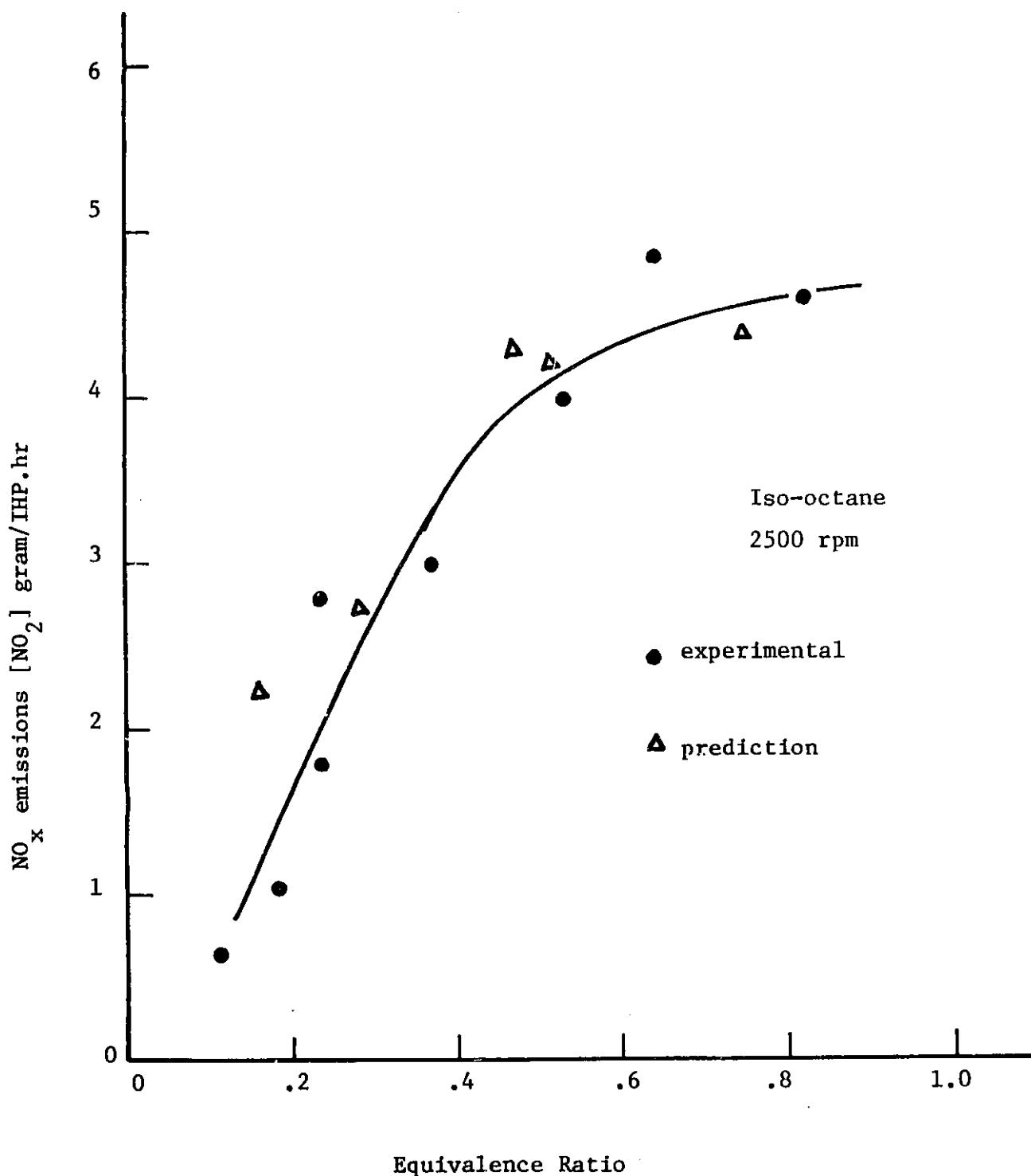


Fig. 22 NO<sub>x</sub> vs. Equivalence Ratio

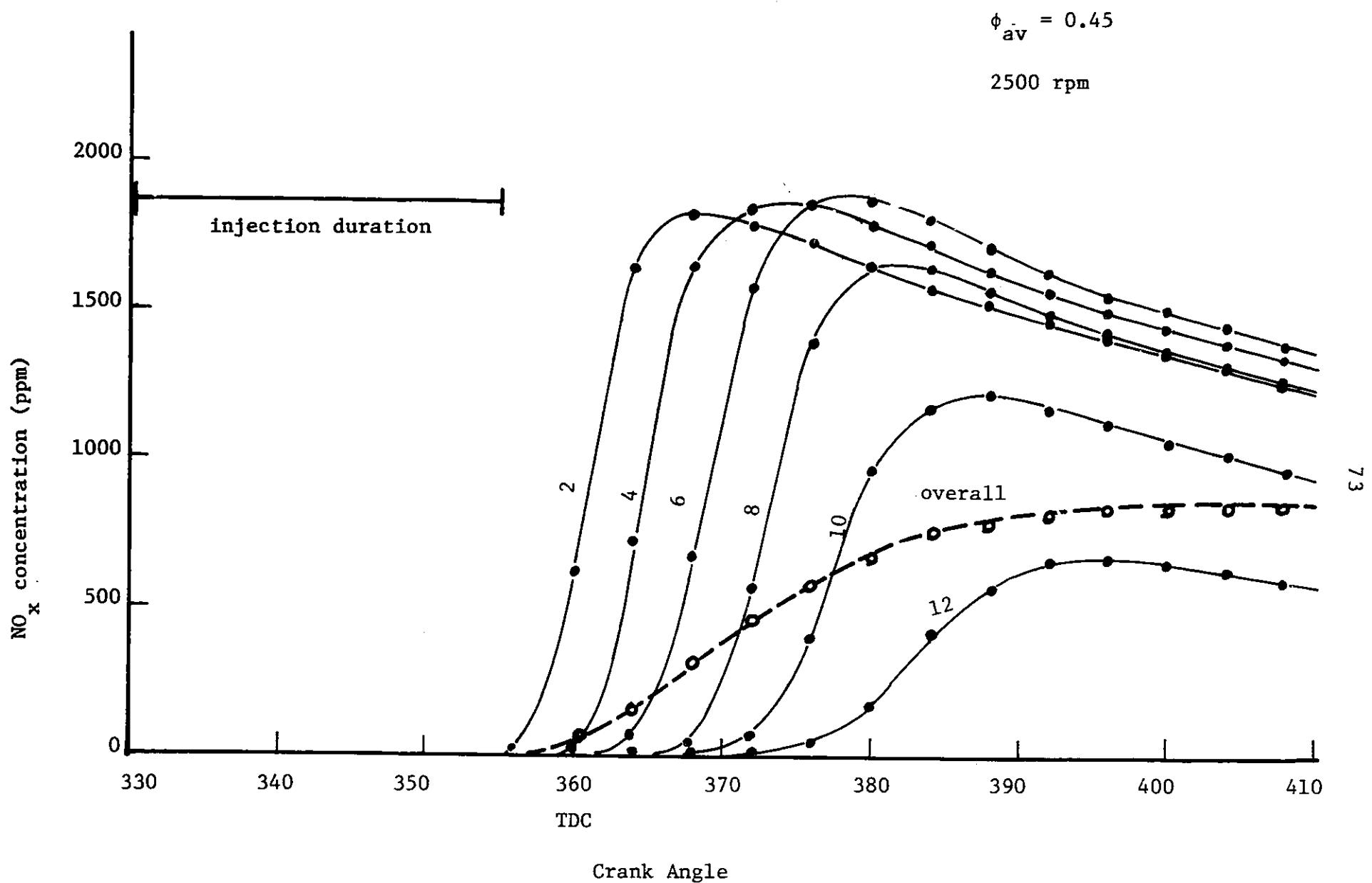


Fig. 23 NO Concentration in Each Element

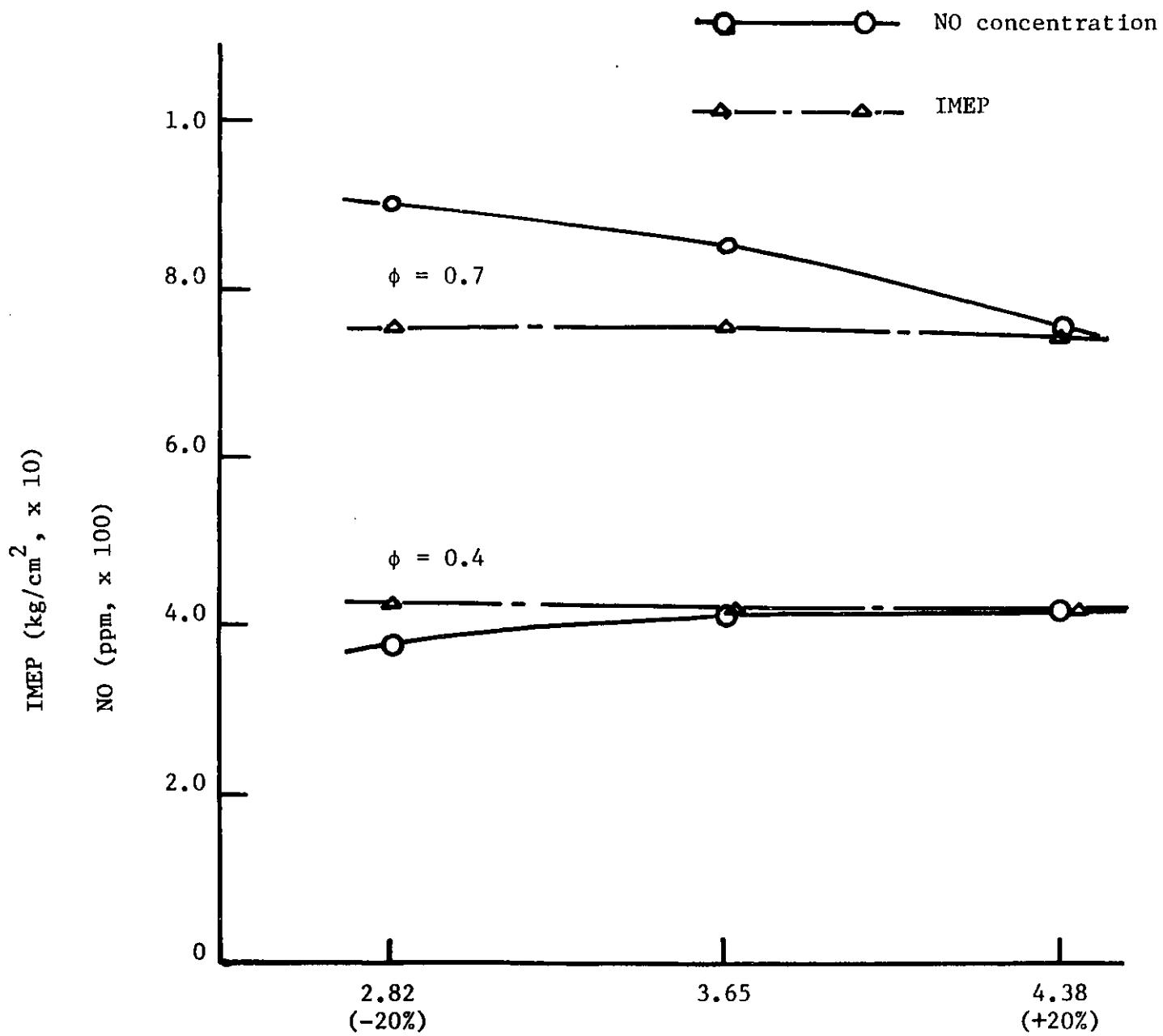


Fig. 24 The Effects of Swirl Ratio on Indicated Mean Effective Pressure and NO Concentration

## Appendix A

### Gas Exchange Process

During a discussion of exhaust and intake phases in the model description, it was seen that a knowledge of discharge-coefficient and the effective flow areas for both exhaust and intake valves were required. In this section, the experimental data on engine port steady flow tests (obtained from Texaco) will be reported.

Figure 13 and 14 shows the results from the tests mentioned above for the intake and exhaust port in the form of a plot of flow coefficient vs. valve lift to effective valve diameter ratio (L/D).

The mass flow rates through exhaust and intake valves have been treated as quasi-steady flow through a restriction. The governing equations can be written as follows:

$$\dot{M} = C_v A_v \left( \frac{RT_o}{P_o} \right) (\gamma RT)^{1/2} \left\{ \frac{2}{(\gamma-1)} \right\} \left[ \left( \frac{P_2}{P_o} \right)^{2/\gamma} - \left( \frac{P_2}{P_o} \right)^{\frac{\gamma+1}{2(\gamma-1)}} \right]^{1/2}$$

For choked flow, with the condition for choked flow being:

$$\frac{P_o}{P_s} > \left( \frac{\gamma+1}{2} \right)^{\frac{\gamma}{\gamma-1}}$$

and

$$\dot{M} = C_v A_v \left( \frac{P_{oc}}{RT_{oc}} \right) (\gamma RT_o)^{1/2} \left\{ \left[ \frac{2}{(\gamma+1)} \right]^{\frac{(\gamma+1)}{2(\gamma-1)}} \right\}^{1/2}$$

where  $C_v$  = valve discharge coefficient

$A_v$  = valve flow area

$P_o, T_o$  = upstream stagnation pressure and temperature

$P_2$  = downstream static pressure

The logic to take care of the reverse flows through the valves has been put into the computer program. When there is reverse flow into the intake system (during valve overlap), the mass that flows past the intake valve is recorded. Its composition and temperature while in the intake system are assumed to be the same as those in the combustion chamber gas when intake valve opens. It has been assumed that, before any fresh charge can enter the chamber, all the mass that left the chamber during reverse flow is pulled back in first. For  $\text{NO}_x$  calculation  $\text{NO}_x$  mass transfer through the intake valve is taken into consideration.

## Appendix B

### Friction Loss

The following procedure for determining FMEP for a conventional spark ignition engine is taken from Bishop(33). The equations have been empirically correlated with data from engines ranging from single to eight cylinders, 4:1 to 17:1 compression ratio, and 0.75 to 2.5 bore to stroke ratio.

1.  $FMEP_{\text{misc \& pumps}} = 0.39(N/1000)^{1.5}$
2.  $FMEP_{\text{cam gear}} = [30 - (4N/1000)]GH^{1.75}/B^2S$
3.  $FMEP_{\text{bearing}} = (KB/S)N/1000$
4.  $FMEP_{\text{crank case}} = \Sigma \text{Eqns. 1,2,3}$
5.  $FMEP_{\text{blowby}} = [(P_a - P_1)/14.2]^{1/2} [1.72 R_c^{0.4} - (0.49 + 0.015 R_c) (N/1000)^{1.185}]$
6.  $V_p/1000 = SN/6000$
7.  $FMEP_{\text{viscous piston}} = (21.93M/BS) V_p/1000$

$$8. \text{ FMEP}_{\text{static ring tension}} = 2.11 S_n^2 / B^2$$

$$9. \text{ FMEP}_{\text{ring gas pressure}} = [(P_a - P_1) / 14.2] [2.35 S/B^2] [0.088 R_c + 0.182 R_c^{(1.33 - (0.121 V_p / 1000))}]$$

$$10. \text{ FMEP}_{\text{total}} = \Sigma \text{ Eqns. } 4, 5, 7, 8, 9$$

### Symbols

B: cylinder bore diameter (in)

C: number of cylinder

D: total engine displacement (in<sup>3</sup>)

G: number of intake valves per cylinder

H: intake valve head diameter (in)

K: journal bearing size coefficient

M: equivalent length of piston skirt (projected area of skirt ÷ cylinder bore diameter)

N: revolutions per minute of crankshaft

P<sub>a</sub>: dry atmospheric pressure (psia)

P: intake manifold vacuum (positive, when less than atmospheric pressure) (psig)

R<sub>c</sub>: compression ratio

S: piston stroke (in)

$v_p$ : mean piston velocity (ft/min)

n: total number of piston rings per cylinder

## Appendix C

### Thermodynamic Properties (hydrocarbon-air combustion)

The thermodynamic properties of the unburned and burned gases must be determined continuously during the entire cycle analysis. In most cases, the assumption of local chemical equilibrium can be justified and; in principal, for a given pressure and temperature, the mass action equations could be solved directly for species concentrations from which the desired thermodynamic properties could be derived. Alternatively, the species concentration which minimized the Gibbs free energy of the system could be calculated. Both approaches are quite involved and the calculations are expensive and time-consuming.

Our calculations use a computational method which is based on curve fitting data obtained from detailed thermochemical calculations to a functional form obtained from a consideration of carbon-air combustion.

This method was developed by M. Martin(21) and additional work done by S.D. Hires(34).

The following effects are taken into consideration by this method:

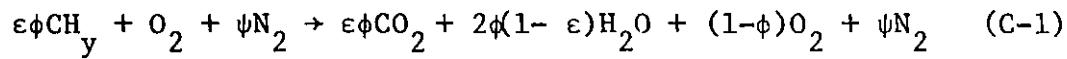
- i) Fuel vapor coefficient for unburned, air and residual gas mixtures.
- ii) Chemical dissociation effect above  $1000^{\circ}\text{K}$  for burned gases.

**I Composition**

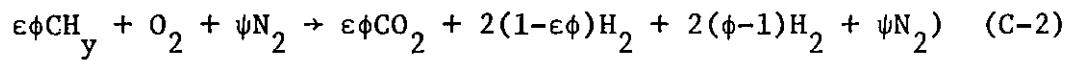
- unburned gas
  - i) fuel vapor
  - ii) burned gas (residual gas)
  - iii) air
- burned gas
  - i) burned gas

**II Combustion reaction equations (hydrocarbon-air, under 1000°K)**

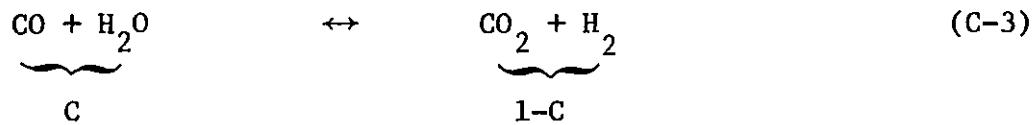
- i) lean mixtures ( $\phi < 1$ )



- ii) rich mixtures ( $\phi > 1$ )



and water gas reaction



This reaction is in equilibrium with equilibrium constant  $K(T)$ . "C" is obtained by solving the following equation for its positive root.

$$(1-K) C^2 + 2[1-\epsilon\phi + K(\phi-1 + \epsilon\phi)]C - 2K\epsilon\phi(\phi-1) = 0 \quad (C-4)$$

$K(T)$  is determined by curve fitting JANAF Table data(35) over the temperature range  $400-3200^{\circ}\text{K}$  and is given by:

$$\ln(K(T)) = 2.743 - 1.761/t - 1.611/t^2 + 0.2803/t^3 \quad (C-5)$$

where

$$t = T/1000 \quad (T = {}^{\circ}\text{K})$$

The coefficients for species are shown in Table C-1.

TABLE C-1

i	Species	$\phi \leq 1$	$\phi > 1$
1	$\text{CO}_2$	$\epsilon\phi$	$\epsilon\phi-C$
2	$\text{H}_2\text{O}$	$2(1-\epsilon)\phi$	$2(1-\epsilon\phi) + C$
3	CO	0	C
4	$\text{H}_2$	0	$2(\phi-1)-C$
5	$\text{O}_2$	$1-\phi$	0
6	$\text{N}_2$	$\psi$	$\psi$

$$\text{sum} \quad (1-\epsilon) + 1 + \psi \quad (2-\epsilon)\phi + \psi$$

where

$\psi$  = the molar N:O ratio of the product

$y$  = the molar H:C ratio of the fuel

$\epsilon = 4/(4+y)$

$\phi$  = the fuel-air equivalence ratio

### III Grams of product per mole of O<sub>2</sub> reactant

$$\tilde{M} \sim \phi(8\epsilon+4) + 32 + 28\psi \quad (C-6)$$

### IV Specific enthalpy and specific heat at constant pressure

$$\tilde{M} C_p = \sum_{i=1}^6 x_i \sum_{j=1}^4 (a_{ij} t^{j-1} + a_{5j}/t^2) \quad (C-7)$$

$$\tilde{M} h = \sum_{i=1}^6 x_i \sum_{j=1}^4 (a_{ij} t^j/j - a_{5j}/t + a_{6j}) \quad (C-8)$$

The coefficients  $a_{ij}$  are obtained by curve fitting JANAF Table data to the above functional form. The values of  $a_{ij}$  are given in Table C-2. The resultant  $C_p$  is in cal/g - °K and  $h$  is in Kcal/g.

TABLE C-2

## Coefficients for Polynomial Fit to Thermodynamic Properties

Coefficients for  $100^{\circ}\text{K} < T < 500^{\circ}\text{K}$ 

i	Species	$a_{i1}$	$a_{i2}$	$a_{i3}$	$a_{i4}$	$a_{i5}$	$a_{i6}^*$
1	$\text{CO}_2$	4.7373	16.653	-11.232	2.8280	.006767	-93.75793
2	$\text{H}_2\text{O}$	7.8097	- .20235	3.4187	-1.1790	.001436	-57.0800
3	CO	6.9738	- .82383	2.9420	-1.1762	.0004132	-27.196
4	$\text{H}_2$	6.9919	.16170	- .21821	.29682	-.016252	- .11819
5	$\text{O}_2$	6.2957	2.3884	- .031479	-.32674	.004359	.103637
6	$\text{N}_2$	7.0922	- 1.2958	3.2069	-1.2022	-.0003458	- .013967
7	$\text{C}_8\text{H}_{18}^{**}$	- .55313	181.62	-97.787	20.402	-.03095	-60.518

Coefficients for  $500^{\circ}\text{K} < T < 6000^{\circ}\text{K}$ 

i	Species	$a_{i1}$	$a_{i2}$	$a_{i3}$	$a_{i4}$	$a_{i5}$	$a_{i6}^*$
1	$\text{CO}_2$	11.940	2.0886	- .47029	.037363	-.58945	-97.1418
2	$\text{H}_2\text{O}$	6.1391	4.6078	- .93560	.066695	.03358	-56.6259
3	CO	7.0996	1.2760	- .28775	.022356	-.15987	-27.7346
4	$\text{H}_2$	5.5557	1.7872	- .28813	.019515	.16118	.76498
5	$\text{O}_2$	7.8658	.68837	- .031944	-.002687	-.20139	- .89346
6	$\text{N}_2$	6.8078	1.4534	- .32899	.025610	-.11895	- .33184
7	$\text{C}_8\text{H}_{18}^{**}$	.55313	181.62	-97.787	20.402	-.03095	-60.518

\*picked to give enthalpy datum at  $0^{\circ}\text{K}$

\*\*The coefficients apply to 2,2,4 trimethyl pentene (iso-octane). Different equations may be needed for different fuels.

## V) Molecular weight of the burned mixture

$$\bar{M} = \begin{cases} \tilde{M}/((1-\varepsilon)\phi + 1 + \psi) & \phi \leq 1 \\ \tilde{M}/((2-\varepsilon)\phi + \psi) & \phi > 1 \end{cases}$$

**APPENDIX D Computer Program**

## Program Listing

```

C
C *** PREDICTING THE DETAILED PERFORMANCE AND EMISSION CHARACTERISTICS*** C
C *** OF THE TEXACO CONTROLLED COMBUSTION-STRATIFIED CHARGE ENGINE *** C
C
C *** THIS PROGRAM HAS BEEN DEVELOPED IN ORDER TO PREDICT THE *** C
C *** DETAILED PERFORMANCE AND THE NOX EMISSION CHARACTERISTICS OF THE ** C
C *** TCCS, STRATIFIED CHARGE ENGINE, GIVEN ENGINE GEOMETRY, FUEL PROPERTIES C
C *** AND THE OPERATING CONDITIONS.                                     *** C
C
C *** THE DETAILS OF THE THEORY *** C
C *** AND ANY OTHER INFORMATION REGARDING THIS PROGRAM CAN BE HAD FROM *** C
C *** SAB(H)-HIRAKI, 31-159, 253-2388                                     *** C
C
C *** ALL RIGHTS RELATED TO THIS PROGRAM ARE RESERVED BY SLOAN AUTOMOTIVE C
C *** LABORATORY, M.I.T. C
C
C ***WARNING*** THIS PROGRAM IS NOT FINAL VERSION. THIS PROGRAM WILL C
C BE CHANGED WITHOUT NOTICING IN FUTURE. C
C
C INPUT VARIABLES
C SEE INPUT SUBROUTINE
C
C OUTPUTS
C ANGLE= CRANK ANGLE DEG
C P,PRESS= CYLINDER PRESSURE ATA
C RPPM= NOX CONCENTRATION PPM
C WNO= NOX MASS G*10**6
C NUM=ELEMENT NUMBER
C #=1 NOT YET BURNED
C      2 PLUME IS DEVELOPING
C      3 PLUME HAS FULLY DEVELOPED
C T,T,AV= TEMPERATURE OF THE ELEMENT
C ITEM= UNBURNED TEMPERATURE K(FOR JET ELEMENT)
C RTEME= BURNED TEMPERATURE K(FOR JET ELEMENT)
C MASS= TOTAL MASS OF THE ONE ELEMENT MG
C PMASS= PLUME MASS MG(FOR JET ELEMENT)
C RMASS= BURNED GAS MASS MG(FOR JET ELEMENT)
C V = VOLUME CM*3
C FOUT= EQUIVALENCE RATIO
C CP= SPECIFIC HEAT AT CONSTANT PRESSURE CAL/G K
C ENTH= ENTHALPY CAL/G
C RPPM= NO CONCENTRATION PPM
C WNO= MASS OF NO G*10**6
C R= JET LOCATION RADIAL CM
C Z= JET LOCATION AXIAL CM.
C DEG= JET LOCATION TANGENTIAL DEG
C HLOSE= HEAT LOSS CAL
C RATIO= BURNED MASS FRACTION
C PS= OUTPUT POWER TOTAL SINCE INTAKE VALVE OPENS WPS
C AEFFI= INTAKE EFFECTIVE FLOW AREA CM**2
C GWT= INTAKE MASS FLOW G/S
C AEFF= EXHAUST EFFECTIVE FLOW AREA CM**2
C GWE= EXHAUST MASS FLOW G/S
C
C SUBROUTINES REQUIRED
C 1. RUNIGR
C 2. CPFRA
C 3. IMPOR
C 4. EXPOR

```

```

C   5. HEATR
C   6. TINPUT
C   7. CALCUL
C   8. DELTA
C   9. DCAL
C 10. JET
C 11. VGAS
C 12. CONT
C 13. FNT
C 14. VOLCY
C 15. HPROP
C 16. CLDPRO
C 17. DEPIVS
C 18. DMODT
C 19. FOTB
C 20. TWODIM
C 21. HPROP
C 22. PTCHEM
C 23. NXNSOL
C 24. FRICL  FRICTIONS
C

```

```

COMMON/EPROP/  TECHF(100),EFUEL(100),EANGL(100),EMWT(100),
1 DHFUEL(100),DHLOS(100),DEMAS(100),DEUMAS(100),
1 ERGAS(100),ECP(100),FENTH(B,100),EMASS(B,100),EEQUI(B,100),
1 EVOL(B,100),ETEMP(B,100),PCYL(B)
COMMON /STATE/ ANGLE,ANGLE,JCOND,NSTEP,NSTEP,IF
COMMON /STAT/ PPM,JLAST,NJET,PHIO,FGK
COMMON /TIMIG/ ATNTO,AEXTD,AINTC,AFXTC,AFUELS,AFUULE
COMMON /GEOMT/ STROKE,BORE,CONL,VOLFAK,VCUP,RCUP,CYLN
COMMON /SJM/ STGINI,STGEXT,STOEXT
COMMON /HETPS/ NDIVID,TMETAL(10),DHTRC(10),ARF(10)
COMMON /HETP/ PRASE,TRASE,VRASF,COHT1,COHT2,COHT,RHR(10)
COMMON /SJM/ TTGINT,TTGEXT,TTOFXT,TTUHTR(10),TOHTR(10),PS
COMMON /FUELP/ FUEL,FKCAL,ZM,ZN,PST,SAFC,VACAL
COMMON /JETS/ RJET(50),HJET(50),AJET(50),BJET(50),THFP(50),
1 VRJET(50),VZJET(50),WJET(50),VJET(50),AIN,I(50),RHJET(50),
2 PITCH(50)
COMMON /PLUME/ PMASS(50),BMASS(50),RPLUM(50),HRMASS(50)
COMMON /JETDAT/ NSWIR,A_PHA,BFTA,PH345
COMMON /SUPGAS/ FSWIR,WSWIR,SDECAY
COMMON /COMP/ PPLUM0,FNTUR,RLFSP,ASPAR,KSCALF
COMMON /OSPE/ LPT,INP,LINECO,LINEST,TEL,LTTEL
COMMON /NOXSP/ CONNO(100),PPMNO(100),NO(100),SUMDN(100),PPMEXT
DIMENSION ZMOFR(5),TMSP(100)
PFAL#4 MBAR
COMMON /FUELP/ AF(6),FMW,CX,HY,OZ,OLOVER
COMMON /OXDANT/ XI/CMPSTN/X(7),MRAR
COMMON /CONT/ ASTIN,ASTCL,ASTCR,ASTEX,ASTOV,PRININ,PRINCL,PRINFY,
1 PRINOV
COMMON /INFL/ NINEF,XINFF(20),YINFF(20),AREIND,PINT,TINT,GINT,
1 FOUINT,AREINT,XINV
COMMON /EXFL/ NEXFF,XEXFF(20),YEXFF(20),AREEXD,PEXT,TEXT,GEXT,
1 TLEFT,TLLEFT,OLEXT,OFLDX,ELEFT,AREEXT,XEXV
COMMON /AMRTE/ TAMR,PAWR
COMMON /FRIO/ RSKTPT,FCDE,RTNGN,FMED(10)
DIMENSION HTEMP(50),PLTEMP(50),PLFNT(50)
DIMENSION YTEMP(10),YDP(10)
DIMENSION YDM(2),YDM(2)

```

```

C DATA OF SPECIFIC HEAT AT CONSTANT PRESSURE VS TEMPRATURE
C DATA OF TEMPERATURE
R DATA XTEMP/
  1 500.,1000.,1500.,2000.,2250.,2500.,2750.,3000.,3250.,3500./
C DATA OF SPECIFIC HEAT AT CONSTANT PRESSURE
  DATA YCP/
    1 0.26,0.3,0.34,0.37,0.43,0.51,0.67,0.84,1.24,1.6/
C
C CARD READER AND LINE PRINTER
  INP=5
  LPT=6
C
C JCOND=1 VALVE OVERLAP PERIOD
C JCND=2 INTAKE PROCESS
C JCND=3 COMPRESSION PERIOD
C JCND=4 COMBUSTION AND EXPANSION PERIOD
C JCND=5 EXHAUST PROCESS
C
  9001 CONTINUE
    ASTEP=2.0
    PSI=3.76
C
C INITIALIZE COMBUSTION CONDITION
C IFCHE=1 NOT YET BURNED
C IFCHE=2 PLUME IS DEVELOPING IN THE JET
C IFCHE=3 PLUME IS FULLY DEVELOPED
  DO 1010 I=1,100
    IFCHE(I)=1
    COMNO(I)=0.
  1010 CONTINUE
    EMAX=10.
    MAXITG=15
    JLAST=1
    LITFL=1
    RESFRK=0.
C
C INPUT SUBROUTINE
C
  CALL INPUT
C
C NOCUL=0 PERFORMANCE ONLY
C NOCUL=1 (NO) CALCULATION WILL BE DONE
  NOCUL=1
C DO YOU WANT NOX CALCULATION?
  READ(INP,302) NOCUL,PPMEXT
C
C CALCULATION STARTING CRANK ANGLE AND ENDING CRANK ANGLE
  READ(INP,23) ANGLES,ALAST
  DEL=ZN/ZM
  EFUEL(1)=0.
  ENTINI=ENT(TINT,EQINT,SAFC)
  IF=1
  ANGLE=ANGLE$S
  ANGLE1=ANGLES
  CALL VOLCY(ANGLE,EVOL(2,1),DVCYL,STROKE,BORE,CONL,VCLFAR,VCUP)
  VCYLO=EVOL(2,1)
  FENTH(2,1)=ENT(ETEMP(2,1),EEQUT(2,1),SAFC)
  ENTIN2=EENTH(2,1)

```

```

CALL HPROD( PCYL(2), ETEMP(2+1), FFQINT(2+1) * DEL * PST * DUM * DUM * DUM *
1 DUM * DUM, EMWT(1) * ERGAS(1) * CVRG * DUM)
FCP(1)=ERGAS(1)/41.443+CVHG
EMASS(2+1)=PCYL(2)*EVOL(2+1)/(ERGAS(1)*ETEMP(2+1))

C INITIAL CONDITION
100 TTGINT=0.
TTGEXT=0.
TTOFXT=0.
JGLFFT=0
TMAX=0.
PMAX=0.
PS=0.
PSTN=0.
PSFX=0.
JCOND=0
ENTINT=ENTIN2
200 CONTINUE
DO 10 I=1,NDIVID
TOHTR(I)=0.
10 TTQHTR(I)=0.

C SWIRL DECAYING FACTOR FSWIR=1. AT THE TIME OF INTAKE VALVE CLOSING
FSWIP=1.
3000 CONTINUE
PCYL0=PCYL(2)

C CALL OPERA

C RUNG KUTTA METHOD
CALL RUNGK(ENTINT)
ANGLE1=ANGLE1+ASTEP
TTGINT=TTGINT+STGINT*ASTEP
TTGEXT=TTGEXT+STGEXT*ASTEP
TTOFXT=TTOFXT+STOEXT*ASTEP
DO 3900 I=1,NDIVID
3900 TTQHTR(I)=TTQHTR(I)+TOHTR(I)*ASTEP

C CHECK THE INTAKE FLOW
IF(JCOND.GE.3) GO TO 570
IF(TTGINT.GT.0.) GO TO 572

C INTAKE FLOW IS RESIDUAL GAS
ENTINT=ENTIN2
GO TO 570

C INTAKE FLOW IS FRESH AIR
572 ENTINT=ENTIN1
570 CONTINUE
CALL VOLCY(ANGLE1,VCYLN,VCYLN,STROKE*BORE*CONL,VCLEAR,VCUP)
DPS=((PCYL(2)+PCYL0)/2.-PAMB)*(VCYLN-VCYL0)*CYLN*RPM/900000.
VCYL0=VCYLN
PS=PS+DPS
IF(JCOND-2) 580,580,590
580 PSIN=PSIN+DPS
GO TO 590
590 IF(JCOND-5) 590,595,590
595 PSFX=PSFX+DPS
590 DO 16 I=1,NDIVID
16 TTQHTR(I)=TTQHTR(I)+TOHTR(I)*ASTEP

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      IF(IGLFFT) 500,500,510
500 GLEFT=GLEFT-STGEXT
      IF(GLFFT) 520,520,510
520 IGLFFT=1
510 CONTINUE
      IF(JCOND.NE.4) GO TO 4500

C   COMBUSTION ROUTINE

C   ESTIMATE THE PLUME TEMPERATURE
      DO 3700 I=1,IF
      IF(IECHE(I).EQ.2) GO TO 3400
      URTTEMP(I)=FTEMP(2,I)
      PLTEMP(I)=FTEMP(2,I)
      PLFNT(I)=FFNTH(2,I)
      GO TO 3700
3800 FNTJET=FFNTH(2,1)
      CALL TWODIM(10,XTEMP,YCP+PLTEMP(I),PLCP1)
      PLCP=PLCP1
      ENTPL=(EENTH(2,1)*EMASS(2,I)-ENTJET*(EMASS(2,I)-PMASS(I))/
1 PMASS(I))
      DPLT=(ENTPL-PLFNT(I))/PLCP
      DO 3820 J=1,3
      PLT=PLTEMP(I)+DPLT
      TDUM2=PLTEMP(I)+DPLT/3.
      TDUM3=PLTEMP(I)+DPLT*2./3.
      TDUM4=PLTEMP(I)+DPLT
      CALL TWODIM(10,XTEMP,YCP,TDUM2,CPDUM2)
      CALL TWODIM(10,XTEMP,YCP,TDUM3,CPDUM3)
      CALL TWODIM(10,XTEMP,YCP,TDUM4,CPDUM4)
      DPLT=(ENTPL-PLFNT(I))*(1./PLCP1+2./CPDUM2+2./CPDUM3+1./CPDUM4)/6.
3820 CONTINUE
      PLENT(I)=ENTPL
      PLTEMP(I)=PLT
3700 CONTINUE
      IF(NOCUL.EQ.0) GO TO 4500

C   CALCULATION OF NOX CHANGE BY MASS TRANSFER
      DO 4012 I=2,IF
      CONNO(I)=CONNO(I)+CONNO(1)*SUMDM(I)/(EMASS(2,I)-SUMDM(1))
4012 CONTINUE
      CONNO(1)=CONNO(1)+CONNO(1)*SUMDM(1)/(EMASS(2,I)-SUMDM(1))
      DO 4010 I=1,IF
      TMSPI(I)=EMASS(2,I)/EMWT(I)
      IF(IECHF(I).EQ.1) GO TO 4020
      IF(IECHE(I).EQ.3) GO TO 4040
      PLSPI=PMASS(I)/EMWT(I)
      GO TO 4050
4040 PLSPI=TMSPI(I)
4050 CONTINUE
      CALL FQTR(PLTEMP(I),PCY_(2),FFOUT(2,I),IFLAG,ZMDFR)
      IF(PLTEMP(I).GT.2400.) GO TO 4022
      TTNOV=1
      GO TO 4024
4022 TTNOV=4
4024 ASTNO=ASTEP/FLOAT(TTNOV)
      DO 4026 TTNO=1,IINOV
      CALL DMOST(PLTEMP(I),PCYI(2),PLSPI+ZMDFR,IFLAG,CONNO(I),
1 DCNO)

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      CONNO(I)=CONNO(I)+DCONNO*ASTNO/(RPM*5.)
4020 CONTINUE
4020 RPMNO(I)=1000000.*CONNO(I)/TWSPI(I)
WNO(I)=30.*CONNO(I)
4010 CONTINUE
    TWSPI=0.
    TCONNO=0.
    TTMSPI=0.
    TWNO=0.
    DO 4030 I=1,IF
    TCONNO=TCONNO+CONNO(I)
    TTMSPI=TTMSPI+TMSPI(I)
    TWNO=TWNO+WNO(I)
4030 CONTINUE
    TPPM=1000000.*TCONNO/TTMSPI
4500 CONTINUE
    LINECO=LINECO-1
    IF(LINECO) 2000,2000,2010
C
C PRINT OUT
2000 GO TO (2100,2200,2300,2400,2500),JCONV
C
C VALVE OVERLAP PERIOD
2100 GGNT=STGINT*CYLN*6.*RPM
GGXT=STGEXT*CYLN*6.*RPM
HTRS1=-TOHTR(1)
HTRS2=-TTDHTR(1)
WRITE(LPT,2900) ANGLE1,PCYL(2),ETEMP(2,1)*EVOL(2,1),PS,
1 FMASS(2,1),HTRS1 ,HTRS2 ,AREINT,GGNT,AREEXT,GGXT
GO TO 9100
C
C INTAKE PROCESS
2200 GGNT=STGINT*CYLN*6.*RPM
HTRS1=-TOHTR(1)
HTRS2=-TTDHTR(1)
WRITE(LPT,2910) ANGLE1,PCYL(2),ETEMP(2,1)*EVOL(2,1),PS,
1 FMASS(2,1),HTRS1 ,HTRS2 ,AREINT,GGNT
GO TO 9100
C
C COMPRESSION PROCESS
2300 SPAT=WSWIR*180./(3.1416*5.*RPM)
HTRS1=-TOHTR(1)
HTRS2=-TTDHTR(1)
WRITE(LPT,2920) ANGLE1,PCYL(2),ETEMP(2,1)*EVOL(2,1),PS,
1 FMASS(2,1),HTRS1 ,HTRS2 ,FSWTR,SRAT
GO TO 9100
C
C COMBUSTION PERIOD
C EXPANSION PERIOD
2400 CONTINUE
    IF(IE.EQ.1) GO TO 2300
    HTRS1=-TOHTR(1)
    HTRS2=-TTDHTR(1)
    TRATBU=0.
    DO 2410 I=2,IF
2410 TRATBU=TRATBU+HRMASS(I)
    TRATBU=TRATBU/FUEL
    SPAT=WSWIR*180./(3.1416*5.*RPM)
    IF(HOCNL.EQ.0) GO TO 5010
    TWNOXX=TWNO*10.*#6

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      WRITE(LPT,2930) ANGLE1,PCYL(2),PS,FS*IR,SRAT,HTRSP
      WRITE(LPT,2931) TRATRI,VCYLV,PHIO,TPPM,TWNXX,HTRSI
      GO TO 5015
5010 WRITE(LPT,2930) ANGLE1,PCYL(2),PS,FS*IR,SRAT,HTRSP
      WRITE(LPT,2932) TRATRI,VCYLV,PHIO, HTRSI
5015 DO 5020 I=1,IF
      HHLOS=DHLOS(I)
      IF(NOCUL,EQ.0) GO TO 5022
      IF(I.EQ.1) GO TO 5024
C
C NOX AND JET ELEMENT
      AJE=AJET(I)*180./3.1416
      ACO=THEP(I)*180./3.1416
      EMASMG=EMASS(2,I)*1000.
      PMASMG=PMASS(I)*1000.
      RMASMG=RMASS(I)*1000.
      RATBU=HRMASS(I)/FFUFL(I)
      WNOMMG=WNO(I)*10.**6
      WRITE(LPT,2936) I,IFCHE(I),ETEMP(2,I),PLTEMP(I),RATBU
      1 EMASMG ,PMASMG ,RMASMG ,EVOL(2,I),EEQUI(2,I),ECP(I).
      2 EENTH(2,I),PPMNO(I),WNOMMG,RJET(I),HJET(I),AJE,BJET(I),ACO,HHLOS
      GO TO 5020
C
C NOX AND AIR
5024 EMASMG=EMASS(2,I)*1000.
      WNOMMG=WNO(I)*10.**6
      WRITE(LPT,2937) I,IECHE(I),ETEMP(2,I),
      1 EMASMG, EVOL(2,I),EEQUI(2,I),ECP(I).
      2 EENTH(2,I),PPMNO(I),WNOMMG, HHLOS
      GO TO 5020
C
C PERFORMANCE AND JET
5022 IF(I.EQ.1) GO TO 5026
      AJE=AJET(I)*180./3.1416
      ACO=THEP(I)*180./3.1416
      EMASMG=EMASS(2,I)*1000.
      PMASMG=PMASS(I)*1000.
      RMASMG=RMASS(I)*1000.
      RATBU=HRMASS(I)/FFIFL(I)
      WRITE(LPT,2934) I,IFCHE(I),ETEMP(2,I),PLTEMP(I),RATBU
      1 EMASMG ,PMASMG ,RMASMG ,EVOL(2,I),EEQUI(2,I),ECP(I).
      2 EENTH(2,I), RJET(I),HJET(I),AJE,BJET(I),ACO,HHLOS
      GO TO 5020
C
C PERFORMANCE AND AIR
5026 EMASMG=EMASS(2,I)*1000.
      WRITE(LPT,2938) I,IFCHE(I),ETEMP(2,I),
      1 EMASMG, EVOL(2,I),EEQUI(2,I),ECP(I).
      2 EENTH(2,I), HHLOS
5020 CONTINUE
      GO TO 4100
C
C EXHAUST PROCESS
2500 GGXT=STGEA*TCYLNP6.*PPM
      HTRSI=-T0HTR(1)
      HTRS2=-T1HTR(1)
      WRITE(LPT,2940) ANGLE1,PCYL(2),FTEMP(2,I),EVOL(2,I),PS,
      1 EMAS(2,I),HTRSI ,HTRS2 ,ARFFXT,GGXT
      GO TO 4100
2900 END IF(I.EQ.1).

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      1           1X,F6.2+1X,F5.0+1X,F6.0+1X,F6.2+2X,F8.3+
      1           E11.3  +E11.3  +1X,F6.2+1X,F7.2+2X,F6.2+1X,F7.2)
2910 FORMAT(1H ,F5.1,
      1           1X,F6.2+1X,F5.0+1X,F6.0+1X,F6.2+2X,F8.3+
      1 F11.3  +F11.3  +1X,F6.2+1X,F7.2 )
2920 FORMAT(1H ,F5.1,
      1           1X,F6.2+1X,F5.0+1X,F6.0+1X,F6.2+2X,F8.3+
      1 F11.3+F11.3+1X,F6.3+1X,F6.2)
2930 FORMAT(1X,1X,F5.1+2X,IPRFS$,=1,F6.2+1X,IPS=1,F6.1+1X,FSWIP=1,F6.3+
      1 1X,'S,RT=1,F6.3+1X,SCUM,H,REJ=1,E9.3)
2931 FORMAT(2X,EHTOTAL,14X,F7.3+21X,2F7.2+14X,F7.0+30X,E9.2)
2932 FORMAT(2X,SHTOTAL,14X,F7.3+21X,2F7.2+14X,          44X,E9.2)
2934 FORMAT(2X,T2,1X,T2+2F7.0+F7.3+3F7.1+2F7.2+F7.3+F7.1+14X,
      1 F6.1,F6.2,F6.0,F6.3,F6.0,E9.2)
2936 FORMAT(2X,T2,1X,T2+2F7.0+F7.3+3F7.1+2F7.2+F7.3+F7.1+F7.0+F7.2,
      1 F6.1,F6.2,F6.0,F6.3,F6.0,E9.2)
2937 FORMAT(2X,T2,1X,T2, F7.0+14X,F7.1+14X+2F7.2+F7.3+F7.1+F7.0,
      1 F7.0,     18X,1P2X,E9.2)
2938 FORMAT(2X,T2,1X,T2, F7.0+14X,F7.1+14X+2F7.2+F7.3+F7.1+
      1 32X,12X,E9.2)
2940 FORMAT(1H ,F5.1,
      1           1X,F6.2+1X,F5.0+1X,F6.0+1X,F6.2+2X,F8.3+
      1 F11.3, E11.3 +1X,F6.2+1X,F7.2)
9100 CONTINUE
LTNFC0=LINFST
2010 IF(PMAX=PCYL(2)) 7000,7030,7030
7000 PMAX=PCYL(2)
PMAXAN=ANGLE1
7030 CONTINUE
C
C   IF THE TEMPERATIRES OF EVERY ELEMENTS ARE BELOW TEMLOW(AROUND 1700K).
C   THEREWILL BE NO CHANGE IN NO VALUE.
C   WE WILL CONSIDER ONLY ONE AVERAGE ELEMENT.
TEMLOW=2200.
IF(JCOND.NE.4) GO TO 7300
AAN=ANGLE1-(ANGLE1+30.)
IF(AAN.LT.0.) GO TO 7300
IF(IE,EO,1) GO TO 7300
IF(ETEMP(2,2).GT.TEMLOW) GO TO 7300
IF(ETEMP(2,IE).GT.TEMLOW) GO TO 7300
C
C   CALCULATE THE TOTAL MASS AND ENTHALPY
TENTH=0.
TMASS=0.
DO 7320 I=1,IF
    TENTH=TENTH+FENTH(2,I)*REMASS(2,I)
    TMASS=TMASS+EMASS(2,I)
7320 CONTINUE
C
C   CALCULATE THE AVERAGE ENTHALPY
AVENT=TENTH/TMASS
C
C   CALCULATE THE AVERAGE TEMPERATURE
C   FIRST FIND OUT THE ELEMENT WHICH ENTHALPY IS CLOSE TO THE
C   AVERAGE ENTHALPY
DENTM=1000.
IT=1
DO 7330 I=1,IF
    DENT=ARS(AVENT-FENTH(2,I))
    IF(DENTM.LT.DENT) GO TO 7330

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DENTM=DENT
IT=1
7320 CONTINUE
C
C DEFINE THE NEW PROPERTIES
ETEMP(2,1)=ETEMP(2,1)+ (AVENT-FFNTH(2,1))/FCP(1)
FFQUI(2,1)=PHI0
FFNTH(2,1)=AVENT
EMASS(2,1)=TMASS
CALL HPROD(PCYL(2),FTFMP(2,1),FFQUI(2,1)*DFL,PST,ENTHLP,CSURP,
1 CSUBT,RHO,DRHO0T,DRHO0P,EMWT(1),FRGAS(1),CVBG,FBGR)
FCP(1)=FRGAS(1)/4.447*CVHG
EVOL(2,1)=VCYLN
TF=1
WRITE(LPT,7340)
WRITE(LPT,7342) PCYL(2),ETEMP(2,1),FFQUI(2,1),FFNTH(2,1),
1 EMASS(2,1)
IF(NOCUL.EQ.0) GO TO 7331
C
C NOX AMOUNT WILL BE DEFINED.
C EXHAUST NOX ON MASS BASE
ANOXEX=TWN0*TTGINT/TMASS*PPM/120.
WRITE(LPT,7450) TPPM,ANOXEX
7331 CONTINUE
WRITE(LPT,7420)
WRITE(LPT,7430)
7340 FORMAT(//,10X,*-*EXPANSION PROCESS IS CALCULATED AS ONE ELEMENT**  

1*1)
7342 FORMAT(15X,1BHPRESSURE = ,F10.2,'ATA',/,  

1 15X,1RHAV. TEMPERATURE = ,F10.1,'< DEG',/  

2 15X,1RHAV. FQUI. RATIO = ,F10.3,/  

3 15X,1RHAV. ENTHALPY = ,F10.2,'CAL/G',/  

4 15X,1BHTOTAL MASS = ,F10.4,'G')
7420 FORMAT(/2X,4HTHD,3X,4H P ,3X,4H T ,3X,4H V ,3X,4HWNRK,  

1 3X,7HCYL,MAS,3, ' HEAT TRANSFER,7X,4HFSWR,3X,4HS,PT)
7430 FORMAT(2X,4HDFG ,3A,4HATA ,3X,4H K ,2X,5HCM**3,3X,4H PS ,
1 3X,7H G ,3X,15H CA/A CAL ,11X,3X,4HPPM)
7450 FORMAT(//,10X,*-*EXHAUST NOX***1,/  

1 15X,15HNOX CONCEN. = ,F10.1,'PPM',/  

2 15X,15HTOTAL MASS = ,E12.3,'G')
7300 CONTINUE
IF(ANGLE1=ALAST) 7040,7050,7050
7040 GO TO 3000
7050 CONTINUE
ITEXT=1
QMANI=TTGEYT/TTGEXT
TEXT=700.
7240 DO=ENT(TEXT,FFOUT(2,1),SAFC)-QMANI
R0=DO/QMANI
IF(ABS(R0)-0.003) 7220,7220,7230
7230 IF(ITEXT-2) 7200,7210,7210
7200 ITEXT=2
XPOM(1)=700.
YR0M(1)=R0
TEXT=700.
GO TO 7240
7210 CALL CONI(TEXT,R0,0.,0.,XPOM,YR0M,ITEXT)
ITEXT=ITEXT+1
IF(ITEXT-2) 7240,7220,7220
7220 CONTINUE

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ITFL=ITFL+1
WRITE(LPT,9090) TEXT
GO TO 7050
7070 CONTINUE
IF( !TFL-LITFL ) 7260,7260,7050
7260 ANGLE1=ANGLE1-720.
GO TO 100
7050 CONTINUE
VSTROK=BORF*BORE*STROKE/4.*3.1416
CALL FRCT
WRITE(LPT,4092) FMFP(2),FMFP(3),FMFP(4),FMFP(5),FMFP(6),
1 FMFP(7),FMFP(8),FMFP(1)
ATMFP=PS/VSTROK*7500000./(RPM/120.)
PIMFP=PSIN/VSTROK*7500000./(PPM/120.)
PFMEP=PSFX/VSTROK*7500000./(RPM/120.)
RMFP=AIMEP-FMEP(1)
RHP=RMFP*VSTROK/7500000.*(RPM/120.)
AISFC= FUEL*3600./PS*PPM/120.
PSFC= FUEL*3600./RHP*PPM/120.
WRITE(LPT,4000) PIMFP,PSIN
WRITE(LPT,4010) PEMFP,PSEX
WRITE(LPT,4020) AIMEP,PS,AISFC
WRITE(LPT,4030) RMFP,RHP,PSFC
RHERE=TT*WTR(1)/(FIIFL*(FCAL-VACAL))
PFRMI=CYLN*PPM/2.
DO 17 I=1,NDIVID
17 TTQHTR(I)=TTQHTR(I)*PFRMI
WRITE(LPT,4055)
WRITE(LPT,4056) (TTQHTR(I),I=1,NDIVID),RHERE
WRITE(LPT,4070) PMAX,PMAKAN
23 FORMAT(RF10.0)
301 FORMAT(I2)
302 FORMAT(12,F10.0)
4000 FORMAT(//,10X,1PIMFP=1.F8.2,1G/CM**2*,5X,1PSIN=1.F8.2,1HP*)
4010 FORMAT(1H .10X,1PEMFP=1.F8.2,1G/CM**2*,5X,1PSFX=1.F8.2,1HP*)
4020 FORMAT(1H ./,10X,1AIMEP=1.F8.0,1G/CM**2*,5X,1THP=1.F8.2,1HP*,
1 5X,1AISFC=1.F8.2,1G/THP,HR*)
4030 FORMAT(1H ./,10X,1 RMFP=1.F8.0,1G/CM**2*,5X,1RHP=1.F8.2,1HP*,
1 5X,1 PSFC=1.F8.2,1G/RHP,HR*)
4055 FORMAT(1H ./,10X,1HEAT REJECTION= CAL/MTN*)
4056 FORMAT(1H . 9X,15HTOTAL 4. RFJ = ,F10.4,/,*
1 10X,15HCYL. LINER = ,F10.4,/,*
2 10X,15HPISTON TOP = ,F10.4,/,*
3 10X,15HPISTON CUP = ,F10.4,/,*
4 10X,15HCYL. HEAD = ,F10.4,/,*
5 10X,15HINT. VALVE = ,F10.4,/,*
6 10X,15HXH. VALVE = ,F10.4,/,*
7 7X,18-HFAT RFJ./FUEL = ,F10.3)
4070 FORMAT(1H ./,10X,1PEAK CYL PRESS=1.F10.1,1AT,FS,1,1DEG. CA*)
4090 FORMAT(1H ./10X,1EXHAUST TEMPERATURE=1.F8.1,1KDFG*)
4092 FORMAT(//,1**PREDICTION OF THE FRICTION LOSS**1,/
1 5X,16H1SC. AND PUMPS= , F12.3.7HG/CM**2*/,
1 5X,16HCA4 GEAR = , F12.3.7HG/CM**2*/,
1 5X,16HBEARING = , F12.3.7HG/CM**2*/,
1 5X,16HOL.AY = , F12.3.7HG/CM**2*/,
1 5X,16HVISCOS PISTON = , F12.3.7HG/CM**2*/,
1 5X,16HSRING TENSION = , F12.3.7HG/CM**2*/,
1 5X,16HSRING GAS PRESS = , F12.3.7HG/CM**2*/,
1 4X,1-----1,/
1 5X,16 HTOTAL LOSS = , F12.3.7HG/CM**2*)

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6001 FORMAT(2X,2I2,7E12.4)
6010 FORMAT(//,F10.1)
6000 FORMAT(2X,2I2,9E12.4)
6050 FORMAT(2E12.4)
6080 FORMAT(6F10.2,PF10.0,3F10.4)
9000 READ(IUP,301) NEXTO
    IF(NEXTO.EQ.1) GO TO 9001
    CALL EXIT
END
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SUBROUTINE DCAL

C
C C CALCULATION OF HEAT RELEASE FOR EACH ELEMENT
COMMON/FPROP/ 1FCHF(100),EFUEL(100),EANGL(100),FMWT(100),
1 DHFUEL(100),DHLDS(100),DIEMAS(100),DOEMAS(100),
1 ERGAS(100),ECP(100),FENTH(B,100),FMASS(B,100),FEQUI(B,100),
1 FVOL(B,100),FTEMP(B,100),PCYL(B)
COMMON /STATE/ ANGLF1,ANGLE,JCOND,ASTEP,NSTEP,IE
COMMON /STAT1/ PPM,JLAST,NJET,PHIO,EGR
COMMON /FUELP/ FUEL,FYCAL,ZM,ZN,PSI,SAFC,VACAL
COMMON /JETS/ RJFT(50),HJET(50),AJET(50),BJET(50),THER(50),
1 VRJET(50),VZJFT(50),WJFT(50),VJET(50),AINJ(50),RHJET(50),
2 PITCH(50)
COMMON /PLUME/ PMASS(50),RPLUM(50),HRMASS(50)
COMMON /JFTDAT/ NSWIR0,ALPHA,HETA,RHGAS
COMMON/COMP/ RPLUM0,ENTUR,RLFSP,ASpark,TSCALE
DFL=ZN/ZM
IF(IE.EQ.1) GO TO 300
DO 100 I=2,IE
AJE=AJET(I)*180./3.1416
C HEAT RELEASE =0 UNLESS SPECIFIED LATER
DHFUEL(I)=0.
C CHECK WHETHER THE FUEL ELEMENT REACHES THE SPARK PLUG OR NOT.
IF(AJE.LT.ASpark) GO TO 100
IF(PMASS(I).GT.1.E-7) GO TO 400
C SET THE INITIAL PLUME MASS AND GURNED MASS
PPLUM(I)=RPLUM0
PMASS(I)=RHJET(I)**4./3.*3.1416*RPLUM0**3
C SCALE FACTOR
PMASS(I)=PITCH(I)/2.*PMASS(I)
BMASS(I)=PMASS(I)**2./3.
IECHE(I)=2
400 DO 410 IP=1,10
C TURBULENT ENTRAINMENT RATE
UP=FNTUR*VJET(I)
DPMASS= SQRT(RHJFT(I)*RHJET(I)**4.*3.1416*RPLUM(I)**2.*IP)
DPMASS=DPMASS*ASTEP/(6.*RPM)/10.
C SCALE FACTOR
DPMASS=DPMASS*PITCH(I)/2.
C EFFECT OF FLAME COMING BACK
IF(IECHE(2).NE.3) GO TO 402
DPMASS=DPMASS**2.
402 CONTINUE
PMASS(I)=PMASS(I)+DPMASS
IF(PMASS(I).LT.FMASS(2,I)) GO TO 420
PMASS(I)=FMASS(2,I)
IECHE(I)=3
420 TCHA=TSCALE/RLFSP
DPMASS=(PMASS(I)-BMASS(I))/TCHA*ASTEP/(6.*RPM)/10.
C
BMASS(I)=BMASS(I)+DPMASS
C NEXT EQUATION INCLUDES THE SCALE FACTOR ABOUT CALCULATION PITCH
RPLUM(I)=(PMASS(I)**3./PITCH(I)/(RHJFT(I)**4.*3.1416))**0.373

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410 CONTINUE
  CALL UPROP(PCYL(1),ETEMP(1,I),FFQUT(2,I)*DEL,PSI+0.,ENTAIR,
  1 DUM,DUM,DUM,DUM,DUM,DUM)
  CALL HPROD(PCYL(1),ETEMP(1,I),FFQUT(2,I)*DEL,PSI,FNTGAS,
  1 DUM,DUM,DUM,DUM,DUM,DUM,DUM)

C INCLUDING THE FORMATION ENTHALPY
  XX=(ENTAIR-FNTGAS)*1000./FKCAL/FEOUT(2,I)*(SAFC+FFQUT(2,I))
  IF (XX-1.) 430,440,440
440 XX=1.
430 HRMASO=HRMASS(1)
  HRMASS(I)=FFUFL(I)*RMASS(I)/EMASS(2,I)*XX
  DHFUEL(I)=(HRMASS(I)-HRMASO)*FKCAL/ASTEP
  TRMASS=TRMASS+HRMASS
  TORMAS=TORMAS+DBMASS
100 CONTINUE
300 DHFUEL(1)=0.
  RETURN
  END

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SUBROUTINE INPUT
COMMON/EPROP/ IECHF(100),EFUEL(100),EANGL(100),EMWT(100),
1 DHFUEL(100),DHLDS(100),DIEMAS(100),DOEMAS(100),
1 ERGAS(100),ECP(100),FENTH(8,100),FMASS(8,100),EEQUI(8,100),
1 EVOL(8,100),FTEMP(8,100),PCYL(8)
COMMON /STAT1/ RPM,JLAST,NJET,PHIO,EGR
COMMON /TIMIG/ ATINT,AFTXT,AINTC,AEXTC,AFUELS,AFUELLE
COMMON /GDMT/ STROKE,BORE,CONL,VCLFAR,VCUP,RCUP,CYLN
COMMON /HETRS/ NDIVID,TMETAL(10),OHTRC(10),ARE(10)
COMMON /STATE/ ANGLE1,ANGLE,JCOND,ASTEP,NSTEP,TF
COMMON /FUELP/ FUEL,FKCAL,ZM,ZN,PST,SAFC,VACAL
COMMON /JETS/ RJET(50),HJET(50),AJET(50),BJET(50),THER(50),
1 VRJET(50),VZJET(50),WJET(50),VJET(50),AINJ(50),RHJET(50),
2 PITCH(50)
COMMON /PLUME/ PMASS(50),BMASS(50),RPLUM(50),HRMASS(50)
COMMON /JETDAT/ WSWIR0,ALPHA,RETA,RHGAS
COMMON /SURGAS/ FSWIR,WSNIR,SDFCAY
COMMON/COMR/ RPLUM0,FNTUR,RLFSP,ASPARK,TSCALE
COMMON /OSOPE/ LPT,TNP,LINECO,LINEST,TEL,LITEL
REAL*4 MBAR
COMMON /FUEL/ AF(6),FNW,CX,HY,DZ,DLOWER
COMMON/OXDANT/XT/CMPSTN/X(7),MBAR
COMMON/CONTL/ ASTIN,ASTCL,ASTCR,ASTEX,ASTOV,PRININ,PRINCL,PRINEX,
1 PRINOV
COMMON/INFI0/ NINEF,XINEF(20),YINEF(20),AREIND,PINT,TINT,GINT,
1 EQUINT,ARFINT,XINV
COMMON/FXFLO/NFXEF,XEXEF(20),YEXEF(20),AREEXD,PEXT,TEXT,GEXT,
1 IGLEFT,TLFFT,QEXT,QFLDW,ELEFT,AREEXT,XEVX
COMMON /AMRTE/ TAMR,PAMR
COMMON /HETR1/ PBASE,TBASE,VBASE,COHT1,COHT2,COHT,+HR(10)
COMMON /FRDT/ RSKTRT,FCDE,RINGN,FMEP(10)
DIMENSION YINLI(20),XCOEI(20),YCOEI(20),YEXLT(20),XCOFE(20),
1 YCOEE(20)
TNP=5
IPT=6
RFCSRK=0.
DEL=ZN/ZM
WRITE(LPT,3000)
3000 FORMAT(1H1,2X,***CYCLF SIMULATION FOR DIRECT INJECTION ENGINE**,
1VERSION 18**)
READ(INP,3010)
WRITE(LPT,3010)
3010 FORMAT(80H
1
)
WRITE(LPT,3020)
3020 FORMAT(1H .//,1H ,33X,*TABLE OF INPUT DATA AND INITIAL ENGINE COND
ITIONS*,/,5X,120(1H*))
C
C READ AND WRITE THE DATA OF ENGINE GEOMETRY
C
C STROKE=STROKE(CM)
C CONL=CONNECTING POD(CM)
C VCLFAR=CLEARANCE VOLUME( EXCLUDING CUP VOLUME,CM**3)
C VCUP=CUP VOLUME(CM**3)
C RCUP= CUP RADIUS (CM)
C CYLN= NUMBER OF CYLINDER
    READ(INP,23) STROKE,BORF,CONL,VCLEAR,VCUP,RCUP,CYLN
C
C READ AND WRITE THE DATA OF VALVE AND FUEL INJECTION TIMING
C

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C AINTO=INTAKE VALVE STARTS TO OPEN(CRANK DEGREE, AROUND -10)
C AEXTO=EXHAUST VALVE STARTS TO OPEN (AROUND 520)
C AINTC=INTAKE VALVE STARTS TO CLOSE(AROUND 200)
C AEXTC=EXHAUST VALVE STARTS TO CLOSE(AROUND 10)
C AFUELS=FUEL INJECTION STARTS (AROUND 330)
C AFULE= FUEL INJECTION ENDS (AROUND 355)
C READ(INP,21) AINTO,AEXTO,AINTC,AEXTC,AFUELS,AFULE
C
C READ AND WRITE FUEL PROPERTIES
C
C ZM= CHEMICAL FORMULA, NUMBER OF H
CZN= CHEMICAL FORMULA, NUMBER OF C
C SAFC= CHEMICALLY CORRECT AIR-FUEL RATIO
C FKCAL= LOWER HEATING VALUE OF THE FUEL
C VACAL=LATENT HEAT VALUE (CAL/G)
C READ(INP,23) ZM,ZN,SAFC,FKCAL,VACAL
C CX=ZN
C HY=ZN
C QLOWER=FKCAL/1000.
C AF(1)=-0.553
C AF(2)=182.
C AF(3)=-97.9
C AF(4)=20.4
C AF(5)=-0.0309
C AF(6)=-60.5
C XI=3.76
C ENW=0.
C OZ=0.
C
C READ AND WRITE THE DATA OF THE ENGINE OPERATING CONDITION
C
C FUEL=TOTAL FUEL AMOUNT/ 1 SHOT (GRAM)
C RPM=ENGINE SPEED (RPM)
C EGR=EXHAUST GAS RECIRCULATION
C READ(INP,23) FUEL,RPM,EGR
C
C HOW MANY REGIONS WILL YOU TAKE FOR HEAT TRANSFER AREA?(NDIVID=6)
C NDIVID=6
C
C ELEMENT 1 IS FOR TOTAL
C NDIVID=NDIVID+1
C
C READ AND WRITE THE DATA OF THE TEMPERATURE INSIDE ENGINE
C
C TR= TEMPERATURE OF PISTON TOP/
C TINT= TEMPERATURE OF INTAKE VALVE
C TEXV= TEMPERATURE OF EXHAUST VALVE
C TW= TEMPERATURE OF CYLINDER WALL
C TCYLH= TEMPERATURE OF CYLINDER HEAD
C READ(INP,23) TP,TINV,TEXV,TW,TCYLH
C TMETAL(2)=TW
C TMETAL(3)=TP
C TMETAL(4)=TP
C TMETAL(5)=TCYLH
C TMETAL(6)=TINV
C TMETAL(7)=TEXV
C
C CALCULATIONS FOR THE DISTANCES FROM THE CENTER POINT
C THESE DATA WILL BE USED TO CALCULATE THE VELOCITIES AT THE WALL
C RHR(2)=RORF/2.
C RHR(3)=(RORF/2.+RCUP)/2.

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PHR(4)=RCUP
PHR(5)=RORF/(2.*1.414)
PHR(6)=RORF/4.
PHR(7)=RORF/4.

C
C HEAT TRANSFER COEFFICIENTS
C
C COHT1,COHT2= HEAT TRANSFER COEFFICIENT
C   COHT1=2.28
C   COHT2=0.0072
C   COHT=ADJUSTING TOTAL HEAT TRANSFER AMOUNT(MAYRF 1)
C   READ(INP,23) COHT1,COHT2,COHT

C
C READ AND WRITE THE DATA OF INITIAL JET CONDITIONS
C
C ATNJV=JET DIRECTION ANGLE FROM VERTICAL LINE (DEGREE)
C AINJT=JET DIPIETION ANGLE FROM TANGENTIAL LINE (DEGREE)
C RINIT= JET RADIAL LOCATION WHEN FUEL IS INJECTED (CM)
C RINIT= JET INITIAL RADIUS (CM)
C   READ(INP,23) ATNJV,AINJT,RINIT,RINIT
C   ATNJV= AINJV*3.1416/180.
C   AINJT= AINJT*3.1416/180.

C
C READ AND WRITE DATA OF AIR ENTRAINMENT PARAMETER
C
C WSRATO= SWIRL RATIO AT RDC (*RPM)
C ALPHA= ENTRAINMENT PARAMETER FOR PARALLEL VELOCITY DIFFERENCE
C   (0.11 IS RECOMMENDED)
C BETA= ENTRAINMENT PARAMETER FOR NORMAL VELOCITY DIFFERENCE
C   (BETA=0.6 IS RECOMMENDED)
C RHFUEL= DENSITY OF FUEL (GRAM/CM**3)
C RHGAS= DENSITY OF SURROUNDING GAS (GRAM/CM**3)
C SDECAY = SWIRL DECAYING FACTOR (6.5E-6 IS RECOMMENDED FOR
C   TCCS ENGINE)
C   READ(INP,23) WSRATO,ALPHA,BETA,RHFUEL,RHGAS,SDECAY
C   WSWIRO=3.1416/180.*RPM*6.*WSRATO

C
C READ DATA OF COMBUSTION PARAMETER
C
C RPLUM0= INITIAL PLUME RADIUS(CM)
C ENTUR= TURBULENCE ENTRAINMENT PARAMETER
C RLFSR= LAMINAR FLAME SPEED(CM/SFC)
C ASPARK=SPARK PLUG LOCATION FROM FUEL INJECTION NOZZLE(DEG)
C   READ(INP,23) RPLUM0,ENTUR,RLFSR,ASPIRK

C
C
C DATA OF INTAKE AND EXHAUST SYSTEM
C DINV= DIAMETER OF INTAKE VALVE
C SINV=MAXIMUM LIFT OF INTAKE VALVE
C XINV=NUMBER OF INTAKE VALVE
C DEXV= DIAMETER OF EXHAUST VALVE
C SEXV= MAXIMUM LIFT OF EXHAUST VALVE
C XEXV=NUMBER OF EXHAUST VALVE
C   READ(INP,23) DINV,SINV,DEXV,SEXV,XINV,XEXV
C   APETND=3.1416*DINV*SINV*XINV
C   APFEXTD=3.1416*DEXV*SEXV*XEXV
C   APE(3)=3.1416/4.* (RORF+RDFE-RCUP+RCUP*4.)
C   APE(4)=VCUP*2./RCUP
C   APE(6)=3.1416/4.*DTNV*DINV
C   APE(7)=3.1416/4.*DEXV*DEXV

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ARE(5)=3.1416/4.*BORE*BORE-ARE(6)-ARE(7)
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C
C DATA OF FRICTIONS
C   RSKIRT= EQUIVALENT LENGTH OF PISTON SKIRT( PROJECTED ARE OF SKIRT
C           / CYLINDER BORE DIAMETER)
C   FCOE= JOURNAL BEARING SIZE COEFFICIENT
C   RINGN= TOTAL NUMBER OF PISTON RINGS PER CYLINDER
C   RFAD(1NP,22) RSKIRT,FCOE,RINGN
C READ DATA OF VALVE LIFT VS. NORMALIZED CRANK ANGLE FOR INTAKE VALVE
  READ(INP,301) NINEF
  READ(INP,301) NINCO
  READ(INP,23) (XINEF(I),I=1,NINEF)
  READ(INP,23) (YINLI(I),I=1,NINFE)
  READ(INP,23) (XCOEI(I),I=1,NINCO)
  READ(INP,23) (YCOEI(I),I=1,NINCO)
  DO 1000 I=1,NINEF
    VLIFR=SINV*YINLI(I)/DTINV
    CALL TWODIV(NINCO,XCOEI,YCOEI,VLIFR,COEF)
    YINFEF(I)=YINLI(I)*COEF
1000 CONTINUE
C READ DATA OF VALVE LIFT VS. NORMALIZED CRANK ANGLE FOR EXHAUST VALVE
  READ(INP,301) NEXEF
  READ(INP,301) NEXCO
  READ(INP,23) (XEXEF(I),I=1,NEXEF)
  READ(INP,23) (YEXLI(I),I=1,NEXEF)
  READ(INP,23) (XCOEE(I),I=1,NEXCO)
  READ(INP,23) (YCOEE(I),I=1,NEXCO)
  DO 1010 I=1,NEXEF
    VLIFR=SEXV*YEXLI(I)/DENV
    CALL TWODIV(NEXCO,XCOEE,YCOEE,VLIFR,COEF)
    YEXEF(I)=YEXLI(I)*COEF
1010 CONTINUE
C
C HOW MANY ELEMENTS DO YOU WANT TO DIVIDE THE INJECTED FUEL INTO ?
C 10 ELEMENTS ARE RECOMMENDED
  READ(INP,301) NJET
C
C AMBIENT CONDITION
C   TAMR= AMBIENT TEMPERATURE
C   PAMR= AMBIENT PRESSURE
  READ(INP,23) TAMR,PAMR
C
C INTAKE AND EXHAUST PRESSURE
C   PINT=INTAKE PRESSURE (ATA)
C   PEXT=EXHAUST PRESSURE (ATA)
  READ(INP,23) PINT,PEXT,TINT
C
C COMPUTING INCREMENT
  READ(INP,23) ASTIN,ASTCL,ASTCR,ASTEX,ASTOV
C
C PRINT CONTROL DATA
  READ(INP,23) PRININ,PRINCL,PRINEX,PRINOV
C
C INITIAL ENGINE CONDITION
  READ(INP,23) PCYL(2),FTEMP(2,1),EFQUT(2,1),TEXT
  ELEFT=EFQUT(2,1)
  TLEFT=ETEMP(2,1)
C
C COMPRESSION RATIO

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DISP=3.1415*BORE*ROPE/4.*STROKE
CR=(VCLEAR+VCUP+DISP)/(VCUP+VCLEAR)

C TAYLOR MICRO SCALE
TSCALE=SINV/CP*0.17
VINIT= FUFL/RHFUEL/(3.1416*BINIT**2*(AFUELE-AFUELS))*(6.*RPM)
WRITE(6,5200)
WRITE(6,5210) VINIT
5200 FORMAT(2X,'INITIAL JET SPEED')
5210 FORMAT(10X,'VINIT=1.F12.1,CM/SEC')

C SET THE INITIAL CONDITIONS FOR ALL JET ELEMENTS
ASTCB=(AFUFLE-AFUELS)/FLOAT(NJFT)
ASTEP=ASTCR
NNJET=NJET+1
DO 100 I=2,NNJET
BJET(I)=BINIT
THFR(I)=0.
VJET(I)=VINIT
WJET(I)=VINIT*SIN(AINJV)*COS(AINJT)/RINIT
VRJET(I)=-VINIT*SIN(AINJV)*SIN(AINJT)
VZJET(I)=VTINIT*COS(AINJV)
RJFT(I)=RINIT
HJET(I)=0.
AJET(I)=0.
RHJET(I)=RHFUFL
RPLUM(I)=RPLUM0
PMASS(I)=0.
BMASS(I)=0.
HRMASS(I)=0.
AINJ(I)=AFJFLS+FLOAT(I-2)*ASTEP
C NEXT ASSUMPTION( FEQUI=3. ) WAS MADE FOR GETTING APPROPRIATE
C THERMODYNAMIC PROPERTIES
FFQUI(2,I)=3.
DD=AFUELE-((FLOAT(I)-1.)*ASTEP+AFUELS)
IF(DD.LT.0.) GO TO 90
EMASS(2,I)=3.1416*BINIT**2.*VINIT*ASTEP/(6.*RPM)*RHFUEL
EFUEL(I)=EMASS(2,I)
PITCH(I)=ASTEP
GO TO 100
90 EMASS(2,I)=3.1416*RINIT**2.*VINIT*(AFUELE-((FLOAT(I)-2.)*ASTEP+
1 AFUELS))/(6.*RPM)*RHFUEL*ASTEP
EFUEL(I)=EMASS(2,I)
PITCH(I)=AFUELE-((FLOAT(I)-2.)*ASTEP+AFUELS)
GO TO 110
100 CONTINUE
110 CONTINUE

C CALCULATION OF INTAKE AIR PROPERTIES
EQUIINT=EGR+FLEFT*SAFC/((1.-EGP)*(ELEFT+SAFC)+EGR*SAFC)
WRITE(LPT,7020)
WRITE(LPT,7010) STROKE,AINT0,ZM,TP,
1 CONL,AEXT0,ZV,TW,
2 ROPE,AINTC,SAFC,TCYL4,
3 VLCFAR,AEXTC,FKCAL,TINV
WRITE(LPT,7011) VCUP,AFUELS,VACAL,TEXV,
5 AFUFLF,RHFUEL
WRITE(LPT,7020)
ATNVV=ATNJV*180./3.1416
AINTT=ATNJT*180./3.1416

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      WRITE(LPT,7030) WSRATO,PPLUM0,
1           AINVV,FNTUR,
1           AINTT,ALPHA,RLESP,
3           BINIT,BFTA,ASPART,
4           RINIT,RHGAS
      WRITE(LPT,7031) RCIUP,SDFCAY,TSCALE
      WRITE(LPT,7020)
      WRITE(LPT,7040) RPM,PTNT,ASTOV,PRINOV,
1   FUEL,TINT,ASTIN,PRININ,
2   EGR,EQUINT,ASTCL,PRTNCL
      WRITE(LPT,7041) ASTCR,PRINCL,
1   PAMB,PEXT,ASTCL,PRTNCL,
2   TAMR,TEXT,ASTEX,PRINEX,
3   ELEFT
      WRITE(LPT,7020)
      WRITE(LPT,7050) DINV,ARF(6),PCYL(2),
1   SINV,ARF(7),COHT,FTEMP(2,1),
2   XINV,ARF(3),COHT,FFQUI(2,1)
      WRITE(LPT,7051) ARE(4),COHT2,TEXT,
4   DEXV,ARF(5),
5   SEXV,
6   XEXV
      WRITE(LPT,7020)
      WRITE(LPT,7060) RSKIRT,
1   FCOE,
?   RINGN
      WRITE(LPT,7020)
      WRITE(LPT,7100)
      WRITE(LPT,7110)
      WRITE(LPT,7000) (XINEF(I),I=1,NINEF)
      WRITE(LPT,7120)
      WRITE(LPT,7000) (YINFF(I),I=1,NINFF)
      WRITE(LPT,7140)
      WRITE(LPT,7110)
      WRITE(LPT,7000) (XEXEF(I),I=1,NEXEF)
      WRITE(LPT,7120)
      WRITE(LPT,7000) (YEXFF(I),I=1,NEXFF)
      RETURN
23 FORMAT(8F10.0)
6020 FORMAT(5E12.4)
6030 FORMAT(6E12.4)
6040 FORMAT(4E12.4)
6050 FORMAT(2E12.4)
6060 FORMAT(I2)
6070 FORMAT(10E12.4)
301 FORMAT(I2)
7000 FORMAT(10X,10F10.3)
7010 FORMAT(32H          ENGINE GEOMETRY      *,*
1           32H          TIMING            *,*
2           36H          FUEL PROPERTIES    *,*
3           30H          FSTIMATE TEMPERATURES  */,*
4 2X,12HSTROKE  =,F10.3,8HCM  *,*
5 17H  INT.VAL.OPEN =,F9.1,6HDEG  *,*
6 19H  ZM(ND. OF H)  =,F10.1,7H  *,*
7 18H  PISTON TOP(TP) =,F10.1,1HK,/,*
8 2X,12HCON.ROD  =,F10.2,8HCM  *,*
9 17H  EX4.VAL.OPEN =,F9.1,6HDEG  *,*
1 19H  7N(ND. OF C)  =,F10.1,7H  *,*
2 18H  CYL.WALL(TW)  =,F10.1,1HK,/,*
3 2X,12HRDRF    =,F10.3,8HCM  *,*

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4 17H INT.VAL.CLOSF =, F9.1.6HDFG \*\*,  
 5 19H SAFC(STOTCH.A/F)= \*, F10.1.7H \*\*,  
 6 18H CYL.HEAD(TCYLH)=, F10.1.1HK./,  
 7 2X.12HCLEAR.VOL. =, F10.2.8HCM\*\*3 \*\*,  
 8 17H EXH.VAL.CLOSEF =, F9.1.6HDFG \*\*,  
 9 19H LOWER HEATING =, F10.0.7H CA-/G\*,  
 5 18H INT.VALVF(TINV)=, F10.1.1HK)  
 7011 FORMAT(2X,  
 2 12HCUP VOL. =, F10.2.8HCM\*\*3 \*\*,  
 3 17H FUEL INJ.START=,F9.1.6HDFG \*\*,  
 4 19H VAPORIZING HFAT =, F10.0.7H CA-/G\*,  
 5 18H EXH.VALVE(TEXV)=,F10.1.1HK./,  
 6 32X,  
 7 17H FUEL INJ.END =, F9.1.6HDFG \*\*,  
 8 19H DENSITY =, F9.3.7HG/C\*\*3 +1H\*)  
 7020 FORMAT(2X.128H-----  
 1-----  
 2--- )  
 7030 FORMAT(42H INITIAL JET DATA \*\*,  
 1 44H JET MIXING PARAMETER \*\*,  
 2 43H PLUME MODEL \*\*,  
 3 2X.20HJET DIRECTION\*\* ,19X,1H\*,  
 4 27H SWIRL RATIO AT PDC =,F10.3.74\*RPM \*\*,  
 5 23H INITIAL PLUME RADIUS =,F10.4.74 CM \*\*,/,  
 6 2X.20H ANGLE(VERTICAL) =,F10.2.104 DEG \*\*,  
 7 27H AIR FNTRAIN. PARAMETER , 16X,1H\*,  
 8 23H FNTRATN. PARAMETER =, F10.3.9X,1H\*/,  
 9 2X.20H ANGLE(TANGENTIAL)= ,F10.2.10H DEG \*\*,  
 1 27H ALPHA =, F10.3.6X,1H\*,  
 1 23H LAM. FLAME SPEED =, F10.2.10H CM/SEC \*\*,/,  
 2 22H JET RADIUS =,F10.5.10H CM \*\*,  
 3 27H BETA =, F10.3.6X,1H\*,  
 4 23H SPARK PLUG LOCATION =, F10.2.10H DEG \*\*,/,  
 5 22H JET LOCATION(R) =, F10.3.10H CM \*\*,  
 6 27H DENSITY OF SURROUN. GAS =,F10.5.7H G/CC \*\*,  
 7 8X,19H(FROM INJ. NOZZLE) )  
 7031 FORMAT(  
 8 22H PISTON CUP RADIUS =, F10.3.10H CM \*\*,  
 9 27H SWIRL DECAY FACTOR =, E10.3.6X,1H\*,  
 1 23H TAYLOR MICRO SCALE =, F10.4.104 CM )  
 7040 FORMAT(2X,31H ENGINE CONDITION \*\*,  
 1 31H INTAKE CONDITIONS \*\*,  
 2 31H COMPUTING INTERVALS \*\*,  
 3 31H PRINT CONTROL \*\*,  
 4 2X.15HENGTE SPEED =, F8.0.8H RPM \*\*,  
 5 15H PRESSURE =, F8.3.8H ATA \*\*,  
 6 15H VALVE OVERLAP=, F8.2.8H DEG \*\*,  
 6 15H VALVE OVERLAP=, F8.2.8X,/,  
 8 2X.15HFUEL AMOUNT =, F8.5.8H G/SHOT\*,  
 9 15H TEMPERATURE =, F8.2.8H K \*\*,  
 9 15H INTAKE =, F8.2.8H DEG \*\*,  
 1 15H INTAKE =, F8.2.8X,/,  
 2 2X.15HFGR =, F8.3.7Y,1H\*,  
 3 15H EQUI. RATIO =,F8.3.7X,1H\*,  
 4 15H COMPRESSION =, F8.2.8H DFG \*\*,  
 5 15H COMPRESSION =, F8.2 )  
 7041 FORMAT(2X,  
 6 31H AMBIENT CONDITIONS \*\*,  
 7 31H EXHAUST CONDITIONS(ASSUME) \*\*,  
 8 15H COMBUSTION =, F8.2.8H DFG \*\*,

9 15H COMBUSTION =. F8.2.8X,/  
 9 2X.15HPRESSURE =. F8.2.RH ATA \*,  
 9 15H PRESSURE =. F8.2.8H ATA \*,  
 2 15H EXPANSION =. F8.2.8H DEG \*,  
 3 15H EXPANSION =. F8.2.8X,/  
 42X.15HTEMPERATURE =. F8.2.8H K \*,  
 5 15H TEMPERATURE =. F8.2.8H K \*,  
 6 15H EXHAUST =. F8.2.8H DEG \*,  
 7 15H EXHAUST =. F8.2.8X,/  
 4 32X.1H\*,  
 5 15H EQUI. RATIO =. F9.3.7X.1H\*)  
 7050 FORMAT(2X,31H) INTAKE VALVE \*.  
 1 31H HEAT TRANS. AREA \*,  
 2 31H HEAT TRANS. COEFF \*,  
 3 31H INITIAL CONDITION \*,/  
 4 2X.15HDIAVETER =. F9.3.7H CM \*,  
 5 15H INTAKF VALVE =. F9.3.7H CM\*\*?,  
 6 31H (WOSCHNI'S EQ.) \*,  
 7 15H CYL. PRESS. =. F9.2.7H ATA \*,/  
 8 2X.15HLIFT =. F9.3.7H CM \*,  
 9 15H EXHAUST VALVE =. F9.3.7H CM\*\*?,  
 9 15H COHT =. F9.5.6X.1H\*,  
 1 15H CYL. TEMP. =. F9.1.7H DEG \*,/  
 2 2X.15HNUMOFR =. F9.1.6X.1H\*,  
 3 15H PISTON TOP =. F9.3.7H CM\*\*?,  
 4 15H COHT1 =. F9.5.6X.1H\*,  
 5 15H CYL. EQUI. =. F9.3)  
 7051 FORMAT(2X,31H) EXHAUST VALVE \*,  
 1 15H PISTON TOP =. F9.3.7H CM\*\*?,  
 2 15H COHT2 =. F9.5.6X.1H\*,  
 3 15H EXHAUST TEMP. =. F9.1.7H DEG \*,/  
 4 2X.15HDIAVETO =. F9.3.7H CM \*,  
 5 15H CYL. HEAD =. F9.3.7H CM\*\*?,  
 6 2X.15HLIFT =. F9.3.7H CM \*,  
 7 15H CYL. WALL =. 7X.9 VARIABLE \*,/  
 8 2X.15HNUMBER =. F9.1.6X.1H\*)  
 7060 FORMAT(2X,31H) FRTICION LOSS \*,/  
 1 2X.15HPISTON SKIRT =. F9.3.7H CM \*,/  
 2 2X.15HJOU. BEAR. COF =. F9.3.6X.1H\*,/  
 3 2X.15HNO. OF RINGS =. F9.1.6X.1H\*)  
 7100 FORMAT(1H1.//,2X,  
 1 \*INTAKE VALVE--EFFECTIVE FLOW AREA VS. CRANK ANGLE\*)  
 7110 FORMAT(5X,\*NORMALIZED CRANK ANGLE\*)  
 7120 FORMAT(5X,\*NORMALIZED EFFECTIVE FLOW AREA\*)  
 7140 FORMAT(//,2X,  
 1 \*EXHAUST VALVE--EFFECTIVE FLOW AREA VS. CRANK ANGLE\*)  
 END

## SUBROUTINE RUNGE(ENTINT)

C THIS PROGRAM WAS MADE FOR OPERATING RUNGE-KUTTA METHOD

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COMMON/FPROP/ JFCHE(100),EFJEL(100),EANGL(100),FMWT(100),
1 DHEUEL(100),DHLDS(100),DIEMAS(100),DOEMAS(100),
1 FHRAS(100),ECP(100),FENTH(R,100),FMASS(B,100),EERUT(R,100),
1 FVOL(R,100),FTEMP(P,100),PCYL(R)
COMMON /TIMIG/ AINTO,AEXTD,AINTC,AEXTG,AFUELS,AFUELLE
COMMON /STATE/ ANGLE1,ANGLE,JCOND,ASTEP,NSTEP,IE
COMMON /STAT/ RPM,ILAST,NJET,PHIO,FSH
COMMON /GEOM/ STROKE,BORE,CONL,VCLFR,VCUP,RCUP,CYLN
COMMON /HETRS/ NDIVID,MTMETAL(10),DHTRC(10),ARE(10)
COMMON /HETRI/ PRASE,TBASE,VRASE,COHT1,COHT2,COHT,RHR(10)
COMMON /SUM1/ STGINT,STGEXT,STOEXT
COMMON /SUM2/ TTGINT,TTGEXT,TTDEXT,TTUHTR(10),TQHTR(10),PC
COMMON /FUELP/ FUEL,EKCAL,ZM,ZN,PST,SAFC,VACAL
PFAL*4 MBAR
COMMON /FUELP/ AF(6),ENW,CX,HY,DZ,DLOWER
COMMON /OXDANT/ XT/CMPSTN/X(7),MRAR
COMMON /JETS/ PJET(50),HJET(50),AJFT(50),BJFT(50),THER(50),
1 VPJET(50),VZJET(50),WJET(50),VJET(50),AINJ(50),RHJET(50),
? PITCH(E0)
COMMON /PLANE/ PHASS(50),BMASS(50),RPLUM(50),HRMASS(50)
COMMON /JETDATA/ VSWTR0,ALPHA,BETA,PH3AS
COMMON /SURGAS/ FSWTR,WSKIR,SDFCAV
COMMON /COMR/ RPLUM0,EMTUP,RLFSP,ASPARK,TSCALE
COMMON /TNFLD/ NINEF,XTNFF(20),YINEF(20),AREIND,PINT,TINT,GINT,
1 EQUINT,ARFINT,XINV
COMMON /EXFLD/NFXEF,XEXEF(20),YFXEF(20),AREEXD,PEXT,TEXT,GEXT,
1 TLEFT,TLFFT,DEXT,DFLOW,ELEFT,AREEXT,XEXV
COMMON /NOXSP/ CONNO(100),PPMNO(100),VN0(100),SUMDN(100),PPMEXT
DIMENSION SUMHT(30)
DEF=ZN/74
STGINT=0.
STGFAT=0.
STOFAT=0.
GINIT=0.
GEXT=0.
DXXT=0.
PESFRK=0.0
NSTEP=1
1FE=1E+1
11 31 I=1+1FE
SUMHT(I)=0.
?1 CONTINUE
00 24 I=1,NDIVD
24 TQHTR(I)=0.
AANGLE=AANGLE1
30 TJ(20,20,22,22,22)+JCOND0
22 CALL VGAS(0.001,0.001,RPM,ANGLE1,DUM,UJM,WSWIR,DUM,FSWTR)
FSWIR=FSWIR-SDFCAV*WSWIR*WSWIR*ASTEP/(5.*RPM)
30 TJ 21
20 FSI=1.0
WSWIR=WSIPO
?1 CONTINUE
1F(JCOND0,*1.4) G1 TO 30
?1 FE 40

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C CALCULATION OF JET MODEL IN ORDER TO GET THE ENTRAPMENT AIR
 30 DTEMAS(1)=0.
C CHECK WHETHER NEW FUEL ELEMENT IS INJECTED OR NOT
 31 IF(JET1=JET) 1010,1020,1020
1010 AXX=AFLUE+10.
  IF(ANGLE.GT.AXX) GO TO 40
  IE=IE+1
  FTEMP(2,IE)=FTEMP(2,1)
  CALL UPUPD(PCYL(2),FTEMP(2,IE),FEQJI(2,IE),DEL,PSI,
  1 FFSFRK,EENTH(2,IE),CSUR2,CSURT,RHO,DRHODT,DRHODP,CHI,
  2 FEGAS(IE),CVRG)
  FFNTH(2,IE)=FFNTH(2,IE)*1000.
  EMAT(IE)=EMAR
  ECP(IE)=EPMGAS(IE)/41.443*CVRG
  EVOL(2,IE)=FMASS(2,IE)*FEGAS(IE)*FTEMP(2,IE)/PCYL(2)
1020 CONTINUE
  DO 32 I=2,IE
  FEQUIO=FEQJI(2,I)
  EMASSO=FMASS(2,I)
  IF(EMASS(2,I).LT.0.040) GO TO 35
  IF(EMASS(2,I).GT.DOFMAS(1)) GO TO 37
C ALL AIR HAS BEEN ENTRAINED BY JET
35 ALPHA=0.
  BETA=0.
37 CONTINUE
  IF(HJFT(I).LT.0.2) GO TO 220
  IF(RJET(I).LT.1.0) GO TO 222
  JSTEP=4
  GO TO 230
222 JSTEP=8
  GO TO 230
220 JSTEP=50
230 CALL JET(RJET(T),HJFT(I),AJET(T),BJET(I),THER(I),VRJFT(I),
  1 VZJET(I),WJET(I),TOM,EMASS(2,T),ASTEP,JSTEP,RPM,ANGLE,PITCH(T),
  1 FSWIR,WSWTP)
  VJET(I)=SQRT(VRJFT(I)**2+VZJET(I)**2+(RJET(I)*WJET(I))**2)
  VOL=(3.1416*RJET(I)**2*(1.-THER(I)/(2.*3.1416))+BJET(I)**2
  1 *SIN(THER(I)/2.)*VJET(I)*PITCH(T)/(6.*RPM))
  BHJFT(I)=FMASS(2,I)/VOL
  FFUJI(2,I)=FFUFL(I)*(SAFC+EEDUI(2,1))/(EMASS(2,I)-FFUFL(I))
  1 +FFQJI(2,1)
  FEQJI(3,I)=(FEQJI(2,I)-FEQUIO)/ASTEP
  DTEMAS(I)=TOM/ASTEP
  SWDTI(I)=TOM
  DOFMAS(T)=0.
  DOFMAS(1)=DOFMAS(1)+DTEMAS(I)
  FMASS(2,I)=FMASSO
  FEQJI(2,I)=FEQUIO
220 CONTINUE
  SWDTM(1)=-DOFMAS(1)*ASTEP
  DTEMAS(1)=0.
  FEQJI(3,I)=0.
340 CONTINUE
  PCYL(1)=PCYL(2)
  DO 100 T=1,TE
  FMASS(1,I)=FMASS(2,I)
  FEQJI(1,I)=FEQJI(2,I)
  EVOL(1,I)=EVOL(2,I)

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ETEMP(1,I)=ETEMP(2,I)
FENTH(1,I)=FENTH(2,I)
100 CONTINUE
ANGLE=ANGLE+1
CALL CALC1(DVCYL,ENTINT)
CALL DELTA(DVCYL,ENTINT)
STGINT=STGINT+GINT/6.
STGEXT=STGEXT+GEXT/6.
STOEXT=STOEXT+OEXT/6.
DO 120 I=1,NDIVID
120 TOHTR(I)=TOHTR(I)+OHTRC(I)/6.

C SECOND STEP
C
NSTEP=NSTEP+1
PCYL(4)=PCYL(3)*ASTEP
PCYL(1)=PCYL(2)+PCYL(4)/2.
DO 200 I=1,IE
EMASS(4,I)=EMASS(3,I)*ASTEP
FEQUL(4,I)=FEQUL(3,I)*ASTEP
EVOL(4,I)=EVOL(3,I)*ASTEP
ETEMP(4,I)=ETEMP(3,I)*ASTEP
FENTH(4,I)=FENTH(3,I)*ASTEP
EMASS(1,I)=EMASS(2,I)+EMASS(4,I)/2.
FEQUL(1,I)=FEQUL(2,I)+FEQUL(4,I)/2.
EVOL(1,I)=EVOL(2,I)+EVOL(4,I)/2.
ETEMP(1,I)=ETEMP(2,I)+ETEMP(4,I)/2.
FENTH(1,I)=FENTH(2,I)+FENTH(4,I)/2.
IF (IECHE(I).EQ.1) GO TO 210
CALL HPRUD(PCYL(1),ETEMP(1,I),FEQUL(1,I),DEL,PSI,FNTHLP,
1 CSUBP,CSURT,RHO,DPHOUT,DRHODP,EMWT(I),ERGAS(I),CVBG,FRG2)
GO TO 212
210 CALL UPROP(PCYL(1),ETEMP(1,I),FEQUL(1,I),DEL,PSI,RESRK,ENTHLP,
1 CSUBP,CSURT,RHO,DPHOUT,DRHODP,CHI,ERGAS(I),CVBG)
EMWT(I)=EMBAP
212 CONTINUE
FCM(I)=ERGAS(I)/41.443+CVBG
SUMHT(I)=SUMHT(I)-OHL0S(I)/5.
220 CONTINUE
ANGLE=ANGLE+ASTEP/2.
CALL CALC1(DVCYL,ENTINT)
CALL DELTA(DVCYL,ENTINT)
STGINT=STGINT+GINT/2.
STGEXT=STGEXT+GEXT/2.
STOEXT=STOEXT+OEXT/2.
DO 225 I=1,NDIVID
225 TOHTR(I)=TOHTR(I)+OHTRC(I)/3.

C THIRD STEP
C
PCYL(5)=PCYL(3)*ASTEP
PCYL(1)=PCYL(2)+PCYL(5)/2.
DO 300 I=1,IE
EMASS(5,I)=EMASS(3,I)*ASTEP
FEQUL(5,I)=FEQUL(3,I)*ASTEP
EVOL(5,I)=EVOL(3,I)*ASTEP
ETEMP(5,I)=ETEMP(3,I)*ASTEP
FENTH(5,I)=FENTH(3,I)*ASTEP
EMASS(1,I)=EMASS(2,I)+EMASS(5,I)/2.
FEQUL(1,I)=FEQUL(2,I)+FEQUL(5,I)/2.

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EVOL(1,I)=EVOL(2,I)+EVOL(5,I)/2.
ETEMP(1,I)=ETEMP(2,I)+ETEMP(5,I)/2.
FFNTH(1,I)=FFNTH(2,I)+FFNTH(5,I)/2.
IF(IECHE(I).EQ.1) GO TO 310
CALL HPROD(PCYL(1),ETEMP(1,I),FFQUI(1,I)*DEL,PST,FNTHLP,
1 CSUBP,CSURT,RHO,DRH00T,DRH00P,EMWT(I),ERGAS(I),CVBG,FRGR)
GO TO 312
310 CALL HPROP(PCYL(1),ETEMP(1,I),FFQUI(1,I)*DEL,PST,RESFRK,ENTHLP,
1 CSUBP,CSURT,RHO,DRH00T,DRH00P,CHT,ERGAS(I),CVBG)
EMWT(I)=EMBAP
312 CONTINUE
ECP(1)=ERGAS(I)/41.443+CVBG
SUMHT(I)=SUMHT(I)-OHL05(I)/3.
300 CONTINUE
ANGLE=ANGLE1+ASTEP/2.
CALL CALC(DVCYL,ENTINT)
CALL DELTA(DVCYL,ENTINT)
STGINT=STGINT+GINT/3.
STGEXT=STGEXT+GEXT/3.
STOEXT=STOEXT+OEXT/3.
DO 320 I=1,N01VID
320 TOHTH(I)=TOHTH(I)+OHTRC(I)/3.

C
C   FOURTH STEP
C
PCYL(6)=PCYL(3)*ASTEP
PCYL(1)=PCYL(2)+PCYL(6)
DO 400 I=1,TE
EMASS(6,I)=EMASS(3,I)*ASTEP
FFQUI(6,I)=FFQUI(3,I)*ASTEP
EVOL(6,I)=EVOL(3,I)*ASTEP
ETEMP(6,I)=ETEMP(3,I)*ASTEP
FFNTH(6,I)=FFNTH(3,I)*ASTEP
EMASS(1,I)=EMASS(2,I)+EMASS(6,I)
FFQUI(1,I)=FFQUI(2,I)+FFQUI(6,I)
EVOL(1,I)=EVOL(2,I)+EVOL(6,I)
ETEMP(1,I)=ETEMP(2,I)+ETEMP(6,I)
FFNTH(1,I)=FFNTH(2,I)+FFNTH(6,I)
IF(IECHE(I).EQ.1) GO TO 410
CALL HPROD(PCYL(1),ETEMP(1,I),FFQUI(1,I)*DEL,PST,FNTHLP,
1 CSUBP,CSURT,RHO,DRH00T,DRH00P,EMWT(I),ERGAS(I),CVBG,FRGR)
GO TO 412
410 CALL HPROP(PCYL(1),ETEMP(1,I),FFQUI(1,I)*DEL,PST,RESFRK,ENTHLP,
1 CSUBP,CSURT,RHO,DRH00T,DRH00P,CHT,ERGAS(I),CVBG)
EMWT(I)=EMBAP
412 CONTINUE
ECP(1)=ERGAS(I)/41.443+CVBG
SUMHT(I)=SUMHT(I)-OHL05(I)/3.
400 CONTINUE
ANGLE=ANGLE1+ASTEP
CALL CALC(DVCYL,ENTINT)
CALL DELTA(DVCYL,ENTINT)
STGINT=STGINT+GINT/6.
STGEXT=STGEXT+GEXT/6.
STOEXT=STOEXT+OEXT/6.
DO 420 I=1,N01VID
420 TOHTK(I)=TOHTH(I)+OHTRC(I)/6.

C
C   FIFTH STEP
C

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PCYL(7)=PCYL(2)*ASTEP
PCYL(2)=PCYL(2)+(PCYL(4)+2.*PCYL(5)+2.*PCYL(6)+PCYL(7))/6.
GO TO 500 I=1,TE
FMASS(7,I)=FMASS(3,I)*ASTEP
FEQUI(7,I)=FEQUI(7,I)*ASTEP
EVOL(7,I)=EVOL(3,I)*ASTEP
ETEMP(7,I)=ETEMP(3,I)*ASTEP
FFNTH(7,I)=FFNTH(3,I)*ASTEP
EMASS(2,I)=FMASS(2+I)+(FMASS(4,I)+2.*EMASS(5,I)+2.*EMASS(6,I))
1 +EMASS(7,I))/6.
FEQUI(2,I)=FEQUI(2,I)+(FEQUI(4,I)+2.*FEQUI(5,I)+2.*FEQUI(6,I))
1 +FEQUI(7,I))/6.
EVOL(2,I)=EVOL(2,I)+(EVOL(4,I)+2.*EVOL(5,I)+2.*EVOL(6,I))
1 +EVOL(7,I))/6.
ETEMP(2,I)=ETEMP(2,I)+(ETEMP(4,I)+2.*ETEMP(5,I)+2.*ETEMP(6,I))
1 +ETEMP(7,I))/6.
FFNTH(2,I)=FFNTH(2,I)+(FFNTH(4,I)+2.*FFNTH(5,I)+2.*FFNTH(6,I))
1 +FFNTH(7,I))/6.
IF(IECHE(I).EQ.1) GO TO 510
CALL UPROP(PCYL(1),ETEMP(1,I),FEQUI(1,I),DEL,PSI,ENTHLP,
1 CSUHP,CSUPT,PHO,DRHO0T,DRHO0P,EMWT(I),ERGAS(I),CVBG,EBGR)
GO TO 512
510 CALL UPROP(PCYL(1),ETEMP(1,I),FEQUI(1,I),DEL,PSI,RESFRK,ENTHLP,
1 CSUHP,CSUPT,PHO,DRHO0T,DRHO0P,CHI,ERGAS(I),CVBG)
EMNT(I)=MRAP
512 CONTINUE
ECP(I)=ERGAS(I)/41.443+CVBG
DHL0S(I)=(SUMHT(I)-DHL0S(I)/6.)*ASTEP
500 CONTINUE
C I INJECTED FUEL HAS SAME TEMP AND ENTHALPY AS AIR.( THIS ASSUMPTION IS
C NECESSARY FOR THE ACCURATE CALCULATION. BECAUSE THE MASS JUST AFTER
C INJECTION IS SO SMALL THAT IT WILL CAUSE A LARGE AMOUNT OF ERROR.)
1 IF(ANGLE.GT.AFUEL0) GO TO 530
1 IF(I.EQ.1) GO TO 530
ETEMP(2,IE)=ETEMP(2,I)
FFNTH(2,IE)=FFNTH(2,I)
530 CONTINUE
RETURN
END

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SUBROUTINE CALCU(DVCYL,FNTINT)

C THIS SUBROUTINE IS TO SET THE DATA FOR SUBROUTINE RUNGE
COMMON/EPROP/ TECHE(100),EFUEL(100),EANGL(100),EMWT(100),
1 DHFUEL(100),DHLDS(100),DIEMAS(100),DOEMAS(100),
1 ERGAS(100),ECP(100),FENTH(8,100),EMASS(8+100),EEQUI(8,100),
1 EVOL(8,100),ETEMP(8,100),PCYL(8)
COMMON /TIMIG/ AINTO,AEXT0,AINTC,AFUELS,AFUELE
COMMON /STATE/ ANGLF1,ANGLE,JCOND,ASTEP,NSTEP,IE
COMMON /GEOMT/ STROKE,BORE,CONL,VCLEAR,VCUP,RCUP,CYLN
COMMON /HETRS/ NDIVID,TMETAL(10),QHTRC(10),ARF(10)
COMMON /HETRI/ PRASF,TBASE,VBASE,COHT1,COHT2,COHT,RHR(10)
COMMON /SUM2/ TTGINT,TTGEXT,TTDEXT,TTQHTR(10),TOHTR(10),PS
COMMON /STAT1/ RPM,JLAST,NJET,PHIO,EGR
COMMON /FUELP/ FUEL,FKCAL,ZM,ZN,PSI,SAFC,VACAL
COMMON /JETS/ RJET(50),HJET(50),AJET(50),BJET(50),THER(50),
1 VRJET(50),VZJET(50),WJET(50),VJET(50),AINJ(50),RHJET(50),
2 PITCH(50)
COMMON /PLUME/ PMASS(50),BMASS(50),RPLUM(50),HRMASS(50)
COMMON /JETDAT/ WSWIRG,ALPHA,BETA,RHgas
COMMON /INFL0/ NINEF,XTNEF(20),YINEF(20),ARETND,PINT,TINT,GINT,
1 EQUINT,ARFINT,XINV
COMMON/EXFL0/NFXEF,XEXEF(20),YEXEF(20),AREEXD,PEXT,TEXT,GFXT,
1 IGLEFT,TLEFT,DEXT,QFLOW,ELEFT,ARFEEXT,XEXV
COMMON/COMR/ RPLUM0,ENTUR,RLFSP,ASPRK,TSCALE

C CYLINDER VOLUME
CALL VOLCY(ANGLE,VCYL,DVCYL,STROKE,BORE,CONL,VCLEAR,VCUP)

C HEAT TRANSFER
CALL HEATR

C NO HEAT RELEASE FOR ELEMENT 1 (AIR)
DHFUEL(1)=0.
GO TO (100,200,300,400,600),JCOND

C WHEN THE INTAKE AND EXHAUST VALVE OPEN
C INTAKE PORT CALCULATION
100 CALL INPOR
DIEMAS(1)=GINT
IF(GINT) 700,710,710

C INTAKE FLOW IS FROM PORT TO CYLINDER
710 EEQN=EEQUI(1,1)
EEQN=(EMASS(1,1)*EFQUI(1,1)*(EQUINT+SAFC)+GINT*EQUINT*
1 (EEQUI(1,1)+SAFC))/(EMASS(1,1)*(EQUINT+SAFC)+GINT*(EFQUI(1,1)
2 +SAFC))
EEQUI(3,1)=EEQN-EEQN
QFLOW=GINT*FNTINT
GO TO 720

C INTAKE FLOW IS FROM CYLINDER TO PORT (BACK FLOW)
700 EFQUI(3,1)=0.
QFLOW=GINT*ENT(ETEMP(1,1),EEQUI(1,1),PCYL(1))

C EXHAUST PORT CALCULATION
720 CALL EXPOR
DOEMAS(1)=-GEXT
EMASS(3,1)=GINT+GEXT
QFLOW=QFLOW+GEXT*FENTH(1,1)

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GO TO 2000
C
C WRDN THE INTAKE PROCESS CALCULATION
C INTAKE PORT CALCULATION
200 CALL INPOR
    DIEMAS(1)=GINT
    IF(GINT) 800,B10,B10
C
C INTAKE FLOW IS FROM PORT TO CYLINDER
B10 EEQO=EEQUI(1,1)
    EEQN=(EMASS(1,1)*EEOUT(1,1)*(EQUINT+SAFC)+GINT*EQUINT*
    1 (EEQUI(1,1)+SAFC))/(FMASS(1,1)*(EQUINT+SAFC)+GINT*(EEQUI(1,1)
    2 +SAFC))
    EEQUI(3,1)=EEQN-EEQO
    QFLOW=GINT*FNTINT
    GO TO B20
C
C INTAKE FLOW IS FROM CYLINDER TO PORT (BACK FLOW)
'800 EEQUI(3,1)=0.
    QFLOW=GINT*EENTH(1,1)
820 GEXT=0.
    QEXT=0.
    EMASS(3,1)=GINT
    GO TO 2000
C
C COMPRESSION AND EXPANSION
300 EEQUI(3,1)=0.
    EMASS(3,1)=0.
    QFLOW=0.
    GINT=0.
    GEXT=0.
    QEXT=0.
    GO TO 2000
C
C COMBUSTION AND EXPANSION PROCESS
400 CONTINUE
    IF(IE.EQ.1) GO TO 300
    IF(NSTEP.GE.2) GO TO 410
    CALL DCAL
C
C THE EFFECT OF PUSHING THE FUEL ELEMENT INTO CYLINDER
    IF(ANGLE.GE.AFUELE) GO TO 410
    DDV=EVOL(1,IE)/ASTEP
410 CONTINUE
    QFLOW=-DOEMAS(1)*EENTH(1,1)
    GINT=0.
    GEXT=0.
    QEXT=0.
    IF(ANGLE.GE.AFUELE) GO TO 420
    DVCYL=DVCYL-DDV
420 CONTINUE
    GO TO 2000
C
C EXHAUST VALVE OPEN
600 EEQUI(3,1)=0.
    CALL EXPOR
    DOEMAS(1)=-GEXT
    EMASS(3,1)=GEXT
    QFLOW=GEXT*FENTH(1,1)
2000 RETURN
    END

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## SUBROUTINE FRIC

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C
C CALCULATION OF THE FRICTION LOSSES
C THIS PROGRAM WAS ORIGINALLY MADE BASED ON IN.-LB UNITS.
COMMON /STAT1/ RPM,JLAST,NJET,PHIO,FSR
COMMON /GEOMT/ STROKE,BORE,CONL,VCLEAR,VCUP,RCUP,CYLN
COMMON /INFL0/ NINEF,XINF(20),YINF(20),AREIND,PINT,TINT,GINT,
1 FQUINT,ARFINT,XINV
COMMON /AMRIE/ TAMR,PAMR
COMMON /FRIDT/ RSKIRT,FCOE,RINGN,FMEP(10)
FAC1=2.54
FAC2=1000./14.2
BOREX=BORE/FAC1
STROX=STROKE/FAC1
RSKIX=RSKIRT/FAC1
CR=(3.1416*BORE*BORE*STROKE/4.+VCUP+VCLEAR)/(VCUP+VCLEAR)
C
C MISCELLANEOUS AND PUMPS
FMEP(2)=FAC2*0.39*(RPM/1000.)**1.5
C
C CAM GEAR
DINTV=SQRT(AREIND*4./(3.1416*XINV))/FAC1
FMEP(3)=FAC2*(30.-(4.*RPM/1000.))*XINV*DINTV**1.75/(BOREX*BOREX
1*STROX)
C
C BEARING
FMEP(4)=FAC2*(FCOE*BOREX/STROX)**RPM/1000.
C
C BLOWBY
XX=ABS(PAMR-PINT)
IF(XX.LT.0.) XX=0.
FMEP(5)=FAC2*SQRT(XX)*(1.72*CR**0.4-(0.49+0.015*CR)*(RPM/1000.)**
1 1.185)
C
C VISCOUS PISTON
FMEP(6)=FAC2*(21.93*RSKIX/(BOREX*STROX)*STROX*RPM/5000.)
C
C STATIC RING TENSION
FMEP(7)=FAC2*2.11*STROX*RINGN/(BOREX*BOREX)
C
C RING GAS PRESSURE
FMEP(8)=FAC2*XX*(2.35*STROX/(BOREX*BOREX))*(0.088*CR+0.182*CR**_
1 (1.33-(0.121*STROX*RPM/5000.)))
C
C TOTAL FRICTION LOSS
FMEP(1)=0.
DO 100 I=2,8
FMEP(1)=FMEP(1)+FMEP(I)
100 CONTINUE
RETURN
END

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SUBROUTINE VGAS(RJET,HJET, RPM, ANGLE,VRGAS,VZGAS,WSWIR,VPTS,
1 FSWIR)

C
C
C  CALCULATION OF THE GAS VFLOCITY SURROUNDING THE JET
COMMON /GEOMT/ STROKE,BORE,CONL,VCLEAR,VCUP,RCUP,CYLN
COMMON /JETDAT/ WSWIRO,ALPHA,BETA
C RJET=JET RADIUS FROM CENTER(CM) (GIVEN)
C HJET=JET VERTTCAL LOCATION FROM CYLINDER HEAD (GIVEN)
C RPM= ENGINE SPEED (GIVEN)
C ANGLE= CRANK ANGLE (DEG),TDC=360 (GIVEN)
C VRGAS=VELOCITY COMP. OF RADIAL DIRECTION (GIVEN)
C VZGAS=VELOCITY COMP. OF VERTICAL DIRECTION (GIVEN)
C WSWIR=ANGULAR VELOCITY(RAD/SEC) (GIVEN)
C VPIS= PISTON SPEED(CM/SEC) (GIVEN)
C FSWIR=CONSERVATION RATIO OF SWIRL (GIVEN)
C STROKE ,BORE,CONL,VCLEAR,VCUP,RCUP,WSWIRO ARE GIVEN IN COMMON
C (SEE THE INPUT ROUTINE TO CHECK THE MEANINGS OF THESE VALUES)
C NO SUBROUTINES ARE REQUIRED
RCYL=BORE/2.
AK1=VCUP/(3.1416*RCYL*RCYL)
AK2=VCUP/(3.1416*RCUP*RCUP)
ANG=ANGLE*3.1416/180.
ANG0=3.1416

C
C  PISTON HIGHT FROM THE PISTON TO THE CYLINDER HEAD
HIGH=SQRT(1.-(STROKE/2.*SIN(ANG)/CONL)**2.)
HIGH=VCLEAR/(3.1416*BORE*BORE/4.)+STROKE/2.*((1.-COS(ANG))
1 +CONL*(1.-HIGH))

C
C  PISTON HIGHT AT BDC
HIGH0=SQRT(1.-(STROKE/2.*SIN(ANG0)/CONL)**2.)
HIGH0=VCLEAR/(3.1416*BORE*BORE/4.)+STROKE/2.*((1.-COS(ANG0))
1 +CONL*(1.-HIGH0))

C
C  PISTON SPEED
VPIS=SQRT(CONL*CONL-STROKE*STROKE/4.*SIN(ANG)*SIN(ANG))
VPIS=STROKE/2*SIN(ANG)+STROKE*STROKE/4.*SIN(ANG)*COS(ANG)/VPIS
VPIS=VPIS*3.1416/180.*RPM*6.
XX=HIGH/AK1
IF(RJET.LT.RCUP) GO TO 100
IF(HJET.LT.HIGH) GO TO 200
VZGAS=0.
VRGAS=0.
GO TO 400

C
C  GAS VELOCITY COMPONENTS ABOVE THE PISTON( FLAT PART)
200 VRGAS=RJET/(2.*AK1)*(RCYL*RCYL/(RJET*RJET)-1.)*VPTS/(XX*(1.+XX))
VZGAS=HJET/HIGH*VPIS
GO TO 400
100 IF(HJET.LT.HIGH) GO TO 300

C
C  GAS VELOCITY COMPONENTS INSIDE THE CUP
VRGAS=0.
VZGAS=(AK1-AK2+HJET)/(AK1+HIGH)*VPIS
GO TO 400

```

```

C GAS VELOCITY COMPONENTS ABOVE PISTON CJP
300 VRGAS=RJET/(2.*AK1)*(1.-AK2/AK1)/(XX*(XX+AK2/AK1))
  VRGAS=-VRGAS*VPIS
  VZGAS=(1.-RCYL*RCYL/(RCJP*RCUP*(XX+1.)))*HJET/HIGH*VPIS
C
C GAS VELOCITY (TANGENTIAL COMPONENT)
400 WSWIR=(HIGH+AK1)/(HIGH+AK1)*WSWIR0*(AK2*RCUP**4.
  1 +HIGH*RCYL**4.)/(AK2*RCUP**4.+HIGH*RCYL**4.)
  WSWIR=WSWIR*FSWIR
  RETURN
  END
  SUBROUTINE CONT(XX,YY,X1,Y0,X,Y,N)
  DIMENSION X(2),Y(2)
  IF(N>2) 10,20,30
10 X(1)=XX
  Y(1)=YY
  XX=XX+X1
  N=2
  RETURN
20 X(2)=XX
  Y(2)=YY
  N=3
  GO TO 60
30 IF((Y(2)-Y0)*(YY-Y0)) 40,50,50
40 X(1)=XX
  Y(1)=YY
  GO TO 60
50 X(2)=XX
  Y(2)=YY
60 XX=(Y0-Y(1))*(X(2)-X(1))/(Y(2)-Y(1))+X(1)
  RETURN
  END

```

SUBROUTINE JET(RJET,HJET,AJET,RJET,THER,VRJET,V7JET,WJET,TDM,  
1 AMJET,ASTEP,JSTEP,RPM,ANGLE,PITCH,FSWIR,WSWIR)

```

C THIS SUBROUTINE IS FOR GETTING JET TRAJECTORY AND AIR ENTRAINMENT
C COMMON /GEOMT/ STROKE,BORE,CONL,VCLEAR,VCUP,RCUP,CYLN
C COMMON /JETDAT/ WSWIRO,ALPHA,BETA,RHGAS
C RJET=RADIAL JET LOCATION FROM CENTER(CM) (GIVEN AND RETURNED)
C HJET=VERTICAL JET LOCATION FROM CYL. HEAD (GIVEN AND RETURNED)
C AJET=TANGEN. JET LOCATION FROM NOZZLFHEAD (GIVEN AND RETURNED)
C AJET=TANGEN. JET LOCATION FROM INJECTION NOZZ. (GIVEN AND RETURNED)
C RJET=JET RADIUS(CM) (GIVEN AND RETURNED)
C THER=CONTACTING ANGLE(PAD) (GIVEN AND RETURNED)
C VRJET=JET VELOCITY OF RADIAL DIRECTION(CM/SEC) (GIVEN AND RETURNED)
C V7JET=JET VEL. VERTICAL DIRECTION(CM/SEC) (GIVEN AND RETURNED)
C WJET=JET ANGULAR VELOCITY(RAD/SEC) (GIVEN AND RETURNED)
C TDM=ENTRAINED MASS(G/GIVEN TIME) (RETURNED)
C AMJET=JET MASS(G) (GIVEN AND RETURNED)
C ASTEP=CALCULATION INTERVAL OF MAIN PROGRAM(DEG) (GIVEN)
C JSTEP=HOW MANY TIMES DO YOU WANT TO CALCULATE IN ONE CALCULATION
C           INTERVAL OF MAIN PROGRAM (GIVEN)
C RPM=ENGINE SPEED(RPM) (GIVEN)
C ANGLE=CRANKANGLE (DEG). TDC =360 (GIVEN)
C PITCH=PITCH OF JET ELEMENT(GIVEN INPUT ROUTINE (GIVEN)
C FSWIR=CONSERVATION RATIO OF SWIRL (GIVEN)
C STROKE ,BORE,CONL,VCLEAR,VCUP,RCUP,WSWIRO,ALPHA,BETA,RHGAS ARE
C GIVEN IN COMMON
C (SEE THE INPUT ROUTINE TO CHECK THE MEANINGS OF THESE VALUES)
C SUBROUTINE REQUIRED:
C   VGAS
C   CONT
C     DIMENSION XX(2),YY(2)
C     RCUP=2.463R
C     PCYL=BORE/2.
C     TDM=0.
C     AASTEP=ASTEP/FLOAT(JSTEP)
C     C1=ASTEP/(6.*RPM)
C     C2= AASTEP/(6.*RPM)
C     C3=1./(6.*RPM)
C     VJET=SQRT(VRJET**2 +V7JET**2 +(RJET*WJET)**2 )
C     DO 3000 I=1,JSTEP
C       RHJET=AMJET/((3.1416*RJET)**2*(1.-THER/(2.*3.1416))+BJET**2
C     1 *SIN(THER)/2.)*VJET*PITCH/(6*RPM))
C       ANGLJ=ANGLF+FLOAT(I)*AASTEP
C       ANG=ANGLJ*3.1416/180.
C       HIGH=SQRT(1.-(STROKE/2.*SIN(ANG)/CONL)**2 )
C       HIGH=VCLEAR/(3.1416*BORE*BORE/4.)+STROKE/2.*((1.-COS(ANG))
C     1 +CONL*(1.-HIGH))

C     GAS VELOCITY SURROUNDING THE JET
C     CALL VGAS(RJET,HJET,RPM, ANGLJ,VRGAS,V7GAS,WSWIR,VPTS,FSWIR)
C     1111 FORMAT(7E12.4)

C     CALCULATION OF THE PARALLEL VELOCITY COMPONENT TO THE JET
C     VI=SQRT(VRJET**2 +(RJET*WJET )**2 +V7JET**2 )
C     VI=(VRJET*VRGAS+RJET**2.*WSWIR*WJET+V7JET*V7GAS)/VI

C     CALCULATION OF THE NORMAL VELOCITY COMPONENT TO THE JET
C     VN=VRGAS**2 +(RJET*WSWIR)**2 +V7GAS**2
C     XXX=VN-VI**2

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```

IF(XXX.GT.0.) GO TO 50
VN=0.
GO TO 60
50 VN=SQRT(VN-VI**2)
60 CONTINUE

C
C CHANGES OF MASS AND VELOCITY COMPONENTS OF THE JET
C CHANGE OF MASS(G)
DM= VJET*SQRT(RHJFT/RHGAS)*RHGAS*PITCH/(5.*RPM)
DM=DM*2.*3.1416*PJFT*(ALPHA*ARS(VJFT-VT)+BETA*ARS(VN))
DM=DM*(1.-THER/(2.*3.1416))
DM=DM*C2
TDM=TDM+DM
AMJET=AMJET+DM

C CHANGE OF VERTICAL VELOCITY
DVZ=DM/AMJET*(VZGAS-VZJFT)
C CHANGE OF RADIAL VELOCITY
DVR=AMJET*PJET*(WJET**2 - RHGAS/RHJET*WSWIR**2 )
DVR=DVR*C2
DVR=(DVR-(VRJFT-VRGAS)*DM)/AMJET
C CHANGE OF ANGULAR VELOCITY
DW=((WSWIR-WJET)*PJET*DM-2.*AMJET*VRJET*WJET*C2)/(AMJET*PJET)
C CHANGE OF TOTAL JET VELOCITY
DV=(PJET**2.*WJET*DW+PJET*WJET**2 *VRJET*C2+VRJET*DVR+VZJFT*DZV)
DV=DV/VJET

C
C NEW STATE CONDITIONS OF THE JET
VJET=VJET+DV
WJET=WJET+DW
VRJET=VRJET+DVR
VZJET=VZJET+DVZ
RJET=PJET+VRJFT*C2
ALJFT=VJET*PITCH/(5.*RPM)
VOLJE=DM/RHGAS+(AMJET-DM)/RHJFT
C JET RADIUS WITHOUT CONTACTING ANY WALL
BJFT0=SQRT(VOLJE/(3.1416*ALJFT))
HJET=HJET+VZJET*C2
AJFT=AJET+WJET*C2

C
C CALCULATION OF THE JET CONFIGURATION
X1=RJET+PJFT0
X2=HJET+BJFT0
X5=HIGH+VCUP/(3.1416*PCUP*RCUP)
IF(HJFT.GT.HIGH) GO TO 100
IF(RCYL.GT.X1) GO TO 200
IF(RCYL.GT.PJFT) GO TO 300

C
C JFT IS RESTRICTED BY THE CYLINDER WALL (VRJET=0.)
VRJET=0.
PJFT=1.414*PJFT0
THER=3.1416
RJET=PCYL
GO TO 2000

C
C JFT IS CONTACTING WITH THE CYLINDER WALL
300 NN=0
X3=PJFT
X4=PCYL
GO TO 1500
200 IF(X2.LT.HIGH) GO TO 400

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IF(X1.LT.RCUP) GO TO 400
IF(RJET.LT.RCUP) GO TO 500
C
C JET IS CONTACTTING WITH THE PISTON HEAD
NN=0
X3=HJET
X4=HIGH
GO TO 1500
C
C JET IS NOT CONTACTING
400 RJET=RJETO
THFR=0.
GO TO 2000
100 IF(RJET.LT.RCUP) GO TO 600
SL=ABS(HJET-HIGH)
SR=ABS(RJET-RCUP)
IF(SL.GT.SR) GO TO 700
C
C JFT IS RESTRICTED BY THE PISTON HEAD(V7JET=VPIS)
V7JFT=VPIS
RJET=1.414*RJFT0
THFR=3.1416
HJFT=HIGH
GO TO 2000
700 IF(HJET.GT.X5) GO TO 800
C
C JFT IS RESTRICTED BY THE PISTON CUP(VRJET=0.)
VRJET=0.
RJET=1.414*RJFT0
THFR=3.1416
RJFT=RCUP
GO TO 2000
C
C JFT IS RESTRICTED BY THE PISTON CUP EDGE(VRJET=0. AND V7JET=VPIS)
800 VRJFT=0.
V7JET=VPIS
RJET=RCUP
HJFT=X5
RJFT=1.414*RJFT0
GO TO 2000
600 IF(RCUP.LT.X1) GO TO 900
IF(X5.LT.X2) GO TO 1000
C
C JFT IS IN THE PISTON CUP WITHOUT ANY RESTRICTION
RJFT=RJETO
THFP=0
GO TO 2000
1000 IF(X5.LT.HJET) GO TO 1100
C JET IS CONTACTTING WITH THE PISTON BOTTOM
C
NN=0
X3=HJET
X4=X5
GO TO 1500
C
C JET IS RESTRICTED BY THE PISTON BOTTOM
1100 RJET=1.414*RJFT0
THFR=3.1416
HJFT=X5
V7JET=VPIS

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GO TO 2000
900 IF(RCUP.LT.RJET) GO TO 1200
C
C JET IS CONTACTING WITH THE PISTON CUP WALL
500 NM=0
X3=RJET
X4=RCUP
GO TO 1500
C
C JET IS RESTRICTED BY THE PISTON CUP WALL
1200 RJET=1.414*RJETO
THER=3.1416
RJET=RCUP
VRJFT=0.
GO TO 2000
C
C SOLVE THE CONTACTING ANGLE
1500 ITEL=1
1550 IF(RJET.GT.(X4-X3)) GO TO 1500
RJET=X4-X3
1600 ANG1=2.*ATAN(SQRT(RJFT*RJET-(X4-X3)*(X4-X3))/(X4-X3))
THER=ANG1
AREA1=3.1416*RJFT*RJET*(1.-ANG1/(2.*3.1416))+((X4-X3)*SIN(ANG1
1 /2.))*RJET
AREA2=3.1416*RJETO*RJFT0
ERR0=(AREA1-AREA2)/AREA2
IF(ABS(ERR0).LT.0.005) GO TO 2000
Y0=0.
XNEXT=0.1
CALL CONT(RJET,ERR0,XNEXT,Y0,XX,YY,NV)
1998 FORMAT(2E12.4)
ITEL=ITFL+1
IF(ITFL.GT.30) GO TO 1990
GO TO 1550
1990 WRITE(6,1999)
1999 FORMAT('STOP DUE TO THE OVER ITERATION')
2000 CONTINUE
3000 CONTINUE
RETURN
END

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## SUBROUTINE OPERA

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C
C THIS SUBROUTINE IS FOR OPERATION OF EACH PROCESS
COMMON/EPMOP/ TECHE(100),EFUEL(100),EANGL(100),FMWT(100),
1 DHFUEL(100),DHLDS(100),DIEMAS(100),DOEMAS(100),
1 ERGAS(100),ECP(100),FENTH(R,100),FMASS(R+100),FEQUI(R,100),
1 FVOL(8,100),FTEMP(R,100),PCYL(8)
COMMON /STATE/ ANGLF1,ANGLE,JCOND,ASTEP,NSTP,IF
COMMON /FUELP/ FUEL,FKCAL,ZM,ZN,PST,SAFC,VACAL
COMMON /TIMIG/ ATNT0,AEXT0,AINTC,AEXTC,AFUELS,AFULE
COMMON /OSOPE/ LPT,INP,LINECO,LINEST,ITEL,LTEL
COMMON/CONTL/ ASTIN,ASTCL,ASTCR,ASTEX,ASTOV,PRININ,PRINCL,PRINEX,
1 PRINOV
COMMON /STAT1/ RPM,JLAST,NJET,PHIO,EGR
COMMON /HETR1/ PRASF,TBASE,VBASE,COHT1,COHT2,COHT,RHR(10)
COMMON /GEOMT/ STROKE,BORE,CONL,VCLEAR,VCUP,RCUP,CYLN
COMMON /SUV2/ TTGINT,TTGEXT,TTQEXT,TTQHTR(10),TQHTR(10),PS
COMMON/INFI/ NINEF,XINFF(20),YINEF(20),AREEND,PINT,TINT,GINT,
1 EQUINT,AREINT,XINV
COMMON /AMPIE/ TAMR,PAMB
COMMON /NOXSP/ CONNO(100),PPMNO(100),WNO(100),SUMDM(100),PPMEXT
ANGLE=ANGLE+ASTEP
100 IF(ANGLE-AEXTC) 100,120,120
100 IF(JCOND-1) 110,9000,9000
110 IF(JLAST.EQ.1) GO TO 112
C
C SET THE LAST COMPUTING STEP
ASTEP=ATNT0-(ANGLE-ASTEP)
ANGLE=AINT0
JLAST=1
GO TO 9000
C
C INTAKE AND EXHAUST VALVE OPEN
112 JCOND=1
JLAST=0
ASTEP=ASTOV
LINEST=IFIX(PRINOV)
LINECO=0
WRITE(LPT,7000)
WRITE(LPT,7010)
WRITE(LPT,7020)
WRITE(LPT,7030)
GO TO 9000
120 IF(ANGLE-AINTC) 130,140,140
130 IF(JCOND-2) 150,9000,9000
150 IF(JLAST.EQ.1) GO TO 152
ASTEP=AEXTC-(ANGLE-ASTEP)
ANGLE=AEXTC
JLAST=1
GO TO 9000
C
C INTAKE VALVE OPENS
152 JCOND=2
JLAST=0
ASTEP=ASTIN
LINEST=IFIX(PRININ)
LINECO=0
WRITE(LPT,7200)
WRITE(LPT,7010)

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      WRITE(LPT,7220)
      WRITE(LPT,7230)
      GO TO 9000
140 IF(ANGLE-AFUELS) 160,170,170
160 IF(JCOND=3) 180,9000,9000
180 IF(JLAST,EQ,1) GO TO 182
      ASTEP=AINTC-(ANGLE-ASTEP)
      ANGLE=AINTC
      JLAST=1
      GO TO 9000

C   C  COMPRESSION PROCESS
182 JCOND=3
      JLAST=0
      ASTEP=ASTCL
      LINEST=IFIX(PRINCL)
      LINECO=0

C   C  CALCULATE THE OVERALL EQUIVALENCE RATIO
C
      PHI0=0.5
      DO 172 I=1,4
      FRES=(EMASS(2,1)-TTGINT)*PHI0/(SAFC+1.)
      FEGR=TTGINT*PHI0*EGR/(SAFC+1.)
      PHI0=(FUEL+FRES+FEGR)/(EMASS(2,1)-FRES+FEGR)*SAFC
172 CONTINUE

C   C  CALCULATE THE VOLUMETRIC EFFICIENCY
      DEL=ZN/ZM
      CALL UPROP(PAMR,TAMR,0.,DEL,PST,0.,DJM,DUM,DUM,DUM,DUM,
     1 DUM,RGAS,DUM)
      DISP=3.1415/4.*BORE*BORE*STROKE
      THMASS=PAMR*DISP/(RGAS*TAMB)
      EFFVOL=TTGINT/THMASS

C   C  CORRECT THE EQUIVALENCE RATIO OF CHARGED AIR
      EEQUI(2,1)=(FRES+FEGR)/(EMASS(2,1)-FRES+FEGR)*SAFC
      TBASE=ETEMP(2,1)
      PBASE=PCYL(2)
      VRASE=EVOL(2,1)

C   C  NOX CONCENTRATION FOR CHARGED AIR
      CONNO(1)=(EMASS(2,1)-TTGINT)/EMWT(1)*PPMEXT/1000000.
      1 + TTGINT*EGR/EMWT(1)*PPMEXT/1000000.
      PPMNO(1)=1000000.*CONNO(1)*EMWT(1)/EMASS(2,1)
      WNO(1)=30.*CONNO(1)
      WRITE(LPT,6100) PHI0
      WRITE(LPT,6120) EFFVOL
      WRITE(LPT,6140) EEQUI(2,1)
      WRITE(LPT,6160) PPMNO(1),WNO(1)
      WRITE(LPT,7400)
      WRITE(LPT,7010)
      WRITE(LPT,7420)
      WRITE(LPT,7430)
      GO TO 9000
170 IF(ANGLE-AFEXT0) 190,200,200
190 IF(JCOND=4) 210,192,192
192 IF(ANGLE-AFUELF=20.) 9000,9000,194
194 ASTEP=ASTCL
      GO TO 9000

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210 IF(JLAST.EQ.1) GO TO 212
ASTEP=AFUELS-(ANGLE-ASTEP)
ANGLE=AFUELS
JLAST=1
GO TO 9000
C
C FUEL STARTS TO BE INJECTED
C COMBUSTION AND EXPANSION
212 JLAST=0
JCOND=4
ASTEP=ASTCR
LINFST=IFIX(PRINCL)
LINECO=0
WRITE(LPT,7600)
WRITE(LPT,7010)
WRITE(LPT,7620)
WRITE(LPT,7630)
GO TO 9000
200 IF(ANGLE-AINT0-720.) 220,230,230
220 IF(JCOND-5) 240,9000,9000
240 IF(JLAST.EQ.1) GO TO 242
ASTEP=AEXTD-(ANGLE-ASTEP)
ANGLE=AEXTD
JLAST=1
GO TO 9000
C
C EXHAUST VALVE OPENS
242 JCOND=5
JLAST=0
ASTEP=ASTEXY
LINFST=IFIX(PRINFX)
LINECO=0
IF(IE.EQ.1) GO TO 244
C
C CALCULATE THE TOTAL MASS AND ENTHALPY
TENTH=0.
TMASS=0.
DO 7320 I=1,IF
TENTH=TENTH+EENTH(2,I)*EMASS(2,I)
TMASS=TMASS+EMASS(2,I)
7320 CONTINUE
C
C CALCULATE THE AVERAGE ENTHALPY
AVFTN=TENTH/TMASS
C
C CALCULATE THE AVERAGE TEMPERATURE
C FIRST FIND OUT THE ELEMENT WHICH ENTHALPY IS CLOSE TO THE
C AVERAGE ENTHALPY
DENTM=1000.
TI=1
DO 7330 I=1,IF
DENT=ABS(AVENT-EENTH(2,IT))
IF(DENTM.LT.DENT) GO TO 7330
DENTM=DENT
II=I
7330 CONTINUE
C
C DEFINE THE NEW PROPERTIES
ETFMP(2,1)=FTFMP(2,IT)+(AVENT-EENTH(2,IT))/FCP(IT)
FFQ1(2,1)=PH10

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FENTH(2,1)=AVENT
EMASS(2,1)=TMASS
CALL HPROD(PCYL(2),FTEMP(2,1),FFOUT(2,1),DEL,PSI,ENTHLP,CSURP,
1 CSUBT,RHO,DRH0DT,DRH0DP,EMWT(1),ERGAS(1),CVBG,EBGR)
ECP(1)=ERGAS(1)/41.443+CVBG
EVOL(2,1)=VCYLN
IE=1
C
C NOX AMOUNT WILL BE DEFINED.
C EXHAUST NOX ON MASS BASE
ANOXEX=TWN0*TTGINT/TMASS*RPM/120.
WRITE(LPT,7340)
WRITE(LPT,7342) PCYL(2),ETEMP(2,1),EEQUI(2,1),FENTH(2,1),
1 EMASS(2,1)
WRITE(LPT,7450) TPPM,ANOXEX
7340 FORMAT(//,10X,*-*EXPANSION PROCESS IS CALCULATED AS ONE ELEMENT**,
1**)
7342 FORMAT(15X,18HPRESSURE      = ,F10.2,'ATA',/)
1 15X,18HAV. TEMPERATURE = ,F10.1,'< DEG',/
2 15X,18HAV. EQUI. RATIO = ,F10.3,/
3 15X,18HAV. ENTHALPY   = ,F10.2,'CAL/G',
4 15X,18HTOTAL MASS    = ,F10.4,'G')
244 CONTINUE
WRITE(LPT,7800)
WRITE(LPT,7810)
WRITE(LPT,7820)
WRITE(LPT,7230)
GO TO 9000
230 JCOND=5
9000 ANGLE=ANGLE-ASTEP
RETURN
6100 FORMAT(//,10X,*OVERALL EQUIVALENCE RATIO = ,F12.3)
6120 FORMAT(10X,*VOLUMETRIC EFFICIENCY= ,F12.3)
6140 FORMAT(10X,*CORRECT CHARGED AIR PHT = ,F12.3)
6160 FORMAT(10X,*INDUCED AIR AND REG. GAS NOX*,/
1 15X,*PPM = ,F12.1,5X,*MASS = ,E12.3,*G*)
7000 FORMAT(1H1.5X,*INTAKE AND EXHAUST VALVE OPEN*,/)
7010 FORMAT(1H,*OUTPUT DATA*)
7020 FORMAT(2X,4HTHED,3X,4H P ,3X,4H T ,3X,4H V ,3X,4HWORK,
1 3X,7HCYL.MAS,3X,15H HEAT TRANSFER,6X,4HAEFT,3X,4H GWT,5X,
2 4HAEFF,3X,4H GWE)
7030 FORMAT(2X,4HDFG ,3X,4HATA ,3X,4H K ,2X,5HCM**3,3X,4H PS ,
1 3X,7H KG ,3X,15H CAL/A CAL ,5X,5HCM**2,3X,4H G/S,4X,
2 5HCM**2,3X,4H G/S,/)
7200 FORMAT(1H1.5X,*INTAKE VALVE OPEN*,/)
7220 FORMAT(2X,4HTHED,3X,4H P ,3X,4H T ,3X,4H V ,3X,4HWORK,
1 3X,7HCYL.MAS,3X,15H HEAT TRANSFER,5X,4HAEFT,3X,4H GWT)
7230 FORMAT(2X,4HDFG ,3X,4HATA ,3X,4H K ,2X,5HCM**3,3X,4H PS ,
1 3X,7H G ,3X,15H CAL/A CAL ,5X,5HCM**2,3X,4H G/S,/)
7400 FORMAT(1H1.5X,*COMPRESSION*,/)
7420 FORMAT(2X,4HTHED,3X,4H P ,3X,4H T ,3X,4H V ,3X,4HWORK,
1 3X,7HCYL.MAS,3X,15H HEAT TRANSFER,7X,4HFSWR,3X,4HS,RT)
7430 FORMAT(2X,4HDFG ,3X,4HATA ,3X,4H K ,2X,5HCM**3,3X,4H PS ,
1 3X,7H G ,3X,15H CAL/A CAL ,11X,3X,4HPPM)
7450 FORMAT(//,10X,*-*EXHAUST NOX***,*)
1 15X,15HNOX CONCN. = ,F10.1,*PPM*,/
2 15X,15HTOTAL MASS = ,E12.3,*G*)
7600 FORMAT(1H1.5X,*COMBUSTION AND EXPANSION*,/)
7620 FORMAT(2X,4HTHED,3X,*PRESS*,9X,*PSI,7X,*FSNTR,7X,15,RT1,7X,
1 *PPM*,9X,*WN0*,/,1X,

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1 3HNUJM+1X,2H\*\*.3X+4HT,4V,3X,4HRTEM,3X,4HR,RT,  
1 3X+4HMASS,3X+4HPMAS,3X+4HB4AS, 3X,4H V +3X+4HFQUT,3X+4H CP,  
2 3X+4HENTH,3X+4H PPM,3X,4H WND,1X,1RH JET LOCATIONS +1X,  
1 4HRJET,1X,5HC,ANG +2X+4H,T, )  
7630 FORMAT( 6X,4X,4H K +3X,4H K +3X+4X +3X,4H MG +3X,4H MG .  
1 3X,4H MG +2X,5HCM+\*3, 7X+2X,5HCAL/G,2X,5HCAL/G,2X,4H PPM.  
2 1X,7HG\*10\*\*6,1X,5H(CM)+ 1X,5H DEG +2X,4H CM +2X,  
3 4H DEG,2X,4H CAL)  
7800 FORMAT(1H1.5X,\*EXHAUST VALVE OPEN\*,/)  
7820 FORMAT(2X ,4HTHED,3X,4H P +3X,4H T +3X,4H V +3X,4HWORK.  
1 3X,74CYL,MAS,3X+15H HEAT TRANSFER,5X,4HAEFE,3X,4H GWE)  
END

```

SUBROUTINE EXPOR
C
C EXHAUST PORT CALCULATION
C THIS PROGRAM WAS ORIGINALLY MADE USING METER-KG UNIT
C
C
COMMON/EPROP/ IECHE(100),EFJEL(100),EANGL(100),EMWT(100),
1 DHFUEL(100),DHLDS(100),DEMAS(100),DOFMAS(100),
1 ERGAS(100),ECP(100),FFNTH(9,100),FMASS(R,100),FEQUI(R,100),
1 EVOL(R,100),ETEMP(R,100),PCYL(R)
COMMON/FXFL_O/NFXFF,XFXFF(20),YEXEF(20),AREEXT,PEXT,TEXT,GEXT,
1 IGLLEFT,TLEFT,DXEXT,DXLEFT,APFFXT,XEXV
COMMON /STATE/ ANGLE,JCOND,ASTEP,NSTEP,IE
COMMON /TIMIG/ ATINTO,AFXTO,ATNTC,AFXTC,AFUEL3,AFUEL4
COMMON /FUEL_P/ FUEL,FKCAL,ZM,ZN,PSI,SAFC,VACAL
COMMON /STAT1/ RPM,LAST,NJET,PHIO,EGR
IF(PEXT-PCYL(1)) 50,50,60
C EXHAUST FLOW IS FROM CYLINDER TO EX. PORT
C P VALUE DOESN'T CHANGE MUCH.
50 CEXT=-1.
RHIGH=ERGAS(1)*9.8
RHIGH=PCYL(1)*10000.
PREX=PEXT/PCYL(1)
EHIGH=FEQUIT(1,1)
IF(IGLLEFT) 51,51,52
C IGLLEFT=1 THERE IS RESIDUAL GAS
C IGLLEFT=0 THERE IS NOT RESIDUAL GAS
52 THIGH=ETEMP(1,1)
AKCYL=1.34
AKHIGH=AKCYL
GO TO 100
51 THIGH=TLEFT
RHIGH=ERGAS(1)*9.8
AKLEF=1.34
AKHIGH=AKLEF
GO TO 100
C EXHAUST FLOW IS FROM EX. PORT TO CYLINDER
60 RHIGH=ERGAS(1)*9.8
CEXT=1.
EHIGH=FEQUIT(1,1)
RHIGH=PEXT*10000.
PREX=PCYL(1)/PEXT
THIGH=ETEMP(1,1)
AKEXT=1.34
AKHIGH=AKEXT
C CALCULATE THE EFFECTIVE EXHAUST FLOW AREA
100 IF(ANGLE<360.) 150,150,160
150 ANAE=(ANGLE-(AFXTO-720.))/(AFXTC-(AFXTO-720.))
GO TO 200
160 ANAE=(ANGLE-AFXTO)/(AFXTC-AFXTO+720.)
200 CALL TWO DIM(YEXEF,XEXFF,YEXEF,ANAE,AREFAC)
APFFXT=AREEXT*AREFAC
APFFXT=AREEXT/10000.
PRCRIT=(2./(AKHIGH+1.))**(AKHIGH/(AKHIGH-1.))
C CHECK WHETHER FLOW IS CHOKED OR NOT
IF(PRCRIT-PREX) 300,300,310
C
C CHOKED

```

```
310 PPREX=PRCRIT
C
C  NEXT EQUATION IS BASED ON METER -KG UNTT
300 GEXT=          SORT(ABS(2.*AKHIGH*9.8/RHIGH/THIGH
1 / (AKHIGH-1.)*(PPREX**12./AKHIGH)-PPREX**((AKHIGH+1.)*
2 / AKHIGH)))
GEFT=O4IGH*ARFFXT/6.*PPM*GEFT
GEFT=CEXT*GFT
GFT=GEFT*1000.
AREFFXT=AREFFXT*10000.
IF (CEXT) 410,410,400
410 TMANI=THIGH*PPREX**1.(AKHIGH-1.)/AKHIGH
OEXT=GEFT*ENT(TMANI,FHIGH,SAFC)
GO TO 1000
400 OEXT=GEFT*ENT(TEXT,FHIGH,SAFC)
1000 RETURN
END
```

C SUBROUTINE VOLCY(ANGLE,VCYL,DVCYL,STROKE,BORE,CONL,VCLFAR,VCUP)  
PAI=3.141593  
ANGRAD=ANGLE\*PAI/180.  
HSTROK=STROKE/2.  
C DFLTA VOLUME CALCULATION  
DVCYL=PAI\*BORE\*\*2/4.\*((HSTROK\*SIN(ANGRAD)+HSTROK\*\*2\*SIN(ANGRAD))  
1 \*COS(ANGRAD))/SQRT(CONL\*\*2-HSTROK\*\*2\*SIN(ANGRAD)\*\*2)\*PAI/180.  
C VOLUME CALCULATION  
DISTTB=CONL\*(1.-SQRT(1.-(HSTROK/CONL)\*\*2\*SIN(ANGRAD)\*\*2))  
1 +HSTROK\*(1.-COS(ANGRAD))  
VCYL=VCLEAR+VCUP+PAI\*BORE\*\*BORE/4.\*DISTTB  
RETURN  
END  
C

```
SUBROUTINE TWOPOINT(N,X,Y,XIN,YOUT)
DIMENSION X(1),Y(1)
XDUMMY=XIN
IF(XDUMMY-X(1)) .NE. 810,810,810
510 XDUMMY=X(1)
810 CONTINUE
IF(XDUMMY-X(N)) .NE. 820,820,820
520 XDUMMY=X(N)
820 CONTINUE
J=0
3 J=J+1
5 IF(XDUMMY-X(J)) .LT. 2,3
? YOUT=Y(J)
GO TO 4
1 YOUT=Y(J)-(X(J)-XDUMMY)/(X(J)-X(J-1))*(Y(J)-Y(J-1))
4 RETURN
END
```

```

SUBROUTINE HEATR

C   HEAT TRANSFER CALCULATION
      COMMON /FPROP/  TCHF(100),KFJFL(100),FANGI(100),FMWT(100),
     1 DHEUFL(100),DHLDS(100),DIEMAS(100),DUEMAS(100),
     1 ERGAS(100),ECP(100),FFNTH(B,100),FMASS(B,100),FEOUT(B,100),
     1 FVOL(B,100),ETEMP(B,100),PCYL(B)
      COMMON /STATE/  ANGI,F1,ANGLE,JCOND,ASTEP,NSTEP,IF
      COMMON /STAT1/  RPM,JLAST,NJET,PHIN,FGR
      COMMON /GEOMT/  STROKE,BORE,CONL,VCLFAR,VCUP,RCUP,CYLN
      COMMON /HETPS/  NOIVTD,TMETAL(10),DHTRC(10),ARF(10)
      COMMON /JETS/  PJET(50),HJET(50),AJET(50),BJET(50),THEP(50),
     1 VPJET(50),VZJET(50),WJET(50),WJET(50),ATNJ(50),RHJET(50),
     2 PITCH(50)
      COMMON /SUPGAS/  FSWIR,WSNIR,SDFCAV
      COMMON /HETR1/  PRASF,TRASE,VRASF,COHT1,COHT2,COHT,RHR(10)
      DIMENSION HTCO2(10),HT1(10)
      ANGRAD=ANGLE*B.1416/180.
      CALL VOLCY(ANGLE,CYLV,DIUM,STROKE,BORE,CONL,VCLFAR,VCUP)

C   GET THE H.T. AREA OF CYLINDER WALL
C
      ARF(2)=(CYLV-VCUP)*4./BORE
      DO 200 I=1,NOIVTD
      DHTRC(I)=0.
200  CONTINUE
      DO 202 I=1,TF
      DHLDS(I)=0.
202  CONTINUE
      HTCON1=COHT+B014.*B0RF**(-0.2)*PCYL(1)**0.8/(2.16*10.**R*PPM)
      GO TO (210,210,220,220,210),JCOND

C   THERMOPIC TE+PERAPURF
220  PTSEN=PRASF*(VRASF/CYLV)**1.32
      HTCON2=COHT1*(STROKE*PPM/30.)*100.*COHT2*CYLV*TRASE/(PRASF
      1.*VRASF)*(PCYL(1)-PTSEN)
      GO TO 230

C   FOR PROCESS --INTAKE,EXHAUST AND VALVE OVERLAP
210  PISEN=PCYL(1)
      HTCON2=COHT1*(STROKE*PPM/30.)
230  CONTINUE
      DO 300 I=2,NOIVTD
C
      C   0.4 IS AN ADJUSTING FACTOR
      HTCO2(I)=(HTCON2+WSNIR*R*HTH(I)*0.4)**0.8
300  CONTINUE
      IF(IE,FO,1) GO TO 1000
      TAPEA=0.
      DO 2400 J=1,TF
      I=IF+1-J
      IF(I,FO,1) GO TO 2120

C   THE AREA OF JET CONTACTING WITH WALL
      AREATH=PJET(I)*SIN(THER(I)/2.)*2.*VJET(I)*PITCH(I)/(6.*RPM)
      TAPEA=TAPEA+AREATH

C   CHECK WHETHER THE PISTON CUP IS FULL WITH JET ELEMENTS OR NOT
C

```

```

IF(TAREA.GT.AR(4)) GO TO 2000
RTAREA=AR(2)+AR(3)+AR(5)+AR(6)+AR(7)

C PISTON CUP IS NOT FILLED WITH JET ELEMENTS
DHL0S(I)=HTCON1*ETEMP(1,I)**(-0.53)*HTCO2(4)*ARFATH*
1 (ETEMP(1,I)-TMETAL(4))
DHTPC(4)=DHTPC(4)+DHL0S(I)
DHTPC(1)=DHTPC(1)+DHL0S(I)
GO TO 2900

C PISTON CUP IS FILLED WITH JET ELEMENTS
2000 IFILL=1
2100 AA=ARFATH*HTCON1*ETEMP(1,I)**(-0.53)
RTAREA=AR(2)+AR(3)+AR(5)+AR(6)+AR(7)
2116 DO 2110 JJ=2,NDIVID
IF(IFILL.EQ.0) GO TO 2112
IF(JJ.EQ.4) GO TO 2110
2112 HTI(JJ)=AA*AR(JJ)/RTAREA*HTCO2(JJ)*(ETEMP(1,I)-TMETAL(JJ))
DHTPC(JJ)=DHTPC(JJ)+HTI(JJ)
DHL0S(I)=DHL0S(I)+HTI(JJ)
DHTPC(1)=DHTPC(1)+HTI(JJ)
2110 CONTINUE
GO TO 2900

C FOR ELEMENT 1
2120 XX=AR(4)
IF(IFILL.EQ.0) GO TO 2114
AA=(AR(2)+AR(3)+AR(4)+AR(5)+AR(6)+AR(7)-TARFA)*HTCON1*
1 ETEMP(1,I)**(-0.53)
RTAREA=AR(2)+AR(3)+AR(5)+AR(6)+AR(7)
GO TO 2116
2114 RTAREA=AR(2)+AR(3)+AR(5)+AR(6)+AR(7)+AR(4)-TAREA
XX=AR(4)
AR(4)=AR(4)-TAREA
AA=TARFA*HTCON1*ETEMP(1,I)**(-0.53)
GO TO 2116
2900 CONTINUE
AR(4)=XX
GO TO 9000
1000 HTCO11=HTCON1*ETEMP(1,I)**(-0.53)
DO 1900 I=2,NDIVID
DHTPC(I)=HTCO11*HTCO2(I)*(ETEMP(1,I)-TMETAL(I))*AR(I)
DHTPC(1)=DHTPC(1)+DHTPC(I)
1900 CONTINUE
DHL0S(I)=DHTPC(I)
9000 RRETURN
END

```

```

SUBROUTINE DELTA(DVCYL,FNTINT)
COMMON/FPROP/ 1ECHF(100),EFJFI(100),EANGI(100),FMWT(100),
1 DHFUFL(100),DHLOS(100),DIEMAS(100),DOEMAS(100),
1 FRRAS(100),ECP(100),FFNTH(8,100),FMASS(8,100),FEDOUT(8,100),
1 FVOL(8,100),FTEMP(8,100),PCYL(8)
COMMON/STATE/ ANGLE,I,ANGLE,JCOND,NSTEP,MSTEP,TE
COMMON/FXFLD/NFXFF,XEXFF(20),YFFXFF(20),AREEXT,PEXT,TEXT,GEXT,
1 IGLLEFT,TLEFT,DXEXT,DFLOW,FLEFT,ARFFEXT,XEXV
DIMENSION DO(100),HFNTH(100)
AJ=42.68
DO 50 I=1,IE
DO(I)=DHFUFL(I)-DHLOS(I)
HFNTH(I)=FFNTH(1,I)
50 CONTINUE
F'ITCYL=HFNTH(1)
AA=DO(1)+QFLOW -(DITEMAS(1))
1 DOEMAS(1)*HFNTH(1)
AA=AA+EVOL(1,1)/(EMASS(1+1)*ECP(1)*FTEMP(1,1))+ (DITEMAS(1)
1 -DOEMAS(1))/FMASS(1+1)*EVOL(1,1)
BP=EVOL(1,1)*FVOL(1,1)/(EMASS(1+1)*ECP(1)*FTEMP(1,1)*A)
1-FVOL(1,1)/PCYL(1)
IF(IE.LT.2) GO TO 200
DO 100 I=2,IE
AA=AA+EVOL(1,I)/(EMASS(1+I)*ECP(1)*FTEMP(1,I))* (DO(I)
1 +DIEMAS(I)*HFNTH(I)) -DOEMAS(I)*HFNTH(I) -(DITEMAS(I)
2 -DOEMAS(I)*HFNTH(I)) +(DIEMAS(I)-DOEMAS(I))/EMASS(1,I)
3 *EVOL(1,I)
PP=BP+EVOL(1,I)*FVOL(1,I) /(EMASS(1+I)*ECP(1)
1 *FTEMP(1,I)*A.I)-EVOL(1,I)/PCYL(1)
100 CONTINUE
200 PCYL(3)=(DVCYL-AA)/BP
FVOL(3,1)=FVOL(1,1)/(FMASS(1,1)*ECP(1)*FTEMP(1,1))
1 +(DO(1)+QFLOW -(DITEMAS(1))
2 -DOEMAS(1)*HFNTH(1)) +(DIEMAS(1)-DOEMAS(1))/FMASS(1,1)
3 *EVOL(1,1)+(FVOL(1,1)*FVOL(1,1)/(EMASS(1+1)*ECP(1)*FTEMP(1,1)
4 *A.I))-FVOL(1,1)/PCYL(1)*PCYL(3)
ETEMP(3,1)=FTEMP(1,1)*(PCYL(3)/PCYL(1)+EVOL(3,1)/FVOL(1,1)
1 -(DITEMAS(1)-DOEMAS(1))/EMASS(1,1))
FMASS(3,1)=DITEMAS(1)-DOEMAS(1)
FFNTH(3,1)=ECP(1)*FTEMP(3,1)
IF(IE.LT.2) GO TO 400
DO 300 I=2,IE
EVOL(3,I)=EVOL(1,I)/(EMASS(1,I)*ECP(1)*FTEMP(1,I))
1 +(DO(I)+DITEMAS(I)*HFNTH(I)) -DOEMAS(I)*HFNTH(I) -(DITEMAS(I)-
2 -DOEMAS(I)*HFNTH(I)) +(DIEMAS(I)-DOEMAS(I))/EMASS(1,I)
3 *EVOL(1,I)+(FVOL(1,I)*FVOL(1,I)/(EMASS(1+I)*ECP(1)*FTEMP(1,I)*A.I)
4 -EVOL(1,I)/PCYL(1))*PCYL(3)
ETEMP(3,I)=FTEMP(1,I)*(PCYL(3)/PCYL(1)+EVOL(3,I)/FVOL(1,I)-
1 -(DITEMAS(I)-DOEMAS(I))/EMASS(1,I))
FMASS(3,I)=DITEMAS(I)-DOEMAS(I)
FFNTH(3,I)=ECP(1)*FTEMP(3,I)
300 CONTINUE
400 RETURN
END

```

```

FUNCTION ENT(T,E,XXX)
C TO CALCULATE THE ENTHALPY OF GAS AT LOW PRESSURE .(T<1800 K)
C THIS SUBROUTINE IS USED FOR CALCULATING THE ENTHALPY OF INITIAL GAS
C IN THE CYLINDER, INTAKE AIR AND EXHAUST GAS.
C IT IS RECOMMENDED THAT M.MARTIN'S PROGRAMS BE USED FOR HIGH PRESSURE
C OR HIGH TEMPERATURE GASES.
C
      SAFC=14.4
      IF(E.LT.0.01) GO TO 100
      AF=SAFC/E
      GO TO 200
100 AF=0.
200 CONTINUE
      IF(T>200.) 10,10,20
10 ENT =-0.405671 +0.243753*T -0.164508E-4*T**2 +0.157984F-7
     1 *T**3+0.253172E-10*T**4 -0.179767E-13*T**5
      TF(AF) 99.99.40
40 FNT =ENT +(14.9607 -0.126357*T +0.769710E-3*T**2-0.517585F-6
     1 *T**3 +0.595961F-10*T**4 +0.833377E-13*T**5 )/(AF+1.)
      RETURN
20 FNT =11.3175 +0.190755*T +0.637625E-4*T**2 -0.182173F-7*T**3
     1 +0.223445E-11*T**4
      IF(AF) 99.99.30
30 FNT =ENT +(-42.2372 +0.199892*T +0.871219F-4*T**2 +0.600828F-7
     1 *T**3 -0.299545F-10*T**4 +0.391857F-14*T**5 )/(AF+1.)
99 RETURN
END

```

\*\*\*\*\* VERSION 1.0 \*\*\* 5/29/74 \*\*\*\*\*

C C SUBROUTINE HPROD

**PURPOSE:**

TO CALCULATE THE SPECIFIC ENTHALPY OF THE PRODUCTS OF HYDRO CARBON-AIR COMBUSTION AS A FUNCTION OF TEMPERATURE AND PRESSURE, USING AN APPROXIMATE CORRECTION FOR DISSOCIATION. THE PARTIAL DERIVATIVES OF H WITH RESPECT TO THESE VARIABLES ARE ALSO CALCULATED, ALONG WITH THE GAS DENSITY AND ITS PARTIAL DERIVATIVES

**USAGE:**

CALL HPROD(P,T,PHI,DEL,PSI,FNTHLP,CSURP,CSURT,RHO,DRHODT,  
DRHOOP)

**DESCRIPTION OF PARAMETERS:**

**GIVEN:**

**P** - ABSOLUTE PRESSURE OF PRODUCTS (ATM)  
**T** - TEMPERATURE OF PRODUCTS (DEG K)  
**PHI** - EQUIVALENCE RATIO (FUEL/AIR RATIO DIVIDED BY THE  
 CHEMICALLY CORRECT FUEL/AIR RATIO)  
**DEL** - MOLAR C:H RATIO OF THE PRODUCTS  
**PSI** - MOLAR N:O RATIO OF THE PRODUCTS

## **RETURNS:**

ENTHLP - SPECIFIC ENTHALPY OF THE PRODUCTS (KCAL/G)  
 CSUBP - PARTIAL DERIVATIVE OF ENTHLP WITH RESPECT TO T  
           AT CONSTANT P (CAL/G-DEG K)  
 CSURT - PARTIAL DERIVATIVE OF ENTHLP WITH RESPECT TO P  
           AT CONSTANT T (CC/G)  
 RHO - DENSITY OF THE PRODUCTS (G/CC)  
 DRHODT - PARTIAL DERIVATIVE OF RHO WITH RESPECT TO T AT  
           CONSTANT P (G/CC-DEG K)  
 DRHODP - PARTIAL DERIVATIVE OF RHO WITH RESPECT TO P AT  
           CONSTANT T (G/CC-ATM)

**REMARKS:**

- 1) ENTHALPY DATUM STATE IS AT T = 0 ABSOLUTE WITH  
O<sub>2</sub>, N<sub>2</sub>, H<sub>2</sub> GASFOUS AND C SOLID GRAPHITE
  - 2) IN CASE OF PROBLEMS CONTACT MIKE MARTIN AT 253-2411  
(ROOM 3-339 D)

## SUBROUTINES AND FUNCTION SUBPROGRAMS REQUIRED:

C DERTVS, CLDPRD

## METHOD:

C SEE MARTIN & HEYWOOD 'APPROXIMATE RELATIONS FOR THE THERMO-  
C DYNAMIC PROPERTIES OF HYDROCARBON-AIR COMBUSTION PRODUCTS'.

```
SUBROUTINE HPROD(P,T,PHT,DEL,PSI,FNTHLP,CSUAP,CSURT,RHO,DRHO0T,
1 DRHO0P,AMWT,RAVG,CVAVG,ENERGY)
LOGICAL RICH,LFAN,NOTHOT,NOTWRM,NOTC_D
```

## INITIALIZE PARAMETERS USED IN THE CA\_CULATION

DATA AHFC02,AHFH20,AHFC0/-93.965,-57.103,-27.200/  
DATA ROVR2/.99345E-3/  
DATA TCOLn,THOT /1000.,1100./

```

C
RICH = PHI .GE. 1.0
LEAN = .NOT. RICH
NOTHOT = T .LT. THOT
NOTCLD = T .GT. TCOLD
NOTWRM = .NOT. (NOTCLD .AND. NOTHOT)
EPS=(4.*DEL)/(1. + 4.*DEL)

C
C USE SIMPLE ROUTINE FOR LOW TEMPERATURE MIXES
C
IF (NOTCLD) GO TO 5
CALL CLDPRD(P,T,PHI,DFL,PSI,ENTHLP,CSURP,CSURT,RHO,DRHOOT,
1 DRHOOP,IER,AMWT)
GO TO 30

C
C CALCULATE EQUILIBRIUM CONSTANTS FOR DISSOCIATION.
C (NOTE THAT UNITS ARE INVERSE PRESSURE TO THE 1/2 POWER)
C
5 AK1 = .39E-4 * EXP(-.3*FPS + 34000./T)
AK2 = .14E-3 * EXP(1.3*FPS + 29000./T)

C
C CALCULATE A, X, Y, AND U AS IN NOTES
C
A = ((2.- FPS + PST)/(4.*P*AK1*AK2))**(.33333333)

C
T1 = 2.- EPS + PSI
T2 = 1. + 2.*T1
T3 = EPS*A
X = A*(3.*T1 + T2*T3)/(3.*(1.+ 2.*T3)*T1 + 2.*T2*T3*T3)

C
Z = (1.- PHI)/X
IF (RICH) Y = X/(1.- .64*Z + .30*Z**2)
IF (LEAN) Y = X*(1.+ Z + .36*Z**2)/(1. + .36*Z) - (1. - PHI)
U = (2. - FPS + PST)*(1.- 2.*FPS*X)/(4.*AK1*AK2*P*X)

C
C CALCULATE THE ENTHALPY OF FORMATION FOR THIS APPROXIMATE
C COMPOSITION
C
ENTFOR = 1000.*R0V2*(((117. + 30.*FPS)*Y + 135.*EPS*U))
XH2O = 2.*((1.- FPS)*PHI)
T1 = 7.*PST + 5.*Y + 3.*J
T2 = PSI - 3.*Y - U

C
IF (LEAN) GO TO 10

C
RCVT = 2. + 2.*((7. - 4.*EPS)*PHI + T1)
RCVV = 4. + (2.- 3.*FPS)*PHI + T2
XC02 = 2.- (2.- FPS)*PHI
XC0 = 2.*((PHI - 1.))
ENTFOR = ENTFOR - 1000.*R0V2*13.*((PHI - 1.)/FP.
GO TO 20

C
10 RCVT = 7. + (9. - 8.*FPS)*PHI + T1
RCVV = 1. + (5.- 3.*FPS)*PHI + T2
XC0 = 0.
XC02 = EPS*PHI

C
20 ENTFOR = ENTFOR + (XC02*AHFC02 + XH2)*AHFH20 + XC0*AHFC0
C
C ADD IN TRANSLATIONAL, VIBRATIONAL, AND ROTATIONAL TERMS TO GFT

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```

C      TOTAL ENTHALPY
C
C      TV = (3000.- 2000.*EPS + 300.*PSI)/(1.- .5*EPS + .09*PSI)
C      TV = TV/( EXP(TV/T) - 1.)
C      AMCP = (8.*EPS + 4.)*PHI + 32. + 28.*PSI
C
C      ENTHLP = (ROVR2*(RCVT*T + RCVV*TV*2.) + ENTFOR)/AMCP
C
C      CALCULATE AVERAGE MOLECULAR WEIGHT, AND GET DENSITY BY
C      USING THE PERFFCT GAS LAW
C
C      IF (LFAN)  AMWT = AMCP/(1. + (1.- EPS)*PHI + PSI + Y + U)
C      IF (RICH)  AMWT = AMCP/((2.- EPS)*PHI + PSI + Y + U)
C      RHO = .012187*AMWT*T
C
C      GET PARTIAL DERIVATIVFS BY WAY OF A SURROUTINF CALL
C
C      CALL DERIVS(P,T,PHI,EPS,PSI,A,X,Y,U,AMWT,CSURP,CSURT,DRHODT,
C      1 DRHOOP)
C
C      IF CALCULATING FOR AN INTERMEDIATE TEMPERATURE, USE A WEIGHTED
C      AVERAGE OF THF RESULTS FROM THIS ROUTINE AND THOSE FROM THE
C      SIMPLE ROUTINE
C
C      IF (NOTWRM) GO TO 30
C
C      CALL CLOPRD(P,T,PHI,DFL,PSI,TH,TCP,TCT,TRHO,TDRT,TDRP,IER,AMWT)
C      W1 = (T - TCOLD)/(THOT - TCOLD)
C      W2 = 1.0 - W1
C
C      ENTHLP = W1*ENTHLP + W2*TH
C      CSURP = W1*CSURP + W2*TCP
C      CSURT = W1*CSURT + W2*TCT
C      RHO = W1*RHO + W2*TRHO
C      DRHODT = W1*DRHODT + W2*TDRT
C      DRHOOP = W1*DRHOOP + W2*TDRP
C
C      30 RAVG=R2.057/AMWT
C      CVAVG=CSURP-1.98/AMWT
C      ENERGY=1000.*ENTHLP-1.98*T/AMWT
C
C      RETURN
C      END

```

```

***** VERSION 1.1 ***
C
C      SUBROUTINE CLDPRD
C
C      PURPOSE:
C          TO CALCULATE THE SPECIFIC ENTHALPY OF THE PRODUCTS OF HC-AIR
C          COMBUSTION AT TEMPERATURES AND PRESSURES WHERE DISSOCIATION
C          OF THE PRODUCT GASES MAY BE IGNORED. THE DENSITY OF THE
C          PRODUCT GAS IS ALSO CALCULATED, AS ARE THE PARTIAL
C          DERIVATIVES OF BOTH OF THESE QUANTITIES WITH RESPECT TO
C          PRESSURE AND TEMPERATURE.
C
C      USAGE:
C          CALL CLDPRD(P,T,PHI,DEL,PSI,ENTHLP,CSUBP,CSUBT,RHO,DRHODT,
C                      DRHODP,IER)
C
C      DESCRIPTION OF PARAMETERS:
C      GIVEN:
C          P      - ABSOLUTE PRESSURE OF PRODUCTS (ATM)
C          T      - TEMPERATURE OF PRODUCTS (DEG K)
C          PHI    - EQUIVALENCE RATIO (FUEL/AIR RATIO DIVIDED BY THE
C                   CHEMICALLY CORRECT FUEL/AIR RATIO)
C          DEL    - MOLE C:H RATIO OF THE PRODUCTS
C          PSI    - MOLE N:O RATIO OF THE PRODUCTS
C
C      RETURNS:
C          ENTHLP - SPECIFIC ENTHALPY OF THE GAS (KCAL/G)
C          CSUBP - PARTIAL DERIVATIVE OF ENTHLP WITH RESPECT TO T
C                   AT CONSTANT P (CAL/G-DEG K)
C          CSUBT - PARTIAL DERIVATIVE OF ENTHLP WITH RESPECT TO P
C                   AT CONSTANT T (CC/G)
C          RHO   - DENSITY OF THE MIXTURE (G/CC)
C          DRHODT - PARTIAL DERIVATIVE OF RHO WITH RESPECT TO T AT
C                   CONSTANT P (G/CC-DEG K)
C          DRHODP - PARTIAL DERIVATIVE OF RHO WITH RESPECT TO P AT
C                   CONSTANT T (G/CC-ATM)
C          IER   - FLAG. SET TO 1 FOR T<100 DEG K
C                   2 FOR T> 6000 DEG K
C                   0 OTHERWISE
C
C      REMARKS:
C          1) ENTHALPY DATUM STATE IS AT T = 0 ABSOLUTE WITH
C             O2,N2,H2 GASEOUS AND C SOLID GRAPHITE
C          2) IN CASE OF PROBLEMS CONTACT MIKE MARTIN AT 253-2411
C             (ROOM 3-339 D)
C
C      SUBROUTINES AND FUNCTION SUBPROGRAMS NEEDED:  NONE
C
C      METHOD:
C          DESCRIBED IN APPENDIX IV OF WRITEUP
C
***** SURROUNING CLDPRD(P,T,PHI,DEL,PSI,ENTHLP,CSUBP,CSUBT,RHO,
C                      DRHODT,DRHODP,IER,MRAR) *****
C
C      LOGICAL RLICH,LFAN
C      DIMENSION A(5,6,2),X(6)
C      DIMENSION A1(36),A2(36)

```

```

EQUIVALENCE (A1(1),A(1,1,1)),(A2(1),A(1,1,2))
REAL*4 MRAR,K

C      INITIALIZE PARAMETERS. AND CHECK TO SEE IN WHAT TEMPERATURE
C      RANGE WE ARE SO THAT THE CORRECT FITTED COFFICIENTS WILL BE
C      USED. FLAG TEMPERATURES TOO BIG OR TOO SMALL
C
C      DATA A1/11.94033,2.088581,-0.47029,.037363,-.589447,-97.1418,
1  6.139094,4.60783,-.9356009,.06669498,.0335801,-56.62588,
2  7.099556,1.275957,-.2877457,.022355,-.1598696,-27.73464,
3  5.555680,1.787191,-.2881342,.01951547,.1611828,.76498,
4  7.865847,.6883719,-.031944,-.00268708,-.2013873,-.893455,
5  6.807771,1.453404,-.328985,.02561035,-.1189462,-.331935/
C      DATA A2/4.737305,16.65283,-11.23249,2.928001,.00576702,-93.75793,
7  7.809672,-.2023519,3.418708,-1.179013,.00143629,-57.08004,
8  6.97393,-.8238319,2.942042,-1.176239,.0004132409,-27.19597,
9  6.991878,.1617044,-.2182071,.2968197,-.01625234,-.118189,
&  6.295715,2.388387,-.0314788,-.3267433,.00435925,.103637,
- 7.092199,-1.295825,3.20688,-1.202212,-.0003457938,-.013967/
C
C      RICH = PHI .GT. 1.0
C      LEAN = .NOT. RICH
C      EPS = 4.*DFL/(1. + 4.*DFL)
C      IFL = 0
C      IF (T .LT. 100.) IFL = 1
C      IF (T .GT. 6000.) IFL = 2
C      IR = 1
C      IF (T .LT. 500.) IR = 2
C
C      GET THE COMPOSITION IN MOLES/MOLE OXYGEN
C
C      IF (RICH) GO TO 10
C      Y(1) = EPS*PHI
C      X(2) = 2.* (1.- EPS)*PHI
C      X(3) = 0.
C      X(4) = 0.
C      X(5) = 1.- PHI
C      GO TO 20
10  T = 1000./T
K = EXP(2.743 + 7*(-1.761 + 2*(-1.611 + 7*.2803)))
ALPHA = 1. - K
BETA = (2.* (1.- EPS)*PHI) + <*(2.* (PHI - 1.) + EPS*PHI))
GAMMA = 2.*K*EPS*PHI*(PHI - 1.)
C = (- BETA + SQRT(BETA*BETA + 4.*ALPHA*GAMMA))/(2.*ALPHA)
X(1) = EPS*PHI - C
X(2) = 2.* (1.- EPS)*PHI + C
X(3) = C
X(4) = 2.* (PHI - 1.) - C
X(5) = 0.
20  X(6) = PSI
C
C      CONVERT COMPOSITION TO MOLE FRACTIONS AND CALCULATE AVERAGE
C      MOLECULAR WEIGHT
C
C      IF (LEAN) TMOLFS = 1. + PSI + PHI*(1.-EPS)
C      IF (RICH) TMOLFS = PSI + PHI*(2.-EPS)
C      DO 30 J = 1,6
30  X(J) = X(J)/TMOLFS
      MRAR = ((8.*EPS + 4.)*PHI + 32. + 28.*PSI)/TMOLFS
C

```

C CALCULATE H, CP, AND CT AS IN WRITEUP. USING FITTED  
 C COEFFICIENTS FROM JANAF TABLES

```

C ENTHLP = 0.
C CSURP = 0.
C CSURT = 0.
C ST = T/1000.
DO 40 J = 1,6
  TH = ((( A(4,J,IR)/4.*ST + A(3,J,IR)/3. )*ST
1    + A(2,J,IR)/2. )*ST + A(1,J,IR) )*ST
1    TCP = (( A(4,J,IR)*ST + A(3,J,IR) )*ST
1    + A(2,J,IR) )*ST + A(1,J,IR)
  TH = TH - A(5,J,IR)/ST + A(6,J,IR)
  TCP = TCP + A(5,J,IR)/ST*#?
  ENTHLP = ENTHLP + TH*X(J)
40  CSURP = CSURP + TCP*X(J)
  ENTHLP = ENTHLP/MBAR
  CSURP = CSURP/MBAR

```

C NOW CALCULATE RHO AND ITS PARTIAL DERIVATIVES  
 C USING PERFECT GAS LAW

```

C RHO = .012187*MBAR*p/T
C DRHODT = -RHO/T
C DRHODP = RHO/p

```

```

C      ALL DONE
C      RETURN
END

```

```

SUBROUTINE DERIVS(P,T,PHI,EPS,PST,A,X,Y,U,AMWT,CSURP,CSURT,
1 DRHOOT,DRHOOP)
LOGICAL RICH,LFAN
DATA ROVR2/.99745/
DATA SCALF/41.29287/

C
RICH = PHI .GE. 1.0
LFAN = .NOT. RICH

C
C3 = (117. + 30.*EPS)*1000.
C4 = 1.35E5*EPS
C5 = 2.0 - EPS + PST
C6 = 5.0 - 2.*EPS + 2.*PST

C
DUDTPX = 6.3E4*U/T**2
DUDPTX = -U/P
DUDXPT = -U/(X*(1. - 2.*EPS*X))

C
DADTP = (3.4E4*2./3.)*A/T**2
DADPT = -A/(3.*P)

C
AP = EPS*A
T5 = 3.*C5
DXDA = T5*(T5 + 2.*C6*AP)/(T5*(1. + 2.*AP) + 2.*C6*AP**2)**2

C
Z = (1. - PHI)/X
IF (LEAN) DYDX = (1. + .72*Z)/(1. + .36*Z)**2
IF (RICH) DYDX = (1. - 1.28*Z + .90*Z**2)/(1. - .64*Z + .3*Z**2)**2

C
DYDTP = DYDX*DXDA*DADTP
DYDPT = DYDX*DXDA*DADPT
DUDTP = DUDXPT*DXDA*DADTP + DUDTPX
DUDPT = DUDXPT*DXDA*DADPT + DUDPTX

C
DHFDPT = C3*DYDPT + C4*DUDPT
DC2DPT = -2.* (3.*DYDPT + DUDPT)
DC1DPT = 5.*DYDPT + 3.*DUDPT
DHFDTP = C3 * DYDTP + C4*DUDTP
DC2DTP = -2.* (3.*DYDTP + DUDTP)
DC1DTP = 5.*DYDTP + 3.*DUDTP

C
TV0 = (3000. - 2000.*FPS + 300.*PST)/(1. - .5*EPS + .09*PST)
FARG = FXP(TV0/T)
TV = TV0/(FARG - 1.)
DTVDTDP = TV0*FARG/(T*(FARG - 1.))**2 *TV0

C
AMCP = (8.*EPS + 4.)*PHI + 32. + 28.*PST
C1 = 7.*PST + 5.*Y + 3.*U
C2 = 2.* (PST - 3.*Y - U)
IF (LEAN) C1 = C1 + 7. + (9. - 8.*EPS)*PHI
IF (RICH) C1 = C1 + 2. + 2.* (7. - 4.*EPS)*PHI
IF (LEAN) C2 = C2 + 2.* (1. + (5. - 3.*FPS)*PHI)
IF (RICH) C2 = C2 + 2.* (4. + (2. - 3.*EPS)*PHI)

C
CSURP = ROVR2/AMCP*(C1 + T*DC1DTP + C2*DTVDTDP + TV*DC2DTP
1 + DHFDTP)
CSURT = ROVR2/AMCP*(T*DC1DPT + TV*DC2DPT + DHFDPT)*SCALF

C
IF (LFAN) G = 1. + (1.-FPS)*PHT + PST + Y + U
IF (RICH) G = (2.-FPS)*PHI + PST + Y + U

```

G = -AMCP/R\*\*2  
DMOPT = G\*(DYDTP + DUNTP)  
DMOPT = G\*(DYOPT + DUNPT)  
C  
DRHODT = .012187\*P/T\*(DMOPT - AMWT/T)  
DRHODP = .012187/T\*(AMWT + P\*DMOPT)  
C  
RETURN  
END

## SUBROUTINE INPOR

```

C
C  INTAKE PORT CALCULATION
C  THIS PROGRAM WAS ORIGINALLY MADE USING METER-KG UNIT
COMMON/EPROP/ TECHF(100),EFUEL(100),EANGLE(100),EMWT(100),
1 DHFUFL(100),DHLOS(100),DIEMAS(100),DOEMAS(100),
1 ERGAS(100),ECP(100),FENTH(8,100),FMASS(8,100),FEQUI(8,100),
1 EVOL(8,100),FTEMP(8,100),PCYL(8)
COMMON/INFL/ NINFF,XINFF(20),YINFF(20),AREIND,PINT,TINT,GINT,
1 EQUINT,ARFINT,XINV
COMMON /STATE/ ANGLE1,ANGLE,JCOND,ASTEP,NSTEP,TE
COMMON /TIVIG/ AINTO,AEXTD,AINTC,AEXTC,AFUELS,AFUULE
COMMON /STAT1/ RPM,JLAST,NJET,PHIO,EGR

C
IF(PINT-PCYL(1)) 50,50,60

C
C  INTAKE FLOW IS FROM CYLINDER TO PORT (BACK FLOW)
50 CINT=-1.
RHIGH=ERGAS(1)*9.8
PHIGH=PCYL(1)*10000.
PRIN=PINT/PCYL(1)
THIGH=FTEMP(1,1)
AKHIGH=1.35
GO TO 100

C
C  INTAKE FLOW IS FROM PORT TO CYLINDER
C  P VALUE DOESN'T CHANGE MUCH.
60 RINT=ERGAS(1)*9.8
CINT=1.
RHIGH=RINT
PHIGH=PCYL(1)*10000.
PRIN=PCYL(1)/PINT
THIGH=TINT
AKHIGH=1.35

C
C  CALCULATE THE FFFFCTIVE INTAKE FLOW AREA
100 ANAI=(ANGLE-AINTO)/(AINTC-AINTO)
CALL TWODIV(NINFF,XINFF,YINFF,ANAI,AREFAC)
AREINT=AREIND*AREFAC
AREINT=AREINT/10000.

C
C  NEXT EQUATION IS BASED ON METER-KG UNIT
GINT=          SORT(ABS(2.*AKHIGH*9.8/RHIGH/THIGH
1  /(AKHIGH-1.)*(PRIN**2./AKHIGH)-PRIN**4/(AKHIGH+1.)
2  /AKHIGH)))
GINT=PHIGH*ARFINT/8./RPM*GINT
GINT=GINT*CINT
GINT=GINT*1000.
AREINT=AREINT*10000.
RETURN
END

```

C SUBROUTINE UPROP UPRP 30  
 C PURPOSE: UPRP 40  
 C TO CALCULATE THE ENTHALPY AND DENSITY OF A HOMOGENOUS MIXTURE UPRP 50  
 C OF AIR, RESIDUAL GAS, AND FUEL AS A FUNCTION OF UPRP 60  
 C EQUIVALENCE RATIO, TEMPERATURE, AND PRESSURE UPRP 70  
 C UPRP 80  
 C UPRP 90  
 C USAGE: UPRP 100  
 C CALL UPROP(P,T,PHI,DEL,PSI,RESFRK,ENTHLP,CSURP,CSURT,RHO, UPRP 110  
 C DRHOOT,DRHODP,CHI) UPRP 120  
 C UPRP 130  
 C UPRP 140  
 C DESCRIPTION OF PARAMETERS: UPRP 150  
 C GIVEN:  
 P - ABSOLUTE PRESSURE OF PRODUCTS (ATM) UPRP 160  
 T - TEMPERATURE OF PRODUCTS (DEG K) UPRP 170  
 RESFRK - RESIDUAL GAS FRACTION UPRP 180  
 PHI - EQUIVALENCE RATIO (FUEL/AIR RATIO DIVIDED BY THE UPRP 190  
 CHEMICALLY CORRECT FUEL/AIR RATIO) UPRP 200  
 GIVEN IN COMMON AREA /FJEL/: UPRP 210  
 AF(I) - 6 DIMENSIONAL VECTOR OF ENTHALPY COEFFICIENTS SUCH UPRP 220  
 THAT THE ENTHALPY OF FUEL VAPOR AS A FUNCTION UPRP 230  
 OF TEMPERATURE ( T DEG K ) IS GIVEN BY: UPRP 240  

$$H(T) = AF(1)*ST + (AF(2)*ST^{#2})/2 + (AF(3)*ST^{#3})/3$$
 UPRP 250  

$$+ (AF(4)*ST^{#4})/4 - AF(5)/ST + AF(6)$$
 UPRP 260  
 WHERE ST = T/1000 AND H(T) = <KCAL/MOLE> UPRP 270  
 FOR MOST APPLICATIONS THE ENTHALPY FUNCTION H(T) SHOULD UPRP 280  
 BE VALID OVER AT LEAST THE FOLLOWING TEMPERATURE RANGE: UPRP 290  

$$300 < T < 1000$$
 UPRP 300  
 ENTHALPY DATUM STATE IS AT T = 0 ABSOLUTE WITH O2,N2, UPRP 310  
 AND H2 GASFOUS AND C SOLID GRAPHITE. UPRP 320  
 ENW - AVERAGE NUMBER OF NITROGEN ATOMS PER FUEL MOLECULE UPRP 330  
 CX - AVERAGE NUMBER OF CARBON ATOMS PER FUEL MOLECULE UPRP 340  
 HY - AVERAGE NUMBER OF HYDROGEN ATOMS PER FUEL MOLECULE UPRP 350  
 OZ - AVERAGE NUMBER OF OXYGEN ATOMS PER FUEL MOLECULE UPRP 360  
 QLOWER - LOWER HEATING VALUE (KCAL/G) UPRP 370  
 XI - MOLAR N:O RATIO OF THE OXIDANT (FOR AIR XI = 3.76) UPRP 390  
 UPRP 400  
 RETURNS:  
 DEL - MOLAR C:H RATIO OF THE PRODUCTS UPRP 410  
 PSI - MOLAR N:O RATIO OF THE PRODUCTS UPRP 420  
 CHI - EQUIVALENCE RATIO OF THE PRODUCTS FOR AN EQUIVALENT UPRP 430  
 HYDROCARBON-OXIDANT COMBUSTION UPRP 440  
 ENTHLP - SPECIFIC ENTHALPY OF THE PRODUCTS (KCAL/G) UPRP 450  
 CSUPP - PARTIAL DERIVATIVE OF ENTHLP WITH RESPECT TO T UPRP 460  
 AT CONSTANT P (CAL/G-DEG K) UPRP 470  
 CSUBT - PARTIAL DERIVATIVE OF ENTHLP WITH RESPECT TO P UPRP 480  
 AT CONSTANT T (CC/G) UPRP 490  
 RHO - DENSITY OF THE PRODUCTS (G/CC) UPRP 500  
 DRHOOT - PARTIAL DERIVATIVE OF RHO WITH RESPECT TO T AT UPRP 510  
 CONST VT P (G/CC-DEG K) UPRP 520  
 DRHODP - PARTIAL DERIVATIVE OF RHO WITH RESPECT TO P AT UPRP 530  
 CONSTANT T (G/CC-ATM) UPRP 540  
 UPRP 550  
 RETURNS IN COMMON AREA CMPSTN:  
 X(1) - CARBON DIOXIDE MOLE FRACTION UPRP 560  
 X(2) - WATER VAPOR MOLE FRACTION UPRP 570  
 X(3) - CARBON MONOXIDE MOLE FRACTION UPRP 580  
 X(4) - HYDROGEN MOLE FRACTION UPRP 590  
 X(5) - OXYGEN MOLE FRACTION UPRP 600  
 X(6) - NITROGEN MOLE FRACTION UPRP 610  
 X(7) - FUEL MOLE FRACTION UPRP 620  
 UPRP 630

C MBAR - MOLECULAR WEIGHT OF UNBURNED MIXTURE UPRP 640  
C  
C REMARKS:  
C 1) ENTHALPY DATUM STATE IS AT T = 0 ABSOLUTE WITH UPRP 650  
C O2,N2,H2 GASFOUS AND C SOLID GRAPHITE UPRP 660  
C 2) THIS IS A MODIFIED VERSION OF MIKE MARTIN'S SUBROUTINE UPRP 670  
C UPROP. IN CASE OF PROBLEMS CONTACT COLIN FERGUSON AT UPRP 680  
C 253-5348 (ROOM 31-158) UPRP 690  
C UPRP 700  
C UPRP 710  
C UPRP 720  
C UPRP 730  
C UPRP 740  
C SUBROUTINES AND FUNCTION SUBPROGRAMS NEEDED: NONE UPRP 750  
C  
C METHOD:  
C DESCRIBED IN APPENDIX A OF HIRES ET AL. SAE PAPER # 760161 UPRP 760  
C  
C\*\*\*\*\* SURROUNTING UPROP(P,T,PHI,DEL,PSI,RESFRK,ENTHLP,CSUPP,CSURT,RHO,  
C DRHOOT,DRHOOP,CHI,PAVG,CVAVG) UPRP 770  
C COMMON /FUEL/ AF(6),ENW,CX,HY,OZ,QLOWER UPRP 780  
C LOGICAL RICH,LEAN UPRP 790  
C DIMENSION A(6,7,2)  
C DIMENSION A1(42),A2(42),TABLE(7)  
C EQUIVALENCE (A1(1),A(1,1,1)),(A2(1),A(1,1,2))  
C REAL#4 MBAR,K  
C COMMON /OXDANT/ XI /CMPSTN/ X(7),MBAR  
C  
C INITIALIZE PARAMETERS, AND CHECK TO SEE IN WHAT TEMPERATURE RANGE WE ARE SO THAT THE CORRECT FITTED COEFFICIENTS WILL BE USED. FLAG TEMPERATURES TOO BIG OR TOO SMALL  
C  
C DATA A1/11.94033,2.088581,-0.47029,.037363,-.589447,-97.1418, UPRP 800  
1 6.139094,4.60783,-.9356009,6.569498E-02,.0335801,-56.62588, UPRP 810  
2 7.099556,1.275957,-.2877457,.022356,-.1598696,-27.73464, UPRP 820  
3 5.555680,1.787191,-.2881342,1.951547E-02,.1611829,.76498, UPRP 830  
4 7.865847,.6883719,-.031944,-2.68708E-03,-.2013873,-.893455, UPRP 840  
5 6.807771,1.453404,-.328985,2.561035E-02,-.1189462,-.331935, UPRP 850  
6 6\*0.0/  
DATA A2/4.737305,16.65283,-11.23249,2.828001,6.76702E-03,-93.75793 UPRP 1000  
7 ,7.809672,-.2023519,7.418708,-1.179013,1.43629F-03,-57.08004, UPRP 1010  
8 6.97393,-.8238319,2.942042,-1.175239,4.132409F-04,-27.19597, UPRP 1020  
9 6.991878,-.1617044,-.2132071,.2968197,-1.525234E-02,-.118189, UPRP 1030  
& 6.295715,2.388387,-.0314788,-.3267433,4.35925F-03,.103637, UPRP 1040  
- 7.092199,-1.295825,3.20688,-1.202212,-3.457938E-04,-.013967, UPRP 1050  
\$ 6\*0.0/  
DATA TABLE /-1.,1..1..-1.,0.,0.,0./ UPRP 1060  
C  
C ENTER INTO ARRAYS A1 AND A2 THE FUEL PARAMETERS UPRP 1070  
C  
C DO 5 I=1,6 . UPRP 1080  
5 A1(I + 36)=AF(I) UPRP 1090  
A2(I + 36)=AF(I) UPRP 1100  
RICH = PHI .GT. 1.0 UPRP 1110  
LEAN = .NOT. RICH UPRP 1120  
W = ENW/CX UPRP 1130  
Z = OZ/CX UPRP 1140  
DEL = CX/HY UPRP 1150  
EPS = 4.\*DEL/(1. + 4.\*DEL - 2.\*DEL\*\*2) UPRP 1160  
IFR = 0 UPRP 1170  
IF (T .LT. 100.) IFR = 1 UPRP 1180  
IF (T .GT. 6000.) IFR = 2 UPRP 1190  
IR = 1 UPRP 1200  
IF (T .LT. 500.) IR = 2 UPRP 1210  
C UPRP 1220  
C UPRP 1230  
C UPRP 1240

```

C           GET THE COMPOSITION IN MOLES/MOLE OXYGEN OF OXIDANT      UPRP1250
C           PCTRES = RFSFRK                                         UPRP1250
C           PCTNEW = 1.0 - RESFRK                                     UPRP1250
C           IF (RICH) GO TO 10                                       UPRP1270
C           X(1) = EPS*PHI*PCTRES                                    UPRP1280
C           X(2) = (2.*(1. - EPS) + EPS*7)*PHI*PCTRES               UPRP1290
C           X(3) = 0.                                              UPRP1300
C           X(4) = 0.                                              UPRP1310
C           X(5) = (1. - PHI)*PCTRES + PCTNEW                      UPRP1320
C           DCDT = 0.                                              UPRP1330
C           GO TO 20                                             UPRP1340
10 ZT = 1000./T                                              UPRP1350
C           K = EXP(2.743 + 7T*(-1.761 + ZT*(-1.611 + ZT*.2803))) UPRP1360
C           DKDT = -K*7T*(-1.761 + 7T*(-3.222 + 7T*.9409))/T        UPRP1370
C           ALPHA = 1.0 - K                                         UPRP1380
C           RETA = 2.*(1. - EPS*PHI) + K*(2.*PHI - 1.) + EPS*PHI       UPRP1390
C           BETA = RETA + EPS*PHI*7                                UPRP1400
C           GAMMA = 2.*K*EPS*PHI*(PHI - 1.)                         UPRP1410
C           C = (-BETA + SQRT(RETAT*BETA + 4.*ALPHA*GAMMA))/(2.*ALPHA) UPRP1420
C           DCDT = -DKDT*(C*C + (2.*PHI - 1.) + EPS*PHI)*C - GAMMA/K   UPRP1430
C           DCDT = DCDT/(2.*ALPHA*C + BETA)                         UPRP1440
C           X(1) = (EPS*PHI - C)*PCTRES                            UPRP1450
C           X(2) = (2.0*(1. - EPS*PHI) + EPS*PHI*Z + C)*PCTRES      UPRP1460
C           X(3) = C*PCTRES                                         UPRP1470
C           X(4) = (2.0*(PHI - 1.) - C)*PCTRES                      UPRP1480
C           X(5) = PCTNEW                                           UPRP1490
20 X(6) = XI + EPS*PHI*W/2.*PCTRES                           UPRP1500
C           X(7) = PCTNEW * EPS*PHI/CX                             UPRP1510
C           CONVENT COMPOSITION TO MOLE FRACTIONS AND CALCULATE AVERAGE MOLECULAR WEIGHT      UPRP1520
C           IF (LEAN) TMOLES = XI + (1. + EPS*PHI/CX)*PCTNEW          UPRP1530
C           + (1. + (1. - EPS)*PHI + EPS*PHI*(Z + W/2.))*PCTRES    UPRP1540
C           IF (RICH) TMOLES = XI + (1. + EPS*PHI/CX)*PCTNEW          UPRP1550
C           + ((2. - EPS)*PHI + EPS*PHI*(Z + W/2.))*PCTRES        UPRP1560
C           DO 30 J = 1.7                                            UPRP1570
30 X(J) = X(J)/TMOLES                                         UPRP1580
C           MBAR = EPS*PHI*(12. + 1./DEL + 16.*Z + 14.*W) + 32. + 28.*XI UPRP1590
C           MBAR = MBAR/TMOLES                                      UPRP1600
C           CALCULATE H, CP, AND CT AS IN WRITEUP, USING FITTED COEFFICIENTS FROM JANAF TABLES      UPRP1610
C           FNTHLP = 0.                                              UPRP1620
C           CSURP = 0.                                              UPRP1630
C           CSURT = 0.                                              UPRP1640
C           ST = T/1000.                                            UPRP1650
C           DO 40 J = 1.7                                            UPRP1660
C           TH = (((A(4,J,IR)/4.*ST + A(3,J,IR)/3.)*ST + UPRP1670
1          + A(2,J,IR)/2.)*ST + A(1,J,IR))*ST                  UPRP1680
C           TCP = ((A(4,J,IR)*ST + A(3,J,IR))*ST + UPRP1690
1          + A(2,J,IR))*ST + A(1,J,IR)                         UPRP1700
C           TH = TH - A(5,J,IR)/ST + A(5,J,IR)                   UPRP1710
C           TCP = TCP + A(5,J,IR)/ST*2                          UPRP1720
C           ENTHLP = FNTHLP + TH*X(J)                            UPRP1730
40 CSURP = CSURP + TCP*X(J) + 1000.*TH*DCDT*PCTRES*TABLE(J) UPRP1740
C           ENTHLP = ENTHLP/MBAR                                     UPRP1750

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```

C CSURP = CSUBP/MRAP          UPRP1850
C NOW CALCULATE RHO AND ITS PARTIAL DERIVATIVES   UPRP1860
C USING PERFECT GAS LAW           UPRP1870
C
C RHO = .012187*MBAR*p/T          UPRP1880
C DRHODT = -RHO/T                UPRP1890
C DRHODP = RHO/P                 UPRP1900
C
C CALCULATE PSI AND CHI FOR BURNED GASES        UPRP1910
C
C PSI = (XI + EPS*PHI*W/2.)/(1. + EPS*Z*PHI/2.)  UPRP1920
C CHI = PHI*(1. + EPS*Z/2.)/(1. + EPS*Z*PHI/2.)  UPRP1930
C
C RAVG=82.057/MRAR             UPRP1940
C CVAVG=CSUBP-1.98/MRAP         UPRP1950
C
C ALL DONE!                      UPRP1960
C RETURN                         UPRP1970
C END                           UPRP1980
                                UPRP1990
                                UPRP2000
                                UPRP201

```

```

SUBROUTINE EQIR(TTTT,PPP,PHTC,IFLAG,Z)
C
C VARTABLES LIST
C
REAL*8 DPPATM,DPTEMP,DEQIB,XMOFR
DIMENSION DEQIR(4),XMOFR(14),YMOFR(14),Z(5)
C CALCULATE RATIOS OF H/C,N/C,O/C,AND C/C WHERE C=1.
TTEMP=TTTT
PATM=PPP
SLR=15.1
ERURN=1./PHTC
IF(TEMP.LT.1800.) GO TO 101
IFLAG=0
WHY=(12.*SLR-137.4)/(-SLR+25*137.4)
XWHY=1.+25*WHY
DEQIR(1)=WHY
DEQIB(2)=1.
DEQIB(4)=2.*XWHY*ERURN
DEQIB(3)=3.764*DEQIB(4)
C
C CALCULATE N AND NO EQIR, AND EQIB. MOLE FRACTIONS
DPPATM=PATM
DPTEMP=TEMP
CALL PTCHEW(DPTEMP,DPPATM,DEQIR,XMOFR,1SENT)
DO 100 I=1,14
YMOFR(I)=XMOFR(I)
100 CONTINUE
GO TO 103
101 IFLAG=1
DO 102 J=1,14
102 YMOFR(J)=0.
103 Z(1)=YMOFR(2)
Z(2)=YMOFR(5)
Z(3)=YMOFR(8)
Z(4)=YMOFR(9)
Z(5)=YMOFR(14)
RETURN
END

```

```

SUBROUTINE DNO0T(TTTT,PPPP,TOTMOL,ZM0FR,IFLAG,XNO,F)
C
C VARIABLE LIST
C
C
C      F      FINAL EVALUATION OF R.H.SIDE RATE EQUATION
C      W,X,Y,Z  DUMMY VARIABLES
C      VOL      VOLUME OF ELEMENT
C      XNO      AMOUNT OF NITRIC OXIDE
C      RC1F     RATE CONSTANT FOR FIRST REACTION, FORWARD
C      RC1R     RATE CONSTANT FOR FIRST REACTION, REVERSE
C      RC2F     RATE CONSTANT FOR SECOND REACTION, FORWARD
C      RC2R     RATE CONSTANT FOR SECOND REACTION, REVERSE
C      TEMP     TEMPERATURE OF ELEMENT
C      RTEMP    RECIPROCAL OF TEMP
C
C DIMENSION ZM0FR(5)
C TEMP=TTTT
C PAtM=PPPP
C VOL=B2.06*TEMP*TOTMOL/PAtM
C IF(TEMP.LT.1800.) GO TO 2000
C IF(IFLAG.GT.0) GO TO 2000
C IF(TOTMOL.LT.0.0) GO TO 2000
C
C 4. COMPUTE RATE CONSTANTS (FUNCTIONS OF TEMPERATURE ONLY)
C RTEMP=1.9857*TEMP
C RC1F=7.6E+13*EXP(-75460./RTEMP)
C RC1R=1.6E+13
C RC2F=6.4E+09*EXP(-6255./RTEMP)*TEMP
C RC2R=1.5E+09*EXP(-38720./RTEMP)*TEMP
C RCOH=4.1E+13
C
C TMOLNO=ZM0FR(4)*TOTMOL
C TMOLN=ZM0FR(3)*TOTMOL
C XMOLCO=ZM0FR(1)
C
C 5. CALCULATE DNO/DT=F (VOL,TEMP,PAtM,ERURN,ZM0FR,XNO)
C ZR=RC1R*ZM0FR(4)
C WR=RC2F*ZM0FR(5)+RCOH*ZM0FR(2)
C CAPL=ZR/WR
C ALPHA=XNO/TMOLNO
C
C TERM1=2.*RC1R*TMOLN*TMOLNO/VOL*(1.-ALPHA*ALPHA)
C TERM2=1.+ALPHA*CAPL
C F=TERM1/TERM2
C
C GO TO 3000
2000 F=0.
3000 CONTINUE
RETURN
END

```

```

C SUBROUTINE PTCHEM ( TMP, PRS, D, XMOFR, ISENT )
C
C THE ORIGINAL MIT EQUILIBRIUM PTCHEM SUBROUTINE HAS BEEN REDUCED
C AND IS DESIGNED TO PROCESS 4 ELEMENTS & 14 SPECIES
C
C ARRAY D CONTAINS RATIOS OF ELEMENTS H, C, N, O RESPECTIVELY:
C
C F.G., DATA D / 1.43, 1.0, 13.0, 3.46 /
C
C
C ARRAY XMOFR CONTAINS MOLE FRACTIONS OF EACH SPECIES:
C SYMBOLS OF EACH SPECIES 1 TO 14 (HEX'E') ARE AS FOLLOWS:
C
C 0      'HCO ', 'CO ', 'CO2 ', 'H ', 'OH ', 'H2 ', '
C 1      'H2O ', 'N ', 'NO ', 'NO2 ', 'N2 ', 'N2O '
C 2      'O ', 'OP ', '/ '
C
C INPUT: ( DOUBLE PREC. )
C
C TMP = TEMPERATURE ( DEGREES K )
C PRS = PRESSURE ( ATMOSPHERES )
C D   = ARRAY(4) ( RATIO, 4 ELEMENTS )
C
C OUTPUT: ( DOUBLE PREC. )
C
C XMOFR = ARRAY(14) ( MOLE FRACTIONS, 14 SPECIES )
C ISENT = ERROR CODE:
C     0 = NO ERROR
C     1 = TEMP TOO HIGH
C     2 = TEMP TOO LOW
C     3 = ( UNUSED )
C     4 = TOO MANY ITERATIONS, RESULTS DOUBTFUL, LOOK UP NU
C     5 = TOO MANY ITERATIONS
C     6 = THERE ARE NO GASES PRESENT
C     7 = CHECK IF THERE ARE ENOUGH SPECIES
C     8 = TOO MANY TRIPS FOR T
C
C AUTHOR: DAN DANTZER      LATEST REVISION 12/14/72
C ADAPTED FOR USE WITH PCHEM BY TOM MIKUSI CURRENT TO 5/23/74
C
C IMPLICIT REAL*8(A-H,O-Z)
C
C EQUIVALENCE ( ITOTSP, 4 )
C EQUIVALENCE ( ITOTSP, 41 )
C EQUIVALENCE ( NELEM , N )
C EQUIVALENCE ( G(1,1), CMV(1) )
C
C DIMENSION D(1), XMOFR(1)
C DIMENSION A(4,14), ZL(14,8)
C DIMENSION ZL1(55), ZL2(55)
C DIMENSION K2(2)
C DIMENSION RTP(5)
C
C FOLLOWING ARRAYS ARE IN ELEMENT IN SIZE
C
C DIMENSION DD(4), XMU(4), XNJ(4), F(4), F(4,4)
C
```

```

C FOLLOWING ARRAYS ARE *NELEM* +2 = *INXNSL*          00001970
C DIMENSION R(6), G(6,6)                                00001980
C FOLLOWING ARRAYS ARE *TTOTSP*                          00001990
C DIMENSION CMN(14), CP(14), CPT(14), X(14), XMAX(14) 00002000
C DIMENSION HORT(14), SR(14), C(14)                   00002010
C DIMENSION VHORT(14)                                 00002020
C COMMON / HOPT / HORTSM,SMOHDT,XMU,RTP,SUMNI        00002030
C NSAME = INITIALIZATION FLAG                         00002040
C NFLEM = NR OF ELEMENTS INVOLVED                  00002050
C ITOTSP = TOTAL NR OF SPECIES INVOLVED            00002060
C DATA NSAME / 0 /                                     00002070
C DATA NELEM / 4 /                                    00002080
C DATA INXNSL / 6 /                                  00002090
C DATA ITOTSP / 14 /                                 00002100
C DATA DD,XNII,E,F / 28*0.030 /                      00002110
C DATA R, G / 42 * 0.000 /                            00002120
C DATA A, CP, CPT, X, XMAX / 112 * 0.000 /           00002130
C CMN IS NOT INITIALIZED WHEN IT LIES WITHIN ARRAY G 00002140
C ARRAY ZL(K,J) CONTAINS THE HI-TEMP DATA FOR EACH OF 14 SPECIES 00002150
C K = SPECIES NR ( 1 - 14 )                           00002160
C J = DATA ( 1 - 8 EACH SPECIES )                     00002170
C DATA WAS TAKEN FROM ORIGINAL DATA SET ( CARDS ), ARRANGED IN 00002180
C ROW,COL (14,8), BUT DATA STATEMENT INTERNALLY STORES 00002190
C BY COL,ROW; THEREFORE, DATA MUST BE REVERSED FOR PROG EXEC. 00002200
C ORIGINAL DATA ARRANGEMENT MAINTAINED FOR CONVENIENCE IN MAKING 00002210
C CHANGES TO SPECIES DATA.                           00002220
C NR OF CONTINUATION CARDS LIMITED TO 19             00002230
C CONTINUATION COL #6 CONTAINS THE HEXIDECIMAL SPECIES NR 00002240
C DATA ZL1 /                                         00002250
1 9.3434439D 00, 2.9512196D 00,-6.7088366D-01, 5.0901942D-02, 00002260
1 -4.1140777D-01,-6.9903499D 00, 6.2395554D 01, 2.3009987D 00, 00002270
2 7.0995644D 00, 1.2759552D 00,-2.8774744D-01, 2.2356123D-02, 00002280
2 -1.5986955D-01,-2.9023636D 01, 5.4823700D 01, 1.2890015D 00, 00002290
3 1.1940331D 01, 2.0885811D 00,-4.7029203D-01, 3.7363116D-02, 00002300
3 -5.8944768D-01,-9.9468796D 01, 6.2207169D 01, 2.3269949D 00, 00002310
4 4.9679995D 00,-5.9678716D-13, 1.9345219D-13,-1.8732195D-14, 00002320
4 -7.4194935D-14, 5.0619217D 01, 3.3404419D 01, 1.0119925D 00, 00002330
5 5.6197815D 00, 1.9668446D 00,-3.8645178D-01, 2.7364515D-02, 00002340
5 1.3418680D-01, 8.0923529D 00, 5.0777405D 01, 2.0489998D 00, 00002350
6 5.5556803D 00, 1.7971914D 00,-2.8813416D-01, 1.9515470D-02, 00002360
6 1.6118270D-01,-1.2590199D 00, 3.8126053D 01, 2.0239993D 00, 00002370
7 6.1390944D 00, 4.6078291D 00,-9.3550094D-01, 6.6594975D-02, 00002380
7 3.3580098D-02,-5.9687856D 01, 5.1456772D 01, 7.0519965D 00 / 00002390
DATA ZL2 /                                         00002400
8 5.1632023D 00,-1.8977487D-01, 3.6921006D-02, 3.6241105D-03, 00002410
8 -3.2719155D-02, 1.1134157D 02, 4.2783066D 01, 1.0359793D 00, 00002420
9 7.5180625D 00, 1.0245209D 00,-2.3033735D-01, 1.7926671D-02, 00002430
9 -1.9369543D-01, 1.8756821D 01, 5.8378296D 01, 2.0729971D 00, 00002440

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A 1.2123282D 01, 1.2564093D 00,-3.0117296D-01, 2.3658749D-02, 00002570
A -6.2256289D-01, 2.3839598D 00, 6.8810959D 01, 3.1109982D 00, 00002580
R 6.8077699D 00, 1.4534035D 00,-3.2898575D-01, 2.5610346D-02, 00002590
R -1.1894619D-01,-2.4038353D 00, 5.3165161D 01, 2.0719986D 00, 00002600
C 1.2365961D 01, 1.7261782D 00,-4.0528846D-01, 3.1418435D-02, 00002610
C -5.8120877D-01, 1.4105570D 01, 6.4331467D 01, 3.1099997D 00, 00002620
D 5.1006309D 00,-1.5177220D-01, 4.8953138D-02,-2.8814352D-03, 00002630
D 8.9299418D-03, 5.8080948D 01, 4.4752548D 01, 1.0379944D 00, 00002640
E 7.8658457D 00, 6.8837190D-01,-3.1944100D-02,-2.6870817D-03, 00002650
F -2.0138729D-01,-2.9684544D 00, 5.7424637D 01, 2.0749989D 00, / 00002660

C
C
C
C IF(NSAME)2000,2000,2004 00002570
2000 NSAME=1 00002580
AP=1.9872600 00002590
ITMAX = 500 00002700
ITW = 400 00002710
DIF = 15.000 00002720
DIF1 = DIF 00002730
T = 1.000 00002740
TLUB = 6000. 00002750
XN=N 00002760
TOL1 = .01n0 00002770
TOL3 = .00001n0 00002780
TOL5 = 1.00-5 00002790
TOL6 = .1Dn 00002800
TOL7 = 10.000 00002810
C
C ARRAY A(I,K) CONTAINS NR OF ATOMS PER ELEMENT ( IN SPECIES ) 00002820
C
C I = ELEMENTS H, C, N, O RESPECTIVELY 00002830
C K = SPECIES NR 00002840
C
C
A(1,1) = 1. 00002850
A(1,4) = 1. 00002860
A(1,5) = 1. 00002870
A(1,6) = 2. 00002880
A(1,7) = 2. 00002890
A(2,1) = 1. 00002900
A(2,2) = 1. 00002910
A(2,3) = 1. 00002920
A(3,8) = 1. 00002930
A(3,9) = 1. 00002940
A(3,10)= 1. 00002950
A(3,11)= 2. 00002960
A(3,12)= 2. 00002970
A(4,1) = 1. 00002980
A(4,2) = 1. 00002990
A(4,3) = 2. 00003000
A(4,5) = 1. 00003010
A(4,7) = 1. 00003020
A(4,9) = 1. 00003030
A(4,10)= 2. 00003040
A(4,12)= 1. 00003050
A(4,13)= 1. 00003060
A(4,14)= 2. 00003070
C
C LOAD DATA INTO SPECIES ARRAY 7L 00003080
C
C

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```

    II = 0          00003170
    DO 1050 K = 1,7 00003180
    I = K + 7      00003190
    DO 1050 J = 1, B 00003200
    II = II + 1    00003210
    ZL(K,J) = ZL1(II) 00003220
1050 ZL(I,J) = ZL2(II) 00003230
    DO 3010 I = 1,N 00003240
    XMU(I) = 0.0 00003250
3010 CONTINUE 00003260
C 00003270
C 00003280
C     END OF ONE-TIME INITIALIZATION 00003290
C 00003300
2004 IF ( TMP - 200.0 ) 2112, 2112, 2355 00003310
2355 CONTINUE 00003320
    IF ( TMP - TLUR ) 2012, 2012, 2009 00003330
2009 ISENT=1 00003340
    GO TO 5000 00003350
2112 ISENT=2 00003360
    GO TO 5000 00003370
2012 CONTINUE 00003380
    TK = TMP / 1.00+3 00003390
    XLP = DLOG ( PRS ) 00003400
C 00003410
C     START OF ORIGINAL *HS* SUBROUTINE 00003420
C 00003430
    DO 5004 K10 = 1, M 00003440
    IF ( ZL(K10,1) ) 5003, 5002, 5003 00003450
5002 HORT(K10) = 0.11111111D0 00003460
    SR (K10) = -1.006 00003470
    GO TO 5004 00003480
5003 HORT(K10) = ((((( ZL(K10,4) * TK / 4.00 + ZL(K10,3) / 3.000 ) *
    1   TK + ZL(K10,2) / 2.00 ) * TK + ZL(K10,1) ) * TK -
    2   ZL(K10,5) / TK + ZL(K10,6) ) / ( AR * TK )
    SR(K10) = ( ZL(K10,1) * DLOG(TK) + TK * ( ZL(K10,2) +
    1   ZL(K10,3) * 0.500 * TK + ZL(K10,4) * TK **2 / 3.00 ) -
    2   ZL(K10,5) * 0.500 / TK **2 + ZL(K10,7) ) / AR 00003490
5004 C(K10) = HORT(K10) - SR(K10) + XLP 00003500
C 00003510
C     END OF ORIGINAL *HS* SUBROUTINE 00003520
C 00003530
    ISENT=0 00003540
    ITER=0 00003550
    ITTPDG=0 00003560
    TOL4 = 0.1D0 00003570
    YMAX = 0. 00003580
    DO 412 J=1,M1 00003590
    XMAX(J) = 1.0D10 00003600
    DO 412 I=1,L 00003610
    IF ( A(I,J) ) 412,412,413 00003620
413 IF ( D(I)/A(I,J) > XMAX(J) ) 414,412,412 00003630
414 XMAX(J) = D(I)/A(I,J) 00003640
412 CONTINUE 00003650
    X0=0.0D0 00003660
    DO 90 I=1,N 00003670
90 X0=X0+D(I) 00003680
    AWD = X0 / XN 00003690
    Y0=0.0D0 00003700
    DO 93 J=1,M 00003710
93 X0=X0+A(J) 00003720
    AWD = X0 / XN 00003730
    Y0=0.0D0 00003740
    DO 93 J=1,M 00003750
93 X0=X0+A(J) 00003760

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```

93      Y0=Y0+ XMAX(J)          00003770
      X0= DMIN1(X0,Y0)          00003780
      X0=X0*1.0500             00003790
      DO 825 J=1,M1            00003800
825      XMAX(J)=XMAX(J)*1.0500 00003810
C
C      CAUTION*** ASSUMPTION: THAT EACH ELEMENT MOLE RATIO DIVIDED BY 00003820
C      THE SUM OF THE RATIOS WILL BE GREATER THAN 0.01:           00003830
C      IF = OR < 0.01, THEN MUST USE FOLLOWING ROUTINE:           00003840
C      I.E., REMOVE THE 'C' COMMENT FROM COL 1 FROM HERE TO LABEL 530 & 00003850
C      FROM LABEL 503 TO 475                                         00003860
C      NOTE: ARRAY K2 IS DIMENSIONED (2)                           00003870
C
C      SUM IS NOT DEFINED IN ORIGINAL PROGRAM                   00003880
C      SUM = 0.0           00003890
      DO 525 I = 1,N           00003900
525      SUM = SUM + D(I)           00003910
C
      L1=0           00003920
      NG05=1           00003930
      RATIO = .0100           00003940
      DO 526   I=1,N           00003950
      IF (D(I)/SUM - RATIO )    527,527,526 00003960
527      L1=L1+1           00003970
      K2(L1) =I           00003980
526      CONTINUE           00003990
      NL= L1           00004000
      IF (NL)  528,528,529 00004010
528      NG05 =1           00004020
      GO TO 530           00004030
529      NG05=2           00004040
530      CONTINUE           00004050
C
C      ITER4=0           00004060
      NG06=1           00004070
      RH2=1.000           00004080
C
C      END OF ENTRY INITIALIZATION & CHECKING OF TEMPERATURE 00004090
C
C      BEGINNING OF MAIN PROGRAM LOOP                         00004100
C
      99      NGO=1           00004110
      ITER2=0           00004120
      IF (ITER2 - 1)    473,473,474 00004130
474      RH2=DSORT(H2)           00004140
      RH2=DMIN1(RH2*1.000)        00004150
473      NG01=1           00004160
      DO 101   J=1,M1           00004170
      SUM= C(J)           00004180
      DO 1002  I=1,N           00004190
      SUM=SUM+ XMU(I)*A(I,J)        00004200
1002      CP(J)= SUM           00004210
      DO 1012  J=1,M1           00004220
      CPT(J)= CP(J)           00004230
1012      DO 1001  I=1,N           00004240
1001      DD(I)= D(I)           00004250
      LI= 0           00004260
      SUMEX=0.000           00004270
      DO 102   J=1,M1           00004280

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```

        J1=J
        IF (L>T(J)+ 30.000) 420,420, 421
421 XJ=DEXP(-CPT(J))
        SUMFX=SUMFX+XJ
102   X(J)=XJ
        IF (SUMFX-1.000-TOL1*R42) 103,103,107
103   IF (SUMEX-1.000+TOL1*R42) 112,104,104
104   L1=1
        DO 105 I=1,N
        SUM=0.0
        DO 105 J=1,M
        SUM=SUM+ A(I,J)*X(J)
106   F(I,1) = SUM
        YMAX = X0
        GO TO 123
420   CPT1 = CPT(J1)
        DO 423 J=1,M
        J1= J
        CPT2 = CPT(J1)-CPT1
        IF (CPT2 +30.000) 420,420,422
422 X(J) =DEXP1-CPT2)
423   CONTINUE
107   SUM=0.000
        DO 416 J=1,M
416   SUM= SUM+ X(J)
        SUM= X0/SUM
        DO 108 J= 1,M
        X(J)=X(J)*SUM
        DO 109 I=1,N
        SUM= DD(I)
        DO 110 J=1,M
110   SUM = SUM -A(I,J)*X(J)
109   DD(I)= SUM
        GO TO 123
112   DO 113 J=1,M
113   X(J)= 0.000
123   L=L1
C
C     L = 0 OR 1 ONLY
C
        IF (L) 131,131, 200
131   DO 132 I=1,N
132   XNU(I)=-DD(I)
        GO TO 23
430   DO 431 J=1,M
        CMN(J)= 0.000
        DO 431 I=1,N
        CMN(J)=CMN(J)+XNU(I)*A(I,J)
        COMP=TOL5*TOL5/H2
        XNUD=0.000
        DO 432 I=1,N
432   XNUD= XNUD+ XNU(I)*D(I)
446   H= -XNUD
        ITTRDG=ITTRDG+1
        IF (ITTRDG-5000) 2358,2358,2356
2356 TSENT = 8
        GO TO 5000
2358 CONTINUE
        DO 437 J=1,M
437   CPT(J)= CP(J) + T*CMN(J)

```

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EXMIN= 1.0D10          00004970
DO 510 I=1,M           00004980
  IF (CPT(J) - EXMIN)   511,510,510 00004990
511 CONTINUE           00005000
      EXMIN= CPT(J)     00005010
510  CONTINUUF         00005020
      SUMEX =0.070       00005030
      DO 513 J=1,M       00005040
        IF(CPT(J)-EXMIN-DIF1) 517,517,516 00005050
516  X(J)= 0.070       00005060
      GO TO 513         00005070
517 X(J) =DEXP(EXMIN -CPT(J)) 00005080
      SUMEX =SUMEX +X(J) 00005090
518  CONTINUE           00005100
      IF (EXMIN ) 521,521 , 519 00005110
519 IF(SUMEX*DEXP(-EXMIN)-1.0D0) 443,521,521 00005120
521  PROD = X0 /SUMFX 00005130
      DO 522 J=1,M       00005140
522  H= H+ PROD* X(J)*CMN(J) 00005150
443  CONTINUE           00005160
      IF (H) 458,458,457 00005170
457  T0=T               00005180
      H0= H               00005190
      GO TO (448,459) , NGO 00005200
448  T= T+T             00005210
      IF (T - 1.0015 ) 446, 446, 908 00005220
908 ISFNT = 7           00005230
      GO TO 5000           00005240
459  T1=T               00005250
      NGO=?               00005260
459 IF(DABS(H/H2)-TOL3) 453,453,460 00005270
460  IF ((T1-T0)**2-COMP) 453,453,452 00005280
452  T=0.500*(T0+T1)   00005290
      GO TO 446           00005300
453  DO 454 I=1,N       00005310
454  XMU(T) = XMII(I) + T* XNU(I) 00005320
      GO TO 99             00005330
C
C     L = 1 AT THIS POINT
C
200 SDUM = 0.000          00005340
      SUM = 0.000           00005350
      DO 2 I = 1, N         00005360
        SDUM = SDUM + F(I,I) * F(I,I) 00005370
2  SUM = SUM + F(I,I) * D(I) 00005380
      E(I) = SUM / SDUM 00005390
      G(1,1) = 0.000          00005400
      Y1 = 0.000           00005410
      Z1 = 0.000           00005420
71  SUM = E(I) + G(1,1) * Z1 00005430
      IF ( SUM )10, 10, 11 00005440
10  Z1 = 0.000           00005450
      GO TO R              00005460
11  IF ( SUM - YMAX ) 471, 471, 472 00005470
472 Z1 = YMAX           00005480
      GO TO R              00005490
471 Z1 = SUM           00005500
13  IF ( DARS( Z1 - Y1 ) - TOL3 ) 15, 15, 13 00005510
13  Y1 = Z1             00005520
      GO TO 71             00005530
                                00005540
                                00005550
                                00005560

```

```

15 00 16 I = 1, N          00005570
16 XNU(I) = -DD(I) + F(I+1) * Z1 00005580
    DO 19 J = 1, M          00005590
19 X(J) = X(J) + Z1          00005600
C   L = 0 OR I BELOW THIS POINT 00005610
C
23   DO 24 I=1,N          00005620
    IF(DABS(XNU(I)) - TOL4 * AVO) 24,24,25 00005630
24   CONTINUE
    NG01=2
    GO TO 330
25   GO TO (550,551), NG06 00005640
551   ITER4=ITER4+1
    IF (L) 550,550,814 00005650
A14 IF (ITER4-20)550,552,552 00005660
552   ITER4=0
    NG01=2
    GO TO 330
550   H0=0.000
    DO 26 I=1,N          00005670
26   H0=H0+XNU(I)**2
    H2= H0
    T0=0.000
    T=1.000
    GO TO 330
C
C   SEE COMMENTS ABOVE ( LABEL 527 )
C
503 CONTINUE
C
    GO TO (475,476),NG05 00005680
475 K = ITER - (ITER / N ) * N 00005690
    IF (K) 531,532,531 00005700
532   K=N
531   DO 540 L1=1,NL 00005710
    IF(K2(L1)-K) 540,541,540 00005720
540   CONTINUE
    GO TO 475
541 IF(DABS(XNU(K))-TOL5*D(K)) 475,475,542 00005730
542 IF(DABS(XNU(K))-1.0-15)475,475,8000 00005740
R000 SUM=XNU(K)
    DO 543 I=1,N          00005750
543   XNU(I)=0.000
    XNU(K)=SUM
    H0=SUM*SUM
    DIF1=100.000
    H2=H0
    T0=0.000
    T=1.000
    GO TO 430
475   DIF1=DIF
C
    GO TO 430
330   ITER=ITER+1
    IF (ITER - ITW) 331,670,670 00005760
670 ISFNT = 4
    GO TO 5079
C
331   GO TO (503,500),N301 00005770
                                00005780
                                00005790
                                00005800
                                00005810
                                00005820
                                00005830
                                00005840
                                00005850
                                00005860
                                00005870
                                00005880
                                00005890
                                00005900
                                00005910
                                00005920
                                00005930
                                00005940
                                00005950
                                00005960
                                00005970
                                00005980
                                00005990
                                00006000
                                00006010
                                00006020
                                00006030
                                00006040
                                00006050
                                00006060
                                00006070
                                00006080
                                00006090
                                00006100
                                00006110
                                00006120
                                00006130
                                00006140
                                00006150
                                00006160

```

C

```

500      NTOT=N+1.          00006170
        DO 820  I=1,N          00006180
820      DO(I)=XMU(I)          00006190
        DO A21 J=1,M1          00006200
821      CPT(J)=X(J)          00006210
        IF (I,L)    727,727,502 00006220
502      XBAR=Z1              00006230
        ITER2 = 1              00006240
750 IF (XBAR) 727, 727, 701 00006250
701      G(N+1,N+1)= 0.000 00006260
        DO 704  K=1,M          00006270
        SUM=- C(K)            00006280
        DO 705  I=1,N          00006290
705      SUM=SUM-XMU(I)*A(I,K) 00006300
        IF (SUM -30.000)425,727, 727 00006320
425      X(K) = XBAR*DEXP(SUM) 00006330
704      CONTINUE
        DO 706  I=1,N          00006340
        SUM=0.000            00006350
        DO 707  K=1,M          00006360
707      SUM=SUM +A(I,K)*X(K) 00006370
        SUM=SUM/XBAR          00006380
        G(I*N+1) =SUM          00006390
        G(N+1,I) =SUM          00006400
        R(I) = D(I)-SUM*XBAR 00006410
        DO 708  J=1,N          00006420
        SUM= 0.000            00006430
        DO 709  K=1,M          00006440
709      SUM=SUM - A(I,K)*A(J,K)*X(K) 00006450
706      G(I,J)=SUM          00006460
        SUM=-XBAR            00006470
        DO 710  K=1,M          00006480
710      SUM=SUM+X(K)          00006490
        R(N+1) =SUM/XBAR          00006500
        DO 728  I=1,N          00006510
        IF(DABS(R(I)) - TOL6*AVD) 728,728,727 00006520
728      CONTINUE
        GO TO 730              00006530
727      DO 903  I=1,N          00006540
        IF(DABS(XN(I)) -TOL5*D(I)) 903,903,801 00006550
903      CONTINUE
        DO A22  I=1,N          00006560
822      XMU(I)=DD(I)          00006570
        DO A23  J=1,M1          00006580
823      X(J)=CPT(J)          00006590
        GO TO 5079             00006600
801      TOL4=0.100*TOL4          00006610
        NGS6=2                  00006620
        H2=1.000            00006630
        GO TO 99                00006640
730      IPP=NXNSOL(INXNSL,NTOT,G,R) 00006650
        IF(IPP-2)8001,727,8001 00006660
8001  ITER2=ITER2+1          00006670
        DO 465  I=1,N          00006680
        IF(DABS(R(I)) -TOL7) 465,465,727 00006690
465      CONTINUE
        DO 731  I=1,NTOT          00006700
        IF(DABS(R(I)) - TOL5) 731, 731, 739 00006710
731      CONTINUE

```

```

      GO TO 737
733   DO 734 I=1,N
734   XMU(1)= XMU(I)+R(I)
      XBAR =XBAR+ R(N+1)
      GO TO 750
739   CONTINUE
      IF (ITER2- ITMAX) 733,740,740
740 ISENT=5
      GO TO 5000
C
C      TEST IF X(J) NEGATIVE
C
737   DO 470 J=1,N
      IF (X(J)) 801,470,470
470   CONTINUE
C
C      END OF MAIN PROGRAM LOOP
C
5079 SUMNI =0.000
      DO 5010 I = 1, M
      SUMNI = SUMNI + X(I)
5010 CONTINUE
      IF (SUMNI) 751, 752, 751
752 ISENT=6
      GO TO 5000
751 CONTINUE
      DO 5011 I = 1, M
5011 XM0FR(I) = X(I) / SUMNI
C
C      NOTE: ROUTINE TO CHECK FOR A SINGULAR DERIVATIVE MATRIX
C      IN RTP & RPP ARRAYS HAS BEEN REMOVED.
C
C      ADDITIONAL CALCULATIONS REQUIRED BY HPCHEM:
C
      NP11 = N + 1
      DO 6000 I= 1,N
      DO 6000 J= 1,N
      G(I,J) = 0.000
      DO 6000 K= 1,M
      G(I,J) = G(I,J) - A(I,K)*A(J,K)* X(K)
6000 CONTINUE
      DO 6001 I = 1,N
      G(I, NP11) = 0.000
      G(NP11, I) = 0.000
      DO 6002 K = 1,M
      G(I, NP11) = G(I, NP11) + A(I,K)* X(K)
      G(NP11, I) = G(NP11, I) + A(I,K)* X(K)
6002 CONTINUE
      G(I, NP11) = G(I, NP11) / XBAR
      G(NP11, I) = G(NP11, I) / XBAR
6001 CONTINUE
      G(NP11, NP11) = 0.0
      XBAR = SUMNI
      XHPRIM = 0.0
      HORTSM = 0.0
      DO 6010 I = 1,N
      RTP(I) = 0.0
6010 CONTINUE
      DO 6030 K = 1,M
      XHPRIM = XHPRIM + X(K) * ((7L(K,4)*TK + 7L(K,3))*TK + 7L(K,2))
6030

```

```

1 * TK + ZL(K,1) + ZL(K,5)/(TK*TK) 1 00007360
XHORT(K) = X(K) * HORT(K) 00007370
HORTSM = HORTSM + XHORT(K) 00007380
DO 6020 I = 1,N 00007390
RTP(I) = RTP(I) - A(T,K) * XHORT(K) 00007400
6020 CONTINUE 00007410
6030 CONTINUE 00007420
RTP(NP11) = HORTSM / YB42 00007430
NPL = N + L 00007440
DO 6040 I = 1,NPL 00007450
RTP(I) = RTP(I) / TMP 00007460
6040 CONTINUE 00007470
TPP = NXNSOL(INXVSL,NPL,S,RTP) 00007510
CSURP = 0.0 00007540
DO 6060 K = 1,M 00007550
RTPA = 0.0 00007560
DO 6050 I = 1,N 00007570
RTPA = RTPA + RTP(I) * A(I,K) 00007580
6050 CONTINUE 00007590
CSURP = CSURP + (HORT(K)/TMP - RTPA)*XHORT(K) 00007600
6060 CONTINUE 00007610
SMDHDT = XHPRIM + AR*TMP*(CSURP + RTP(NP11)*HORTSM/SUMNI) 00007620
C 00007630
RETURN 00007640
C 00007650
C ERROR: SET MOLE FRACTIONS TO 0. 00007660
C 00007670
5000 DO 5100 I = 1, ITOTSP 00007680
5100 XMOPR(I) = 0. 00007690
RETURN 00007700
END 00007710

```

```

FUNCTION NXNSOL(IM,IN,A,B)          00007720
CNXNSOL                               00007730
  IMPLICIT REAL*8(A-H,O-Z)
  DIMENSION A(2),B(2)
  INTEGER XROW
  XROW(K000FX,K001FX)=K001FX*M-M*K000FX
  M=IM
  N=IN
  NI=N-1
  DO 44 J=1,NI
    K=J
    J1=J+1
    JJ=XROW(J,J)
    WS1=DARS(A(JJ))
C   LOOP TO FIND LARGEST           00007740
  DO 11 L=J1,N
    LJ=XROW(L,J)
    WWS1=DARS(A(LJ))
    IF (WS1-WWS1) 12,11,11
  12 WS1=WWS1
    K=L
    11 CONTINUE
    IF (J-K) 13,31,31
C   $ IF DIAG NOT LARGEST INTERCHANGE ROWS 00007750
  13 DO 26 L=1,N
    JL=XROW(J,L)
    KL=XROW(K,L)
    WS1=A(JL)
    A(JL)=A(KL)
  26 A(KL)=WS1
    WS1=B(J)
    B(J)=B(K)
    B(K)=WS1
  31 DO 33 L=J1,N
    JL=XROW(J,L)
    IF (A(JL)) 33,54,33
  33 A(JL)=A(JL)/A(JJ)
    R(J)=R(J)/A(JJ)
    DO 43 L=1,N
      IF (L-J) 37,43,37
  37 LJ=XROW(L,J)
  38 DO 41 L2=J1,N
    LL2=XROW(L,L2)
    JL2=XROW(J,L2)
    A(LL2)=A(LL2)-A(LJ)*A(JL2)
    R(L)=R(L)-A(LJ)*R(J)
  43 CONTINUE
  44 CONTINUE
C   LAST COLUMN HAS NOT BEEN DONE YET 00007760
  NN=XROW(N,N)
  IF (A(NN)) 45,54,46
  45 R(N)=B(N)/A(NN)
  DO 50 L=1,N
    LN=XROW(L,N)
  50 R(L)=B(L)-A(LN)*R(N)
  NXNSOL=1
  RETURN
  54 NXNSOL=2
  RETURN
  END

```

-----C20049.DAT RHN #28 JUL. 28 '77-----  
 9.842 9.842 16.8275 12.7 57.29 2.46 1.  
 -20. 480. 200. 14. 330. 355.  
 16.5 9.0 14.45 10020. 64.4  
 0.0196 2000. 0.  
 650. 500. 700. 500. 650.  
 2.28 0.0032 1.6  
 34. 15. ? 0.02227  
 3.65 0.08 0.75 0.80 0.012 0.0000065  
 0.1 0.22 200. 50.  
 4.57 1.625 2.95 1.625 1.  
 7. 1. 3.  
 18  
 0  
 0. 0.058 0.096 0.135 0.173 0.211 0.25 0.288  
 0.308 0.692 0.712 0.75 0.789 0.827 0.865 0.904  
 0.942 1.0  
 0. 0.029 0.096 0.304 0.544 0.755 0.911 0.991  
 1.0 1.0 0.991 0.911 0.755 0.544 0.304 0.096  
 0.029 0.0  
 0.0 0.05 0.1 0.15 0.2 0.25 0.3 0.35  
 0.4  
 0.0 0.08 0.135 0.19 0.25 0.3 0.35 0.41  
 0.47  
 18  
 10  
 0. 0.058 0.096 0.135 0.173 0.211 0.25 0.288  
 0.308 0.692 0.712 0.75 0.789 0.827 0.865 0.904  
 0.942 1.0  
 0. 0.029 0.096 0.304 0.544 0.755 0.911 0.991  
 1.0 1.0 0.991 0.911 0.755 0.544 0.304 0.096  
 0.029 0.0  
 0.0 0.05 0.1 0.15 0.2 0.25 0.3 0.35  
 0.4 0.46  
 0.0 0.15 0.25 0.35 0.44 0.52 0.57 0.61  
 0.63 0.65  
 8  
 310. 1.  
 0.960 1.035 310.  
 2. 2. ? ? ?  
 1. 1. 1. 1.  
 1.27 640. 0.5 540.  
 0.420.  
 -10. 710.  
 1

\*\*CYCLE SIMULATION FOR DIRECT INJECTION ENGINE\*\* VERSION 1\*\*\*  
 ----C20058.DAT RUN #37 JUN. 28 '77-----

TABLE OF INPUT DATA AND INITIAL ENGINE CONDITIONS

INITIAL JET SPEED

VINIT= 9530.0CM/SEC

ENGINE GEOMETRY	*	TIMING	*	FUEL PROPERTIES	*	ESTIMATE TEMPERATURES
STROKE	= 9.842CM	* INT.VAL.OPEN = -20.0DEG	* ZMINO. OF HJ	= 16.5	* PISTON TCR(TP) =	650.0K
CCV.RCD	= 16.83CM	* EXH.VAL.OPEN = 480.0DEG	* ZNIND. OF C)	= 9.0	* CYL.WALL(TH)	= 600.0K
BCRE	= 9.842CM	* INT.VAL.CLOSE = 200.0DEG	* SAFC(STGICH,A/F)=	14.4	* CYL.HEAD(TCYLH)=	650.0K
CLEAR.VOL.	= 12.70CM**3	* EXH.VAL.CLOSE = 14.0DEG	* LOWER HEATING	= 10020. CAL/G*	INT.VALVE(TINV)=	500.0K
CLP VCL.	= 57.25CM**3	* FUEL INJ.START= 330.0DEG	* VAPORIZING HEAT	= 64. CAL/G*	EXH.VALVE(TEXV)=	700.0K
		* FUEL INJ.END = 360.0DEG	* DENSITY	= 0.8000G/CM**3*		

INITIAL JET DATA

INITIAL JET DATA		JET MIXING PARAMETER	*	PLUME MODEL
JET DIRECTION**		* SWIRL RATIO AT BDC	= 3.650*RPM	* INITIAL PLUME RADIUS = 0.1000 CM *
ANGLE(VERTICAL)	= 34.00 DEG	* AIR ENTRAIN. PARAMETER		* ENTRAIN. PARAMETER = 0.220 *
ANGLE(TANGENTIAL)	= 15.00 DEG	* ALPHA	= 0.070	* LAM. FLAME SPEED = 200.00 CM/SEC *
JET RADIUS	= 0.02227 CM	* BETA	= 0.350	* SPARK PLUG LOCATION = 50.00 DEG *
JET LOCATION(R)	= 2.000 CM	* DENSITY OF SURROUD. GAS	= 0.01200 G/CC *	(FROM INJ. NOZZLE)
PISTON CUP RADIUS	= 2.460 CM	* SWIRL DECAY FACTOR	= 0.650E-05	* TAYLOR MICRO SCALE = 0.0236 CM

ENGINE CONDITION

ENGINE SPEED	*	INTAKE CONDITIONS	*	COMPUTING INTERVALS	*	PRINT CONTROL
ENGINE SPEED	= 2000. RPM	* PRESSURE	= 0.960 ATA	* VALVE OVERLAP	= 2.00 DEG	* VALVE OVERLAP= 1.00
FUEL AMOUNT	= 0.02970 G/SHOT*	TEMPERATURE	= 310.00 K	* INTAKE	= 2.00 DEG	* INTAKE = 1.00
EGR	= 0.0	* EQUI. RATIO	= 0.0	* COMPRESSION	= 2.00 DEG	* COMPRESSION = 1.00
AMBIENT CONDITIONS		* EXHAUST CONDITIONS(ASSUME)		* COMBUSTION	= 3.75 DEG	* COMBUSTION = 1.00
PRESSURE	= 1.00 ATA	* PRESSURE	= 1.03 ATA	* EXPANSION	= 2.00 DEG	* EXPANSION = 1.00
TEMPERATURE	= 310.00 K	* TEMPERATURE	= 786.00 K	* EXHAUST	= 2.00 DEG	* EXHAUST = 1.00
		* EQUI. RATIO	= 0.500			

INTAKE VALVE

DIAMETER	*	HEAT TRANS. AREA	*	HEAT TRANS. COEFF	*	INITIAL CONDITION
DIAMETER	= 4.570 CM	* INTAKE VALVE = 16.403 CM**2*		[WCSCHNI'S EQ.]	* CYL. PRESS. =	1.27 ATA
LIFT	= 1.625 CM	* EXHAUST VALVE= 6.835 CM**2*	COHT	= 1.60000	* CYL. TEMP. =	786.0 DEG
NUMBER	= 1.0	* PISTON TOP = 57.066 CM**2*	COHT1	= 2.28000	* CYL. EQUI. =	0.500
EXHAUST VALVE		* PISTON TOP = 46.576 CM**2*	COHT2	= 0.00320	* EXHAUST TEMP.=	786.0 DEG *
DIAMETER	= 2.950 CM	* CYL. HEAD = 52.840 CM**2*				
LIFT	= 1.625 CM	* CYL. WALL = VARIABLE*				
NUMBER	= 1.0					

FRICITION LOSS

PISTON SKIRT	*
PISTON SKIRT	= 7.000 CM *
JCU. BEAR. COE	= 1.000 *
NO. OF RINGS	= 3.0 *

INTAKE VALVE--EFFECTIVE FLOW AREA VS. CRANK ANGLE

NORMALIZED CRANK ANGLE

0.0	0.058	0.096	0.135	0.173	0.211	0.250	0.288	0.308	0.692
-----	-------	-------	-------	-------	-------	-------	-------	-------	-------

0.712	0.750	0.789	0.827	0.865	0.904	0.942	1.000		
-------	-------	-------	-------	-------	-------	-------	-------	--	--

NORMALIZED EFFECTIVE FLOW AREA

0.0	0.000	0.005	0.044	0.132	0.240	0.345	0.409	0.417	0.417
-----	-------	-------	-------	-------	-------	-------	-------	-------	-------

0.409	0.345	0.240	0.132	0.044	0.005	0.000	0.0		
-------	-------	-------	-------	-------	-------	-------	-----	--	--

EXHAUST VALVE--EFFECTIVE FLOW AREA VS. CRANK ANGLE

NORMALIZED CRANK ANGLE

0.0	0.058	0.096	0.135	0.173	0.211	0.250	0.288	0.308	0.692
-----	-------	-------	-------	-------	-------	-------	-------	-------	-------

0.712	0.750	0.789	0.827	0.865	0.904	0.942	1.000		
-------	-------	-------	-------	-------	-------	-------	-------	--	--

NORMALIZED EFFECTIVE FLOW AREA

0.0	0.001	0.015	0.116	0.310	0.480	0.592	0.644	0.650	0.650
-----	-------	-------	-------	-------	-------	-------	-------	-------	-------

0.644	0.592	0.480	0.310	0.116	0.015	0.001	0.0		
-------	-------	-------	-------	-------	-------	-------	-----	--	--

## INTAKE AND EXHAUST VALVE OPEN

CUTPUT DATA											
THED DEG	P ATA	T K	V CM**3	WCRK PS	CYL.MAS KG	HEAT TRANSFER CAL/A CAL	AEFI CM**2	GWI G/S	AEFE CM**2	GWE G/S	
-8.0	1.31	792.	75.	-0.00	0.043	-0.862E-02 -0.345E-01	0.01	-0.16	0.17	-2.99	
-6.0	1.33	792.	73.	-0.00	0.043	-0.887E-02 -0.700E-01	0.03	-0.28	0.13	-2.47	
-4.0	1.35	793.	71.	-0.00	0.043	-0.901E-02 -0.106E+00	0.05	-0.73	0.09	-1.85	
-2.0	1.35	791.	70.	-0.00	0.042	-0.901E-02 -0.142E+00	0.08	-1.22	0.05	-1.17	
0.0	1.34	788.	70.	-0.01	0.042	-0.886E-02 -0.177E+00	0.11	-1.69	0.02	-0.49	
2.0	1.31	783.	70.	-0.00	0.041	-0.854E-02 -0.212E+00	0.21	-2.35	0.02	-0.30	
4.0	1.25	773.	71.	-0.00	0.040	-0.793E-02 -0.243E+00	0.42	-5.27	0.01	-0.24	
6.0	1.16	758.	73.	-0.00	0.039	-0.698E-02 -0.271E+00	0.63	-7.71	0.01	-0.16	
8.0	1.06	741.	75.	-0.00	0.038	-0.583E-02 -0.295E+00	0.84	-8.55	0.01	-0.09	
10.0	0.98	725.	77.	-0.00	0.037	-0.471E-02 -0.313E+00	1.09	-6.60	0.01	0.02	
12.0	0.95	721.	81.	-0.00	0.037	-0.397E-02 -0.329E+00	1.59	3.43	0.00	0.04	
14.0	0.95	724.	84.	-0.00	0.039	-0.407E-02 -0.346E+00	2.08	10.18	0.0	0.01	

## INTAKE VALVE OPEN

CUTPUT DATA		P	T	V	WORK	CYL.MAS	HEAT TRANSFER	AETI	GWI
THED	DEG	ATA	K	CM**3	PS	G	CAL/A CAL	CM**2	G/S
16.0	0.95	726.	89.	-0.00	0.041	-0.426E-02	-0.363E+00	2.57	11.68
18.0	0.95	727.	94.	-0.00	0.043	-0.445E-02	-0.381E+00	3.06	13.06
20.0	0.93	692.	99.	-0.01	0.047	-0.376E-02	-0.396E+00	3.66	22.59
22.0	0.92	657.	105.	-0.01	0.052	-0.190E-02	-0.403E+00	4.27	33.03
24.0	0.92	616.	111.	-0.01	0.059	0.416E-04	-0.403E+00	4.88	39.28
26.0	0.92	583.	118.	-0.01	0.066	0.195E-02	-0.395E+00	5.48	43.92
28.0	0.93	555.	126.	-0.01	0.074	0.378E-02	-0.380E+00	6.06	47.65
30.0	0.93	530.	134.	-0.01	0.083	0.551E-02	-0.358E+00	6.63	50.90
32.0	0.93	509.	142.	-0.01	0.092	0.716E-02	-0.329E+00	7.20	54.04
34.0	0.93	491.	151.	-0.01	0.101	0.871E-02	-0.295E+00	7.76	57.05
36.0	0.93	475.	161.	-0.02	0.111	0.102E-01	-0.264E+00	8.23	59.45
38.0	0.93	462.	170.	-0.02	0.121	0.115E-01	-0.208E+00	8.59	61.29
40.0	0.93	450.	180.	-0.02	0.132	0.128E-01	-0.156E+00	8.94	63.59
42.0	0.93	440.	191.	-0.02	0.143	0.141E-01	-0.100E+00	9.30	65.94
44.0	0.93	431.	202.	-0.02	0.154	0.153E-01	-0.190E-01	9.57	68.11
46.0	0.93	423.	213.	-0.02	0.166	0.164E-01	0.265E-01	9.65	69.36
48.0	0.93	415.	224.	-0.02	0.178	0.175E-01	0.956E-01	9.72	70.87
50.0	0.93	407.	236.	-0.03	0.190	0.186E-01	0.171E+00	9.72	72.26
52.0	0.93	403.	248.	-0.03	0.202	0.196E-01	0.249E+00	9.72	73.41
54.0	0.93	399.	261.	-0.03	0.214	0.206E-01	0.131E+00	9.72	74.95
56.0	0.93	393.	273.	-0.03	0.227	0.215E-01	0.41PE+00	9.72	76.21
58.0	0.93	385.	285.	-0.03	0.240	0.225E-01	0.508E+00	9.72	77.35
60.0	0.93	385.	299.	-0.04	0.253	0.234E-01	0.601E+00	9.72	78.39
62.0	0.93	382.	312.	-0.04	0.266	0.243E-01	0.699E+00	9.72	79.30
64.0	0.92	379.	325.	-0.04	0.280	0.252E-01	0.800E+00	9.72	80.10
66.0	0.92	376.	339.	-0.04	0.293	0.261E-01	0.904E+00	9.72	80.79
68.0	0.92	374.	352.	-0.05	0.307	0.270E-01	0.101E+01	9.72	81.36
70.0	0.92	371.	366.	-0.05	0.320	0.278E-01	0.112E+01	9.72	81.82
72.0	0.92	369.	379.	-0.05	0.334	0.287E-01	0.124E+01	9.72	82.16
74.0	0.92	367.	393.	-0.05	0.348	0.295E-01	0.136E+01	9.72	82.40
76.0	0.92	365.	406.	-0.05	0.361	0.303E-01	0.148E+01	9.72	82.53
78.0	0.92	364.	420.	-0.06	0.375	0.311E-01	0.160E+01	9.72	82.55
80.0	0.92	362.	434.	-0.06	0.389	0.319E-01	0.173E+01	9.72	82.46
82.0	0.92	361.	447.	-0.06	0.403	0.327E-01	0.186E+01	9.72	82.27
84.0	0.92	360.	461.	-0.06	0.416	0.335E-01	0.199E+01	9.72	81.98
86.0	0.92	359.	474.	-0.07	0.430	0.343E-01	0.213E+01	9.72	81.59
88.0	0.92	354.	487.	-0.07	0.443	0.350E-01	0.227E+01	9.72	81.10
90.0	0.93	357.	500.	-0.07	0.457	0.357E-01	0.242E+01	9.72	80.50
92.0	0.93	354.	513.	-0.07	0.470	0.365E-01	0.255E+01	9.72	79.82
94.0	0.93	355.	526.	-0.08	0.483	0.372E-01	0.271E+01	9.72	79.03
96.0	0.93	353.	539.	-0.08	0.496	0.379E-01	0.286E+01	9.72	78.15
98.0	0.93	354.	551.	-0.08	0.509	0.385E-01	0.302E+01	9.72	77.18
100.0	0.93	353.	564.	-0.08	0.522	0.392E-01	0.317E+01	9.72	76.12
102.0	0.93	352.	576.	-0.08	0.534	0.399E-01	0.333E+01	9.72	74.97
104.0	0.93	352.	588.	-0.09	0.547	0.405E-01	0.349E+01	9.72	73.73
106.0	0.93	352.	599.	-0.09	0.559	0.411E-01	0.366E+01	9.72	72.40
108.0	0.93	352.	611.	-0.09	0.571	0.417E-01	0.382E+01	9.72	71.00
110.0	0.94	352.	622.	-0.09	0.582	0.424E-01	0.399E+01	9.72	69.51
112.0	0.94	351.	633.	-0.09	0.593	0.429E-01	0.417E+01	9.72	67.05
114.0	0.94	351.	643.	-0.09	0.604	0.434E-01	0.444E+01	9.72	66.31
116.0	0.94	351.	653.	-0.09	0.615	0.439E-01	0.451E+01	9.72	64.60
118.0	0.94	351.	664.	-0.10	0.626	0.444E-01	0.469E+01	9.72	62.82
120.0	0.94	351.	673.	-0.10	0.636	0.449E-01	0.487E+01	9.72	60.98
122.0	0.94	351.	683.	-0.10	0.646	0.454E-01	0.505E+01	9.72	59.07
124.0	0.94	351.	692.	-0.10	0.655	0.459E-01	0.524E+01	9.72	57.11
126.0	0.95	351.	701.	-0.10	0.664	0.463E-01	0.542E+01	9.72	55.10
128.0	0.95	351.	709.	-0.10	0.673	0.467E-01	0.561E+01	9.72	53.03

130.0	0.95	351.	718.	-0.10	C.682	0.471E-01	0.580E+01	9.72	50.91
132.0	0.95	351.	725.	-0.10	C.690	0.475E-01	0.599E+01	9.72	48.76
134.0	0.95	351.	733.	-0.10	C.698	0.478E-01	0.614E+01	9.65	46.43
136.0	0.95	352.	740.	-0.10	C.705	0.481E-01	0.631E+01	9.57	43.59
138.0	0.95	352.	747.	-0.11	C.712	0.484E-01	0.651E+01	9.30	41.40
140.0	0.95	352.	754.	-0.11	C.718	0.487E-01	0.676E+01	8.94	38.40
142.0	0.95	352.	760.	-0.11	C.724	0.490E-01	0.696E+01	8.59	35.78
144.0	0.95	352.	766.	-0.11	C.730	0.492E-01	0.715E+01	8.23	33.40
146.0	0.95	353.	772.	-0.11	C.735	0.494E-01	0.735E+01	7.76	31.09
148.0	0.95	353.	777.	-0.11	C.740	0.494E-01	0.755E+01	7.20	28.37
150.0	0.95	353.	782.	-0.11	C.744	0.498E-01	0.775E+01	6.63	25.68
152.0	0.95	353.	787.	-0.11	C.748	0.499E-01	0.795E+01	6.06	23.54
154.0	0.95	354.	791.	-0.11	C.751	0.500E-01	0.815E+01	5.48	21.28
156.0	0.95	354.	795.	-0.11	C.755	0.501E-01	0.835E+01	4.88	18.99
158.0	0.95	354.	799.	-0.11	C.757	0.502E-01	0.855E+01	4.27	16.72
160.0	0.95	355.	803.	-0.11	C.760	0.502E-01	0.875E+01	3.65	14.48
162.0	0.95	355.	806.	-0.11	C.762	0.503E-01	0.895E+01	3.06	12.26
164.0	0.95	356.	808.	-0.11	C.764	0.503E-01	0.915E+01	2.57	10.26
166.0	0.95	356.	811.	-0.11	C.765	0.503E-01	0.935E+01	2.08	8.42
158.0	0.95	357.	813.	-0.11	C.766	0.502E-01	0.955E+01	1.59	6.56
170.0	0.95	357.	815.	-0.11	C.767	0.502E-01	0.975E+01	1.09	4.72
172.0	0.95	358.	816.	-0.11	C.767	0.501E-01	0.995E+01	0.84	3.27
174.0	0.96	359.	817.	-0.11	C.768	0.501E-01	0.102E+02	0.63	2.40
176.0	0.96	359.	818.	-0.11	C.768	0.500E-01	0.104E+02	0.42	1.56
178.0	0.96	359.	819.	-0.11	C.768	0.499E-01	0.106E+02	0.21	0.80
180.0	0.96	360.	819.	-0.11	C.768	0.498E-01	0.108E+02	0.11	0.23
182.0	0.96	361.	819.	-0.11	C.768	0.497E-01	0.110E+02	0.08	-0.08
184.0	0.95	362.	819.	-0.11	C.768	0.495E-01	0.112E+02	0.05	-0.16
186.0	0.97	363.	817.	-0.11	C.768	0.494E-01	0.113E+02	0.03	-0.14
188.0	0.97	363.	816.	-0.11	C.768	0.493E-01	0.115E+02	0.01	-0.07
190.0	0.98	364.	815.	-0.11	C.768	0.491E-01	0.117E+02	0.01	-0.05
192.0	0.99	365.	813.	-0.11	C.768	0.490E-01	0.119E+02	0.01	-0.05
194.0	0.99	367.	811.	-0.11	C.768	0.488E-01	0.121E+02	0.01	-0.04
196.0	0.99	368.	808.	-0.11	C.768	0.487E-01	0.123E+02	0.00	-0.03
198.0	1.00	369.	806.	-0.11	C.768	0.485E-01	0.125E+02	0.00	-0.02
200.0	1.01	370.	803.	-0.11	C.768	0.483E-01	0.127E+02	0.0	-0.01

OVERALL EQUIVALENCE RATIO = 0.590  
 VOLUMETRIC EFFICIENCY= 0.855  
 CORRECT CHARGED AIR PHI = 0.031  
 INDUCED AIR AND REG. GAS NOX  
 PPM = 52.4 MASS = 0.418E-04G

## COMPRESSION

OUTPUT DATA		P	T	V	WCHK	CYL.MAS	HEAT TRANSFER	FSWR	S.RT	#RPM
THED	DFG	ATA	K	CM**#3	PS	G	CAL/A CAL			
202.0	1.01	371.	799.	-0.11	0.768	0.482E-01	0.129E+02	0.999	3.65	
204.0	1.02	373.	795.	-0.11	0.768	0.480E-01	0.131E+02	0.999	3.65	
206.0	1.03	374.	791.	-0.11	0.768	0.478E-01	0.133E+02	0.998	3.65	
208.0	1.04	375.	787.	-0.11	0.768	0.476E-01	0.135E+02	0.997	3.65	
210.0	1.05	377.	792.	-0.11	0.768	0.473E-01	0.137E+02	0.997	3.65	
212.0	1.06	379.	777.	-0.11	0.768	0.471E-01	0.139E+02	0.996	3.65	
214.0	1.07	380.	772.	-0.12	0.768	0.469E-01	0.140E+02	0.996	3.65	
216.0	1.09	382.	766.	-0.12	0.768	0.466E-01	0.142E+02	0.995	3.65	
218.0	1.10	384.	760.	-0.12	0.768	0.464E-01	0.144E+02	0.994	3.65	
220.0	1.12	386.	754.	-0.12	0.768	0.461E-01	0.146E+02	0.994	3.64	
222.0	1.13	388.	747.	-0.12	0.768	0.459E-01	0.148E+02	0.993	3.64	
224.0	1.15	390.	740.	-0.12	0.768	0.456E-01	0.150E+02	0.992	3.64	
226.0	1.17	392.	733.	-0.13	0.768	0.453E-01	0.151E+02	0.992	3.64	
228.0	1.19	394.	725.	-0.13	0.768	0.450E-01	0.153E+02	0.991	3.64	
230.0	1.20	396.	718.	-0.13	0.768	0.447E-01	0.155E+02	0.991	3.64	
232.0	1.23	399.	709.	-0.14	0.768	0.444E-01	0.157E+02	0.990	3.64	
234.0	1.25	401.	701.	-0.14	0.768	0.440E-01	0.159E+02	0.989	3.64	
236.0	1.27	404.	692.	-0.15	0.768	0.437E-01	0.160E+02	0.986	3.64	
238.0	1.30	406.	683.	-0.15	0.768	0.433E-01	0.162E+02	0.988	3.65	
240.0	1.31	409.	673.	-0.16	0.768	0.430E-01	0.164E+02	0.987	3.65	
242.0	1.35	412.	664.	-0.17	0.768	0.426E-01	0.166E+02	0.987	3.65	
244.0	1.38	415.	653.	-0.17	0.768	0.422E-01	0.167E+02	0.986	3.65	
246.0	1.42	418.	643.	-0.18	0.768	0.419E-01	0.169E+02	0.985	3.65	
248.0	1.45	421.	623.	-0.19	0.768	0.414E-01	0.171E+02	0.985	3.65	
250.0	1.49	424.	622.	-0.20	0.758	0.409E-01	0.172E+02	0.994	3.65	
252.0	1.53	426.	611.	-0.22	0.768	0.404E-01	0.174E+02	0.984	3.66	
254.0	1.57	431.	599.	-0.23	0.768	0.397E-01	0.175E+02	0.983	3.66	
256.0	1.62	435.	598.	-0.24	0.768	0.394E-01	0.177E+02	0.982	3.66	
258.0	1.66	434.	576.	-0.26	0.768	0.388E-01	0.179E+02	0.982	3.67	
260.0	1.71	442.	554.	-0.28	0.768	0.383E-01	0.180E+02	0.981	3.67	
262.0	1.77	447.	551.	-0.30	0.768	0.377E-01	0.182E+02	0.980	3.67	
264.0	1.83	451.	539.	-0.32	0.768	0.370E-01	0.183E+02	0.980	3.68	
266.0	1.99	456.	526.	-0.35	0.768	0.364E-01	0.184E+02	0.979	3.68	
268.0	1.96	461.	513.	-0.37	0.768	0.357E-01	0.196E+02	0.978	3.69	
270.0	2.03	466.	500.	-0.40	0.768	0.350E-01	0.187E+02	0.978	3.69	
272.0	2.11	471.	497.	-0.43	0.768	0.342E-01	0.199E+02	0.977	3.70	
274.0	2.12	476.	474.	-0.47	0.768	0.334E-01	0.190E+02	0.976	3.71	
275.0	2.29	481.	461.	-0.50	0.768	0.325E-01	0.191E+02	0.976	3.71	
278.0	2.34	487.	447.	-0.54	0.768	0.316E-01	0.193E+02	0.975	3.72	
280.0	2.43	493.	434.	-0.59	0.768	0.307E-01	0.194E+02	0.975	3.73	
282.0	2.57	497.	420.	-0.63	0.768	0.297E-01	0.195E+02	0.974	3.74	
284.0	2.71	506.	406.	-0.68	0.748	0.286E-01	0.196E+02	0.973	3.75	
286.0	2.85	512.	393.	-0.74	0.768	0.274E-01	0.197E+02	0.973	3.76	
288.0	2.90	522.	370.	-0.80	0.768	0.261E-01	0.198E+02	0.972	3.78	
290.0	3.14	527.	346.	-0.86	0.768	0.249E-01	0.199E+02	0.971	3.79	
292.0	3.31	534.	352.	-0.92	0.768	0.234E-01	0.200E+02	0.970	3.81	
294.0	3.49	542.	339.	-1.00	0.768	0.218E-01	0.201E+02	0.970	3.82	
296.0	3.61	551.	326.	-1.07	0.758	0.202E-01	0.202E+02	0.969	3.84	
298.0	3.91	559.	312.	-1.16	0.768	0.184E-01	0.203E+02	0.968	3.86	
300.0	4.15	562.	299.	-1.24	0.768	0.165E-01	0.203E+02	0.968	3.88	
302.0	4.42	571.	286.	-1.34	0.768	0.144E-01	0.204E+02	0.967	3.91	
304.0	4.49	597.	273.	-1.44	0.768	0.122E-01	0.204E+02	0.966	3.94	
306.0	5.00	597.	241.	-1.55	0.768	0.073E-02	0.205E+02	0.965	3.97	
308.0	5.34	607.	246.	-1.55	0.768	0.706E-02	0.205E+02	0.965	4.00	
310.0	5.71	613.	236.	-1.73	0.768	0.414E-02	0.205E+02	0.964	4.03	
312.0	6.12	629.	224.	-1.71	0.768	0.945E-03	0.205E+02	0.963	4.07	
314.0	6.57	641.	213.	-2.05	0.768	-0.257E-02	0.205E+02	0.962	4.12	
316.0	7.06	653.	202.	-2.19	0.768	-0.644E-02	0.205E+02	0.961	4.17	

318.0	7.60	665.	191.	-2.34	0.768	-0.107E-01	0.204E+02	0.961	4.23
320.0	8.23	678.	180.	-2.51	0.768	-0.154E-01	0.204E+02	0.960	4.29
322.0	8.86	691.	170.	-2.57	0.768	-0.207E-01	0.203E+02	0.959	4.36
324.0	9.58	705.	161.	-2.85	0.768	-0.264E-01	0.202E+02	0.958	4.44
326.0	10.37	719.	151.	-3.04	0.768	-0.329E-01	0.201E+02	0.957	4.52
328.0	11.24	733.	142.	-3.23	0.768	-0.400E-01	0.199E+02	0.956	4.62
330.0	12.19	748.	134.	-3.43	0.768	-0.479E-01	0.197E+02	0.955	4.74

## COMBUSTION AND EXPANSION

## OUTPUT DATA

VAL *	THER	PRESS	PS	FSWIR	S.RT	PPM	WNO	PPM	PPM	WNO	JET LOCATIONS	RJET C.ANG	H.T.
	K	K	K	MG	PPAS	UMAS	V	EQUI	CP	ENTH	G*10**6 R(CM)	DEG	CM
				MG	MG	MG	CM**3	CAL/G	CAL/G		Z(CM)		CAL
333.7	PRESS.=	14.27	PS= -3.8	FSWIR= 0.953	S.RT= 5.146	SUM.H.REJ=0.192E+02							
TOTAL		C.0				119.35	C.59				52.	42.	
1 1	777.			758.6		117.31	C.03	0.267	193.8		52.	41.	-0.62E-01
2 1	777.	777.	C.0	13.2	0.0	0.0	2.03	5.69	0.432	193.8	48.	0.52	-0.23E+00
337.5	PRESS.=	16.61	PS= -4.2	FSWIR= 0.950	S.RT= 5.506	SUM.H.REJ=0.186E+02							
TOTAL		-0.032				106.53	C.57				52.	42.	-0.83E-01
1 1	805.			742.1		102.19	C.03	0.268	201.4		52.	40.	-0.31E+00
2 2	737.	-192.	-0.012	20.1	1.8	1.5	2.51	3.32	0.349	178.5	31.	0.89	137.-0.13E-02
3 1	805.	805.	C.0	13.4	0.0	0.0	1.81	5.59	0.433	201.4	48.	0.53	33. 0.463 0. 0.0
341.2	PRESS.=	19.31	PS= -4.7	FSWIR= 0.948	S.RT= 5.953	SUM.H.REJ=0.178E+02							
TOTAL		C.001				95.52	C.59				51.	42.	-0.11E+00
1 1	834.			717.9		88.01	C.03	0.269	209.1		52.	39.	-0.40E+00
2 2	903.	1214.	C.019	27.0	6.3	5.7	3.56	2.34	0.337	235.7	37.	1.27	170.-0.34E-02
3 2	770.	-88.	-0.012	20.7	1.8	1.5	2.30	3.20	0.349	187.7	31.	0.92	2.2 1.77 57. 0.790 138.-0.20E-02
4 1	834.	834.	C.0	13.7	0.0	0.0	1.64	5.40	0.433	209.1	48.	0.55	34. 0.467 0. 0.0
345.0	PRESS.=	22.66	PS= -5.1	FSWIR= 0.945	S.RT= 6.491	SUM.H.REJ=0.167E+02							
TOTAL		C.017				86.42	C.59				50.	42.	-0.14E+00
1 1	865.			685.3		74.25	6.03	0.271	217.3		52.	37.	-0.52E+00
2 2	1245.	1830.	C.123	34.2	14.7	13.7	5.29	1.89	0.347	353.7	41.	1.66	2.4 2.57 92. 1.367 177.-0.99E-02
3 2	950.	1314.	C.024	27.9	6.6	6.0	3.26	2.25	0.337	247.9	37.	1.32	2.4 2.22 76. 1.122 168.-0.49E-02
4 2	827.	61.	-0.011	21.5	1.9	1.6	2.11	3.06	0.348	198.6	32.	0.97	2.2 1.75 58. 0.798 138.-0.30E-02
5 1	865.	865.	C.0	14.2	0.0	0.0	1.49	5.14	0.431	217.3	48.	0.57	2.0 1.14 34. 0.476 0. 0.0
349.7	PRESS.=	27.32	PS= -5.4	FSWIR= 0.941	S.RT= 7.098	SUM.H.REJ=0.153E+02							
TOTAL		C.067				79.27	C.59				50.	42.	-0.20E+00
1 1	901.			643.4		60.27	6.03	0.272	227.3		52.	35.	-0.68E+00
2 2	1452.	2201.	C.374	41.8	29.8	28.0	8.03	1.44	0.351	570.0	44.	2.06	2.3 2.85 111. 1.420 170.-0.23E-01
3 2	1321.	1919.	C.140	39.4	16.0	14.9	4.77	1.73	0.348	378.3	41.	1.72	2.4 2.56 96. 1.314 172.-0.13E-01
4 2	1034.	1437.	C.030	28.9	7.0	6.3	2.94	2.17	0.338	267.3	38.	1.37	2.3 2.19 79. 1.105 166.-0.71E-02
5 2	891.	252.	-0.009	22.4	2.0	1.7	1.91	2.91	0.348	212.1	33.	1.01	2.2 1.72 60. 0.807 138.-0.44E-02
6 1	901.	901.	C.0	14.9	0.0	0.0	1.33	4.85	0.429	227.3	49.	0.51	2.0 1.12 35. 0.487 24.-0.11E-02
352.5	PRESS.=	34.40	PS= -5.8	FSWIR= 0.936	S.RT= 7.694	SUM.H.REJ=0.132E+02							
TOTAL		C.114				74.12	C.59				50.	42.	-0.28E+00
1 1	948.			591.2		46.24	C.03	0.274	240.0		52.	32.	-0.93E+00
2 1	2325.	2325.	C.632	50.3	41.8	41.8	9.58	1.18	0.356	732.8	48.	2.60	2.1 3.06 134. 1.341 148.-0.39E-01
3 3	2158.	2138.	C.441	43.4	35.4	35.2	7.53	1.38	0.354	665.5	44.	2.15	2.2 2.83 117. 1.320 159.-0.32E-01
4 3	1745.	1745.	C.277	36.7	26.9	27.6	5.14	1.66	0.357	528.0	42.	1.79	2.3 2.52 100. 1.250 165.-0.23E-01
5 2	1247.	1512.	C.040	30.0	18.3	15.8	2.98	2.08	0.356	352.8	38.	1.43	2.3 2.14 83. 1.083 162.-0.13E-01
6 2	823.	435.	-0.026	23.3	7.8	6.3	1.51	2.78	0.343	197.5	34.	1.06	2.2 1.67 62. 0.813 138.-0.57E-02
7 1	948.	948.	C.0	15.5	0.0	0.0	1.14	4.58	0.427	240.0	49.	0.64	2.0 1.08 36. 0.500 42.-0.26E-02
356.2	PRESS.=	41.54	PS= -6.0	FSWIR= 0.931	S.RT= 8.140	SUM.H.REJ=0.102E+02							
TOTAL		C.314				71.02	C.59				50.	42.	-0.39E+00
1 1	933.			529.5		35.60	C.03	0.276	249.9		52.	29.	-0.12E+01
2 3	2532.	2532.	C.830	58.9	50.3	50.3	10.11	1.00	0.477	814.2	385.	23.71	1.8 3.24 164. 1.263 120.-0.52E-01
3 3	2403.	2403.	C.674	51.7	43.4	43.4	8.38	1.15	0.365	760.6	56.	3.09	2.0 3.05 144. 1.240 133.-0.49E-01
4 3	2214.	2214.	C.516	44.9	36.7	36.7	6.61	1.34	0.354	696.5	45.	2.22	2.1 2.79 125. 1.230 147.-0.43E-01
5 3	1978.	1978.	C.362	37.3	30.0	30.0	4.93	1.61	0.359	615.4	42.	1.85	2.2 2.46 106. 1.189 158.-0.34F-01
6 3	1471.	1471.	C.148	31.0	23.3	23.1	2.97	2.00	0.361	429.8	39.	1.48	2.3 2.07 87. 1.062 159.-0.20E-01
7 2	999.	691.	-0.014	24.1	P.3	6.7	1.39	2.67	0.345	221.3	34.	1.11	2.2 1.60 65. 0.820 139.-0.92E-02
8 1	921.	953.	C.0	16.1	C.0	0.0	1.01	4.36	0.425	249.8	49.	0.68	2.0 1.04 37. 0.513 55.-0.46E-02



5	3	2399.	2399.	1.000	72.5	71.5	71.5	10.89	0.81	0.376	755.3	1952.	146.97	2.4	3.49	273.	1.950	178.-0.81E-01
6	3	2480.	2480.	0.995	66.9	62.7	62.7	10.32	0.88	0.417	787.4	1246.	86.77	2.5	3.47	249.	1.845	180.-0.80E-01
7	3	2502.	2502.	0.997	59.4	53.9	53.9	9.12	1.00	0.463	798.3	393.	24.38	2.5	3.16	222.	1.699	180.-0.79E-01
8	3	2460.	2460.	0.781	52.4	47.9	47.9	7.85	1.13	0.376	781.5	78.	4.37	2.5	2.80	191.	1.582	180.-0.72E-01
9	3	2385.	2385.	0.667	47.1	42.9	42.9	6.91	1.27	0.358	753.4	48.	2.45	2.5	2.42	162.	1.494	180.-0.66E-01
390.7	PRESS.=	41.27	PS=	-2.9	FSWIR=	0.899	S.RT=	5.402	SUM.H.REJ=-.162E+02									
TOTAL			C.950					101.16	C.59			1270.	1057.					-0.42E+00
1	1	884.		223.8				13.62	C.01	0.272	222.7	52.	12.					-0.53E+00
2	3	2073.	2073.	0.999	94.5	92.9	92.8	13.37	0.62	0.328	656.3	280.	280.59	2.4	4.13	336.	1.285	174.-0.40E-01
3	3	2101.	2101.	0.999	90.7	89.1	89.0	12.87	0.65	0.330	661.1	2691.	253.40	2.3	3.51	323.	2.113	169.-0.39E-01
4	3	2106.	2106.	0.999	82.6	81.5	81.4	12.20	C.71	0.330	692.1	2436.	208.28	2.3	3.53	304.	2.043	173.-0.39E-01
5	3	2153.	2153.	0.999	73.1	72.5	72.4	11.41	0.81	0.368	741.9	1999.	151.73	2.4	3.54	284.	1.950	178.-0.40E-01
6	3	2446.	2446.	0.997	67.5	66.9	66.7	10.85	0.87	0.405	773.5	1392.	97.78	2.5	3.57	260.	1.849	180.-0.39E-01
7	3	2524.	2524.	0.977	61.8	59.4	59.1	10.10	C.96	0.461	808.4	628.	40.47	2.5	3.26	234.	1.739	180.-0.40E-01
8	3	2537.	2537.	0.874	54.7	52.4	52.2	8.92	1.09	0.423	812.2	149.	8.61	2.5	2.90	203.	1.624	180.-0.37E-01
9	3	2487.	2487.	0.758	47.2	47.1	46.8	7.84	1.21	0.371	790.4	60.	3.19	2.5	2.52	174.	1.535	180.-0.35E-01
382.7	PRESS.=	38.64	PS=	-2.4	FSWIR=	0.898	S.RT=	5.174	SUM.H.REJ=-.177F+02									
TOTAL			C.964					107.33	0.59			1304.	1083.					-0.38E+00
1	1	862.		209.5				13.27	0.03	0.271	216.7	52.	11.					-0.47E+00
2	3	2021.	2021.	0.999	95.2	94.5	94.4	14.18	C.61	0.326	439.2	2810.	280.74	2.3	4.20	348.	2.285	173.-0.37E-01
3	3	2052.	2052.	0.999	92.2	90.7	90.6	13.65	0.64	0.328	645.0	2649.	253.58	2.3	3.56	336.	2.113	169.-0.36E-01
4	3	2102.	2102.	0.999	83.7	82.6	82.5	12.72	0.70	0.336	676.4	2410.	209.41	2.3	3.58	316.	2.043	173.-0.36E-01
5	3	2307.	2307.	1.000	74.0	73.1	73.0	12.10	0.80	0.359	725.3	2011.	154.46	2.4	3.59	295.	1.974	179.-0.37E-01
6	3	2374.	2374.	0.599	70.0	67.6	67.5	11.65	C.84	0.380	745.5	1421.	103.29	2.5	3.66	271.	1.888	180.-0.37E-01
7	3	2466.	2466.	0.944	64.1	61.8	61.6	10.74	C.92	0.429	782.6	767.	51.17	2.5	3.36	246.	1.779	180.-0.38E-01
8	3	2525.	2525.	0.918	56.9	54.7	54.6	9.88	1.04	0.456	807.1	247.	14.79	2.5	3.00	215.	1.665	180.-0.36E-01
9	3	2494.	2494.	0.808	51.3	49.2	49.1	8.76	1.16	0.382	723.1	79.	4.33	2.5	2.61	186.	1.576	180.-0.34E-01
384.7	PRESS.=	37.06	PS=	-1.8	FSWIR=	0.896	S.RT=	4.973	SUM.H.REJ=-.191E+02									
TOTAL			C.975					114.01	0.59			1328.	1102.					-0.34E+00
1	1	843.		154.3				12.86	C.03	0.270	210.8	52.	11.					-0.41E+00
2	3	1756.	1756.	0.999	98.2	96.2	96.1	15.98	0.60	0.324	621.4	2755.	280.87	2.3	4.28	359.	2.292	172.-0.34E-01
3	3	1930.	1930.	0.999	93.9	92.2	92.1	14.52	0.53	0.326	627.7	2602.	253.71	2.3	3.61	348.	2.159	171.-0.34E-01
4	3	2107.	2107.	0.999	85.1	83.7	83.6	13.74	0.69	0.333	659.0	2374.	209.70	2.4	3.63	328.	2.084	175.-0.34E-01
5	3	2252.	2252.	0.999	73.3	74.0	73.9	12.88	C.78	0.350	705.5	1993.	155.85	2.5	3.65	306.	2.007	180.-0.34E-01
6	3	2302.	2302.	0.998	72.1	70.0	69.8	12.47	0.82	0.362	718.8	1414.	105.80	2.5	3.74	283.	1.922	180.-0.34E-01
7	3	2405.	2405.	0.599	66.4	64.1	64.0	11.85	C.89	0.401	757.5	833.	57.54	2.5	3.45	258.	1.819	180.-0.35E-01
8	3	2501.	2501.	0.954	59.1	56.9	56.8	10.89	1.00	0.471	795.9	363.	22.43	2.5	3.09	227.	1.705	180.-0.34E-01
9	3	2484.	2484.	0.853	53.4	51.3	51.2	9.74	1.11	0.396	790.6	103.	5.86	2.5	2.70	198.	1.616	180.-0.32E-01
346.7	PRESS.=	33.55	PS=	-1.3	FSWIR=	0.895	S.RT=	4.795	SUM.H.REJ=-.203E+02									
TOTAL			C.983					121.19	0.59			1345.	1115.					-0.31E+00
1	1	818.		177.8				12.31	0.03	0.269	204.8	52.	10.					-0.36E+00
2	3	1908.	1908.	0.999	100.4	98.2	98.1	16.09	0.59	0.322	602.8	2595.	281.00	2.3	4.35	371.	2.337	173.-0.32E-01
3	3	1934.	1934.	0.999	95.3	93.9	93.8	15.51	C.61	0.324	608.0	2540.	253.85	2.4	3.66	360.	2.249	174.-0.32E-01
4	3	2047.	2047.	0.999	87.0	85.1	85.0	14.67	0.68	0.330	639.0	2324.	209.88	2.4	3.66	339.	2.161	178.-0.31E-01
5	3	2193.	2193.	0.999	76.8	75.3	75.3	13.75	C.77	0.343	635.2	1963.	156.53	2.5	3.70	317.	2.030	180.-0.32E-01
6	3	2232.	2232.	0.999	74.2	72.1	72.0	13.37	C.79	0.350	697.8	1389.	106.93	2.5	3.83	294.	1.957	180.-0.31E-01
7	3	2329.	2329.	0.999	68.7	66.4	66.3	12.76	C.86	0.375	728.2	848.	60.54	2.5	3.54	270.	1.858	180.-0.33E-01
8	3	2457.	2459.	0.975	61.3	59.1	59.0	11.93	C.96	0.449	776.4	457.	29.19	2.5	3.18	239.	1.745	180.-0.32E-01
9	3	2476.	2476.	0.895	56.4	53.4	53.3	10.82	1.07	0.418	785.9	136.	7.91	2.5	2.79	210.	1.655	180.-0.31E-01
399.7	PRESS.=	31.17	PS=	-0.7	FSWIR=	0.894	S.RT=	4.637	SUM.H.REJ=-.214E+02									
TOTAL			C.999					128.87	0.59			1357.	1125.					-0.27E+00
1	1	727.		160.3				11.51	C.03	0.268	199.1	52.	9.					-0.31E+00
2	3	1848.	1848.	0.999	103.9	100.4	100.3	17.20	0.57	0.321	583.2	2628.	281.14	2.4	4.42	382.	2.417	176.-0.29E-01
3	3	1871.	1871.	0.999	97.2	96.3	96.1	16.61	0.59	0.322	586.4	2465.	254.02	2.4	3.71	371.	2.380	179.-0.29E-01
4	3	1954.	1954.	0.999	87.2	87.0	86.9	15.69	C.66	0.327	618.4	2268.	210.03	2.5	3.73	349.	2.235	180.-0.28E-01
5	3	2135.	2135.	0.999	78.3	76.8	76.7	14.39	C.75	0.338	665.4	1930.	156.87	2.5	3.75	329.	2.054	180.-0.29E-01
6	3	2163.	2143.	0.999	76.2	74.2	74.1	14.34	C.77	0.341	669.9	1358.	107.44	2.5	3.90	305.	1.991	180.-0.29E-01
7	3	2254.	2254.	0.998	71.0	68.7	68.6	13.73	C.83	0.358	700.7	840.	61.87	2.5	3.62	281.	1.897	180.-0.30E-01
8	3	2411.	2411.	0.992	63.5	61.3	61.2	13.04	0.93	0.421	755.6	518.	34.22	2.5	3.27	251.	1.785	180.-0.30E-01
9	3	2459.	2459.	0.933	57.4	55.4	55.3	11.98	1.03	0.447	778.7	178.	10.70	2.5	2.87	221.	1.694	180.-0.29E-01

390.7	PRESS.= 28.93	PS= -0.2 FSWIR= 0.893	S.RT= 4.498	SUM.H.REJ=-.223E+02					
TOTAL	0.994		137.01	0.59		1366.	1132.		-0.24E+00
1 1	776.		10.91	0.01	0.246	193.4	52.	8.	-0.26E+00
2 3	1784.	1794.	0.999	105.1	103.0	102.9	19.43	0.56	0.319
3 3	1817.	1817.	0.999	101.3	99.2	99.1	17.75	0.58	0.321
4 3	1932.	1932.	0.999	90.7	89.2	89.1	16.75	0.65	0.325
5 3	2077.	2077.	0.999	72.8	78.3	78.2	15.70	0.74	0.334
6 3	2096.	2096.	0.999	78.3	76.2	76.1	15.37	0.75	0.336
7 3	2190.	2190.	0.998	73.2	71.0	70.9	14.76	0.80	0.346
8 3	2347.	2347.	0.998	63.6	63.5	63.4	14.13	0.90	0.393
9 3	2434.	2434.	0.995	59.4	57.4	57.3	13.22	1.00	0.456
392.7	PRESS.= 26.82	PS= -0.3 FSWIR= 0.892	S.RT= 4.376	SUM.H.REJ=-.232E+02					
TOTAL	0.997		145.62	0.59		1371.	1136.		-0.21E+00
1 1	755.		10.16	0.03	0.265	187.9	52.	7.	-0.22E+00
2 3	1722.	1722.	0.999	109.3	106.1	105.9	19.77	0.54	0.317
3 3	1771.	1771.	0.999	102.9	101.3	101.2	18.96	0.57	0.320
4 3	1882.	1882.	0.999	92.3	90.7	90.6	17.89	0.64	0.324
5 3	2021.	2021.	0.999	81.4	79.8	79.8	16.79	0.72	0.331
6 3	2031.	2031.	0.999	80.4	78.3	78.2	16.47	0.73	0.332
7 3	2108.	2108.	0.999	75.4	73.2	73.1	15.86	0.78	0.338
8 3	2274.	2274.	0.999	67.7	65.5	65.5	15.24	0.87	0.370
9 3	2392.	2392.	0.993	61.4	59.4	59.3	14.48	0.96	0.433
394.7	PRESS.= 24.87	PS= -0.9 FSWIR= 0.891	S.RT= 4.267	SUM.H.REJ=-.239E+02					
TOTAL	0.999		154.57	0.59		1374.	1139.		-0.18E+00
1 1	735.		9.31	0.03	0.264	182.7	52.	6.	-0.18E+00
2 3	1664.	1664.	0.999	112.4	109.3	109.2	21.19	0.52	0.316
3 3	1726.	1726.	0.999	104.5	102.9	102.8	20.23	0.55	0.318
4 3	1833.	1833.	0.999	93.8	92.3	92.2	19.11	0.61	0.323
5 3	1956.	1956.	0.999	87.9	81.4	81.3	17.95	0.71	0.329
6 3	1752.	1948.	0.944	82.4	80.4	80.3	17.67	0.71	0.329
7 3	2040.	2040.	0.999	77.6	75.4	75.3	17.03	0.76	0.334
8 3	2202.	2202.	0.998	61.8	67.7	67.6	16.41	0.84	0.354
9 3	2344.	2344.	0.999	53.3	61.4	61.3	15.79	0.93	0.407
395.7	PRESS.= 23.06	PS= -1.3 FSWIR= 0.890	S.RT= 4.170	SUM.H.REJ=-.245E+02					
TOTAL	0.999		164.14	0.59		1376.	1140.		-0.16E+00
1 1	715.		8.37	0.03	0.263	177.6	52.	5.	-0.15E+00
2 3	1618.	1618.	0.999	115.5	112.4	112.3	22.70	0.51	0.314
3 3	1642.	1642.	0.999	106.1	104.5	104.5	21.60	0.56	0.317
4 3	1745.	1745.	0.999	95.4	93.8	93.8	20.41	0.62	0.321
5 3	1713.	1713.	0.999	84.5	82.9	82.8	19.19	0.70	0.327
6 3	1707.	1707.	0.999	84.6	82.4	82.3	19.93	0.70	0.327
7 3	1974.	1974.	0.999	79.8	77.6	77.5	18.28	0.76	0.330
8 3	2132.	2132.	0.999	71.0	63.8	69.7	17.64	0.82	0.344
9 3	2275.	2275.	0.999	55.3	63.3	63.3	17.04	0.90	0.381
399.7	PRESS.= 21.30	PS= -1.8 FSWIR= 0.890	S.RT= 4.084	SUM.H.REJ=-.250E+02					
TOTAL	0.999		174.02	0.59		1377.	1140.		-0.13E+00
1 1	697.		7.31	0.03	0.262	172.7	52.	4.	-0.12E+00
2 3	1556.	1556.	0.999	119.5	115.5	115.4	24.29	0.50	0.313
3 3	1640.	1640.	0.999	107.8	105.1	106.1	23.03	0.55	0.316
4 3	1739.	1739.	0.999	97.0	95.4	95.3	21.78	0.61	0.320
5 3	1852.	1852.	0.999	85.0	84.5	84.4	20.50	0.68	0.325
6 3	1951.	1951.	0.999	86.4	84.4	84.3	20.27	0.68	0.325
7 3	1712.	1712.	0.999	82.0	79.8	79.7	19.59	0.72	0.328
8 3	2044.	2044.	0.999	73.9	71.9	71.8	18.93	0.80	0.337
9 3	2207.	2207.	0.999	67.2	69.3	65.2	19.33	0.88	0.362
400.7	PRESS.= 19.89	PS= -2.2 FSWIR= 0.899	S.RT= 4.007	SUM.H.REJ=-.255E+02					
TOTAL	0.999		184.29	0.59		1377.	1141.		-0.11E+00
1 1	680.		5.13	0.03	0.261	168.1	52.	3.	-0.88E-01
2 3	1527.	1527.	0.999	121.6	118.6	118.4	25.96	0.49	0.311
3 3	1599.	1599.	0.999	109.4	107.8	107.7	24.53	0.54	0.315
4 3	1605.	1605.	0.999	98.6	97.0	96.9	23.22	0.60	0.319

5	3	1813.	1813.	0.999	87.6	86.0	85.9	21.97	0.67	0.324	559.2	1733.	157.54	2.5	4.04	394.	2.203	180.-0.17E-01
6	3	1797.	1797.	0.999	88.4	86.4	86.3	21.67	0.67	0.323	549.1	1180.	108.35	2.5	4.33	370.	2.193	180.-0.17E-01
7	3	1953.	1953.	0.999	84.1	82.0	81.9	20.97	0.70	0.326	565.4	725.	63.33	2.5	4.09	350.	2.121	180.-0.18E-01
8	3	1999.	1999.	0.999	76.0	73.9	73.8	20.28	0.77	0.333	606.4	504.	39.71	2.5	3.73	319.	2.011	180.-0.18E-01
9	3	2137.	2139.	0.999	69.1	67.2	67.1	19.67	0.85	0.349	652.0	293.	21.03	2.5	3.32	290.	1.916	180.-0.19E-01

\*\*\*EXPANSION PROCESS IS CALCULATED AS ONE ELEMENT\*\*\*

PRESSURE = 15.98ATA  
 AV. TEMPERATURE = 1663.9K DEG  
 AV. EQUI. RATIO = 0.590  
 AV. ENTHALPY = 515.11CAL/G  
 TOTAL MASS = 0.7078G

\*\*EXHAUST NOX\*\*

NOX CONCEN. = 1377.0PPM  
 TOTAL MASS = 0.173E-01G

THEC DEG	P ATA	T K	V CM <sup>3</sup> /G	WORK PS	CYL.MAS G	HEAT TRANSFER CAL/A CAL	FSWR	S.RY *RPM	
402.7	18.47	1536.	155.	2.53	0.798	-0.500E+00	-0.275E+02	0.888	4.01
404.7	17.20	1559.	226.	3.04	0.798	-0.470E+00	-0.294E+02	0.887	3.94
406.7	16.04	1593.	217.	3.43	0.798	-0.443E+00	-0.312E+02	0.887	3.88
408.7	14.99	1559.	229.	3.81	0.798	-0.419E+00	-0.328E+02	0.886	3.82
410.7	14.03	1534.	241.	4.17	0.798	-0.376E+00	-0.344E+02	0.885	3.77
412.7	13.15	1511.	253.	4.51	0.798	-0.376E+00	-0.359E+02	0.885	3.73
414.7	12.36	1489.	265.	4.83	0.798	-0.357E+00	-0.373E+02	0.884	3.68
416.7	11.63	1468.	278.	5.14	0.798	-0.340E+00	-0.387E+02	0.883	3.65
418.7	10.95	1448.	291.	5.43	0.798	-0.324E+00	-0.400E+02	0.883	3.61
420.7	10.35	1427.	304.	5.71	0.798	-0.310E+00	-0.412E+02	0.882	3.58
422.7	9.79	1410.	317.	5.98	0.798	-0.297E+00	-0.424E+02	0.881	3.55
424.7	9.28	1392.	330.	6.23	0.798	-0.284E+00	-0.436E+02	0.881	3.53
426.7	8.81	1373.	344.	6.47	0.798	-0.273E+00	-0.447E+02	0.880	3.50
428.7	8.38	1359.	357.	6.70	0.798	-0.263E+00	-0.457E+02	0.880	3.48
430.7	7.98	1241.	371.	6.91	0.798	-0.253E+00	-0.467E+02	0.879	3.46
432.7	7.61	1324.	384.	7.12	0.798	-0.244E+00	-0.477E+02	0.879	3.44
434.7	7.27	1314.	398.	7.31	0.798	-0.235E+00	-0.486E+02	0.878	3.42
436.7	6.95	1300.	412.	7.50	0.798	-0.224E+00	-0.495E+02	0.877	3.40
438.7	6.66	1286.	425.	7.67	0.798	-0.220E+00	-0.504E+02	0.877	3.39
440.7	6.39	1274.	439.	7.94	0.798	-0.213E+00	-0.513E+02	0.876	3.37
442.7	6.14	1261.	452.	8.00	0.798	-0.207E+00	-0.521E+02	0.876	3.36
444.7	5.91	1250.	466.	8.15	0.798	-0.201E+00	-0.529E+02	0.875	3.35
445.7	5.69	1236.	479.	8.29	0.798	-0.196E+00	-0.537E+02	0.875	3.33
447.7	5.49	1227.	492.	8.42	0.798	-0.190E+00	-0.545E+02	0.874	3.32
450.7	5.30	1217.	505.	8.55	0.798	-0.185E+00	-0.552E+02	0.874	3.31
452.7	5.13	1207.	519.	8.67	0.798	-0.181E+00	-0.559E+02	0.873	3.30
454.7	4.96	1197.	531.	8.79	0.798	-0.176E+00	-0.566E+02	0.873	3.29
456.7	4.81	1198.	544.	8.90	0.798	-0.172E+00	-0.573E+02	0.872	3.28
454.7	4.67	1179.	556.	9.00	0.798	-0.168E+00	-0.580E+02	0.872	3.28
455.7	4.53	1170.	568.	9.10	0.798	-0.164E+00	-0.586E+02	0.871	3.27
452.7	4.41	1162.	580.	9.19	0.798	-0.161E+00	-0.593E+02	0.871	3.26
454.7	4.29	1154.	592.	9.28	0.798	-0.154E+00	-0.599E+02	0.870	3.25
456.7	4.14	1147.	603.	9.36	0.798	-0.155E+00	-0.605E+02	0.870	3.24
454.7	4.04	1137.	615.	9.44	0.798	-0.152E+00	-0.611E+02	0.869	3.24
470.7	3.99	1132.	626.	9.51	0.798	-0.147E+00	-0.617E+02	0.869	3.23
472.7	3.89	1126.	637.	9.59	0.798	-0.146E+00	-0.623E+02	0.868	3.23
474.7	3.81	1117.	647.	9.55	0.798	-0.144E+00	-0.629E+02	0.868	3.22
476.7	3.73	1113.	657.	9.71	0.798	-0.141E+00	-0.635E+02	0.867	3.21
478.7	3.65	1107.	667.	9.77	0.798	-0.139E+00	-0.640E+02	0.867	3.21
480.0	3.61	1103.	673.	9.81	0.798	-0.137E+00	-0.644E+02	0.866	3.20

## EXHAUST VALVE OPEN

## OUTPUT DATA

THED DES	P ATA	T K	V CM**3	WCRK PS	CYL.MAS G	HEAT TRANSFER CAL/A CAL	AEEF CM**2	GWE G/S
492.0	3.54	1098.	683.	9.96	0.798 -0.127E+00	-0.649E+02	0.00	-0.06
494.0	3.48	1092.	692.	9.91	0.798 -0.125E+00	-0.654E+02	0.01	-0.18
496.0	3.42	1087.	701.	9.96	0.798 -0.123E+00	-0.659E+02	0.01	-0.30
498.0	3.36	1082.	709.	10.01	0.798 -0.121F+00	-0.663E+02	0.01	-0.42
500.0	3.31	1078.	718.	10.05	0.798 -0.120E+00	-0.668E+02	0.01	-0.53
502.0	3.26	1073.	725.	10.09	0.797 -0.119E+00	-0.673E+02	0.02	-0.63
504.0	3.21	1069.	733.	10.13	0.797 -0.117E+00	-0.678E+02	0.02	-0.74
506.0	3.16	1065.	740.	10.16	0.797 -0.115E+00	-0.682E+02	0.05	-1.15
508.0	3.12	1060.	747.	10.20	0.797 -0.114E+00	-0.687E+02	0.09	-2.69
510.0	3.08	1056.	754.	10.23	0.796 -0.113E+00	-0.691E+02	0.13	-4.30
512.0	3.04	1052.	760.	10.26	0.795 -0.111E+00	-0.696E+02	0.17	-5.87
504.0	3.00	1049.	766.	10.28	0.794 -0.110E+00	-0.700E+02	0.22	-7.40
506.0	2.96	1045.	772.	10.31	0.792 -0.109E+00	-0.705E+02	0.47	-11.25
508.0	2.91	1040.	777.	10.33	0.788 -0.107E+00	-0.709E+02	0.78	-23.11
510.0	2.86	1035.	782.	10.35	0.782 -0.105E+00	-0.713E+02	1.09	-33.92
512.0	2.80	1029.	787.	10.37	0.775 -0.103E+00	-0.717E+02	1.39	-44.31
514.0	2.73	1023.	791.	10.39	0.766 -0.100E+00	-0.721E+02	1.70	-54.22
516.0	2.65	1017.	795.	10.40	0.755 -0.976E-01	-0.725E+02	2.26	-67.46
514.0	2.54	1009.	799.	10.42	0.740 -0.944E-01	-0.729E+02	2.87	-85.75
522.0	2.49	1021.	803.	10.43	0.723 -0.904E-01	-0.732E+02	3.47	-102.86
522.0	2.39	990.	806.	10.44	0.703 -0.864E-01	-0.736E+02	4.08	-118.37
524.0	2.29	980.	F08.	10.45	0.681 -0.818E-01	-0.740E+02	4.68	-132.14
524.0	2.17	962.	F11.	10.45	0.658 -0.770E-01	-0.742E+02	5.21	-142.99
525.0	2.09	956.	F13.	10.46	0.632 -0.720E-01	-0.745E+02	5.74	-151.15
512.0	1.74	943.	F15.	10.46	0.606 -0.670E-01	-0.748E+02	6.27	-157.73
512.0	1.92	933.	F16.	10.46	0.579 -0.619E-01	-0.752E+02	6.80	-162.68
534.0	1.73	916.	F17.	10.47	0.551 -0.568E-01	-0.753E+02	7.29	-165.24
534.0	1.59	902.	F18.	10.47	0.524 -0.519E-01	-0.755E+02	7.64	-162.64
532.0	1.49	882.	F19.	10.47	0.498 -0.472E-01	-0.757E+02	7.98	-156.54
542.0	1.39	874.	F19.	10.47	0.474 -0.424E-01	-0.758E+02	8.32	-148.26
542.0	1.31	861.	F19.	10.47	0.451 -0.390E-01	-0.760E+02	8.66	-137.63
544.0	1.23	849.	F18.	10.47	0.430 -0.355E-01	-0.761E+02	8.96	-124.39
545.0	1.17	835.	F17.	10.47	0.412 -0.325E-01	-0.763E+02	9.12	-127.27
546.0	1.11	824.	F16.	10.47	0.397 -0.300E-01	-0.764E+02	9.28	-87.93
550.0	1.07	822.	F15.	10.47	0.386 -0.281E-01	-0.765E+02	9.45	-67.28
552.0	1.05	817.	F13.	10.47	0.378 -0.267E-01	-0.766E+02	9.61	-45.67
554.0	1.04	814.	F11.	10.47	0.375 -0.259E-01	-0.767E+02	9.72	-22.98
556.0	1.04	814.	F08.	10.47	0.374 -0.255E-01	-0.768E+02	9.75	-5.01
558.0	1.04	813.	F06.	10.47	0.373 -0.254E-01	-0.769E+02	9.79	-7.20
560.0	1.04	813.	F03.	10.47	0.371 -0.253E-01	-0.770E+02	9.79	-7.33
562.0	1.04	813.	F09.	10.47	0.370 -0.251E-01	-0.771E+02	9.79	-8.14
564.0	1.04	812.	F05.	10.46	0.369 -0.250E-01	-0.772E+02	9.79	-8.94
566.0	1.04	812.	F01.	10.46	0.367 -0.249E-01	-0.773E+02	9.79	-9.83
568.0	1.04	811.	F01.	10.46	0.365 -0.247E-01	-0.774E+02	9.79	-10.82
570.0	1.04	811.	F02.	10.46	0.363 -0.246E-01	-0.775E+02	9.79	-12.55
572.0	1.04	810.	F07.	10.46	0.361 -0.244E-01	-0.776E+02	9.79	-13.45
574.0	1.04	810.	F05.	10.46	0.358 -0.242E-01	-0.777E+02	9.79	-13.74
576.0	1.04	809.	F06.	10.46	0.356 -0.241E-01	-0.778E+02	9.79	-14.31
578.0	1.04	809.	F03.	10.46	0.354 -0.239E-01	-0.779E+02	9.79	-15.08
580.0	1.04	808.	F04.	10.46	0.351 -0.237E-01	-0.780E+02	9.79	-15.93
582.0	1.04	808.	F07.	10.46	0.348 -0.235E-01	-0.791E+02	9.79	-16.82
584.0	1.04	807.	F06.	10.46	0.345 -0.233E-01	-0.792E+02	9.79	-17.72
586.0	1.04	807.	F03.	10.46	0.342 -0.231E-01	-0.793E+02	9.79	-18.62
588.0	1.04	807.	F07.	10.46	0.339 -0.229E-01	-0.793E+02	9.79	-19.52
590.0	1.04	806.	F18.	10.46	0.335 -0.227E-01	-0.784E+02	9.79	-20.42
592.0	1.04	806.	F09.	10.46	0.332 -0.225E-01	-0.785E+02	9.79	-21.31
594.0	1.04	805.	F01.	10.46	0.328 -0.222E-01	-0.786E+02	9.79	-22.20

596.0	1.04	805.	692.	10.46	0.324	-0.220E-01	-0.787E+02	9.79	-23.09
598.0	1.04	805.	683.	10.46	0.320	-0.214E-01	-0.784E+02	9.79	-23.56
600.0	1.04	804.	673.	10.45	0.316	-0.215E-01	-0.789E+02	9.79	-24.84
602.0	1.04	804.	664.	10.45	0.312	-0.213E-01	-0.793E+02	9.79	-25.70
604.0	1.04	804.	653.	10.45	0.307	-0.210E-01	-0.790E+02	9.79	-26.55
606.0	1.04	803.	643.	10.45	0.303	-0.208E-01	-0.791E+02	9.79	-27.39
608.0	1.04	803.	633.	10.45	0.298	-0.205E-01	-0.792E+02	9.79	-28.22
610.0	1.04	802.	622.	10.45	0.293	-0.202E-01	-0.793E+02	9.79	-29.03
612.0	1.05	802.	611.	10.45	0.288	-0.199E-01	-0.794E+02	9.79	-29.82
614.0	1.05	802.	599.	10.45	0.283	-0.197E-01	-0.795E+02	9.79	-30.59
616.0	1.05	801.	588.	10.45	0.278	-0.194E-01	-0.795E+02	9.79	-31.35
618.0	1.05	801.	576.	10.44	0.273	-0.191E-01	-0.796E+02	9.79	-32.07
620.0	1.05	803.	564.	10.44	0.267	-0.188E-01	-0.797E+02	9.79	-32.77
622.0	1.05	803.	551.	10.44	0.262	-0.185E-01	-0.798E+02	9.79	-33.45
624.0	1.05	800.	539.	10.44	0.256	-0.182E-01	-0.798E+02	9.79	-34.09
626.0	1.05	799.	526.	10.44	0.250	-0.179E-01	-0.799E+02	9.79	-34.70
628.0	1.05	795.	513.	10.44	0.244	-0.176E-01	-0.800E+02	9.79	-35.27
630.0	1.05	798.	500.	10.44	0.238	-0.172E-01	-0.800E+02	9.79	-35.80
632.0	1.05	799.	447.	10.44	0.232	-0.169E-01	-0.801E+02	9.79	-36.29
634.0	1.05	797.	474.	10.43	0.226	-0.166E-01	-0.802E+02	9.79	-36.74
636.0	1.05	797.	461.	10.43	0.220	-0.163E-01	-0.802E+02	9.79	-37.14
638.0	1.05	795.	447.	10.43	0.214	-0.160E-01	-0.803E+02	9.79	-37.49
640.0	1.05	796.	434.	10.43	0.207	-0.156E-01	-0.804E+02	9.79	-37.78
642.0	1.05	795.	420.	10.43	0.201	-0.153E-01	-0.804E+02	9.79	-38.03
644.0	1.05	795.	406.	10.43	0.195	-0.150E-01	-0.805E+02	9.79	-38.21
646.0	1.05	794.	393.	10.42	0.188	-0.146E-01	-0.805E+02	9.79	-38.34
648.0	1.05	794.	379.	10.42	0.182	-0.143E-01	-0.806E+02	9.79	-38.41
650.0	1.05	793.	366.	10.42	0.176	-0.140E-01	-0.807E+02	9.79	-38.41
652.0	1.05	793.	352.	10.42	0.169	-0.137E-01	-0.807E+02	9.79	-38.34
654.0	1.05	792.	339.	10.42	0.163	-0.133E-01	-0.808E+02	9.79	-38.21
656.0	1.05	792.	325.	10.42	0.156	-0.130E-01	-0.808E+02	9.79	-38.01
658.0	1.05	791.	312.	10.42	0.150	-0.127E-01	-0.809E+02	9.75	-37.70
660.0	1.05	795.	299.	10.41	0.144	-0.124E-01	-0.810E+02	9.72	-37.35
662.0	1.05	790.	286.	10.41	0.138	-0.121E-01	-0.810E+02	9.61	-36.89
664.0	1.05	789.	273.	10.41	0.132	-0.118E-01	-0.810E+02	9.45	-36.26
666.0	1.05	788.	261.	10.41	0.126	-0.115E-01	-0.811E+02	9.28	-35.72
668.0	1.05	782.	248.	10.41	0.120	-0.112E-01	-0.811E+02	9.12	-35.13
670.0	1.05	787.	236.	10.41	0.114	-0.109E-01	-0.811E+02	8.26	-34.48
672.0	1.05	787.	224.	10.41	0.109	-0.104E-01	-0.812E+02	8.66	-33.61
674.0	1.05	786.	214.	10.40	0.103	-0.104E-01	-0.812E+02	8.32	-32.69
676.0	1.05	785.	202.	10.40	0.098	-0.101E-01	-0.813E+02	7.98	-31.83
678.0	1.05	781.	191.	10.40	0.093	-0.988E-02	-0.813E+02	7.64	-30.92
680.0	1.05	784.	180.	10.40	0.088	-0.966E-02	-0.813E+02	7.29	-29.95
682.0	1.05	783.	170.	10.40	0.083	-0.944E-02	-0.814E+02	6.80	-28.74
684.0	1.05	783.	161.	10.40	0.078	-0.925E-02	-0.814E+02	6.27	-27.49
686.0	1.05	782.	151.	10.40	0.074	-0.907E-02	-0.815E+02	5.74	-26.28
688.0	1.05	782.	142.	10.40	0.070	-0.891E-02	-0.815E+02	5.21	-25.02
690.0	1.06	781.	134.	10.39	0.066	-0.877E-02	-0.815E+02	4.68	-23.69
692.0	1.06	781.	126.	10.39	0.062	-0.865E-02	-0.816E+02	4.08	-22.16
694.0	1.07	781.	118.	10.39	0.059	-0.857E-02	-0.816E+02	3.47	-20.51
696.0	1.08	781.	111.	10.39	0.056	-0.852E-02	-0.816E+02	2.87	-18.75
698.0	1.09	781.	105.	10.39	0.053	-0.853E-02	-0.817E+02	2.26	-16.76
700.0	1.10	782.	99.	10.39	0.050	-0.862E-02	-0.817E+02	1.70	-14.46
702.0	1.12	784.	94.	10.39	0.048	-0.877E-02	-0.817E+02	1.39	-12.87
704.0	1.13	785.	89.	10.39	0.046	-0.895E-02	-0.818E+02	1.07	-11.41
706.0	1.15	787.	84.	10.38	0.045	-0.920E-02	-0.818E+02	0.78	-9.41
708.0	1.18	780.	81.	10.38	0.044	-0.953E-02	-0.819E+02	0.47	-6.94
710.0	1.22	783.	77.	10.38	0.043	-0.100E-01	-0.819E+02	0.22	-4.02

EXHAUST TEMPERATURE= 811.9KDEG

## \*PREDICTION OF THE FRICTION LOSS\*\*

MISC. AND PUMPS = 77.6820/CM\*\*2  
 CAM GEAR = 101.3100/CM\*\*2  
 BEARINGS = 140.8450/CM\*\*2

BLCRBY = 43.481G/CM\*\*2  
VISCOUS PISTON = 364.137G/CM\*\*2  
RING TENSION = 115.044G/CM\*\*2  
RING GAS PRESS = 7.335G/CM\*\*2

TOTAL LOSS = 851.814G/CM\*\*2

PIMEP= -67.65G/CM\*\*2 PSIN= -0.11INP  
PEMEP= 345.07G/CM\*\*2 PSEX= 0.57HP  
AIMEP= 6240.0/CM\*\*2 IH= 10.38HP ATSFC= 171.64G/IHP.HR  
BMEP= 5188.0/CM\*\*2 BHP= 8.96HP BSFC= 198.78G/BHP.HR

HEAT REJECTION= CAL/MIN  
TOTAL H. REJ = 0.8189E+05  
CYL. LINER = 0.2751E+05  
PISTON TOP = 0.1673E+05  
PISTON CLP = 0.2045E+05  
CYL. HEAD = 0.1515E+05  
INT. VALVE = 0.7221E+04  
EXH. VALVE = 0.1322E+04

HEAT REJ./FUEL = 0.277

PEAK CYL PRESS= 52.0AT367.5DEG. CA