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**PEBBLE: A Two-Dimensional
Steady-State Pebble-Bed-Reactor
Thermal-Hydraulics Code**

D. R. Vondy

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UNION CARBIDE CORPORATION
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**PEBBLE: A TWO-DIMENSIONAL STEADY-STATE PEBBLE-BED-REACTOR
THERMAL-HYDRAULICS CODE**

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COMPUTER CODE ABSTRACT

1. Code. PEBBLE, ORNL Version 1 (1980).¹
2. Problem. The two-dimensional (RZ) steady-state pebble bed reactor thermal hydraulics problem.
3. Method. A relatively straight forward accelerated iterative procedure is used to solve the coolant thermal hydraulics problem² cast in the stream function form as a mesh-edgepoint finite-difference representation.
4. Related Material. This code is used in the local modular code system³ for reactor analysis providing interfacing with the VENTURE diffusion theory neutronics code and associated capability for calculating reactor histories.⁴
5. Restrictions. With variably dimensioned data arrays, problem size is only limited to available computer memory without provision for data transfer during iteration; typically the thermal hydraulics problem requires less computer time than the neutronics problem but requires as much if not more computer memory. This code is a member of a modular code system and cannot operate in a stand alone mode.
6. Computers. IBM 360, 370, 303X series.
7. Running Time. A 37 x 54 mesh point problem required 32K program and 105K data (double precision), 137K short word total, and required 0.81 minutes processor time, 2.6 minutes clock time on an IBM 3033 two-processor multi-tasking machine.

8. Programming Language. Fortran (some service tasks done in assembly language).
9. Operating System. IBM OS 303X under HASP II multitasking, compiler OS 370 Fortran H Extended (Enhanced), Version 1.3.0, Optimization Level 3.
10. Machine Requirements. Typically 7 disc files are used and 150K short words memory, but the memory requirement depends directly on the problem size (mesh points); the code system operates under a resident driver and managing control module. Codes do not read input data from the stream but only process interface data files admitting free ordering and loop structures.
11. Author. D. R. Vondy
Engineering Physics Division
Box X, Oak Ridge, TN
12. References.
 1. D. R. Vondy, "PEBBLE: A Two-Dimensional Steady-State Pebble Bed Reactor Thermal Hydraulics Code," ORNL-5698 (this report).
 2. K. R. Stroh, "Thermal-Hydraulic Analysis Techniques for Axisymmetric Pebble Bed Nuclear Reactor Cores," Dissertation, Mech. Eng. CSU (LANSL report in progress, 1978).
 3. D. R. Vondy, et al., "A Computation System for Nuclear Reactor Core Analysis," DOE Report, ORNL-5158 (April 1977).

4. D. R. Vondy, T. B. Fowler, and G. W. Cunningham, "VENTURE: A Code Block for Solving Multigroup Neutronics Problems Applying the Finite-Difference Diffusion-Theory Approximation to Neutron Transport, Version 1," ORNL-5062,R1 (November 1977).

13. Material Available. The source program and this documenting report are to be placed in the DOE National Energy Software center with the other codes in this system for distribution. The code consists of about 6,000 source cards.

INTRODUCTION

A reactor core thermal hydraulics calculation is a key component of basic reactor analysis. It extends the assessment of power density peaking to assessment of temperature peaking, an essential enhancement for reliable analysis, for both comparative and absolute evaluation. Temperature feedback is a further increase in the level of sophistication that should increase the reliability of usual analysis and enhance the capability to examine reactivity effects important in stability and sensitivity effort.

The two-dimensional thermal hydraulic code PEBBLE was written originally as a Dissertation at Colorado State University by K. R. Stroh¹ of LANL. The effort came after that in Germany done to support development of the pebble bed reactor concept. The German effort at KFA by K. Petersen² has yet to be formally documented and the code in use there is not available. Additional effort under T. E. Mott by J. Jones and others at TEC³ under ORNL contract was done to incorporate the PEBBLE code into our local computation system for reactor core analysis,⁴ and to incorporate the capability to calculate pebble temperature distributions with account of the effect of the temperature and the neutron exposure history on the thermal conductivity.

The purpose of the effort reported here was to convert this program from an experimental one to a production tool that can be used routinely by the nuclear engineer having only casual interest in the details, and to document the contents and the use requirements. This report is the code documentation. The local version of the code is quite different from the

version received and will not operate in a stand alone mode. It is now a module of the local computation system for reactor core analysis, obtaining data selectively from the interface files including instructions without acquiring data directly from the user input data file, and generating a file of temperature data for temperature feedback, and also saving results that can be recovered. Complete revision of the calculational procedures causes past experience with the code not to be applicable.

The primary sources of the programmed equations are referenced.⁵⁻¹³ The basic formulation involves finite-difference representations of the stream function form of the fluid flow differential equation, the bulk fluid temperature equation, the pebble surface temperature equation, and the pressure equation. These coupled equations are solved by an iterative procedure.

From available information, namely results of calculations done at KFA, there appeared to be serious doubt that accurate results could be produced with a coarse grid of mesh points. There are two possible sources of major discrepancies: the fluid flow modeling and the power density information. The commitment was made in this effort to use the same geometric description used by the neutronics code. Whereas one may typically use 5 radial zones and 12 axial zones in the core for exposure (60 locations of different nuclide concentrations, although many more would be possible), a typical mesh may be 30 radial by 40 axial within the core (1200 locations of different power densities). Since the top and bottom and radial reflector can be eliminated for the hydraulics calculation, it always involves fewer mesh points than the neutronics code and is not

expected to cost any more to solve (being neither multi-group nor eigenvalue type, although the equations are somewhat more complicated.)

Thus the code obtains the geometric description from the same file used by the neutronics code. Fully compatible with this file is the file of point power densities when made available, and this file is used when available. For treating the general case of multiple pebble passes, a different power density file is required for calculating pebble temperatures. The table below summarizes the use of power density data:

File Name	Where Written	Power Density Contents	Priority for Use	
			Hydraulics	Pebble Temperatures
PWDINT	Neutronics	By Mesh point	1	2
ZNPOWD	Exposure ^a (Neutronics)	By Zone/Subzone (By Zone Only)	2	1

^aThe neutronics code does not have power density data available on the subzone subscale (a zone contains one or more subzones) and the exposure code knows nothing of the mesh but does place volume fraction data in the power density file.

The code uses the high energy neutron flux exposure data generated by the exposure code for determining the effect on thermal conductivity (and temperature dependence).

Instructions to the code are fully contained in a single record of 100 numbers and 100 integers in accordance with the computation system requirements, these instructions being easily supplied and subject to revision along the course of a calculation. The code can be accessed one or more times along a calculational path.

The code generates a pebble temperature file (by zone and the subzone subscale) for feedback.

The following basic enhancements were made in this effort:

1. The code was reprogrammed.
2. The difference equations were changed to enhance reliability.
3. The iterative solution process was thoroughly revised and acceleration procedures added.
4. Flexibility was added regarding the use of power density data - Instead of requiring both the point power density data and the zone and optionally the subzone average power densities (granted to be desirable), both may be used, or either. (Basically the hydraulics is done using the point power density data and the pebble temperature calculations using averaged data on a different scale that admits treating multiple pebble passes.)
5. A separate one-dimensional calculation was made compatible.
6. Flexibility was added regarding the treatment of the dependence of thermal conductivity on the exposure, temperature history to either follow the pebble flow or to consider fixed fuel elements.
7. Considerable effort went into additions to make this a production code rather than a stand-alone research tool -- for example, if at all possible a calculation is done (if not, a reason is given, and normal system termination should occur - not overflow, underflow, or blind exit),

and major user difficulties were eliminated. As an example, the code determines the core boundaries from the power density data without being told.

8. Certain technical enhancements were added such as extending the solution to the problem boundaries, improving the inner wall boundary condition for the annular core problem, providing improved problem initialization, and reporting supplemental results such as the power weighted pebble average temperature.

9. Some effort has been expended in making this code a true member of the modular computation system - it does not read input data but does properly interface with other modules, and carries out tasks in accordance with instructions.

10. Saving of results and subsequent recovery has enhanced the capability.

11. Override capability was implemented to allow much of the built-in data to be changed by a user if so desired.

12. Optional equations are incorporated to support application to the prismatic core with coolant flow through holes.

As received, the solution procedure closely followed the suggestions given in Ref. 5 from finite difference thermal hydraulic application experience of the early 1960s. It is noted that during much of this effort the "forward-difference" equation option (for only the bulk temperature, not the other primary variables) was retained. Eventually it was decided

despite warnings regarding experience with non-convergence (programmed message and also in the above reference and in references in the latter), to drop this rather inferior form since it is not as accurate as the "central difference" method. Actually a somewhat modified form of central difference formulation is used. It does appear that recommendations from limited experience in the rather distant past have likely been followed in application efforts. Such blind trust of course may well expedite effort, and this is good. Every methods developer should not have to reinvent the wheel. The propagation of techniques that are based on assumptions and limited test results is, however, very unfortunate. Documentation of methods testing is poor.

IMPLEMENTATION NOTES

Where does the time go in such effort? Much of it goes into searching for a discrepancy or inconsistency on one of the 6,000 Fortran source cards, especially those caused by revisions. But then, given that remote access to the computer has been available only about 50 percent of the time (new computers and operating systems and poor operation), that system messages leave much to be desired for error tracing (OOO stop means information access was attempted outside of the available memory, or any of several other things), and that another's programming is alien (why did he decide to take this action at this point rather than other action elsewhere), the speed of the game is naturally slow.

The objective of this effort was to make available a reliable two-dimensional thermal hydraulics capability in the local reactor core analysis computation system. Of primary interest was the treatment of the graphite moderated core containing spherical fuel pebbles in some degree of random packing and cooled by helium gas having vertical flow. User input requirements were to be minimized to reduce errors; for example, the neutronics geometric description was to be used providing a mesh point layout avoiding the redundancy of a second description, and the code was to determine the boundaries of the active core to establish the extent of the gas flow. In this way a simple set of input data instructions would serve a wide variety of applications; survey calculations could be done at minimum user burden with a high reliability of problem description.

A significant impact on this effort came from the wide class of problems to be treated. Not only could there be more than one pebble type at any location (six for a simple model of the German THTR reactor with a reference fuel management scheme of pebble recycle, six passes without reprocessing), but the data available could take any of several forms. The intent was to use the neutronics point power density distribution and geometric description that goes with it for the heat source, but also allow zone-averaged data to be used if that is all that is made available.

The code is used in load module form unavailable to the user in source deck form thereby effecting high quality assurance in application. However, for routine use of such a code it is necessary to invest considerable effort to overcome minor difficulties that can cause an abort or ridiculous results (although this is of course always possible), to

proof the coding, and to produce adequate information to support application including input error debugging. Perhaps even more effort may be required, however, for the code sponsor, guardian or cognizant and responsible engineer to gain confidence in the contents of an alien code to consider any reported results to have a high level of quality assurance, especially results produced by the casual code system user. Since originators of thermal hydraulics codes often build in data that can not be changed in serious application, revisions are necessary to allow extensive data substitution for effective use on a production basis without the involvement of the originator or coding changes.

This code presented a number of headaches. Storage requirements for containing realistic problems in memory are severe, especially in double precision, requiring compaction of the data storage and multiple use (double allocation). The use of many subroutines to perform trivial functions is not efficient; the original 49 routines were reduced to 21. The thermal hydraulics iterative calculation was a morass of redundant operations that invited thorough revision, yet this had to be done in pieces to avoid total disruption. Common practice in such engineering fields as thermal hydraulics is the incorporation of data in a program wherever needed. Throwing two programs together resulted in two sets of thermal hydraulics data that was worse than merely redundant, they were in disagreement. There were many trivial matters. For example, the edit routines could not handle more than 30 radial mesh points.

What can one say about modification effort on a computer code that leaves a product that requires the inlet pressure to be given in atmospheres and reports the calculated pressure drop in mpa? Incomplete at best.

One always wonders if it pays to revise an alien code or start over from scratch. It is difficult to say and depends somewhat on the situation. The author could not have produced the final product with the amount of effort expended starting from scratch. The likelihood of a discrepancy in the coding would have been higher starting from scratch, although there is some possibility of a defect in this product, hopefully a lower probability the more important the aspect.

The possibilities for a multiplicity of pebble type had a severe impact on this code even without allowing variation in the pebble diameter (which may eventually be needed). One hopes that a procedure can be implemented that calculates a local void fraction consistent with the value used in the neutronics. However, since in the neutronics only the smeared nuclide density need be conserved, the specified volume fractions may range over several possibilities, some of which admit direct interpretation, while others can not be used at all. Therefore, selection must be made from among the possibilities. Selection must be made of a procedure to determine an effective value of the high energy flux exposure (fluence) for estimating the local pebble thermal conductivity when more than one pebble type is involved.

As received, the two-dimensional PEBBLE code and an original TEC² one-dimensional code had been paralleled and partially interfaced for service in the local computation system for reactor analysis. It was found by TEC that all of the terms containing the stream function to be calculated in the finite-difference form were not on the left-hand side of the equation. Recasting the equation reportedly cured the poor convergence characteristics (also reportedly done by GA in their implementation of the original code), but the behavior of a sample non-trivial problem indicated further improvements were necessary.

As received, the code was a mixture of single precision (IBM half-precision) and double precision. This was due to an incomplete reprogramming of the code. Rather than return the code to single precision, the one-dimensional routines and the pebble temperature and edit routines were placed in single precision while the thermal hydraulics calculation was retained in double precision in the hope that additional acceleration procedures to be incorporated would indeed prove most effective with regular rather than IBM half precision. Of course, the penalty is double the data storage requirements. It was assumed that the problems of interest could be core contained and data transfer during iteration thereby avoided and indeed such capability was not programmed (although program and data overlay were done where practical) because local computer operation is now in the virtual memory mode.

The code as received employed an "equation solver" routine that was used four times to calculate the stream function, the bulk fluid temperature, the pebble surface temperature, and the fluid pressure

²Technology for Energy Corporation, Knoxville, Tennessee.

iteratively in finite-difference form at each mesh point. This procedure appeared to be very inefficient causing low computer utilization. The reprogramming eliminates wasted effort and facilitates the use of a more effective iteration scheme with enhanced acceleration to reduce the number of iterations required to effect an acceptable level of convergence. The adoption of a documented procedure for solving equations in difference form can be very ineffective. In this case the form of the equations disguised their nature and inhibited the recasting of them into a more effective form -- indeed inhibited the recognition that there was a better form.

One of the difficulties with modeling RZ geometry in finite-difference form is the large cross sectional area associated with the outer annulus. With 20 radial intervals evenly spaced, a mesh point at the maximum radius has associated with it $100 [1 - (19.5/20)^2] = 5$ percent of the coolant flow that is ignored by setting the axial flow rate to zero at the point. The original coding forced reflective boundary temperature conditions by equating the outer temperatures to the values along the first inner row at both zero radius and maximum radius. This was a rather coarse approximation effectively reducing the number of active points and compromising the results. It also prevented taking into account the flow of heat to the reflector, of considerable interest at low coolant flow rates, and low heat source conditions associated with an after-shutdown state, although such capability remains to be added.

We talk about "foot-dragger's disease" when an equation of the form

$$(a + b)x = cy + ez,$$

where x , y , and z are dependent variables, the others constants, is solved by the procedure

$$x^{n+1} = \frac{1}{a} \left[cy^n + ez^n - bx^n \right],$$

where n is iteration count, rather than by the scheme

$$x^{n+1} = \left(\frac{1}{a+b} \right) \left[cy^n + ez^n \right].$$

Stability and acceleration characteristics are quite different for the various forms. Generally, the latter is the best provided $(a+b)$ is significant, either a or b might be negative. The dependence of x on y and z is now direct, that is, all of the variable to be calculated has been taken to left hand or solution side of the equation.

The number of arithmetic operations done each iterative sweep was reduced by perhaps a factor of four. The accessing of subroutines in the inner-most loop was eliminated by including the full expressions for each equation solved. This permitted extensive revisions to be made to the equations solved. Also, more of the expression for the steam function was moved from the right-hand side of the equation to the left, in addition to what had already been so moved at TEC. Further the bulk fluid and pebble surface temperatures were then obtained simultaneously rather than iterated separately. All of this leads to more effective iteration. Such improvement is essential for routine application for parameter studies of large (many mesh point) problems.

The original coding of this program seems to have been quite sound. Not effective, but sound. That is, no major discrepancies were found, only minor. The coupling into local interface data files and extended calculation of pebble temperatures was superficial at best; it may have satisfied requirements in a specific application, but often it would not. A code should not be placed into routine production use if it either lacks adequate flexibility in application or would not routinely return converged solutions from an iteration process.

Late in this effort it was decided to change the bulk fluid and related surface temperature difference equations from a basic central difference formulation to an upstream difference form for the flow component of the bulk fluid heat balance and consistent heat source. The other terms were left unchanged, which is a bit inconsistent. The result is better convergence characteristics (less underrelaxation required) but lower accuracy (higher finite-difference error). Quite noticeably different results were observed for a coarse mesh point arrangement with the two formulations, but the error has been noted to decrease as more mesh points are added. Most results displayed in this report were obtained prior to the change. (The original code contained an option on central difference/upstream difference, but this involved only the stream function differences, not the heat balance equations.) The central difference form is available on option.

USE INFORMATION

A large amount of data and many options on the calculational flow path are set at default values. Hopefully most of these values are suitable.

Still, the user must carefully check over the requirements and determine what is appropriate for his specific case.

Primary input data requirements are shown in Table 1. Information about the code including interface data file requirements is shown in Table 2. Special interface data files are documented by the coding where they are generated; see the writing of the data for recovery, file TDATAS, for example.

REMARKS ABOUT APPLICATION

The partial differential equation of flow through a bed of fueled pebbles is cast in the stream function form. A set of derived equations relate the dependent variables at neighboring discrete mesh points with finite difference approximations to the partial differential terms. Similarly, the fluid temperatures are approximated from a heat balance, the pebble surface temperatures from another heat balance, and another set of equations relates pressures. The solution is obtained by an iterative scheme.

A number of approximations to a real situation are inherent in the formulation. The reactor core is assumed to have isotropic properties and be packed uniformly with spherical pebbles in each discrete zone. There is no consideration of wall effects on fluid flow nor entrance or exit losses. The outer radial surface is assumed to be insulated in that there is no heat transmitted across this surface.

Table 1. Input Data Requirements

C		
CR		PEBBLE THERMAL HYDRAULICS MODULE INSTRUCTIONS, FILE 'CONTRL'
C		
CW		(THERMAL PEBBLE BED IN RZ OR Z GEOMETRY)
C		
CW		DATE OF THESE USE INSTRUCTIONS, OCTOBER, 1980 --D VONDY, ORNL
C		
CL		PBLINS, (XX(I) , 100), (IX(I) , I=1, 100)
C		
CW		101*MULT + 100
C		
CD		PBLINS PEBBLE THERMAL HYDRAULICS DATA IDENTIFIER (6HPBLINS)
C		
CW*		A * IS PLACED IN COLUMN 3 TO INDICATE THAT THAT DATA MUST
CW*		NORMALLY BE SUPPLIED -- NEED NOTES AND CHECK OLD DECKS
CW*		FLAG TO INDICATE THAT DATA IS USUALLY REQUIRED FOR FLOW THRU
CW*		HOLES IN A SOLID MATRIX
CD		
CD	XX(1)	VOID FRACTION IF TO BE CONSTANT
CD		(DEFAULT VALUE 0.39 LACKING OTHER DATA - THE ZONE
CD		FRACTIONS MAY BE USED AS SOLID FRACTIONS IF .02 <X< .98)
CDX		SPECIAL CONSIDERATIONS WITH FLOW THROUGH HOLES
CD*	XX(2)	INLET TEMPERATURE OF COOLANT, DEG C (DEFAULT 350.35)
CD*	XX(3)	INLET PRESSURE OF COOLANT, ATM (DEFAULT 40)
CD	XX(4)	COOLANT MASS FLOW RATE FOR REACTOR, KG/SEC,
CD		NORMALLY CALCULATED GIVEN INLET AND OUTLET TEMPS
CD*	XX(5)	PEBBLE DIAMETER OR COOLANT HOLE DIAMETER, CM
CDW		THIS IS THE COOLANT FLOW CHARACTERISTIC DIAMETER
CD	XX(6)	REFERENCE HIGH ENERGY NEUTRON FLUX FLUENCE, N/CM**2
CD		APPLIED ONLY IF IX(3) < 0
CD	XX(7)	RECOVERABLE ENERGY FRACTION (DEFAULT 1.0)
CD	XX(8)	REACTOR POWER LEVEL DESIRED, W-TH, USUALLY NOT SET
CDX	XX(9)	EFFECTIVE DIAMETER OF UNIT CELL ABOUT FUEL (INSIDE
CDX		A SHELL OF MATERIAL OUTSIDE, LOCATION OF COOLANT FLOW), CM
CDX		SET EQUAL TO XX(5) IF 0
CD*	XX(10)	RADIUS OF THE ZONE PEBBLE HEAT OR HEAVY METAL CORE
CD		(DEFAULT HALF OF PEBBLE DIAMETER - NO SHELL)
CD*	XX(11)	RADIUS OF THE SUBZONE PEBBLE HEAT OR HEAVY METAL CORE
CD		(DEFAULT HALF OF PEBBLE DIAMETER - NO SHELL)
CU	XX(12)	OUTLET TEMPERATURE OF COOLANT, DEG C (DEFAULT 850.35 IF
CD		XX(4)=0)
CD		(NOT USED IF IX(4) IS NON-ZERO)
CD	XX(13)	FLUENCE MULTIPLIER ON DATA AVAILABLE (DEFAULT 1.0)
CD	XX(14)	RELATIVE PEBBLE GRAPHITE THERMAL CONDUCTIVITY, A
CD		MULTIPLIER ON BUILT IN DATA (DEFAULT 1.0)
CD	XX(15)	ITERATION CONVERGENCE CRITERIA, MAXIMUM RELATIVE ITERATE
CD		CHANGE FOR TERMINATION (DEFAULT 0.00005)
CW		THE OPTION ON BLOCKED FLOW AREA FOLLOWS, USE WITH CAUTION
CD	XX(16)	INSIDE RADIUS (MUST BE ZERO TO BE REALISTIC)
CD	XX(17)	OUTSIDE RADIUS OF BLOCKAGE, CM
CD	XX(18)	DISTANCE BLOCKAGE STARTS FROM COOLANT INLET, CM
CD	XX(19)	HEIGHT OF BLOCKAGE, CM
CD	XX(20)	SOLID BLOCKAGE FRACTION (DEFAULT 0.85 -- USE LARGE VALUES
CD		WITH DISCRETION)

Table 1. (Continued)

CN THE OPTION ON DEFINING CORE BOUNDARIES FOLLOWS
 CN WITHOUT DATA, THE NON-ZERO POWER DENSITY EXTREMES DEFINE CORE
 CD XX(21) INSIDE RADIUS (IF NON-ZERO WILL REQUIRE ADDING THE
 CD ANNUAL INTERNAL SOLID BOUNDARY PLANNED)
 CD XX(22) OUTSIDE RADIUS OF CORE, CM
 CD XX(23) DISTANCE FROM START OF GEOMETRY, TYPICALLY FROM TOP, CM
 CD XX(24) HEIGHT OF CORE, CM
 C
 CN ADDITIONAL OPTIONS AND OVERRIDE DATA VALUES FOLLOW
 CD XX(25) LIMITING PROCESSOR TIME, SECONDS (DEFAULT 120)
 C
 CN INITIAL ACCELERATION COEFFICIENTS ARE MADE PROBLEM DEPENDENT
 CN AND MAY BE ALTERED DURING THE PROBLEM SOLUTION IF DEEMED TO BE
 CN DESIRABLE BY THE AUTOMATED MONITORING PROCEDURES
 C
 CN IT IS QUITE POSSIBLE THAT THE ROUGH ITERATIVE BEHAVIOR EARLY IN
 CN THE HISTORY WILL CAUSE INITIAL COEFFICIENTS TO BE DECREASED
 CN WHICH WOULD REQUIRE INPUT OF SOMEWHAT LARGER VALUES THAN THOSE
 CN EXPECTED TO BE OPTIMUM ASYMPTOTICALLY
 C
 CD XX(26) STREAM FUNCTION OVERRELAXATION COEFFICIENT
 CD XX(27) BULK TEMPERATURE, DITTO, SEE FOLLOWING NOTE
 CN THIS COEFFICIENT MAY BE OF UTMOST IMPORTANCE, AND AN EFFECTIVE
 CN VALUE SHOULD BE SUPPLIED IF KNOWN (BEST PROVEN FOR AT LEAST A
 CN SIMILAR PROBLEM). TYPICALLY THE VALUE IS MUCH LESS THAN 1.
 CD XX(28) SURFACE TEMPERATURE, DITTO
 CN IT IS DIFFICULT TO SEE HOW A VALUE OTHER THAN UNITY WOULD BE
 CN EFFECTIVE HERE
 CD XX(29) PRESSURE, DITTO
 CD XX(30) SPECIFIC HEAT VALUE (5193.)
 C
 CN DATA FOR A SECOND AND THIRD CALCULATION FOLLOW (3 DATUM EACH)
 CD XX(31) NEW INLET COOLANT TEMPERATURE, DEG C (DEFAULT XX(2))
 CD XX(32) NEW OUTLET COOLANT TEMPERATURE, DEG C (DEFAULT XX(12))
 CD XX(33) RELATIVE POWER LEVEL FOR SUBSEQUENT CALCULATION
 CD XX(34) NEW INLET COOLANT TEMPERATURE, DEG C (DEFAULT XX(31))
 CD XX(35) NEW OUTLET COOLANT TEMPERATURE, DEG C (DEFAULT XX(32))
 CD XX(36) RELATIVE POWER LEVEL FOR THIRD CASE (DEFAULT (XX(33))
 (RELATIVE TO THAT FOR THE SECOND CASE)
 C
 C
 CD XX(37) MOLECULAR WEIGHT (4.0026)
 CD XX(38) AZERO (0.0216)
 CD XX(39) AGAS (0.49849)
 CD XX(40) B (0.)
 CD XX(41) C (40.)
 CD XX(42) RGAS (0.08206)
 CD XX(43) BZERO (0.014)
 CD XX(44) PCONA (17.)
 CD XX(45) PCONB (20.5)
 CD XX(46) PCONC (-15.37)
 CD XX(47) BETAK (0.95)
 CD XX(48) GAMMAK (2./3. SPHERE, PI/4. CYLINDER)

Table 1. (Continued)

CD	XX(49)	FC (3.674E-07)
CD	XX(50)	FD (0.7)
CD	XX(51)	FE (0.71)
CD	XX(52)	FF (2.682E-03)
CD	XX(53)	FG (0.0011379)
CD	XX(54)	PH (1.4389E-4)
CD	XX(55)	AFRIC (4.1666) HYDRAULIC EQUATION, FIRST COEFFICIENT
CDX		NOT USED IF IX(13) > 0
CD	XX(56)	BFRC (.1754)
CDX		(1.0 IF IX(13) > 0)
CD	XX(57)	P1 (2.2679E-07)
CD	XX(58)	P2 (3.)
CD	XX(59)	P3 (.1293)
CD	XX(60)	P4 (.3292)
CD	XX(61)	P5 (.277)
CD	XX(62)	P6 (.2426)
CD	XX(63)	P7 (.26)
CD	XX(64)	P8 (.476)
CD	XX(65)	P9 (.41)
CD	XX(66)	P10 (1.176E-04)
CD	XX(67)	P11 (311.)
CD	XX(68)	FOR ONE-DIMENSIONAL CALCULATIONS, RADIAL PEAKING FACTOR
CD		FOR AUXILIARY CALCULATION (DEFAULT 1.2)
CD	XX(69)	P13 (.005)
CD	XX(70)	P14 (2.)
C	XX(71) - XX(83)	REFERENCE THERMAL CONDUCTIVITY DATA
C		USED IF XX(71) .NE. 0
CN		AT NO EXPOSURE, CORRESPONDING TO TEMPERATURES (K) --
CN	300. 350. 400. 500. 600. 700. 800. 900. 1000. 1100. 1200. 1300. 1600.	
CN		REFERENCE POINT C(2) AT T = 350. IS 1.0E WATTS/CM-DEG DELTA T
CN		TO CONVERT GH-CAL TO WATT-SEC, MULTIPLY BY 4.186
CD	XX(84)	P15 (0.1905)
CD	XX(85)	P16 (2./3.)
CD	XX(86)	EOVR (0.1*DP)
CD	XX(87)	EOVA (0.5*DP)
CD	XX(88)-XX(100)	RESERVED
C		
CD	IX(1)	OPTION ON COOLANT FLOW
CD		-1 NO GRAVITY TERM
CD		0- DOWNWARD FLOW
CD		1- UPWARD FLOW
C		
CN		IT MAY BE USEFUL TO CONSIDER THAT AS THE PROBLEMS ARE DESCRIBED
CN		FOR THE NEUTRONICS, FLOW IS FROM THE TOP TO THE BOTTOM
CN		(LEFT TO RIGHT IF ONE DIMENSIONAL)
CN		AND THE COOLANT FLOW MUST BE IN THIS DIRECTION, REASONABLE AT
CN		SEEMS FOR DOWN FLOW OF COOLANT AND PEBBLES, BUT IF THE COOLANT IS
CN		TO FLOW UP AND THE PEBBLES DOWN, THEN THE PROBLEM MUST BE SET UP
CN		QUITE DIFFERENTLY (ZONE NUMBERS RUN UP INSTEAD OF DOWN)
C		
CD	IX(2)	OPTION ON PRESSURE DROP AND FILM COEFFICIENT
CD		0- GERMAN
CD		1- US CORRELATIONS (OLD)
CD	IX(3)	OPTION ON FLUENCE, <0- DONT READ DATA (SEE XX(6))
CD		0,1- CPHIST FILE, CONTINUOUS FUELING
CN		NOTE THAT THIS FLAG MUST BE SET FOR FIXED FUEL EXPOSURE
CD		2- EXPORT FILE, FIXED FUEL EXPOSURE

Table 1. (Continued)

CD	IX(4)	FLUENCE SELECTION, 0,1- USE FIRST RANGE IF AVAILABLE
CD		2- USE SECCND RANGE IF AVAILABLE
CD		3- USE TOTAL IF IT IS AVAILABLE
CW		IF DESIRED DATA IS NOT AVAILABLE, NO DATA IS USED
CD	IX(5)	MEMORY AVAILABLE FOR DATA IN 1000 WORDS
CD		(DEFAULT 20000 ADDED TO RECORD 'DRVINS' CONTENT
CD		WHICH IS THE NUMBER SUPPLIED TO THE CONTROL MODULE)
CD		UNDER VIRTUAL MEMORY, ASSUME FULL CCRE CONTAINED
CD		AND ALLOCATE SPACE ACCORDINGLY
CD	IX(6)	THERMAL CONDUCTIVITY TREATMENT (FOR GROSS HEAT TRANSFER
CD		ACROSS CORE), OPTIONS
CD		<0- NO SOLID PHASE HEAT TRANSFER
CD		0- USE ZONE EXPOSURE DATA AKD SURFACE TEMPERATURE
CD		1- USE SUBZONE EXPOSURE DATA AND SURFACE TEMPERATURE
CD		2- DITTO, BUT VOLUHE FRACTION WEIGHT INSTEAD OF AVERAGE
CD		3- USE BUILT IN AXIAL FUNCTION
CD	IX(7)	DEBUG EDIT LEVEL (0,1,2,3)
CD	IX(8)	EDIT LEVEL OF RESULTS (-1,0,1,2)
CD		EDIT LEVEL IS INDEXED UP IF RESULTS SEEM UNUSUAL
CD	IX(9)	HEAT REMOVAL OPTIONS
CD		0- NORMAL
CD		1- EXCLUDE SOLID CONDUCTION
CD	IX(10)	FUEL ELEMENT GEOMETRY (GRAPHITE, NOW USED ONLY FOR THE
CD		TEMPERATURE CALCULATION IN THE ELEMENT AND AT THE
CD		SURFACE, NOT FOR FLOW)
CD		0- SPHERICAL
CDX		1- CYLINDRICAL (INFINITE LENGTH)
CD*	IX(11)	ITERATION COUNT TERMINATION (DEFAULT ESTIMATED BY CODE)
CD		-NO ITERATION IF <0
CDX	IX(12)	OPTION TO ELIMINATE RADIAL (CROSS) FLOW
CD		0- NORMAL (INCLUDE)
CD		1- EXCLUDE
CD		2- EXCLUDE, AND FIX THE AXIAL FLOW RATE PROPORTIONAL
CD		TO THE AXIAL HEAT LOAD (IDEAL ORIFICING)
CD		3- SAME AS 2 BUT ORIFICE AT INLET INSTEAD OF OUTLET
CW		NOTE THAT THE ABOVE NON-ZERO OPTIONS APPLY TO FIXED TRAVERSE
CW		COOLANT FLOW REQUIRING ADJUSTMENT IN THE DEFAULT COEFFICIENTS
CDX	IX(13)	OPTION FOR FLOW THROUGH HOLES IN SOLID IF > 0
CD		IF 0, THE UPWIND DIFFERENCE IS USED FOR THE BULK
CD		TEMPERATURE FLOW COMPONENT, CENTRAL DIFFERENCE IF <0.
CD	IX(14)	ITERATION PROCEDURE OPTION,
CD		-1- DO NOT INCREASE OVERRELAXATION COEFFICIENTS
CD		0- ADJUST OVERRELAXATION COEFFICIENTS DURING ITERATION
CD		1- DO NOT INCREASE NOR DECREASE COEFFICIENTS
CD	IX(15)	EQUATION SWEEP ORDER,
CD		0- SIGMA-1 (ODD POINTS, THEN EVEN POINTS)
CD		1- NORMAL ORDERED (ONE POINT AFTER THE OTHER, 2 THEN R)
CD	IX(16)	ASYMPTOTIC EXTRAPOLATION PROCEDURE OPTION,
CD		0- NORMAL (ALLCW)
CD		1- DO NOT ALLOW
CD		>1- MINIMUM CYCLE DELAY

Table 1. (Continued)

CD	IX(17)	OPTION ON ASYMPTOTIC EXTRAPOLATION, DATA LEVEL
CD		0- STREAM FUNCTION, TEMPERATURES, PRESSURE
CD		1- STREAM FUNCTION, PRESSURE
CD		2- PRESSURE
CD	IX(18)	OPTION ON THE CALCULATION OF THE LOCAL VOID FRACTION
CD		(OVERRIDDEN BY XX(1), APPLICABLE ONLY WHEN THERE ARE SUBZONES)
CD		0- SUMS ZONE AND SUBZONE VOLUME FRACTIONS
CD		1- USES ONLY ZONE VOLUME FRACTION
CD		2- SUMS ONLY SUBZONE VOLUME FRACTIONS
CD	IX(19)	INITIALIZATION OPTIONS
CD		-1 ONLY FOR SUBSEQUENT CASE THE SOLUTION IS KEPT
CD		0- AUTOMATED PROCEDURE (AXIAL FLUID HEATING)
CD		1- SOMETHING DIFFERENT FOR HE WHO HAS TRIED EVERYTHING
CD	IX(20)	WRITE ZONE TEMPERATURE FILE 'ZNTENP' OPTIONS
CD		-1- NO
CD		0,1- WRITE OVER EXISTING ONE IF ONE EXISTS
CD		OTHERWISE WRITE NEW ONE
CD		2- WRITE OVER NEXT TO LATEST VERSION IF IT EXISTS,
CD		OTHERWISE WRITE NEW ONE
CD		3- GENERATE NEW FILE
CD	IX(21)	SAVE DATA ON AN INTERFACE FILE FOR RECOVERY
CD		-1 SAVE DATA IF CONVERGENCE CRITERIA IS NOT SATISFIED
CD		0 DO NOT SAVE DATA
CD		1 SAVE THE THERMAL HYDRAULICS DATA FOR RECOVERY
CD		2 ALSO SAVE THE PEBBLE THERMAL CONDUCTIVITY DATA
CD		DATA IS SAVED FOR ONLY THE FIRST PROBLEM SOLVED IN A CODE ACCESS
CD	IX(22)	RECOVER DATA FROM AN INTERFACE FILE TO CONTINUE ITERATION
CD		C TO INITIALIZE WITH (PROBLEM MUST BE SIMILIAR)
CD		1- RECOVER ALL DATA (NO REPLACEMENT)
CD		2- DO NOT USE VOID FRACTION, POWER DENSITY, NOR
CD		EXPOSURE DATA FROM FILE (USE NEW DATA)
CD	IX(23)	OPTION TO RECOVER THE PEBBLE THERMAL CONDUCTIVITY DATA
CD		0- DO NOT
CD		1- RECOVER AND USE THE IRRADIATION TEMPERATURE AND
CD		NEUTRON FLUX EXPOSURE FUNCTION DATA
CD		(THIS OPTION REQUIRED TO OBTAIN ONLY EFFECTS OF
CD		SHORT TIME TEMPERATURE CHANGES)
CD		2- RECOVER AND USE DIRECTLY THE THERMAL CONDUCTIVITY
CD		PEBBLE THERMAL DATA MAY BE SAVED OR RECOVERED, BUT NOT BOTH.
CD		DEFAULT PROCEDURES GIVE PREFERENCE TO DATA RECOVERY OVER SAVING
CD		(USED FIRST PROBLEM ONLY)
CD	IX(24)-IX(100)	RESERVED
C		

Table 2. Information About the ORNL Version of the Pebble Program

INTERFACE DATA FILE USAGE	
FILE	DATA USE
----	-----
GEODST	GEOMETRY DESCRIPTION, MESHPOINT AND ZONE LOCATIONS
PWDINT	POWER DENSITY DATA BY MESHPOINT
ZNPOWD	POWER DENSITY (FOR PEBBLE TEMPS), VOLUME FRACTIONS DEFAULT USE IF FILE PWDINT IS NOT AVAILABLE
CPHIST	NEUTRON FLUX EXPOSURE, CONTINUOUS FUELING, OR
EXPORT	NEUTRON FLUX EXPOSURE, FIXED FUEL
TDATAS	SAVE THERMAL HYDRAULICS RESULTS FOR RECOVERY --ONLY A SINGLE VERSION IS PERMITTED TO EXIST
LTEMP	TEMPERATURE RESULTS FOR SUBSEQUENT USE IN OTHER CODES
ONLY ONE VERSION OF THE FILE TDATAS IS ADMITTED, SO DATA CAN NOT BE SAVED AND USED SIMULTANEOUSLY FOR ONE PROBLEM. NOTE THE ORDER ABOVE OF THE WRITING OF THE LAST TWO FILES, AND THEREFORE NORMAL INCREASING UNIT NUMBERS	
ROUTINE NAME	PRIMARY ROLE
-----	-----
MAIN	MAIN ROUTINE DOES SOME INITIAL CHECKING
INIL	FILE HEADER READING, CHECK INSTRUCTIONS, DATA
TIMER	LOCAL ACCESS OF COMPUTER TIME, ETC.
SEK	DATA FILE MANAGEMENT SERVICE ROUTINE
RITE	DATA TRANSFER SERVICE ROUTINE
REED	DATA READING PROCEDURE, ENTRY POINT IN RITE
GETCOR	MEMORY SPACE ACCESS FOR DATA ARRAYS
PRECOR	MEMORY SPACE RELEASE
STRT	LINE ROUTINE THAT CONVEYS DATA ARRAY SPACE
GTDA	ALLOCATION OF SPACE FOR DATA ARRAYS
GEOD	ACCESS DATA FROM GEOMETRY INTERFACE DATA FILE
PDRD	ACCESS OF DATA FROM INTERFACE FILES
PBST	SELECTS CALCULATION PATH, 1 OR 2 DIMENSIONAL USER OVERRIDE OF PRIMARY DEFAULT DATA VALUES
HPBL	DIRECTS THE 2 DIMENSIONAL CALCULATION
BLOC	DATA PROCESSING, HEAT SOURCE, VOID FRACTIONS, DELTAS
INIT	INITIALIZES THE 2 DIMENSIONAL PROBLEM
TRAC	SPECIAL EDIT FOR CHECKING DETAILS
PDEX	ITERATION DRIVER WITH ACCELERATION PROCEDURES
IDER	CALCULATIONS OVER THE MESHPOINTS, ITERATION
WFLU	PRODUCES AUXILIARY INFORMATION DURING ITERATION
POUT	THERMAL HYDRAULICS PRINTOUT, 2 DIMENSIONS
CLTE	PEBBLE TEMPERATURE CALCULATION, 2 DIMENSIONAL
TBAR	MANAGER ROUTINE TO CALCULATE PEBBLE TEMPERATURES
GRAC	ESTIMATION OF THE THERMAL CONDUCTIVITY
XOUT	WRITES THE TEMPERATURE INTERFACE DATA FILE
PBL1	FLUID FLOW FOR 1 DIMENSION
CALT	PEBBLE TEMPERATURE CALCULATION, 1 DIMENSION

Table 2. (Continued)

C	OVERLAY LEVEL	ROUTINES
C	-----	-----
C	A	INIL
C	L	PBST
C	B	GTDA, GEOD, PDRD
C	B	HPD ^Y , HPLU
C	C	BLOC, INIT, TRAC
C	C	PDEX
C	C	POUT, CLTE
C	B	PBL1, CALT
C	PROGRAM STORAGE REQUIREMENTS	
C	USE	SHORT WORDS
C	---	-----
C	PROGRAM	17,000 (33,000 WITHOUT OVERLAY)
C	SYSTEM ROUTINES	6,000
C	MINIMUM DATA ARRAYS	20,000
C		-----
C	TOTAL	43,000
C		

Normally the heat source is the power density data file generated by the VENTURE neutronics code in this computation system. Power density data for the calculation of pebble temperature distribution is produced by the exposure code BURNER. This code also generates the neutron flux exposure (Fluence) data required for the prediction of pebble thermal conductivities. Temperature data generated by the PEBBLE thermal hydraulics code may be used by the other codes to account for the dependence of nuclear microscopic cross sections (temperature feedback). A single geometry description and mesh point arrangement is used by the codes.

In a typical calculation, the steady state continuous fueling reactor core problem is solved by an iterative process that establishes the neutron flux distribution, the nuclide atom density distributions, and the required fuel feed rate to the reactor. This calculation is done in (RZ) geometry assuming azimuthal symmetry of the cylindrical core. The results are used by the thermal hydraulics code PEBBLE to establish the gas coolant flow distribution. The calculated temperatures are then available for assessment and feedback if desired. Subsequent calculations may then be done for such auxiliary results as predicting the effect on the neutron multiplication rate of a power level change (the power coefficient of reactivity).

With this system of codes, the neutron flux level in the reactor core is normalized such that the desired power level is obtained given the energy per fission and capture reactions. This desired power level may be given for a whole reactor while the problem treated is not for the whole

core, so a fraction is specified. In one-dimensional axial traverse problems, the appropriate fraction is the reciprocal of the reactor cross sectional area. With (RZ) geometry the full reactor is represented, the integrals done for the $(2\pi r dr)$ volume element (full θ). Often the energy data supplied to the neutronics problem represents ideal recovery, so a fractional recovery number is specified, usually smaller the smaller the core. The thermal power is increased above the desired value to allow for losses. When power densities are calculated, this loss is not included, so an integral of the power density data yields the reactor (actually problem) power before unrecoverable losses. Such a degree of freedom likely causes more confusion than it is worth, but then the recoverable fraction is usually quite large unless plant requirements are taken out for a small plant.

Given the file of point power density data, this data is used. If this data is not available, available zone, subzone average power density data will be distributed uniformly. Data availability is determined by the presence of the associated data file name in the interface data file tables. Note also that zone, subzone average power density data is used for the calculation of pebble temperatures. Lacking this data file, zone averages are calculated from the point power density file, but subzone data can not be produced nor void fractions extracted. Pebble temperatures are calculated for reference conditions, then for a ten percent reduction in thermal conductivity, and then for apparent near worst case conditions. In the latter, the peak power density data (if available) and the local peak surface temperature are used as calculated for the average power density.

Note that this is not the same thing as taking all worst conditions. Combining conditions that individually are the worst is probably more reasonable for heat removal assessment (although not grossly conservative as might be desired for safety analysis).

In calculating the pebble temperature distribution, a correlation is applied that approximates the effect of exposure to the neutron flux (fluence) at a reference temperature on the thermal conductivity. With pebbles moving through the reactor, there is a drastic change in the exposure temperature and an accumulation of fluence that reduces the conductivity. Further the conductivity at any time depends on the current temperature. This calculation accounts for variation across the pebble at the average zone conditions.

Perturbations present an analysis challenge. Let us assume that an effect of flow rate change is to be determined. If this change is to apply over the history, then a full recalculation must be done. If the perturbation to apply currently, then proper account must be taken of the effect on thermal conductivity and indeed data must be saved after the reference calculation for use in a subsequent calculation.

Consider that the effect on the core multiplication (reactivity) is to be determined for a power level change to support core control, stability analysis. A calculation would be done for reference conditions with temperature feedback accounted for in the core neutronics problem. Then the power level would be changed (at least enough to be significant), and likely the coolant flow rate also altered (as by retaining average core

inlet and outlet coolant temperatures). The calculations would then be redone for the perturbed conditions with account for temperature feedback (but fixed pebble management and compositions). This calculation would be correct only if account were taken of the effect of the current temperature on the pebble thermal conductivity but not a change in the temperature, exposure history effect, requiring data storage and recovery.

Some perturbations are simple to make, but often the thermal hydraulics problem must be solved over again. It is quite generally cost effective in solving such problems and also those involving global iteration loops to save results and recover them for problem initialization.

The flow of gas coolant is in a fixed direction relative to the coordinate system, from top to bottom in the sense that the inlet is at l_1 and the outlet at l_2 , $l_2 > l_1$. Since the neutronic/exposure model of pebble flow is by increasing zone number, the pebble and gas move in the same direction, down, if the mesh indexing increases for the increasing zone numbers along each path. To model upflow of the gas and downflow of the pebbles would require that the mesh indexing of the zones decrease, and, of course, special considerations about the inlet (bottom instead of top) and outlet (top instead of bottom) be accounted for in the neutronics problem description that includes the geometric arrangement and material assignments.

At any location there may be only one "zone" material representing a specific pebble type and composition and having an associated power

density. A second type of pebble may be considered at the same location (in the sense of homogenization of randomly arranged pebbles) with the "subzone" material. Indeed a zone may contain one or none "zone" material pebbles and any number of "subzone" material pebbles. A typical model of the THTR reactor involves six subzone pebble materials at each location representing different exposure stages (six passes) but no zone material pebbles. Two types of pebbles may be involved, as when one is to be loaded with more fertile material and perhaps less fuel than the other, or when recycle and fresh fuel are to be kept separate for recycle and discard considerations. Typically one pebble would be modeled as zone material and the other as subzone material. It is quite unlikely that consistent calculations will be done for complicated situations unless much care is taken to study the requirements and to eliminate discrepancies. Volume fractions are involved and void fractions may be calculated from zone/subzone data (must be if they vary in space), so what may well be adequate for the neutronics calculation may not be adequate for the thermal hydraulics. Check the requirements. Proof the input data. Check the results.

Remarks are offered about major changes within the problem. It is the author's view that considering the equations applied in difference form, the effects of large variations will be but approximated and perhaps not very well. Small local mesh spacings are deemed undesirable at best. Large changes in the void fraction are apt to produce unrealistic results. The user should be aware of the nature of the formulation: first and second order derivatives are approximated directly. Accuracy depends to

some extent on these derivatives changing slowly. A case inviting special concern is that of the programmed blockage calculation. Seldom will a ring of blockage about the reactor be of interest. This leaves only blockage at the centerline as being of significant interest. Full blockage would mean no fluid flow, no heat removal except by secondary mechanisms, and extreme temperatures likely better calculated by more direct means. Do not expect accurate results by assigning blockage to a single mesh interval.

Given converged results, the only reliability checks available to the user regarding the representation of a specific situation with the programmed equations are reducing the mesh spacings and performing calculations for perturbed conditions. The informed user will have gained experience and confidence by solving a series of simple problems admitting interpretation of the results as being realistic or not.

Shown below are results for a reference case illustrating the effects on solution and on solving a few-zone problem of varying the number of mesh points:

Core Meshpoints (RxZ)	Pressure Drop (Atm)	Error in the Overall Heat Balance (Percent)	Peak Exit Coolant (850 mean)	Temperatures (°C)				
				Peak Pebble Surface		Fuel (Hr. v. Metal)		
				Local	Zone Average	Average	Zone Peak	Local Extreme
8 x 4	0.6895	-0.049	957.9	987.4	923.2	672.2	977.0	982.6
16 x 8	0.6918	-0.030	905.8	927.3	881.6	672.2	931.2	957.8
32 x 16	0.6939	0.002	932.9	951.1	858.4	672.2	906.3	970.7
64 x 32	0.6943	0.002	959.8	977.5	851.6	672.2	898.9	1008.2
128 x 64	0.6940	-0.054	970.5	978.8	848.0	672.1	896.2	1016.7
Extrapolate (=)	0.694		974.	979.	847.	672.	894.	1020.

A better resolution of pebble temperatures would be obtained, of course, if the problem were subdivided into more zones. It should be noted that the power density data produced by the neutronics code depend on the mesh. The calculation is for a period of exposure at a uniform loading possibly representative of a start up state for a situation where there is considerable void fraction variation. The increasing peaking indicated with reduced meshspacing is a local effect near the reflector. With higher resolution comes a more accurate distribution of the power density. However, a large void fraction is associated with the edge of a bed of pebbles in the containment vessel. Likely higher flow occurs here and some mitigation of the peaking. Note the attempt to extrapolate the results to estimate the result free of finite-difference error. Additional information about the computer use is shown below:

Core Mesh Points (R _x Z)	IBM-3033 Memory (Short Words)	k _{eff}	Neutronics Problem		Thermal Hydraulics Problem	
			Iterations (Inner times outer)	Computer Processor Time (min)	Iterations	Computer Processor Time (min)
8 x 4	4,000	1.0143	33	0.04	79	0.05
16 x 8	6,500	1.0157	88	0.11	44	0.08
32 x 16	22,900	1.0167	149	0.47	59	0.37
64 x 32	86,100	1.0170	302	2.92	122	2.79
128 x 64	334,000	1.0171	483	15.48	284	25.28

It is noted that the thermal hydraulics problem has roughly the same computation burden as the neutronics problem. The latter had a four group energy structure and the problems were solved in the space-stored mode (inner iteration done at each energy with data transferred once).

Information about the radial flow component is shown below:

Mesh Points (RZ)	Maximum Relative Coolant Flow Rate, Radial Component ^a	Axial/Radial Location (fraction of overall dimension)
8 x 4	+ 0.00747	0.500/0.625
16 x 8	+ 0.00425	0.500/0.500
32 x 16	- 0.00274	0.312/0.938
64 x 32	- 0.00325	0.281/0.938
128 x 64	+ 0.00461	0.500/0.562

^aRelative to the coolant inlet mass flow rate.

A local peak of the radial component of the flow rate occurs at location (0.219/0.938) and has a value of -0.00329 from the finer mesh case. Thus the resolution of the radial flow component is poor with a coarse mesh. Further data presented below for clarification shows the values of the radial component of the flow rate at specific locations as dependent on the mesh:

Mesh Points (RZ)	Location, Axial/Radial				
	0.25/0.25	0.75/0.25	0.5/0.5	0.25/0.75	0.75/0.75
8 x 4	0.00227	0.00363	0.00741	0.00300	0.00488
16 x 8	0.00218	0.00199	0.00425	0.00209	0.00201
32 x 16	0.00131	0.00109	0.00200	0.00023	0.00043
64 x 32	0.00115	0.00095	0.00204	-0.00017	0.00020
128 x 64	0.00149	0.00202	0.00446	-0.00003	0.00088

These results leave one with serious doubt about the accuracy of any result when the radial flow rate makes a significant contribution. Apparently a very fine mesh point spacing is necessary to effect high resolution of the radial flow rate. There may be no serious difficulty when there is but modest variation in the properties such as void fraction and in the heat source, and especially when such changes occur only gradually. It is not clear that the stream function approach is adequate to properly account for radical changes and discontinuities.

Results obtained for a situation of flat radial power density distribution are shown below (coarse zone allocation, only two along each axial traverse):

Axial Intervals	Peak Temperature ($^{\circ}$ K)			Temperatures ($^{\circ}$ K) at 5/6 from top		Pressure Drop (Atm)
	Bulk Coolant	Pebble Surface	Fuel Center	Coolant	Surface	
6	1123.9	1137.8	1189.2	1090.6	1115.6	0.6635
12	1123.2	1130.7	1191.6	1089.6	1115.7	0.6551
24	1123.3	1128.6	1190.9	1089.8	1116.1	0.6573
36	1122.9	1128.9	1191.1	1089.9	1116.2	0.6554
48	1122.8	1128.9	1191.1	1089.9	1116.2	0.6551

Note that even the 12 interval results are relatively good, generally adequate for most any purpose. Integral results are quite similar. For example an effective fuel temperature of 948.6 °K was obtained by weighting with the power density in each case (four significant figures). The calculated pressure drop shown for the 24 axial intervals just happens to be poorly converged due to less effective asymptotic extrapolation of the iterate pressure results in this case.

The dependence of the pressure drop on the equation coefficients is shown below over a range of Reynolds number:

R_e	Bartheis (1972) $\frac{300}{R_e} + \frac{5.71}{R_e 0.095}$	Achenbach (1980) $\frac{320}{R_e} + \frac{6}{R_e 0.1}$	Ergun (1952) $\frac{300}{R_e} + 1.75$
10	30+4.588=34.59	32+4.766=36.77	31.75
100	3+3.687=6.687	3.2+3.786=6.986	4.75
1,000	0.3+2.962=3.262	0.32+3.007=3.327	2.05
10,000	0.03+2.380=2.410	0.032+2.389=2.421	1.78
100,000	0.003+1.913=1.916	0.003+1.897=1.901	1.753

Thus the German data indicates a significantly higher pressure drop than the old Ergun correlation, the more recent Achenbach correlation yielding slightly higher values than the Bartheis correlation, but not significantly different at the high R_e values of primary interest.

ON STORAGE, WORD LENGTH, AND DATA TRANSFER

As received, the code was written mostly in IBM double precision. The primary iteration calculation was left in double precision to enhance acceleration procedures, significantly better solutions not expected. Mixed precision is rather difficult to work with, especially when storage for data arrays is allocated as needed and overlapped as possible to reduce the total requirement, and usually compiled programs execute less efficiently than if all in double precision and of course slower than if all single precision. For a problem of size $I \times J$, storage involves

8($I \times J$)	primary data arrays
3($I \times J$)	arrays for extrapolation
12($I \times J$)	secondary data arrays

The original code had 11 primary arrays and none for extrapolation; with all in double precision, the storage requirement was $46(I \times J)$ short words. Using IBM single precision for the secondary data arrays reduces this to $34(I \times J)$, a reduction of 26 percent.

A problem from routine core analysis effort had $I \times J = 38 \times 55 = 2,090$ mesh points requiring primary storage of 71,060 short words (actual total data storage 79,013 compared with the original requirement of over 100,000).

No data transfer from auxiliary storage is programmed within the iteration procedure, all required data and results are stored. With the recent change in operation of the local computers to virtual memory, such

transfer is handled by the operating system when the data exceeds the memory size. Likely a representative problem can be contained, so data transfer is necessary only for the larger problems, and the amount of data to be transferred would usually be modest so that the virtual memory type of operation should be fairly efficient.

It became evident early in this effort that saving the iterative results in one computer run and recovering them later would be a needed capability. In the event that an adequate level of convergence is not achieved, saving and recovering the data later would avoid the complete loss of the initial investment in computer time. The programmed procedure with default values of the coefficients and choices between the alternatives could prove quite ineffective in a specific application. Of course such restart capability is likely of little utility if the attempt is being made to use the results in additional calculations, as for temperature feedback into the nuclear properties. On the other hand, if a series of similar problems are being solved such as in an iteration loop to completely resolve the temperature feedback problem, then starting with the results of a previous calculation may well be the most efficient procedure and significantly reduce computation costs.

Adding restart capability required about three days work plus one day validation and one day documentation, along with other effort over a two week period. Considerable thought went into the requirements over recent months, how it should be done and where. This time of implementation was minimized by a thorough understanding of what was needed and how this capability could be made available, intimate familiarity with the code and

with the requirements for making data files satisfy the modular code system requirements. Only by a concentrated effort was an effective procedure implemented with relatively straight forward logic. Quite different procedures were required for the one- and two-dimensional routines, and recovery of the pebble thermal data presented quite a challenge. Saving data on a disc is of course trivial; the recovery within a data management system in a flexible and very useful way takes time and so does careful documentation.

About two months went into modifications for treating the prismatic core, flow through holes.

ACCELERATION OF THE ITERATIVE PROCESS

The attempt to accelerate the iterative process was quite frustrating and time consuming. Lacking an applicable theoretical treatment in any detail, error vector analysis, it is not possible to outline an effective procedure. Thus a straight forward formulation could not be given to a programmer for implementation nor even be implemented by this originator. It was not known how much of the original programming would have to be redone until well into the effort. Experimentation was necessary and the success of such was rather hampered by the attempt to rush the process causing extensive testing of procedures that should obviously have been identified as inferior or contained flaws.

No doubt a superior acceleration procedure can be found for a specific problem with account of its behavior under a preferred scheme of iteration.

The attempt, however, was to implement a procedure that showed good performance for a variety of problem types. Extensive and primary testing was done of course with small problems. Only limited experience could be gained with the larger problems to be expected in application due to the high computer cost. The test problem available from the originator contained 22 radial and 25 axial mesh points while the reference case, chosen as representative of application, contained 38 radial and 55 axial points, nearly four times as large. Special cases for testing included one with a uniform distribution of the power density radially, for which the core diameter was varied (to change the height to diameter ratio), the bare reactor core which has an extreme radial power density distribution, and an annular core with nearly a flat radial power distribution.

It is beyond the coverage of this document to present the full details of the iteration procedure available in a Fortran source program listing. At the time this report is being written, the procedures are yet being modified in detail and are subject to major changes should significant improvement be found possible. Involved are constraining the calculated changes in the variables, under/over relaxation to dampen or drive the iterate estimates, and adjustment of the coefficients in an attempt to move toward the optimum, and asymptotic extrapolation.

Each iteration new values of the four primary dependent variables are calculated from difference equations for the discrete mesh approximating the differential equations. These variables are the stream function, the fluid bulk temperature, the pebble surface temperature, and the coolant pressure: ψ , (T_b, T_s) , P , where the temperatures are grouped to indicate a

very close dependence. The equations are quite modified from the original form, for example the two equations for T_b and T_s take the form of two equations for two unknowns and hence are solved simultaneously if the coefficients have numerical significance. So we can consider T_s calculated from the latest estimate of T_b , and there being three primary variables ψ , T_b and P . It was found that given a reasonable approximation for the spatial variation in P , that ψ and T_b have little dependence on changes in P but do depend on each other. Specific aspects of the procedures for acceleration are now discussed. It should be noted that new values of the four primary variables are all obtained at each mesh point in a single sweep loop rather than as done separately over the mesh in the original code.

CONSTRAINTS

Since the axial and radial coolant flow rates are first derivatives of the stream function ψ , a large local change in ψ causes a severe perturbation in the flow rate locally. Various schemes were tried to dampen out such perturbations of most concern in the early iterative history. Good initialization, restraining changes in ψ , dampening calculations of the derivative, σ_1 sweep order discussed below, and restraining asymptotic extrapolation have all been used. Generally a limit of 10 percent increase or decrease in any new iterate estimate was imposed, and a limit of a 50 percent change in the coolant density (after the initial estimate is made) was imposed. A relatively accurate initial estimate is made of the coolant pressure and a reasonable approximation of the axial coolant flow rate with neglect of axial variation in the radial component.

EQUATION SOLVING AND SWEEP ORDER

Generally we expect the use of newly calculated values of the primary variables to accelerate the rate of convergence over use of old values. With a normal ordered sweep, one starts calculating at the first point and proceeds along the first row in order or alternatively along the first column, etc. The result of such a procedure is skewing of the error content into a corner. Also it is not clear whether the required derivatives should be estimated from the past iterate values or using the latest values. With acceleration, one finds that a front of discontinuity moves back across the problem that would appear to cause havoc with estimates of the derivatives. So we expect that flow rate estimates from derivatives of the stream function should be based on the previous iterate set of ψ values and that σ_1 ordering will generally be superior for rapid elimination of the error vectors that dominate in the early history.

. X . X . X X . X . X . X . X .X	Consider the sketch of a group of mesh points in a regular two-dimensional array. Alternate points are shown as X. With only nearest neighbor coupling a point marked \cdot is surrounded by points marked X. With σ_1 sweep ordering, new iterate estimates of the primary variables are obtained at all points marked \cdot in one sweep and then the same is done for all points marked X in a second sweep. Roughly half as many iterations are required by this procedure for full propagation of all boundary conditions as are necessary with normal sweeps (each mesh point senses even the most remote boundary). This leaves some question regarding the optimum estimation of
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derivatives. Flow rates are estimated using only the previous iterate set of ψ values, but otherwise latest values are used.

Given J radial and I axial points, propagation of the remote boundary occurs after $I+J$ iterations with normal ordered sweeps and roughly half that with σ_1 ordering.^a An acceptable level of convergence can be expected only after a few such propagating sweeps. Note the data below:

<u>I+J</u>	<u>3(I+J)</u>
4 (minimum)	12
40	120
400	1200

Thus we expect the number of iterations required to effect an acceptable level of convergence to increase as the number of mesh points increase.

UNDER/OVER RELAXATION

Given iterate estimates of a variable x at location I and iteration n , the equation applied is

$$x_i^n = x_i^{n-1} + \beta_n(x) \left[x_i^{n*} - x_i^{n-1} \right]$$

Where x_i^{n*} is the newly calculated value and $\beta_n(x)$ is the coefficient for this variable and this iteration. Note that $x_i^{n*} - x_i^{n-1}$ is the change in the value of the variable at a location for iteration n , and if $\beta > 1$, the change is increased as an acceleration while if $\beta < 1$, the change is decreased as a dampening technique.

^aLimited testing however did not indicate a general gain from σ_1 ordering over normal ordered sweeps along the flow direction.

Initial values of the coefficients are selected that reflect the expectation that the larger the problem the more difficult it will be to solve. Typical values are:

Variable	\sqrt{J}	Value of β	
		12	50
ψ		1.125	1.3489
T	Upwind difference	0.0932	0.4666
	Central difference	0.233	1.167
T		1.0	1.0
P		1.275	1.4989

Thus the largest coefficient is used for the pressure, next for the stream function, the surface temperature estimate is used as calculated, and dampening is done to the bulk temperature. Much stronger underrelaxation is done with central difference than with the upwind difference formulation. Modest changes are made in these coefficients (5 percent) if deemed desirable from the iterative behavior.

The primary measure of behavior is the maximum relative iterate change in a variable,

$$\epsilon_n(x) = |\max| \left(\frac{x_n - x_{n-1}}{x_{n-1}} \right)$$

For a convergent process we expect

$$|\epsilon_n(x)| < |\epsilon_{n-1}(x)|,$$

but relax this and require

$$|\epsilon_n(x)| < |\epsilon_{n-m}(x)|,$$

where currently $m=3$ is used, but 2 and even 1 are often used, the situation depending on the stability or lack thereof, and on the effectiveness of the initialization procedure. The coefficient is decreased if the above

criterion is not satisfied indicating instability on a cycle of iteration count limiting changes to β . A special indication of overacceleration is judged to be continuing change in sign,

$$\epsilon_n(x) \epsilon_{n-1}(x) < 0 .$$

One might expect that the core pressure drop would converge to a value. Use of the relative iterate change in the core pressure drop has not proven useful in judging the behavior; it may increase during a convergent process. (An overall heat balance has proven even less useful. With an axial flow rate balance forced it is not available as a variable locally across the core nor at the exit.)

The coefficients are increased if a dominant single error vector appears to establish as discussed below. If one is reduced, a maximum value is set (at half the sum of the old and new values) as an upper limit for subsequent increases replacing extreme upper limits set initially.

An attempt is made using maximum relative changes to identify which of the variables (and its coefficient) is driving non-convergent behavior. An automatic iteration count delay is used between iterations when the coefficients are changed. Also the coefficients are set smaller for the first few iterations in an attempt to stabilize the initial behavior.

ASYMPTOTIC EXTRAPOLATION

It is assumed that with continuing iteration a dominant error vector will become evident and can be removed, for iteration n , mesh point l and error vector contribution j ,

$$\begin{aligned} x_i^n &= x_i^\infty + \sum_j \lambda_j^n(x) A_{i,j}(x) \\ &\approx x_i^\infty + \lambda^n(x) A_i(x) \end{aligned}$$

as n increases because $\lambda^n \rightarrow 0$ for $\lambda < 1$. Thus at each point we expect asymptotically from the recursion relationship

$$\lambda(x) = \frac{x_i^n - x_i^{n-1}}{x_i^{n-1} - x_i^{n-2}},$$

and

$$x_i^\infty = x_i^n + \left(\frac{\lambda(x)}{1-\lambda(x)} \right) (x_i^n - x_i^{n-1}).$$

If contamination (error in the iterate estimate) is from a single error vector, this can be extracted leaving a clean solution. Judgement must be made regarding whether or not such a state exists and an accurate estimate of the error vector eigenvalue λ is necessary. It may be noted that often the values of $A_{i,j}$ associated with the largest eigenvalue $\max \lambda_j$ are quite small so that it may surface only late in the iterative history, another surfacing early. Thus estimates of $\max \lambda_j$ tend to change from small to large. If $\max \lambda_j$ is 0.9, the iterative process is rapidly convergent, the error contribution decreasing by 0.9 each iteration. If it is 0.99, the process is slow. The number of iterations required to reduce the error contribution by a factor of Y is given by

$$\begin{aligned} \lambda^N &= Y, \\ N &= \frac{\ln Y}{\ln \lambda}. \end{aligned}$$

Thus for γ of only 0.01, if $\lambda = 0.9$, $N = 44$, while if $\lambda = 0.99$, $N = 458$. Thus it is important to suppress error vectors having large eigenvalues. With effective single error mode extrapolation the error decay goes essentially as the next to largest error vector eigenvalue.

Note that for extrapolation as formulated the latest iterate change is multiplied by $\lambda/(1-\lambda)$, sensitive to $1-\lambda$ as λ approaches unity. Thus a reasonable test of convergence of iterate estimates of λ (and indication that a single error vector dominates) is

$$\left| \frac{\lambda^n(1-\lambda^{n-1})}{\lambda^{n-1}(1-\lambda^n)} \right| < \epsilon_\lambda$$

where n refers to iteration (not an exponent).

The L_1 norm estimate is used,

$$\lambda^n(x) = \frac{\sum_i |x_i^n - x_i^{n-1}|}{\sum_i |x_i^{n-1} - x_i^{n-2}|}$$

Typically some dampening is applied,

$$\lambda_e^n(x) = \left[\lambda^n(x) \lambda^{n-1}(x) \right]^{1/2}$$

Expecting ψ and T_b to have a common behavior,

$$\lambda_e^n(\psi, T_b) = \left[\lambda^n(\psi) \lambda(T_b) \right]^{1/2}$$

And this effective value is given preference (not for pressure).

Note that previous iterate values are required for the variables to be extrapolated. A number of simplifications and approximations may be made

to avoid using extra storage. However, the final scheme in use requires storage for the previous iterate values of ψ , T_b and P . Initially T_s was not extrapolated, but finally the scheme used was

$$\Delta T = \left(\frac{\lambda}{1-\lambda} \right) (T_b^n - T_b^{n-1}) ,$$

$$T_b^\infty = T_b^n + \Delta T ,$$

$$T_s^\infty = T_s^n + \Delta T ,$$

apparently effective.

It should be noted that it is possible for a simple error vector to establish only if the same thing is done each iteration. The procedure must not be changed nor the coefficients. A delay time in iteration count is used after any change is made before allowing another extrapolation or adjusting the under/over relaxation coefficients. When the criteria for the presence of a simple error vector are satisfied, the under/over relaxation coefficients for ψ , T_b , and P are increased individually if extrapolation is done for that variable. Thus the assumption has been made that if the problem is driven hard enough, a simple error vector will not exist, although this is not necessary for the procedure to be effective.

The extrapolation process is constrained. Knowing the maximum relative flux change, negative values of the variables can be avoided, and a simple upper bound is also used,

$$\text{for } x = x^n + F_n (x^n - x^{n-1}),$$

$$F_n = \min \left[\frac{\lambda_n}{1-\lambda_n}, \frac{0.1}{\epsilon_n}, 500 \right].$$

The routine that contains the primary iteration in this code ranged around 10 pages of Fortran listing, over 500 statements plus comments. The local compiler handles this using the default memory size of 270K bytes (69,000 short words). Note that shorter routines could be more efficient with tight loop structures, but could not be viewed as desirable (might or might not make the logic easier to follow). It became a continuous chore as changes were made to tighten this routine to avoid exceeding the compiler capacity (limit in table storage). Actually such tightening was probably good, a desirable exercise that is often not done. It took only about six times for the rather obscure system error message to be printed out indicating capacity exceeded before the author learned to recognize it. Finally the routine was split into two.

CONVERGENCE LEVEL

The iterative process is assumed to be adequately converged if

$$\epsilon_c = \max | \epsilon_n(\psi), \epsilon_n(T_b), \epsilon_n(T_s), \epsilon_n(P), 0.1 \epsilon_n(\Delta P) |$$

is less than the specified or default convergence criteria, where ΔP refers to the pressure drop across the core.

It may be noted that if there were a single error vector present, an absolute error estimate of any point variable would be available,

$$\epsilon_{ab} = \epsilon_n \left(\frac{\lambda_n}{1-\lambda_n} \right),$$

and such is reported as a convergence estimate. Unfortunately the nearer λ_n is to unity, the smaller ϵ_n needs to be to effect the same absolute error convergence level.

EQUATIONS

A loss of energy is associated with coolant flow through a packed bed causing a pressure drop. The variable cross sectional area is a dominating feature. The selected¹ differential equation for the steady state condition is

$$\nabla P = -G\theta + \rho g \quad , \quad (1)$$

where the last term is due to gravity (vertical flow),

P is the pressure

G is the mass flow rate

ρ is the density,

g is the gravitational constant, and

$$\theta = \frac{2B}{\epsilon^2 \rho D_h} \left[\frac{2A\mu\epsilon}{BD_h} + \left(\frac{3.65 \times 10^4}{Re} \right)^{0.095} |G| \right] \quad , \quad (2)$$

where A and B are constants,

μ is the fluid dynamic viscosity,

ϵ is the void fraction,

D_h is the effective hydraulic diameter,

$$D_h = \frac{D_p}{3} \left(\frac{\epsilon}{1-\epsilon} \right) \quad , \quad (3)$$

where D_p is the pebble diameter.

It may be noted that the Reynolds number

$$R_n = \frac{DG}{\mu} \quad (4)$$

or an effective value

$$R_e = \frac{DG}{\mu(1-\epsilon)} \quad (5)$$

is not simply involved (in the first term). The above formulation is used to correlate recent German pressure drop measurements. For the older US data, the term in Eq. (2) involving the R_n to a small power is dropped and a larger value of B is used causing the pressure drop to be estimated to be about 50 percent more than with the German correlation. Typically the value of θ depends primarily on the second term in the brackets of Eq. (2), the inertial term.

A test was made to see the effect of varying the value of the hydraulics equation coefficient A while coefficient B was assigned a fixed value of 0.1754 and the term involving the relative Reynold's Number raised to the 0.095 was included (revision from original code):

Value of A	Pressure Drop (Atm)	Peak Temperature ($^{\circ}$ C)	
		Outlet Coolant	Heavy Metal
4.1666	0.6597	1150.1	1121.1
24.5	0.6768	1153.9	1120.6

Thus the linear term (and the associated coefficient A) plays but a small role, although the effect of its variation on the coolant outlet temperature is larger than was expected and indicates the magnitude of one source of uncertainty.

The continuity of mass equation in (RZ) coordinates is

$$\frac{\partial}{\partial r}(r G_r) + \frac{r \partial}{\partial z} (G_z) = 0 ,$$

where G_r is the radial component of the mass flow rate, and

G_z is the axial component;

$$|G| = [G_r^2 + G_z^2]^{1/2} . \quad (6)$$

Consideration of the continuity equation leads to the stream function ψ , formulated as

$$G_r = - \frac{a}{r} \frac{\partial \psi}{\partial z} , \quad (7)$$

$$G_z = \frac{1}{r} \frac{\partial \psi}{\partial r} , \quad (8)$$

where a is the ratio of bed radius to height making the coordinate references relative.

In this application, the equations are to be applied to an upright cylinder with flow from the top or the bottom. Operating on Eq. (1) with the divergence operator leads to the following pressure balance equation:

$$\frac{\partial^2 p}{\partial r^2} + \frac{1}{r} \frac{\partial p}{\partial r} + \frac{a^2 \partial^2 p}{\partial z^2} + C_1 \left\{ a G_z \frac{\partial \theta}{\partial z} - G_r \frac{\partial \theta}{\partial r} \right\} - a g \frac{\partial \rho}{\partial z} = 0 , \quad (9)$$

where the sign of the last term depends on the flow direction.

The $\nabla \wedge$ operation on Eq. (1) eliminates the pressure term and yields a differential equation for the stream function,

$$a^2 \left(\frac{\partial \theta}{\partial z} \frac{\partial \psi}{\partial z} + \theta \frac{\partial^2 \psi}{\partial z^2} \right) + \left(\frac{\partial \theta}{\partial r} - \frac{\theta}{r} \right) \frac{\partial \psi}{\partial r} + \theta \frac{\partial^2 \psi}{\partial r^2} = 0 . \quad (10)$$

A heat balance on the fluid yields a equation involving the bulk fluid temperature,

$$\frac{1}{r} \frac{\partial}{\partial r} \left(r K_{br} \frac{\partial T_b}{\partial r} \right) + a^2 \frac{\partial}{\partial z} \left(K_{bz} \frac{\partial T_b}{\partial z} \right) + C_2 \left[G_z \frac{\partial T_b}{\partial z} + G_r \frac{\partial T_b}{\partial r} \right] + C_3 H (T_s - T_b) = 0 \quad (11)$$

where K_{br} is the effective radial bulk thermal conductivity coefficient,

K_{bz} is the same axially,

H is the bulk film coefficient,

T_b is the bulk fluid temperature, and

T_s is the pebble surface temperature,

and the film coefficient on the basis of volume rather than surface area is correlated through a Nusselt/Reynolds number correlation.

A heat balance on the solid phase (in a gross sense neglecting local temperatures that would affect the gross transport of heat in the solid phase) yields

$$a^2 \frac{\partial}{\partial z} \left(K_e \frac{\partial T_s}{\partial z} \right) + \frac{\partial}{\partial r} \left(r K_e \frac{\partial T_s}{\partial r} \right) + C_3 H (T_b - T_s) + C_4 q = 0, \quad (12)$$

where K_e is the effective solid phase thermal conductivity and q is the heat source per unit volume.

These equations are cast in a somewhat different form than as programmed in the code as received. For example, use was made of the relationship

$$\frac{\partial}{\partial z} \left(A \frac{\partial B}{\partial z} \right) = \frac{\partial A}{\partial z} \frac{\partial B}{\partial z} + A \frac{\partial^2 B}{\partial z^2}$$

to recast the equations into what would appear to be a more accurate and effective form.

Equations (9-12) are four second order, non-linear equations coupled through the dependent variables. The primary dependent variables are the pressure P , the stream function ψ , the bulk fluid temperature T_b , and the pebble surface temperature T_s . The mass flow rate and its radial and axial components are given by the auxiliary Eqs. (6-8). Note that the stream function ψ appears explicitly only in Eq. (10), the equation used for its solution. Derivatives of the stream function divided by the radius are used directly for the axial and radial components of the mass flow rate.

Each of these four equations is recast in a finite-difference form which in turn is recast to yield an iterate estimate of the value of the variable at a mesh location based on current estimates of the values of the other variables and their derivatives.

Somewhat involved difference equation forms are involved. It is assumed that usually adjacent mesh spacings will be similar. Otherwise reliable forms to estimate derivatives are not assured. Generally these equations reduce to simple forms with a grid of mesh points that tends to assign equal elemental areas to mesh points (equal $\Delta(r^2)$ intervals instead of Δr , equal axial intervals). For mesh location l axial and j radial,

$$\frac{\partial x}{\partial z} \Big|_{l,j} \approx \frac{x_{l+1,j} - x_{l-1,j}}{z_{l+1} - z_{l-1}},$$

$$\left. \frac{\partial^2 x}{\partial z^2} \right|_{i,j} = \frac{\left(\frac{x_{i+1,j} - x_{i-j}}{z_{i+1} - z_i} \right) - \left(\frac{x_{i,j} - x_{i-1,j}}{z_i - z_{i-1}} \right)}{\frac{1}{2} (z_{i+1} + z_i) + \frac{1}{2} (z_i + z_{i-1})}$$

And so on. Thus the iterate form for the iteration n estimate of variable x for a solution of the one-dimensional equation

$$\frac{\partial^2 x}{\partial z^2} + C \frac{\partial x}{\partial z} + S = 0$$

with uniform mesh spacing Δ would be

$$x_i^n = \frac{\Delta^2}{2} \left\{ (x_{i+1}^n + x_{i-1}^n) \left(\frac{1}{\Delta^2} + \frac{C}{2\Delta} \right) + S^h \right\}$$

where superscripts refer to iterate estimates (not exponentials), and use of the latest iterate estimate is considered with a sweep along increasing index.

Certain global requirements are known. Thus incorporated into the procedures was the accounting to renormalize the axial mass flow rate at each row of points each iteration such that the radial integral equaled the total inlet. Similarly the values of the outlet pressure are set equal to the integral (rdr integral) average each iteration. Attempts to force a global heat balance proved unsuccessful (redundant constraints prevent convergence) so that the results contain an error due to the finite-difference representation.

It should be noted that the formulation ignores the effect on the flow distribution of the containing surface. Clearly the value of the radial component of the mass flow is zero at the values of $r=0$ and $r=R$,

$$\left. \frac{1}{r} \frac{\partial \psi}{\partial r} \right|_{r=R} = 0,$$

and also

$$\frac{1}{r} \frac{\partial \psi}{\partial r} \Big|_{r=0} = 0 .$$

although the latter is a bit difficult to enforce directly. Evidently $\partial \psi / \partial r$ approaches zero more rapidly than r approaches zero. It is informative to examine the case of uniform conditions, $G_z = \text{constant}$, $G_r = 0$.

$$G_z = \frac{1}{r} \frac{\partial \psi}{\partial r}$$

$$\psi(r_2) = \int_{r_1}^{r_2} r' G_z dr' = \psi(r_1) + \frac{1}{2} (r_2^2 - r_1^2) \bar{G}_z \quad (13)$$

Thus we expect $\psi(0)=0$ and where $r=R$, $\psi(1)=1/2$.

It is noted that the void fraction at the edge of the bed tends to be large due to the edge effect on packing. Thus the amount of flow near the outside of the bed may indeed be high and heat removal efficiency low (rather than the flow be low due to the effect of the surface of the containment). The effect may be appreciable due to the large area involved (the cross sectional area goes as rdr). Experimental measurements are of considerable importance, and indeed special surface conditioning may be desirable, for coolant and pebble flow. It could be found to be practical to pass smaller pebbles near the containment to prevent a high coolant flow rate here. These pebbles could be loaded heavily with fertile material to effect blanketing and also provide shielding of the radial reflector from high energy neutrons to reduce damage.

The point to be made here is that only limited information can be produced about flow conditions near the containment vessel with this code without further development.

Blockage calculations can be made, but only partial blockage and only about the location $r=0$ makes any sense within the model (an annular block about the core over a range of $r_1 < r < r_2$ is not interesting, and the model is inadequate for treating the local flow condition of zero). For an accurate representation, central blocking must extend to at least the second radial mesh point because of the way derivatives are calculated.

The code was modified to admit solutions for the annular core. Unfortunately the stream function formulation may simply be inadequate. Setting the values of $\psi=0$ at $r=0$ and $\psi=0.5$ at $r=1$ is nice for the cylindrical problem, while enforcing derivative conditions was not found to be simple. For the annular problem, $\psi|_{r_1}$ is set equal to $(1/2)r_1^2$. Although this makes sense considering the limits as $r_1 \rightarrow 0$ and as $r_1 \rightarrow 1$, it is not clear that the results will generally be realistic, so more effort would be required to study the situation and to reformulate the problem if necessary to produce accurate solutions.

Key auxiliary equations are shown here. For the effective fluid conductivity,

$$K_{br} = K_g + C_r G C_p D_p, \text{ and}$$

$$K_{bz} = K_g + C_z G C_p D_p,$$

where the radial and axial coefficients are quite different (typically 0.1 radial, 0.5 axial).

The effective fluid heat transfer coefficient is approximated by

$$k_e = \left[k_g + h_{rv} D_p \right] + \frac{\varepsilon(1-\varepsilon)}{\frac{1}{k_s} + \frac{k_g}{\varepsilon} + D_p(h_p + h_{rs})} \quad (16)$$

where k_s is the solid thermal conductivity with account taken of the temperature and exposure to the neutron flux,

$$\phi = \phi_2 + (\phi_1 - \phi_2) \left[\frac{\varepsilon - P_7}{P_8 - P_7} \right] \quad (17)$$

where

$$\phi_1 = P_5 \left(\frac{k_s}{k_g} \right)^{P_6}, \text{ and}$$

$$\phi_2 = P_3 \left(\frac{k_s}{k_g} \right)^{P_4}, \text{ but}$$

$$\text{if } \varepsilon < P_7, \phi = \phi_2,$$

$$\text{if } \varepsilon \geq P_8, \phi = \phi_1$$

The equations used to account for radiation effects

$$h_{rs} = P_1 \left(\frac{e_m}{2 - e_m} \right) T_s^{P_2}, \quad (18)$$

and

$$h_{rv} = \frac{P_1 T_s^{P_2}}{\left[1 + \frac{\varepsilon(1 - e_m)}{2e_m(1 - \varepsilon)} \right]}, \quad (19)$$

where naturally P_2 is defaulted to a value of 3, but these coefficients may be altered with input data;

$$\epsilon_m = P_9 + P_{10} (T_s - P_{11}) \quad (20)$$

The heat transfer coefficient for the film is approximated by

$$H = \frac{K_g}{D_p} \left\{ P_{14} + \left(R_e^{0.5} + P_{13} R_e \right) \left(\frac{1-\epsilon}{\epsilon} \right) \right\} \quad (21)$$

where

$$R_e = \frac{GD_p}{1-\epsilon} ;$$

for the German data, or for the US data

$$H = \frac{P_{15} K_f R_e^{P_{16}}}{\left[\frac{2D_p \epsilon}{3(1-\epsilon)} \right]} \quad (22)$$

where

$$R_e = \left(\frac{2\sqrt{2}}{3} \right) \frac{GD_p}{(1-\epsilon)} .$$

The German correlation for the fluid thermal conductivity of the film

$$K_g = f_f (1. + f_g P) T_f^{(f_e - f_h P)}$$

where coefficients f are shown that may be altered with input data, and for the viscosity of the film,

$$\mu = f_c T_f^{f_d} ,$$

where locally

$$T_f = \frac{1}{2} (T_b + T_s) .$$

The fluid density is calculated from the equations

$$\rho = \frac{W_m}{V} \quad (23)$$

where

$$V_0 = \frac{R_g T_b}{P} \quad .$$

$$V_n = V_{n-1} + \Delta V_n \quad ;$$

$$\Delta V_n = \frac{\left(\{ [(-PV_n + R_g T_b) V_n + B] V_n + \gamma \} V_n + \delta \right) V_n}{\{ [(R_g T_b V_n + 2B) V_n + 3\gamma] V_n + 4 \delta \}} \quad (24)$$

done recursively with termination at $\Delta V_n/V_n < 10^{-6}$, or $n = 20$ max, where

$$B = B_1 - A_0 - B_2/T_b^2$$

$$\gamma = B_3 T_b + B_4 - B_5/T_b^2$$

$$\delta = B_6/T_b^2$$

For the pebble temperature distribution,³

$$\alpha(T_p) = 1.055 - 0.00057 T_p, \quad \alpha \geq 0,$$

$$H(T) = [1. - 8.45 \times 10^{-8} T(420. + 1.65T)],$$

$$B(T_p) = 1.116 - 0.000269 T_p, \quad B \geq 0,$$

$$F = 8.8 \alpha(T_p) H(T) [1 - \exp\{\beta(T_p) \times 10^{-21} S\}],$$

$$R = \frac{1}{1. + F K(T) [C(T_p) \delta(T) + \{1. - C(T_p)\} A(T)]} \quad (25)$$

$$K_p(e, T) = R K(1);$$

$$K_p \geq 0.705 \text{ (0.1 times the second value in the string).}$$

$$z = K(T)/K_p(e, T),$$

$$G = \frac{(R-1.)}{8.8\alpha(T_r)H(T)K(T)[C(T_r)\delta(T) + \{1. - C(T_r)\}A(T)]}$$

$$S = \frac{-10^{21} \log_{10} (1.-G)}{\beta(T_r)} + \Delta s \quad (26)$$

where additional exposure to the neutron flux is shown as being added directly to S (flux-time, n/cm²), and K(T), A(T), $\delta(T)$ and C(T_r) are obtained by linear interpolation in data strings, T being the estimate for the local temperature and T_r being the irradiation temperature estimate.

The steady state heat transport (by conduction) is solved assuming a uniform source within the meat part of the pebble,

$$\frac{d}{dr} \left(r^2 K \frac{dt}{dr} \right) = -Qr^2, \quad (27)$$

where K is the thermal conductivity and Q the heat source per unit volume. The solutions are cast in a difference form of the differential equations and integrals are then done numerically, as to calculate the meat temperature.

Selecting data in use at the time this is written, for T=T_r=1000 K, S=0.7746, C=0.7, A=0.4354, and K=0.5905;

$$\alpha = 0.485$$

$$H = 0.400$$

$$\beta = 0.847$$

$$F = 3.521 (1 - \exp\{-0.847 S \times 10^{-21}\}),$$

$$R = \frac{1}{1. + 0.3973F} ,$$

$$K_p = 0.62R$$

$$Q = \left(\frac{0.62}{K_p} \right)$$

$$G = 0.715 (Q-1.)$$

$$S = -1.18 \times 10^{21} \log_{10} (1.-G) + \Delta S$$

and so the dependence on exposure in this case is as follows for a initial condition with initial exposure but no further accumulation (with annealing):

S_0	F_0	$K_{p,0}$	S_1	F_1	$K_{p,1}$
0	0	0.62	0	0	0.62
10^{20}	0.286	0.557	4.32×10^{19}	0.126	0.590
10^{21}	2.012	0.345	4.32×10^{20}	1.080	0.433
10^{22}	3.520	0.258	(falls*)		0.258
	3.521	0.258	(falls)		0.258

*Code action is to leave S unaltered so usually S increases and R takes on the value associated with $s \rightarrow \infty$.

Transport of energy within the pebble is of concern because of the associated temperatures and the dependence of these on the power density and the thermal conductivity that degrades with exposure to the neutron flux. Consider the rate of heat transport at the surface of the fueled portion of the pebble,

$$Q = q_f V_f = -KA_f \left. \frac{\partial T}{\partial r} \right|_{f_s}$$

where the heat balance equates the total generation rate, source density times volume to the transport rate which is proportional to the area and the temperature gradient at the surface, the coefficient being the thermal conductivity. Considering that the heat source within the fuel may be related to the average in space of the power density (more apt to be known),

$$q_f r_f^3 = \bar{q} \left(\frac{r_s^3}{f_v} \right)$$

where r_s is the pebble outside radius and f_v is the fill fraction of pebbles (one minus the void fraction),

$$\begin{aligned} \left. \frac{\partial T}{\partial r} \right|_{r_s} &= - \frac{\bar{q} r_f}{3 f_v K} \left(\frac{r_s}{r_f} \right)^3, \text{ sphere} \\ &= - \frac{\bar{q} r_f}{2 f_v K} \left(\frac{r_s}{r_f} \right)^2, \text{ long cylinder.} \end{aligned}$$

Thus for a power density of 5.5 watts/cm³, spherical pebble $r_s=3$ cm, $r_f=2.5$ cm, $f_v=0.61$, and a thermal conductivity of 0.072 cal/cm-°C-sec, 0.301 watt/cm-°C, $T/r = -43.1$ °C/cm. Since this gradient is inversely proportional to the thermal conductivity, reducing it in this case to 2/3 the value increases $\partial T/\partial r$ in magnitude to -64.7.

NO CROSS FLOW, FLOW THROUGH HOLES

There is provision in the code to solve a problem on option without radial cross flow. Note that this solution generally places an upper bound on the temperatures because the effect of cross flow is to reduce the temperature peaking of the coolant.

Also, special equations have been programmed for flow of coolant through cylindrical holes in a solid matrix. As programmed, the option for eliminating cross flow must also be exercised, usually with the assumption of ideal orificing at the inlet or outlet. For flow through holes, the void fraction is used to determine how many holes there are per unit cross-sectional area, and the hydraulic diameter is that of the typical hole. For a collection of different sized holes, this diameter would be an effective weighted value (the square of the flow rate is proportional to the hole diameter). The equations programmed are:

Equation 2 becomes

$$\theta = \frac{BfG}{g\rho\epsilon^2d_h} \quad (28)$$

where d_h is the hole diameter and B is set to 1.0 unless specified differently. Given,

$$R_e = \frac{d_h G}{\mu\epsilon} ,$$

the Fanning friction factor is obtained by iterative solution of the correlating equation

$$f = \max \left[\frac{16}{R_e} , \left\{ \frac{1}{4 \log(R_e \sqrt{f}) - 0.4} \right\}^2 \right] \quad (29)$$

and the film coefficient is obtained from the equation replacing Eq. 21,

$$H = P_{15} \left[R_e \right]^{P_{16}} \left(\frac{c_p \mu}{k} \right)^{P_{14}} \quad (30)$$

(except that the last term is set constant at 0.87 for one-dimensional problems). The surface for heat removal is given per unit volume by

$$\left(\frac{S}{V} \right) = \frac{4\epsilon}{d_h} \quad (31)$$

Also the heat removal mechanisms available to the fluid phase are limited to only axial fluid flow.

In solving these equations for flow through holes it was found that the normal central difference equations for the bulk coolant temperature were so unstable that acceptable results could not be obtained. Upwind temperature difference and heat source were found to effect stability and produce adequate results.

REMARKS ABOUT THE PRINTED RESULTS

The input option on edit level determines the primary arrays that are printed. Generally the axial flow and the bulk fluid and surface temperatures are printed (unless suppressed), but not the radial flow nor the pressure. If the maximum radial flow rate seems high, then the array of radial flow is printed. Higher edit levels produce the array of power density, and the stream function and a flow parameter (θ) printouts.

Debug levels of edit produce elaborate printouts. Even during the iteration process, all calculated properties and thermal hydraulic results at two locations may be obtained. The data associated with coolant properties and heat transfer characteristics are edited on termination of the iteration process. The equation coefficients are printed and key information about the calculation of the local cell temperature distribution.

The normal edit includes the primary input control data (options), a line of edit for each iteration on the thermal hydraulic problem, the key

results from the thermal hydraulics problem and also those from the local cell temperature distribution calculations including average and peak fuel temperatures. A summary table for the thermal hydraulics problem shows primary results including peak and mean coolant outlet temperatures, pressure drop data, and flow balance and heat balance information.

(Incorporating an axial flow balance in the equations solved eliminated any discrepancy in the flow balance as examined.) Special calculations are made to approximate the axial pressure drop at $R/3$ and $2R/3$ locations as a reliability check. In the event that the option to prevent radial "cross" flow is exercised, then the "apparent extreme pressure drop" is of special interest, and indeed the only meaningful pressure drop data when orificing at the inlet or outlet are opted.

Information is printed each iteration. Following the iteration number are the maximum relative changes in the point values of the stream function, the bulk fluid temperature, the surface temperature, and the pressure. Then the value of the overrelaxation coefficient in current use for the stream function is printed followed by the pressure drop at one core traverse in atmospheres, and then the relative fractional error in the overall heat balance (indicating the accuracy of the integral of the outlet coolant flow rate times its temperature). Then five values of dominant iterate error vector eigenvalues are printed, primarily L_1 norm estimates, but the concerned reader is referred to the program source listing for the current procedure.

ON RELIABILITY OF APPARENT SOLUTIONS

It was found that a much tighter convergence level must be satisfied than recent investigators have indicated if the absolute error in local values is to be reduced adequately to admit the claim of reliability. The difficulty lies in uncertainty about the absolute error and possible large error that may be associated with a false mode of flow or temperature distribution. It was found to be essential to start with a reasonable initialization of problem to produce reliable results within a reasonable investment in computation time. The equations that are solved are nonlinear. In some cases they may be nearly linear while in others there are highly nonlinear effects as for strong temperature dependence in heat removal properties. A scheme that works well in one situation may fail in another. The key aspects of reliability are addressed below.

Expect reasonable results. For example, the radial flow distribution should form a reasonable pattern, not one sign change after another along a coordinate.

Uniqueness. Uniqueness of a solution can not be assured, especially with strong nonlinearity contributions. Under the conditions of reasonable power level and coolant flow rate, a unique solution seems to exist. Uniqueness has been tested by both starting a problem from more than one initial condition and effecting tight convergence of the iterative process. Such testing is highly recommended in the event of any doubt about the apparent solution.

Fluid Flow Regime and Stability. At low coolant flow rates, the coolant temperature increases along a path of high heat deposition reducing the flow rate. In three-dimensions there would be local recirculation not realistically in two dimensions. The point where recirculation occurs has not been simple to identify for a particular situation. In some cases instability seems to occur well below 10 percent design power level and coolant flow, while in others well above 10 percent. Evidently the larger the heat source variation over a core and the greater the effect of temperature rise on the flow, the higher the flow rate at which undesirable recirculation could occur. Similarly for reference power generation conditions, the more uniform the flow and the lower its sensitivity to local conditions, the less likelihood of two or more possible flow regimes for a set of conditions.

On Limitations. With the stream function approach, the flow rate, radial or axial, is the derivative of the stream function which is solved as a continuous function. Evidently radical changes in the flow rate are not admitted, certainly not discontinuities. It would make little, if any sense to try to represent a blocked region that did not extend to zero radius (an azimuthal ring). Indeed, only coarse information may be produced about blocking at the center-line.

Definitive information about a low power level and low flow rates may not be produced. Expect eddies to develop as the flow rate decreases that are three-dimensional in nature. So below some low flow rate for a low heat source, a stable two-dimensional solution should not be expected but this may or may not represent requirements for after cooling. Caution is in order.

Convergence. One troubling aspect of converging the iterative process is the nature of the function being solved. The flow rate is the derivative of the stream function. To converge the iterate solution of the flow rate means converging this derivative. It can be argued that a convergence test should be performed on the derivative. Since none is, a tighter convergence of the local values of the function may be necessary than might be expected. We assume that when the iterative process is convergent as indicated by successive values of the function being nearly the same, the derivative of the function as approximated by differences at neighboring points is also converging. This may not be true when large changes occur from iteration. Note that an iterate change of 0.2 percent of 1000° is 2° , and if the error eigenvalue is 0.9, we expect the absolute error to be $2(0.9)/(1-0.9)=18^\circ$, probably significant.

The analyst should become familiar with convergence level requirements for reliable solutions to the class of problems he is solving for the specific solution method applied.

Numerical Instability. At some risk in compromising solution capability, the upstream finite-difference equations were discarded in favor of recast central difference equations, generally more accurate but often less stable. Overrelaxation is used to accelerate the rate of convergence and underrelaxation to effect stability where needed. Decrease the coefficients if necessary.

It is not unusual to find a problem that oscillates. Temperatures at adjacent points may take on values that indicate they have exchanged

locations. If the process is convergent, then fine. The more rapid the rate of convergence, the stronger the dampening, the better.

It should be recognized that strong underrelaxation, as found to be necessary in calculating the bulk coolant and the pebble surface temperatures, is done only with some concern. If new iterate values that are obtained as solutions to the flow and heat balance equations before altering are not better than the old values, then the confidence with which one accepts the iterate solution as being adequately converged must be low. Reliable results may or may not be produced. The analyst should take extreme care in terminating the iterative process and accepting results.

Finite-Difference Error. There is a finite-difference error, but given a reasonable arrangement of mesh points (40x40, not 20x20), and no large, sharp discontinuities, as in properties or void fraction or the heat source, the results should be adequate. Use more mesh points in the neighborhood of large changes or derivatives.

A troublesome discrepancy has not gone away: there may be appreciable error in the overall heat balance. Why in some situations the average coolant exit temperature is off by a fraction of a percent or more is not known. This discrepancy is deemed to have but low importance. Recognize it as a distortion that can't be removed. A uniform axial mesh point spacing has produced the smallest discrepancy in testing.^a

^aFluid and surface temperatures are arbitrarily adjusted on termination to eliminate the overall heat balance error.

If there is concern that the finite-difference error may be serious in a specific situation, a second solution should be obtained, preferably with many more mesh points reducing the spacing.

Modeling Inaccuracy. Every situation will not be modeled accurately with this code. For example, the conditions near a containment surface will not be determined accurately: the flow equations are for a bed of pebbles (not random packed but rather the effective parameters of a bed are used), the edge effects of increased volume and surface effects are not considered nor power density peaking in the neighborhood of a moderator containment. So there should be reservation regarding accurate modeling, while one expects the modeling to be adequate for primary effects.

Coding Error. This code is qualified for routine application to a limited class of problems. Yet errors are possible, either mistakes in solving the equations as intended or in taking action not expected by the user. An unreasonable solution should not be accepted without testing.

SAMPLE PROBLEM

The sample problems are used to guide the user and serve as validation tools for implementation at other sites. Table 3 presents an input data listing for a selected problem and selected edit of the results. Note that information is generated for the thermal hydraulics code by other modules, and extensive testing is then done by multiple accesses of the thermal hydraulics code. Not only is the thermal hydraulic problem solved several ways but the data saving and selected recovery procedures are used.

Table 3. CONTINUED

1.02232E-07	7.95199E-27	9.02701E-26	2.71301E-26	2.41211E-25	9.92428E-13
1.75916E-07	7.22150E-29	1.25051E-27	5.16232E-26	0.0	1.00000E-09
1.36335E-07	2.35100E-24	6.25476E-27	1.79210E-27	2.21420E-26	1.79039E-05
1.95332E-07	8.92220E-10	1.00716E-11	1.66462E-13	1.66462E-16	1.56223E-39
1.01185E-09	1.19767E-10	8.37942E-22	7.00053E-10	1.12422E-10	2.47310E-30
2.79412E-10	2.35303E-10	1.27657E-09	6.15480E-10	1.05250E-07	5.47052E-37
2.32252E-06	1.36200E-06	5.27761E-09	1.90643E-09	5.16905E-08	5.76519E-11
5.71369E-10	5.16799E-06	1.09606E-08	1.03420E-27	1.73795E-09	1.22620E-30
7.16315E-08	1.28935E-09	1.24581E-10	1.40581E-10	1.11157E-08	1.97355E-08
2.09710E-09	9.76672E-05	5.16212E-26	0.0	1.00000E-09	5.13665E-29
2.32290E-06	1.06654E-26	1.30540E-26	1.16367E-07	1.16367E-05	1.17191E-06
2.06792E-09	1.00362E-10	1.56627E-11	1.66532E-06	2.29157E-06	7.27150E-26
2.31320E-09	8.17960E-22	1.55969E-29	2.07700E-10	8.67896E-26	1.30135E-29
1.57776E-10	1.07711E-29	1.48024E-29	1.00624E-07	1.69357E-06	7.19211E-26
1.36200E-06	1.00000E-20	1.39716E-20	1.09040E-07	1.19367E-10	1.79727E-29
1.53812E-07	1.13277E-08	1.28656E-27	1.12975E-06	1.69163E-06	2.16593E-27
1.15533E-08	1.04013E-09	1.40367E-10	2.16564E-08	6.41602E-06	5.96097E-29
1.11037E-08	5.16020E-04	0.0	1.00000E-09	2.07799E-08	2.10932E-04
1.36127E-06	2.56945E-26	2.47620E-27	5.00662E-06	1.66462E-06	2.11227E-29
1.60405E-09	1.17729E-10	1.40265E-06	2.60662E-28	1.35649E-06	6.06435E-29
8.37940E-02	1.57190E-25	1.74812E-10	1.33776E-07	1.71791E-29	1.18511E-09
1.01992E-09	1.70800E-09	6.81368E-27	2.05842E-26	1.21649E-05	1.16230E-04
2.97337E-08	5.26810E-04	2.26113E-27	1.10735E-10	1.30819E-29	2.05932E-07
1.10232E-06	5.59603E-07	1.26262E-08	5.18373E-08	1.53569E-07	2.26360E-20
6.96166E-09	6.76053E-10	2.39510E-26	1.20573E-07	6.21403E-09	5.21733E-30
5.16020E-04	0.0	1.00000E-29	7.06600E-26	2.28542E-26	1.62736E-04
1.50607E-06	5.25067E-07	6.60350E-26	2.37660E-06	2.23403E-09	1.90961E-09
6.06956E-10	1.16139E-06	2.61610E-20	1.56460E-08	9.19759E-09	8.17960E-22
7.39990E-09	1.05007E-10	1.59230E-27	2.17561E-09	1.16366E-09	1.91611E-29
1.59571E-09	6.01060E-07	1.91210E-06	1.66693E-05	1.16200E-06	6.20626E-08
7.26900E-08	2.76416E-07	1.63476E-10	6.23428E-09	1.10070E-07	2.87641E-30
7.57065E-07	6.21161E-04	6.94715E-20	4.66235E-27	1.45729E-20	4.96042E-29
1.07972E-09	2.10913E-27	1.00099E-27	6.41139E-09	6.09153E-04	5.10029E-26
0.0	1.00000E-09	1.29765E-27	2.26366E-06	1.34917E-06	6.12766E-06
7.50666E-07	6.62396E-06	2.60089E-26	1.96843E-09	6.83136E-05	8.96395E-13
1.32565E-06	2.15049E-08	1.56790E-08	1.05040E-08	4.17960E-02	1.15085E-29
1.24662E-10	1.69128E-27	2.20990E-09	1.38320E-09	1.49691E-09	1.61570E-29
6.73306E-07	6.79341E-06	2.06554E-05	1.16200E-26	5.49702E-06	6.95150E-30
2.98966E-07	8.11061E-11	5.18810E-29	1.69629E-27	2.60035E-08	9.16266E-27
9.36952E-08	6.25019E-08	5.51169E-27	6.53632E-26	1.24176E-06	1.68245E-09
1.78422E-08	2.40092E-07	6.41989E-09	6.15051E-08	5.14232E-04	0.0
1.00000E-09	1.40725E-07	2.70002E-26	1.19860E-26	4.50925E-26	9.43270E-07
1.36230E-06	2.77518E-26	1.61400E-29	9.41809E-09	1.68719E-09	1.29607E-06
1.93722E-08	1.47427E-04	1.05390E-20	6.17960E-02	5.07562E-10	1.00040E-10
1.70357E-07	2.67622E-09	1.33366E-25	1.68374E-09	1.26460E-09	7.11254E-07
5.50163E-06	2.15246E-05	1.16200E-04	6.55007E-08	1.32931E-07	1.05556E-27
6.45351E-11	5.81739E-09	6.25101E-27	1.46490E-08	1.03320E-06	1.22637E-07
9.38936E-08	6.12878E-07	5.43882E-04	1.63591E-06	1.82327E-09	1.62975E-04
2.79272E-07	6.80027E-09	9.16110E-20	5.16020E-04	0.0	1.00300E-09
2.21522E-07	2.22631E-04	1.02431E-04	4.73960E-26	1.09461E-06	2.56137E-26
2.86509E-06	1.10611E-09	1.10735E-20	2.08112E-09	1.27222E-06	1.78673E-06
1.37635E-20	1.00971E-04	8.37960E-22	7.26263E-10	9.85356E-11	1.67592E-27
1.84652E-09	1.26301E-09	2.27064E-09	1.15231E-09	7.29024E-07	6.06766E-06
2.59780E-05	1.16200E-04	7.42054E-08	1.13298E-07	1.04275E-07	6.97600E-11
6.28656E-09	6.29467E-07	1.55673E-08	1.12252E-06	1.66555E-07	1.06167E-07
6.57569E-07	6.17100E-06	1.86125E-08	2.09716E-09	1.13180E-08	1.07570E-07
6.96261E-09	9.89602E-08	5.16020E-04	0.0	1.00300E-09	2.51663E-07
2.21531E-06	6.50549E-07	6.88008E-26	1.20811E-06	2.03500E-06	2.91620E-06
1.04295E-09	1.10117E-08	2.61400E-09	1.25322E-06	1.67860E-08	1.29360E-08
9.58197E-09	8.37960E-02	5.72252E-10	9.12527E-11	1.63270E-07	1.58232E-09
1.19600E-09	1.76277E-09	1.00910E-09	7.36644E-07	6.51307E-06	2.79316E-05
1.36200E-04	6.16010E-08	1.21200E-07	2.99920E-07	1.85185E-11	6.61713E-09
6.46409E-07	1.23875E-08	1.19094E-26	1.65019E-07	1.13666E-07	6.90271E-07
6.76132E-08	2.05922E-06	2.29779E-09	8.96166E-09	1.27427E-07	7.04950E-29
1.06607E-07	5.16020E-04	0.0	1.00000E-09	2.73769E-07	2.20667E-26
7.02257E-07	6.97069E-06	1.29162E-26	1.70660E-06	2.93965E-06	8.28037E-10
1.41610E-08	1.06686E-09	1.23615E-26	1.60486E-08	1.23016E-08	9.12857E-09
6.37960E-02	6.51774E-10	6.57678E-11	1.58667E-07	1.32565E-09	1.11960E-09
1.35054E-09	9.66569E-10	7.39178E-07	6.06511E-06	2.96853E-05	1.16200E-04
6.72046E-08	1.27122E-07	2.96469E-07	1.00185E-11	6.88605E-09	4.58478E-07
9.85350E-09	1.26297E-06	1.78402E-07	1.22660E-07	7.16562E-07	7.23463E-08
2.21277E-08	2.45540E-09	7.07163E-29	1.41184E-07	7.12780E-09	1.39271E-07
5.16020E-04	0.0	1.00000E-09	2.89502E-07	2.19610E-06	5.71795E-07
6.02901E-06	1.35211E-06	1.40778E-06	2.95261E-06	6.57960E-10	1.69721E-08
1.41805E-09	1.22420E-06	1.55276E-08	1.18289E-08	8.76186E-09	8.37960E-02
1.57669E-10	8.12530E-11	1.53660E-07	1.09307E-09	1.05267E-09	1.63080E-09
8.99163E-10	7.39358E-07	7.18365E-06	1.07221E-05	1.16200E-04	9.18062E-08
1.31999E-07	2.90608E-07	2.35656E-11	7.01285E-09	6.67269E-07	7.86658E-09
1.20312E-06	1.87363E-07	1.11199E-07	7.32871E-07	7.61817E-08	2.33216E-08
2.57533E-09	5.60527E-09	1.50666E-07	7.18350E-09	1.12690E-07	5.16020E-04
0.0	1.00000E-09	1.00000E-07	2.18921E-06	6.62997E-07	5.06990E-06
1.39660E-06	1.33716E-06	2.95891E-06	5.22610E-10	1.55668E-08	1.73000E-09
1.21672E-06	1.51527E-08	1.18765E-08	8.67230E-09	8.37960E-02	2.63899E-10
7.71922E-11	1.48816E-07	8.90363E-10	9.86138E-10	7.86637E-18	8.42660E-10
7.38537E-07	7.36449E-06	1.17078E-05	1.16200E-04	9.56771E-08	1.15618E-07
2.85896E-07	1.85645E-11	7.13252E-09	4.73766E-07	6.25323E-09	1.31835E-06
1.92731E-07	1.39349E-07	7.66850E-07	7.91767E-08	2.42894E-08	2.66671E-09
6.45332E-09	1.57179E-07	7.22162E-09	1.15318E-07	5.16230E-04	0.0
1.00000E-09	1.09213E-07	2.18368E-06	1.73710E-07	5.09796E-06	1.42896E-26
1.23077E-06	2.96165E-06	6.15701E-10	1.60667E-08	1.97852E-09	1.20918E-06
1.48771E-06	1.12119E-08	6.26356E-09	8.37960E-02	2.25819E-10	7.32680E-11
1.46130E-07	7.18599E-10	9.20719E-10	5.99634E-10	7.93423E-10	7.37366E-07
7.53998E-06	1.28985E-05	1.16200E-04	9.60031E-08	1.18438E-07	2.82412E-07
1.07077E-11	7.22007E-09	4.78636E-07	6.99197E-09	1.33660E-06	1.95198E-07
1.07121E-07	7.57636E-07	6.16033E-20	2.49670E-08	2.72938E-09	2.56630E-09
3.61661E-07	7.26652E-09	1.17335E-07	5.16020E-04	0.0	1.00000E-09
1.52933E-07	2.17924E-08	3.01119E-07	5.11784E-06	1.45311E-06	1.15282E-06
2.96252E-06	1.31280E-10	1.63963E-20	6.17073E-09	1.20319E-06	1.46763E-08
1.18172E-04	8.06664E-08	8.37960E-02	1.40174E-10	6.42928E-11	1.10661E-07

Table 3. CONTINUED

2.22127E-04	8.27065E-07	4.80264E-06	1.93592E-04	2.25299E-06	2.89465E-06
1.02069E-09	1.23360E-08	2.36063E-09	1.26151E-04	1.72990E-08	1.33089E-08
5.04981E-09	8.17960E-02	5.64766E-10	5.37300E-11	1.60502E-07	1.54927E-09
1.20578E-09	1.71761E-09	1.07390E-09	7.37390E-07	6.32065E-06	2.71050E-05
1.26200E-04	7.06259E-08	1.10301E-07	1.03065E-07	3.03137E-11	6.49500E-09
4.00655E-07	1.21903E-04	1.16542E-06	1.55577E-07	1.15040E-07	6.77051E-07
6.56900E-08	1.90045E-04	2.22150E-09	8.01730E-09	3.17067E-07	6.90960E-07
1.02220E-07	5.14020E-04	0.0	1.00000E-09	2.44401E-07	2.21099E-04
6.79542E-07	6.98264E-06	1.21789E-06	1.09402E-04	2.92560E-06	8.10992E-10
1.34067E-04	2.79032E-09	1.24676E-06	1.45304E-04	1.27113E-08	5.41601E-09
6.37960E-02	4.45314E-10	6.79020E-11	1.59902E-07	1.29903E-09	1.13533E-09
1.31640E-09	9.09474E-10	7.41640E-07	6.67411E-04	2.04315E-05	1.36200E-04
6.42755E-08	1.24520E-07	2.90969E-07	2.90160E-11	6.73703E-09	4.53342E-07
9.69120E-09	1.21775E-06	1.60550E-07	1.25042E-07	7.02263E-07	7.03707E-08
2.10217E-06	2.37977E-09	6.96529E-09	3.31059E-07	7.04505E-09	1.06635E-07
5.14020E-04	0.0	1.00000E-09	2.00700E-07	2.22271E-04	5.22900E-07
5.00911E-06	1.27007E-06	1.65526E-06	2.94271E-06	6.43231E-10	1.43309E-08
1.15375E-09	1.23500E-06	1.59035E-08	1.22279E-08	9.05451E-09	6.37960E-02
1.51900E-10	6.30643E-11	1.55240E-07	1.07000E-09	1.06656E-09	1.00416E-09
9.19961E-10	7.43222E-07	6.95072E-06	2.90430E-05	1.36200E-04	6.07953E-08
1.29251E-07	2.94056E-07	2.33370E-11	6.91160E-09	6.25952E-07	7.70221E-09
1.25010E-06	1.77330E-07	1.33010E-07	7.20970E-07	7.41194E-08	2.26130E-08
2.09910E-07	5.51137E-09	3.40773E-07	7.11933E-09	1.10021E-07	5.10020E-04
0.0	1.00000E-09	2.92403E-07	2.19406E-04	4.47209E-07	5.09466E-06
1.32233E-06	1.40037E-06	2.95211E-06	5.10292E-10	1.49733E-08	3.44240E-09
1.22563E-06	1.55075E-04	1.10630E-08	8.76362E-09	8.37960E-02	2.70767E-10
7.07031E-11	1.50503E-07	6.70000E-10	9.90016E-10	7.64730E-10	6.41302E-10
7.43450E-07	7.16013E-06	3.00090E-05	1.36200E-04	9.23996E-09	1.32913E-07
2.91160E-07	1.03400E-11	7.03000E-09	4.69060E-07	6.12700E-09	1.20945E-06
1.02617E-07	1.42137E-07	7.35244E-07	7.71050E-08	2.35361E-08	2.50771E-09
4.37000E-09	3.47497E-07	7.15690E-09	1.12622E-07	5.14020E-04	0.0
1.00000E-09	3.01340E-07	2.19073E-04	3.60465E-07	5.12611E-06	1.35509E-06
1.36970E-06	2.95719E-06	4.05305E-10	1.44497E-08	3.67463E-09	1.21040E-06
1.52952E-08	1.15005E-08	8.53043E-09	6.37960E-02	2.21367E-10	7.44953E-11
1.05016E-07	7.01609E-10	5.31220E-10	5.02300E-10	6.10460E-10	7.43051E-07
7.30061E-06	1.15774E-05	1.36200E-04	9.52710E-08	1.35763E-07	2.00016E-07
1.05076E-11	7.13305E-09	4.70631E-07	4.00201E-09	1.31395E-06	1.05093E-07
1.50052E-07	7.44246E-07	7.94001E-08	2.42071E-08	2.65139E-09	3.47251E-09
1.52137E-07	7.10090E-09	1.14626E-07	5.14020E-04	0.0	1.00000E-09
1.07060E-07	2.10647E-04	2.90027E-07	5.14062E-06	1.37950E-06	1.20352E-06
2.95903E-06	3.22402E-10	1.50100E-08	3.06960E-09	1.21265E-06	1.50752E-08
1.13706E-08	6.30244E-09	6.37960E-02	1.76171E-10	7.02459E-11	1.41193E-07
5.61024E-10	6.31000E-10	4.43770E-10	7.65362E-10	7.42400E-07	7.47770E-06
3.21900E-05	1.36200E-04	9.75403E-08	1.37990E-07	2.05400E-07	1.15035E-11
7.20307E-09	4.70576E-07	3.09494E-09	1.33321E-06	1.45343E-07	1.57547E-07
7.54790E-07	6.13006E-08	2.47097E-08	2.69449E-09	2.76406E-09	3.55326E-07
7.19551E-09	1.16177E-07	5.14020E-04	0.0	1.00000E-09	3.12773E-07
2.10305E-04	2.33002E-07	5.16492E-06	1.39795E-06	1.21960E-06	2.96112E-06
2.56063E-10	1.60067E-08	4.00919E-09	1.20800E-06	1.49060E-08	1.12172E-08
8.18040E-09	6.37960E-02	1.40440E-10	6.50440E-11	1.36633E-07	4.45430E-10
7.94637E-10	3.30319E-10	7.24503E-10	7.41700E-07	7.50696E-06	3.26799E-05
1.36200E-04	9.93059E-06	1.39747E-07	2.03257E-07	9.14594E-12	7.25772E-09
4.01610E-07	3.11100E-09	1.34062E-04	1.03054E-07	1.64590E-07	7.61409E-07
6.25050E-08	2.51976E-08	2.72029E-09	2.20499E-09	3.57497E-07	7.20312E-09
1.17301E-07	5.14020E-04	0.0	1.00000E-09	3.16513E-07	2.10031E-04
1.07120E-07	5.17696E-06	1.41195E-06	1.17169E-06	2.96166E-06	2.04676E-10
1.62909E-08	4.12770E-09	1.20430E-06	1.47757E-08	1.10921E-08	8.05905E-09
6.37960E-02	1.12000E-10	6.12340E-11	1.32131E-07	3.52305E-10	7.25100E-10
2.57903E-10	6.87201E-10	7.41039E-07	7.67404E-06	3.30711E-05	1.36200E-04
1.00043E-07	1.41130E-07	2.81516E-07	7.20366E-12	7.29906E-09	0.03902E-07
2.48440E-09	1.36046E-06	1.01023E-07	1.71117E-07	7.66751E-07	8.41147E-08
2.50640E-08	2.73123E-09	1.76012E-09	3.50959E-07	7.20562E-09	1.10322E-07
5.14020E-04	0.0	1.00000E-09	3.19303E-07	2.17013E-04	1.49999E-07
5.18596E-06	1.42267E-06	1.13510E-06	2.94100E-06	1.42013E-10	1.64630E-08
4.22192E-09	1.20135E-06	1.46671E-06	1.09943E-08	7.95023E-09	0.37960E-02
0.94551E-11	5.64016E-11	1.27491E-07	2.76406E-10	6.54927E-10	1.96369E-10
6.52339E-10	7.40437E-07	7.74351E-04	3.33436E-05	1.36200E-04	1.02006E-07
1.02223E-07	2.00109E-07	5.00420E-11	7.33120E-09	4.85035E-07	1.94670E-08
1.37003E-06	1.77162E-07	1.77250E-07	7.70907E-07	0.50749E-08	2.57050E-08
2.72901E-09	1.40510E-09	3.59926E-07	7.20312E-09	1.19041E-07	5.14020E-04
0.0	1.00000E-09	3.21500E-07	2.17639E-04	1.19576E-07	5.19170E-06
1.43101E-06	1.10696E-06	2.96100E-06	1.27061E-10	1.45937E-08	0.29516E-09
1.19900E-06	1.45419E-08	1.09150E-08	7.05400E-09	0.37960E-02	7.15920E-11
5.10212E-11	1.23335E-07	2.15297E-10	5.01016E-10	1.49430E-10	6.17600E-10
7.39900E-07	7.79913E-06	3.36339E-05	1.36200E-04	1.02930E-07	1.43009E-07
2.70966E-07	6.43971E-12	1.35766E-09	0.87336E-07	1.59147E-09	1.37771E-06
1.72496E-07	1.02800E-07	7.74227E-07	0.54290E-08	2.50300E-08	2.71061E-09
1.12466E-09	1.60553E-07	7.10775E-09	1.19673E-07	5.14020E-04	0.0
1.00000E-09	1.23192E-07	2.17562E-06	9.47217E-08	5.10009E-06	1.43001E-06
1.00370E-06	2.96226E-06	9.52460E-11	1.67100E-08	0.30639E-09	1.19732E-06
1.42404E-06	1.00430E-08	7.77069E-09	0.37960E-02	5.14020E-04	7.0369E-11
1.19166E-07	1.66003E-10	0.99214E-10	1.16003E-10	5.75192E-10	7.39305E-07
7.04550E-06	3.30417E-05	1.36200E-04	1.01721E-07	1.43792E-07	2.77976E-07
1.05000E-12	7.30451E-09	0.00756E-07	1.32200E-09	1.30420E-06	1.67140E-07
1.07090E-07	7.77002E-07	0.63709E-08	2.50676E-08	2.48969E-09	9.33009E-10
1.40963E-07	7.12009E-09	1.20315E-07	5.14020E-04	0.0	1.00000E-09
3.21991E-07	2.35400E-04	1.75439E-07	3.36000E-07	1.72007E-08	1.02130E-05
3.53962E-07	7.03072E-10	1.20400E-11	1.92300E-13	1.40000E-06	0.00047E-09
1.50141E-09	2.33735E-10	0.37960E-02	4.67166E-10	1.11734E-10	2.59041E-08
2.30252E-10	2.06401E-10	1.11236E-09	0.04000E-09	9.42706E-08	1.00546E-07
2.07059E-06	1.36200E-04	6.69472E-09	0.90960E-09	0.60031E-08	5.13073E-11
5.00742E-10	6.63183E-08	1.33701E-08	9.26447E-08	1.36521E-09	1.22075E-08
6.00493E-08	2.91020E-09	2.50071E-10	1.30095E-10	9.91601E-09	1.73060E-08
2.01950E-09	0.55342E-09	5.14020E-04	0.0	1.00000E-09	4.02010E-09
2.33630E-04	9.45090E-07	1.25096E-06	9.16195E-08	1.42051E-05	1.06124E-06
1.01011E-09	2.20171E-10	9.19735E-12	1.45160E-06	2.10004E-08	6.29255E-09
1.01000E-09	0.37960E-02	1.40130E-09	2.09209E-10	7.96142E-08	0.47943E-10
6.07277E-10	2.66940E-09	1.64650E-09	2.00100E-07	1.51756E-06	6.04100E-06
1.40700E-08	1.40640E-08	7.77444E-08	1.74100E-07	1.07641E-10	1.60710E-08

Table 3. CONTINUED

1.39107E-07	2.81586E-08	2.95490E-07	8.99917E-09	3.50532E-08	1.95092E-07
1.01932E-08	1.49136E-09	3.51615E-10	2.10638E-08	5.99251E-08	5.06230E-09
2.79073E-08	5.18020E-09	0.0	1.00000E-09	2.31819E-08	2.31533E-08
1.21632E-06	2.37680E-06	2.37683E-07	1.05351E-05	1.69691E-06	2.10097E-09
1.16039E-09	7.18333E-11	1.41305E-06	2.62201E-08	1.20125E-08	5.00026E-09
8.37960E-02	1.43625E-09	1.00072E-10	1.25594E-07	1.51819E-09	1.11308E-09
3.22726E-09	1.70151E-09	4.44801E-07	2.58132E-06	1.09720E-05	1.36200E-06
2.65754E-08	4.76304E-08	2.12058E-07	1.09125E-10	2.70062E-09	2.25529E-07
2.90820E-08	5.09103E-07	2.63242E-08	5.46336E-08	3.22152E-07	2.00391E-08
0.09302E-09	5.09621E-10	2.10763E-08	1.13295E-07	6.11517E-09	8.75157E-06
5.16020E-06	0.0	1.00000E-09	6.10763E-08	2.29396E-08	1.20308E-06
3.31296E-06	4.25460E-07	7.59354E-06	2.17197E-04	2.03590E-09	2.98058E-09
2.68127E-10	1.37570E-06	2.51131E-08	1.52517E-00	0.23676E-09	8.37960E-02
1.30564E-09	1.53590E-10	1.53177E-07	1.91026E-09	1.31770E-09	3.06203E-09
1.61900E-09	5.67815E-07	1.56123E-06	1.51555E-05	1.36200E-04	1.04562E-08
6.62022E-08	2.63230E-07	9.73092E-11	3.66622E-09	2.95903E-07	2.67527E-08
6.97025E-07	5.00666E-08	7.11127E-08	4.30125E-07	3.09616E-08	7.56031E-09
9.35995E-10	2.00127E-08	1.67670E-07	6.31330E-09	6.35250E-04	5.16020E-06
0.0	1.00000E-09	1.09502E-07	2.27021E-04	1.22021E-06	3.97299E-06
6.46590E-07	5.51262E-06	2.40000E-06	1.79139E-09	5.39380E-05	6.10620E-10
1.30205E-06	2.27361E-08	1.59513E-08	1.01004E-08	0.37960E-02	1.09067E-09
1.32265E-10	1.66173E-07	2.01754E-09	1.37064E-09	3.10005E-09	1.60160E-09
6.46002E-07	4.39400E-06	1.07190E-05	1.36200E-04	0.95650E-08	0.23009E-08
2.91337E-07	7.98190E-11	0.75579E-09	3.40022E-07	2.27026E-08	0.09072E-07
7.77550E-06	0.51559E-06	5.10055E-07	0.11376E-08	1.11100E-08	1.30102E-09
1.60709E-08	2.15150E-07	6.48737E-09	7.59095E-08	5.10320E-04	0.0
1.00000E-09	1.56011E-07	2.25099E-06	1.00000E-04	0.00320E-06	7.00000E-07
4.12476E-06	2.67666E-06	1.49036E-09	7.73380E-09	1.07090E-09	1.31566E-06
2.06366E-08	1.54001E-08	1.06470E-06	0.37960E-02	0.01049E-10	1.16631E-10
1.70151E-07	1.92516E-09	1.34590E-05	2.63334E-09	1.33760E-09	6.93005E-07
5.07230E-06	2.16337E-05	1.36200E-04	5.93149E-08	5.53960E-08	3.03630E-07
6.20000E-11	5.43555E-09	3.45833E-07	1.05639E-08	9.06077E-07	1.02919E-07
9.74520E-08	5.76615E-07	0.97993E-08	1.42075E-08	1.62512E-01	1.36572E-06
2.52609E-07	6.64391E-09	0.54351E-08	5.10020E-04	0.0	1.00000E-09
1.90935E-07	2.20251E-04	9.32501E-07	0.67690E-06	9.20765E-07	3.21691E-06
2.79061E-06	1.21020E-09	9.49903E-09	1.54645E-09	1.29327E-06	1.90566E-08
1.46197E-08	1.05001E-08	0.37960E-02	6.97980E-10	1.05450E-10	1.69371E-07
1.72670E-09	1.20907E-09	2.10056E-09	1.21006E-09	7.19849E-07	5.61361E-06
2.39707E-05	1.36200E-04	6.75201E-08	1.05662E-07	3.07062E-07	0.07200E-11
5.93264E-09	0.12251E-07	1.40761E-08	1.05677E-06	1.20107E-07	1.00535E-07
4.22690E-07	5.60063E-08	1.67069E-04	1.00660E-09	1.00502E-08	2.00416E-07
6.76951E-09	9.27661E-08	5.10020E-04	0.0	1.00000E-09	2.25071E-07
2.23062E-04	7.78679E-07	0.05231E-06	1.02537E-06	2.62003E-06	2.05775E-06
9.72750E-10	1.12326E-08	1.98972E-09	1.27554E-06	1.79226E-08	1.30042E-08
1.01369E-08	0.37960E-02	0.49704E-10	9.72646E-11	1.66322E-07	1.00030E-09
1.22169E-09	1.63311E-09	1.10500E-09	7.33951E-07	6.04200E-06	2.50301E-05
1.36200E-04	7.42407E-08	1.13622E-07	3.06219E-07	3.77322E-11	6.29000E-09
4.31039E-07	1.10316E-08	1.12530E-06	1.40750E-07	1.10757E-07	6.56755E-07
6.25919E-08	1.06467E-08	2.09020E-09	0.57243E-09	3.00003E-07	6.06000E-09
9.84033E-08	5.10020E-04	0.0	1.00000E-09	2.47575E-07	2.22097E-06
6.39504E-07	4.06460E-06	1.10395E-06	2.22045E-06	2.09750E-06	7.72705E-10
1.23934E-08	2.37355E-07	1.26152E-06	7.11312E-08	1.32176E-08	9.75170E-09
0.37960E-02	4.32060E-10	9.08901E-11	1.62260E-07	1.24005E-09	1.51918E-09
1.25316E-09	1.01090E-09	7.41354E-07	6.30021E-06	2.73052E-05	1.36200E-06
7.96037E-08	1.19765E-07	3.03659E-07	2.93219E-11	4.56770E-09	0.00594E-07
9.30600E-09	1.17779E-06	1.52930E-07	1.20332E-07	4.02100E-07	6.71505E-08
2.01030E-08	2.20583E-09	6.76233E-09	3.10540E-09	6.93459E-09	1.02732E-07
5.40020E-08	0.0	1.00000E-09	2.69104E-07	2.21320E-04	5.19959E-07
5.00352E-06	1.16203E-06	1.96665E-06	2.92101E-06	6.12352E-10	1.32646E-08
2.69000E-09	1.25040E-06	1.65307E-08	1.27270E-08	9.40150E-09	0.37960E-02
3.41316E-10	0.55604E-11	1.57000E-07	1.02035E-09	1.00190E-09	9.55712E-10
9.66952E-10	7.05122E-07	6.66710E-06	2.06751E-05	1.36200E-04	0.00377E-08
1.20512E-07	3.00642E-07	7.20947E-11	6.73503E-09	4.50532E-07	7.00992E-09
1.21025E-06	1.61225E-07	1.37377E-07	7.01372E-07	7.07915E-08	2.13500E-08
2.36305E-09	5.33962E-09	3.24460E-07	6.98395E-09	1.06057E-07	5.14020E-06
9.9	1.00000E-09	2.76454E-07	2.20697E-04	4.20060E-07	5.09629E-06
1.20594E-06	1.75045E-06	2.93596E-06	4.05166E-10	1.39195E-08	2.96232E-05
1.20160E-06	1.61055E-08	1.23509E-08	9.12507E-09	0.37960E-02	2.69702E-10
0.07313E-11	1.53170E-07	0.35232E-10	1.01197E-09	7.27006E-10	0.05071E-10
7.46900E-07	6.05812E-06	2.90034E-05	1.36200E-04	0.75110E-08	1.20192E-07
2.97733E-07	1.79606E-11	6.07296E-09	4.61932E-07	5.90030E-09	1.20965E-06
1.66276E-07	1.05904E-07	7.16014E-07	7.36064E-08	2.22650E-08	2.00495E-09
4.22304E-09	3.11415E-07	7.01753E-09	1.00610E-07	5.14020E-04	0.0
1.00000E-09	2.05090E-07	1.20190E-04	3.10127E-07	5.12326E-04	1.23060E-06
1.61646E-06	2.90497E-06	3.80760E-10	1.44346E-08	2.17618E-09	1.23063E-06
1.57090E-08	1.20632E-08	0.09140E-09	0.37960E-02	2.13630E-10	7.60033E-11
1.06510E-07	6.71060E-10	9.41504E-10	5.52033E-10	0.32791E-10	0.47723E-07
7.02519E-06	3.01811E-05	1.36200E-04	9.02797E-08	1.31059E-07	2.95150E-07
1.41495E-11	6.97506E-09	0.67517E-07	0.69556E-09	1.27416E-06	1.60705E-07
1.50050E-07	7.27291E-07	7.59897E-08	2.29602E-08	2.51126E-09	3.30764E-09
3.36260E-07	7.03919E-09	1.10500E-07	5.10020E-04	0.0	1.00000E-09
2.92050E-07	2.10799E-06	2.71610E-07	5.15964E-06	1.26299E-06	1.51500E-06
2.95045E-06	3.05550E-10	1.47917E-08	3.30810E-09	1.22910E-06	1.55515E-08
1.18421E-08	0.69973E-09	0.37960E-02	1.69505E-10	7.10147E-11	1.43056E-07
5.3552E-10	0.70207E-10	0.20427E-10	7.05644E-10	7.67963E-07	7.15776E-06
3.07202E-05	1.36200E-04	9.20047E-08	1.31301E-07	2.92900E-07	1.11070E-11
7.05350E-09	4.71701E-07	3.73700E-09	1.29339E-06	1.69050E-07	1.61607E-07
7.36046E-07	7.78226E-06	2.36066E-08	2.55250E-09	2.65002E-09	3.39630E-07
7.05206E-09	1.12117E-07	5.10020E-04	0.0	1.00000E-09	2.97654E-07
2.19400E-04	2.17907E-07	5.17070E-06	1.20160E-06	1.40010E-06	2.95020E-06
2.42940E-10	1.50009E-08	3.00591E-09	1.22071E-06	1.53600E-08	1.16712E-08
0.54003E-09	0.37960E-02	1.34050E-10	6.66157E-11	1.39220E-07	0.20415E-10
7.90311E-10	3.19812E-10	7.43116E-10	7.47930E-07	7.26312E-06	3.11959E-05
1.36200E-04	9.20180E-08	1.35063E-07	2.91112E-07	0.04910E-12	7.11200E-09
0.75060E-07	2.97776E-09	1.30054E-06	1.67775E-07	1.60035E-07	7.42060E-07
7.92817E-08	2.30090E-08	2.57663E-05	2.11519E-09	3.01973E-07	7.05053E-09
1.13306E-07	5.10020E-04	0.0	1.00000E-09	3.01635E-07	2.19235E-04
1.70611E-07	5.19290E-06	1.29503E-06	1.30330E-06	2.95640E-06	1.93206E-10
1.53030E-08	3.59600E-09	1.22121E-06	1.52267E-08	1.15303E-08	0.40701E-09
0.37960E-02	1.07303E-10	6.16305E-11	1.30630E-07	3.30305E-10	7.25764E-10

Table 3. CONTINUED

5.16220E-06	0.0	1.00000E-09	2.32780E-07	2.21451E-06	6.65007E-07
6.00605E-06	5.62385E-07	2.37050E-06	2.47607E-06	5.45663E-10	1.16000E-00
2.06300E-09	1.27900E-08	1.61617E-08	1.24809E-08	9.15695E-09	8.17963E-00
3.22600E-10	6.69166E-11	1.62163E-07	5.50343E-10	1.37666E-09	8.76265E-00
9.55322E-10	7.15050E-07	6.21769E-06	2.65661E-07	1.36220E-06	7.71636E-00
1.16530E-07	3.03702E-07	2.19563E-11	6.00692E-09	6.02180E-07	6.99725E-00
1.16530E-06	1.16760E-07	1.60126E-07	6.72660E-07	6.55992E-00	1.91266E-00
2.11760E-09	5.03660E-09	2.99355E-07	6.42892E-09	1.01303E-07	5.16022E-00
0.0	1.00000E-09	2.42456E-07	2.22195E-06	1.76072E-07	1.96665E-00
1.03167E-06	2.15303E-06	2.90799E-06	6.17766E-10	1.13817E-06	2.22271E-00
1.27126E-06	1.59210E-04	1.21305E-09	1.00068E-04	6.17460E-02	2.56176E-00
6.95353E-11	1.57691E-07	7.76261E-10	1.30561E-04	6.64956E-10	6.93326E-00
7.16663E-07	6.41709E-06	2.76320E-05	1.36200E-06	6.01906E-00	1.20055E-00
1.31610E-07	1.71664E-11	6.59032E-09	6.50155E-07	5.51721E-09	1.19380E-00
1.41260E-07	1.88815E-07	6.07301E-07	6.83224E-06	1.69785E-00	2.19021E-00
1.67366E-09	1.36360E-07	6.65161E-09	1.33666E-07	5.16220E-00	0.0
1.00000E-09	2.11790E-07	2.21950E-09	1.72161E-07	6.96951E-06	1.06661E-00
1.96191E-06	2.91699E-06	1.61962E-10	1.25366E-00	2.39600E-09	1.26506E-00
1.55430E-00	1.20366E-06	6.68336E-09	6.17960E-02	2.00702E-10	7.61850E-00
1.53026E-07	6.21972E-10	9.47099E-10	5.35132E-10	8.39267E-10	7.40636E-00
6.57667E-06	2.81979E-05	1.36200E-06	6.25660E-04	1.16666E-07	2.99527E-00
1.36775E-11	6.70176E-04	6.56165E-07	6.18756E-07	1.16035E-06	1.63676E-00
1.56462E-07	6.68332E-01	7.00031E-00	2.36315E-00	2.25322E-09	1.13996E-00
1.81116E-07	6.66953E-09	1.05769E-07	5.16220E-06	0.0	1.36306E-00
2.56160E-07	2.21596E-06	2.64579E-07	5.32333E-06	1.00036E-06	1.66066E-00
2.92716E-06	2.71209E-10	1.15154E-06	2.53778E-09	1.26376E-06	1.53652E-00
1.18117E-00	6.70267E-07	6.17760E-02	1.56666E-10	7.16666E-11	1.68311E-00
6.96303E-10	6.55219E-10	1.43616E-10	7.91430E-10	7.61577E-07	6.69966E-00
2.86653E-05	1.36200E-06	6.50135E-06	1.25066E-07	2.97036E-07	1.36193E-00
6.78621E-09	6.63793E-07	1.48196E-04	2.37066E-06	1.63669E-07	1.66627E-00
1.07196E-07	7.21975E-09	2.11260E-08	2.29366E-09	2.66652E-09	1.16036E-00
6.67660E-09	1.07276E-07	5.16220E-06	0.0	1.00000E-09	2.53666E-00
2.21310E-06	1.96322E-07	5.06207E-04	1.10656E-06	1.77722E-06	2.93637E-00
2.85311E-10	1.13693E-04	2.45117E-09	1.25666E-06	1.51557E-00	1.16662E-00
6.56622E-09	6.17600E-02	1.25966E-10	6.00571E-11	1.63556E-07	1.90262E-00
7.66116E-11	2.41267E-10	7.66031E-10	7.62219E-07	6.75766E-06	2.96966E-00
1.36200E-06	6.64567E-08	1.21736E-07	2.96166E-03	6.19267E-10	6.05172E-00
6.64366E-07	2.76656E-09	1.25157E-06	1.61661E-07	1.71736E-07	7.16536E-00
7.15566E-04	2.16967E-06	2.31666E-09	1.07260E-09	1.17401E-07	6.68226E-00
1.08616E-07	5.16220E-06	0.0	1.00000E-09	2.67566E-07	2.23666E-00
1.55613E-07	5.05966E-06	6.12636E-06	1.70811E-06	2.91651E-06	1.70956E-00
1.35362E-06	2.76202E-09	1.25117E-06	1.60066E-00	1.15356E-06	6.61666E-00
6.17960E-01	9.95656E-11	6.07072E-11	1.18662E-07	1.26126E-10	7.09631E-00
2.21011E-10	1.36665E-10	7.42578E-07	6.87625E-06	2.96636E-05	1.16260E-00
6.79666E-08	1.26376E-07	2.95165E-07	6.66206E-02	6.90625E-04	6.67103E-00
2.17656E-04	1.26376E-06	1.40772E-07	7.76267E-07	7.19922E-07	7.66392E-00
2.17656E-06	1.26376E-06	1.40772E-07	7.76267E-07	7.19922E-07	7.66392E-00
5.16020E-04	0.0	1.00000E-09	2.70666E-07	2.09066E-06	1.21967E-00
5.37165E-04	1.11666E-01	1.67766E-06	2.91302E-06	1.15366E-10	1.17126E-00
6.81666E-09	1.25372E-06	1.48916E-08	1.16041E-06	6.33666E-09	1.37963E-00
7.92566E-11	5.17969E-11	1.16081E-07	2.16695E-10	6.68771E-10	1.67126E-00
6.72323E-10	7.64770E-01	6.93662E-06	2.47166E-05	1.16200E-06	6.89771E-00
1.29110E-07	1.96160E-07	2.26672E-10	6.64357E-09	6.43559E-07	1.16666E-00
1.21306E-06	1.17919E-07	1.66250E-07	7.26173E-07	7.56966E-08	2.17666E-00
2.17976E-09	1.26208E-07	1.20266E-07	6.17926E-09	1.10352E-07	5.16022E-00
0.0	1.00000E-09	2.73032E-07	2.07666E-06	6.67666E-06	5.08166E-00
1.13991E-06	1.61661E-06	1.96636E-06	1.05698E-10	1.16512E-00	2.67066E-00
1.26661E-06	1.67651E-04	1.11672E-06	6.20022E-06	6.17963E-06	6.16652E-00
6.95966E-11	1.29666E-07	1.86022E-10	5.57625E-10	2.6155E-10	6.36962E-00
7.92566E-07	6.97778E-06	2.96161E-07	1.16100E-04	6.97967E-06	1.21966E-00
2.93366E-07	6.16612E-12	6.97691E-07	6.70967E-07	1.16667E-09	1.26062E-00
1.16655E-07	1.86666E-07	7.27537E-07	7.61613E-08	2.26661E-00	2.30266E-00
9.85656E-10	2.10612E-07	6.66712E-04	1.10626E-07	5.96313E-06	0.0
1.00000E-09	2.76666E-07	2.10612E-04	7.71665E-08	5.08166E-06	1.16666E-00
1.56201E-06	2.96666E-06	7.66366E-11	1.19766E-00	2.91136E-09	1.26766E-00
1.65266E-06	1.17666E-06	6.11177E-09	6.17066E-02	6.1177E-11	6.66477E-00
1.26966E-01	1.63165E-10	6.76636E-10	9.76927E-11	5.95662E-10	7.62266E-00
7.02666E-06	1.01131E-09	1.16200E-06	9.06766E-08	1.10613E-07	2.76166E-00
1.60856E-10	7.00627E-09	6.76697E-07	1.11665E-09	1.66666E-06	1.10645E-00
1.96676E-07	7.16156E-07	7.66516E-06	2.20977E-09	2.27766E-09	6.06266E-00
1.21669E-07	6.61966E-09	1.11192E-07	5.16020E-04	0.0	1.00000E-09
2.75866E-07	2.35666E-06	2.96265E-07	2.66267E-07	1.17406E-00	1.83225E-00
3.25766E-07	5.66922E-10	7.60967E-10	6.95592E-10	1.66666E-06	6.19166E-00
1.02622E-09	1.56076E-10	6.17963E-02	6.19297E-10	1.06533E-10	2.52666E-00
1.11366E-10	1.67516E-10	1.02870E-09	7.56275E-10	9.06029E-08	6.66066E-00
1.96266E-06	1.36200E-06	6.67262E-09	6.69266E-09	6.66933E-00	6.91766E-00
6.82362E-10	6.67666E-08	1.26056E-08	6.90937E-08	1.00076E-09	1.16622E-00
6.15619E-00	2.76126E-06	2.09702E-10	1.29015E-10	9.50067E-09	1.66666E-00
2.73533E-09	2.76966E-09	5.16020E-06	0.0	1.00000E-09	2.61666E-00
2.16266E-06	7.36116E-07	9.95870E-07	6.10026E-00	1.65722E-05	9.70766E-00
1.25696E-09	1.39566E-10	1.97216E-12	1.66631E-06	1.56120E-08	6.28352E-00
1.16176E-09	6.37966E-02	1.30613E-09	2.32894E-10	7.83019E-08	7.10690E-00
5.67500E-10	2.33766E-09	1.53260E-09	2.66612E-07	1.62832E-06	6.05966E-00
1.36200E-06	1.19197E-08	2.56811E-08	1.29660E-07	1.00472E-10	1.66966E-00
1.16016E-07	2.62766E-08	2.81026E-07	6.19762E-09	1.60406E-00	1.65067E-00
9.25276E-09	1.15266E-09	1.11921E-10	1.76909E-08	5.66666E-00	5.62166E-00
2.68193E-04	5.16020E-06	0.0	1.00000E-09	1.67796E-00	2.12616E-00
9.30176E-07	1.69867E-06	1.57057E-07	1.11166E-09	1.55267E-06	1.66052E-00
6.96796E-10	1.12615E-11	1.66001E-08	1.92166E-08	6.31875E-09	1.16801E-00
6.17960E-02	1.10061E-05	1.76598E-10	1.25332E-07	1.26966E-09	9.42016E-00
2.76217E-09	1.52112E-09	6.15652E-07	2.38831E-06	1.01666E-05	1.36200E-00
2.60622E-00	6.13111E-08	1.99812E-07	9.49257E-11	2.52292E-09	2.13793E-00
2.62766E-06	6.78676E-07	1.66176E-08	5.10519E-08	1.02280E-07	1.76177E-00
1.07962E-09	6.79696E-10	1.98076E-04	9.16661E-08	5.73902E-09	6.56616E-00
5.16020E-06	0.0	1.00000E-09	1.91666E-08	2.13059E-06	9.79266E-00
2.67739E-06	2.83026E-07	8.10866E-06	2.06666E-06	1.39679E-00	1.85752E-00
1.17115E-10	1.61651E-06	1.89016E-08	1.08813E-08	5.67807E-09	6.37966E-00
1.16817E-09	1.66662E-10	1.55780E-07	1.65635E-09	1.18858E-09	2.79117E-00
1.61690E-07	5.28160E-07	1.25980E-06	1.36625E-05	1.16200E-00	1.61266E-00
5.92659E-00	2.66699E-07	8.75336E-11	1.67012E-09	2.66666E-07	2.18266E-00

Table 3. CONTINUED

1.96128E-04	0.0	6.30636E 00	0.0	6.28732E 00	6.00000E 00
5.23063E 00	1.35012E-01	7.37099E 00	7.46963E 00	7.74305E 00	8.00000E 00
7.93575E 00	0.13323E 07	1.90084E-02	6.89950E-02	7.05975E 00	7.66061E 00
7.07900E 00	7.03105E 00	8.13743E 00	3.78611E 00	1.00052E-02	5.75036E 00
6.56925E 00	2.81460E 00	6.46540E 00	6.39370E 00	0.0	6.53929E 00
6.40605E 00	7.26621E 07	7.26716E 00	7.38300E 00	7.23130E 00	7.76260E 00
8.31911E 00	8.10449E 07	8.03600E 00	8.90050E 00	8.23446E 00	8.0
7.71991E-07	7.78455E-07	1.01339E-10	1.01360E-10	1.93332E-06	1.96128E-04
0.0	5.33201E-02	0.0	3.07670E-02	2.66350E-01	5.23063E 00
1.35012E-01	2.00771E-01	6.31116E-01	2.00221E-01	1.30956E-01	8.02200E-02
1.12309E-01	1.98000E-02	6.89950E-02	1.33779E-01	1.00169E-01	1.45030E-01
1.36672E-01	1.77390E-01	5.02370E-01	1.00052E-02	6.56959E-02	1.61773E-01
2.07040E 00	1.55001E-01	7.03105E-02	0.0	4.56981E-02	4.17935E-02
0.53066E-02	0.67270E-02	4.70093E-01	1.68362E-01	2.30647E-01	9.60100E-02
7.42090E-02	1.17012E-01	1.33542E-01	6.97173E-01	0.0	178
1.43251E-01	0.51617E-01	6.50659E-01	0.0	28	3.75753E-02
2.01422E 00	9.00457E-01	1.20970E 00	9.99135E-01	0.0	148
2.39647E-01	1.50320E-01	1.71910E 00	9.97331E-01	1.66500E 00	9.76312E-01
0.0	178	2.67375E 00	3.07207E 00	1.30557E 00	0.0
0.0	28	2.38996E 00	2.60555E 00	2.39005E 00	2.57317E 00
2.40062E 00	0.0	148	2.59917E 00	2.73709E 00	3.05036E 00
3.12016E 00	3.10474E 00	2.96357E 00	0.0	178	9.67631E-01
9.69033E-01	28	0.0	0.0	9.44726E-01	28
9.67091E-01	28	9.67563E-01	3.0	148	9.60562E-01
9.65305E-01	9.66769E-01	9.66450E-01	9.65702E-01	5.60233E-01	0.0
1.63970E-00	1.60523E-00	2.00417E-01	2.00410E-01	0.0	98
0.36521E-05	0.0	1.77256E-05	0.0	108	3.30730E-03
0.0	198	1.10049E-06	0.0	28	0.50605E-00
0.50607E-06	0.0	0.85910E-06	0.0	278	3.79669E-00
0.0	148	0.85910E-06	0.0	28	3.04659E-03
0.0	3.79669E-00	3.33900E-00	0.0	28	3.04659E-03
0.0	5.00000E-00	2.03207E-03	1.54000E-03	0.0	38
5.22697E-03	2.34937E-03	7.00109E-00	2.66591E-03	3.20310E-03	0.0
0.0	28	2.00015E-05	1.72929E-00	0.0	2.00303E-00
0.11240E-00	0.0	1.09935E-03	28	2.96053E-03	28
0.77579E-00	0.67802E-00	1.05023E-03	0.21759E-03	8.00445E-00	3.56570E-00
6.10090E-03	5.30730E-00	0.0	0.0	0.0	0.0
50	0.82200E-01	4.35231E 00	4.35237E 00	3.49753E 00	3.49753E 00
2.06100E-03	2.06100E-03	1.52321E-05	9.26760E 00	2.10095E-01	8.29260E 00
2.27296E 01	0.23615E 02	7.01499E 02	2.10372E 01	1.70801E 01	1.90307E 01
1.60090E 01	1.93190E 01	1.32550E 01	2.30973E-01	6.95900E-01	1.06973E 01
1.60715E 01	1.22259E 01	1.61720E 01	1.09300E 01	3.39667E 00	1.06662E-01
7.03320E 00	4.79923E 00	2.99507E 01	8.58194E 00	6.60021E 00	3.03010E-01
0.60526E 00	2.11691E 01	1.23671E 01	1.23730E 01	1.33776E 01	1.07603E 01
1.00350E 01	1.55700E 01	1.55049E 01	1.59607E 01	1.72295E 01	1.65227E 01
7.25970E-01	0.63365E 00	0.63360E 00	3.59235E 00	3.59230E 00	2.10797E-03
2.10790E-03	1.50179E-05	9.37090E 00	2.21260E-01	8.36560E 00	2.25650E 01
0.37077E 02	0.08190E 02	2.17695E 01	1.05131E 01	2.01367E 01	1.60001E 01
2.01000E 01	1.36219E 01	2.04290E-01	7.10713E-01	1.09365E 01	1.00962E 01
1.27560E 01	1.60527E 01	1.56380E 01	3.57553E 00	1.09097E-01	7.91177E 00
0.85991E 00	3.00209E 01	0.64245E 00	6.12611E 01	3.10500E-01	6.00779E 00
2.17015E 01	1.26933E 01	1.26707E 01	1.15910E 01	1.09011E 01	1.03560E 01
1.60540E 01	1.60035E 01	1.64936E 01	1.60265E 01	1.09510E 01	7.0
0.03150E-06	0.07150E-06	0.06600E-07	1.06600E-07	2.10797E-03	2.10790E-03
1.50179E-05	1.40307E 00	2.21260E-01	5.43350E-01	6.36367E 00	0.37477E 02
0.00190E 02	0.74035E 00	0.75579E 00	7.70170E 00	1.62969E 00	1.10051E 03
2.73910E 00	2.04290E-01	7.10713E-01	1.11493E 00	7.28206E-01	1.50430E 00
1.05750E 00	0.86175E 00	0.0	1.09097E-01	1.12079E 00	1.35372E 00
1.06209E 01	2.70655E 02	1.05055E 00	3.10500E-01	9.07321E-01	9.10360E-01
7.00700E-01	6.90150E-01	7.62203E 00	1.90007E 00	1.49017E 00	9.09715E-01
1.70910E 00	1.60015E 00	1.33252E 00	0.16870E 00	0.0	148
2.23255E-02	1.01407E-01	0.0	38	5.49330E 00	6.20603E-03
0.15390E 00	9.09521E-04	3.0	158	1.21209E-04	2.69030E 00
1.35590E-01	5.10000E 00	2.37119E-02	0.0	148	2.81522E 00
1.00000E 00	0.0	38	1.50295E 00	2.51197E 00	2.00350E 00
2.51390E 00	0.0	158	1.32160E 00	2.07625E 00	2.07262E 00
2.93050E 00	2.70360E 00	0.0	178	3.25000E-02	0.0
3.09050E-02	28	0.0	28	3.32735E-02	28
3.25000E-01	28	3.20360E-02	0.0	148	3.50350E-02
3.06541E-02	3.32113E-02	1.33502E-02	3.02969E-02	1.59809E-02	0.0
0.0	0.0	1.33809E-05	0.0	38	0.0
50	4.05727E-01	0.49775E 00	0.49770E 00	3.56125E 00	3.56125E 00
3.6172E-02	3.61720E-02	3.70205E 01	7.33300E 01	0.80660E 00	1.35521E 01
0.72550E 02	0.52263E 03	7.30090E 03	2.19731E 02	2.00000E 02	2.37015E 02
7.49700E 01	2.03561E 02	6.10567E 01	1.00070E 00	1.15113E 01	2.70106E 01
9.63540E 01	1.00010E 02	6.32130E 01	0.09300E 01	3.55209E 00	3.30515E 01
0.00953E 01	1.13371E 01	5.26202E 02	2.50430E 02	0.92102E 02	6.79990E 00
2.22379E 01	9.31000E 01	8.65090E 01	8.07320E 02	1.03600E 02	5.17620E 02
7.30556E 01	7.09715E 01	7.23060E 01	5.20022E 01	1.11203E 02	6.95052E 01
7.20277E-01	0.75019E 00	0.75020E 00	3.71105E 00	3.71105E 00	3.60672E-02
3.60673E-02	3.75652E 01	7.30781E 01	0.02960E 02	1.36131E 01	0.69635E 02
0.50304E 03	7.30751E 03	2.20377E 04	2.70900E 02	2.37105E 02	7.01376E 01
2.02807E 02	0.09902E 01	1.00471E 00	1.10621E 01	2.70376E 01	9.61652E 01
1.39103E 02	6.32287E 01	8.00095E 01	3.70060E 00	3.31200E 01	0.09717E 01
1.13077E 01	5.20403E 02	2.40607E 02	4.09305E 02	6.77601E 00	2.22300E 01
9.25000E 01	0.70319E 01	0.02530E 02	1.03502E 02	5.15079E 02	7.29672E 01
7.07033E 01	7.32253E 01	5.35550E 01	1.19906E 02	6.95201E 01	2.90265E-05
1.00171E-00	1.00171E-00	9.52125E-06	9.52127E-06	3.60672E-02	3.60673E-02
3.75652E 01	5.09559E 01	0.82960E 00	5.03352E 00	3.51797E 02	4.50300E 03
7.30751E 03	1.00671E 02	2.60051E 02	2.19640E 02	0.90000E 01	1.67291E 02
0.00053E 01	1.00071E 00	1.10621E 01	0.80412E 00	1.57413E 01	1.02300E 02
2.05401E 01	7.26907E 01	0.0	3.31200E 01	2.67232E 01	5.00069E 00
5.20003E 02	2.22075E 02	1.20670E 02	6.77601E 00	1.07200E 01	0.95200E 01
4.60012E 01	3.05577E 02	9.03011E 01	5.00762E 02	6.17109E 01	0.61639E 01
2.59195E 01	2.53076E 01	1.70970E 01	5.30017E 01	0.0	238
6.05055E 01	0.0	3.09190E 01	0.0	148	2.30010E-00
3.00931E 01	1.11391E-01	0.12202E 01	9.65070E-02	0.0	238
2.60700E 00	0.0	2.00700E 00	0.0	148	2.31052E 00

Table 3. CONTINUED

2.07331E-06	2.86903E-06	2.93252E-06	2.70003E-06	0.0	018
6.09751E-06	6.70005E-06	6.45220E-06	6.51905E-06	6.87079E-06	7.01303E-06
0.0	0.0	2.10031E-06	0.0	0.0	0.0
50	0.01320E-01	0.70703E-00	0.70710E-00	3.05710E-00	3.09002E-00
4.41000E-01	4.00007E-01	1.15509E-00	1.29000E-01	5.90100E-01	3.83005E-00
1.03700E-02	1.10910E-00	6.60011E-02	3.60200E-00	3.30000E-01	1.72612E-02
1.20900E-01	2.30020E-01	1.10035E-02	4.09290E-01	6.30199E-00	1.56100E-01
2.03610E-02	4.50920E-01	2.00910E-02	3.37797E-01	3.00790E-00	1.90100E-01
0.70590E-01	1.00092E-02	6.60012E-03	4.07675E-01	5.20000E-01	0.30770E-01
1.30010E-02	2.63065E-01	3.70370E-01	9.00003E-01	6.00013E-02	6.10571E-03
5.00025E-01	1.01107E-01	1.32023E-03	7.71939E-02	1.01092E-03	1.29007E-02
7.95305E-01	4.70005E-00	4.75200E-03	3.00003E-00	3.00135E-00	0.02000E-01
0.01000E-01	1.10095E-00	0.12900E-01	5.91590E-01	3.00092E-00	1.03900E-02
1.10201E-00	6.62200E-02	3.70320E-00	3.19000E-03	1.72007E-02	1.20900E-01
2.35090E-01	1.12771E-02	0.90090E-01	6.31090E-00	1.50159E-01	2.03753E-02
0.00113E-01	2.01001E-02	3.30307E-01	3.65573E-00	1.90000E-01	0.70901E-01
1.02903E-02	6.02227E-03	0.00371E-01	5.20100E-01	0.30022E-01	1.37100E-02
2.60009E-01	3.75202E-01	9.50525E-01	6.62220E-02	0.10079E-03	5.72121E-01
1.01250E-01	1.32270E-01	7.65701E-02	1.31010E-03	1.20200E-02	3.07002E-03
1.70995E-03	1.70590E-01	7.99290E-05	7.99200E-05	0.02000E-01	0.01000E-01
1.10995E-00	1.29005E-01	5.91590E-01	3.00092E-00	1.03900E-02	1.19201E-00
6.62220E-02	3.60337E-00	3.30097E-03	1.60007E-02	2.70700E-00	1.05130E-01
1.05027E-02	0.00090E-01	6.31090E-00	3.12500E-00	2.00529E-01	3.70100E-01
0.23910E-01	2.30000E-01	7.05000E-05	1.90000E-01	0.70901E-01	1.02903E-02
6.02227E-03	0.00371E-01	5.20100E-01	0.30022E-01	1.37100E-02	2.00009E-01
3.75202E-01	5.50525E-01	6.62220E-02	6.10079E-03	0.09120E-01	1.22010E-03
0.93313E-02	7.10252E-02	2.63910E-02	1.12070E-02	0.0	238
2.00000E-02	0.0	2.20559E-02	0.0	100	2.90900E-09
0.20097E-02	1.30200E-01	7.35333E-02	6.77001E-03	0.0	238
2.50299E-00	0.0	2.03000E-00	0.0	100	2.31951E-00
2.07331E-06	2.86903E-06	2.93230E-06	2.73997E-06	0.0	018
7.00050E-11	1.21590E-09	1.10323E-09	1.17535E-09	1.20200E-09	5.00000E-10
0.0	100				
70	1	900			
90	2.90573E-00	2.01031E-00	2.03300E-00	3.00090E-00	3.00097E-00
0.0	30	6.00125E-00	0.0	0.00000E-00	6.07730E-00
0.0	20	6.02770E-00	0.52070E-00	6.70213E-00	7.07510E-00
6.00007E-00	6.70510E-00	0.0	20	7.07190E-00	5.39000E-00
6.60100E-00	6.20711E-00	6.52532E-00	3.62071E-00	0.0	5.60005E-00
6.27273E-00	0.0	5.90190E-00	6.10070E-00	0.0	6.37002E-00
6.35007E-00	7.00000E-00	20	6.00329E-00	6.05199E-00	6.32070E-00
7.00533E-00	6.10530E-00	6.77909E-00	6.92702E-00	6.51250E-00	0.0
70	2	50	30	2	20
	1	20	1	20	1
	2	20	1	2	120
00	6.70003E-01	1.00335E-01	0.50007E-01	1.93907E-01	4.50000E-00
1.90330E-01	3.51095E-00	1.30200E-01	3.51093E-00	1.30207E-01	0.0
0.0	30	7.91039E-00	2.51713E-01	0.0	7.00050E-00
2.51000E-01	1.61090E-01	1.01022E-01	0.0	20	1.00059E-01
3.00903E-01	9.70002E-00	3.00003E-01	1.23061E-01	7.57009E-01	1.00220E-01
2.20000E-01	1.00030E-01	1.20709E-01	1.00000E-01	5.90255E-01	0.0
0.0	20	1.37000E-01	2.21000E-01	1.00170E-01	1.53571E-01
1.12205E-01	1.72001E-01	1.00239E-01	1.62203E-01	1.07000E-01	0.30037E-01
3.50211E-00	1.10000E-01	0.0	6.75576E-00	0.30037E-02	7.00025E-00
1.30501E-01	0.0	5.00005E-00	1.60279E-01	5.60333E-01	1.20009E-01
0.0	5.60770E-00	0.90500E-02	2.07503E-01	9.02555E-02	1.10000E-01
1.90000E-01	1.10000E-01	1.90000E-01	5.95703E-00	2.21003E-01	6.90000E-00
2.10001E-01	1.00055E-01	9.37000E-01	1.50095E-01	2.00002E-01	1.10007E-01
1.00200E-01	1.00002E-01	1.02000E-01	1.15353E-01	2.79000E-01	1.27300E-01
2.05700E-01	0.0	0.0	0.0	0.0	0.0
70	1	20	3	00	1
	3	20	1	3	20
	2	3	20	1	120
00	6.75001E-01	5.15095E-02	0.61503E-00	1.20000E-01	2.60333E-07
0.63507E-00	1.20001E-01	2.65000E-07	7.43907E-00	7.33011E-02	0.00071E-00
3.63900E-00	7.33010E-02	0.00002E-00	0.0	30	1.01000E-01
2.57231E-02	3.79200E-06	0.0	0.16307E-00	2.10007E-02	3.79200E-06
1.17020E-02	2.75715E-02	1.07070E-06	0.0	20	7.10010E-01
0.31709E-02	3.60999E-05	1.00252E-01	1.09077E-02	7.10701E-06	1.70150E-01
3.00000E-02	5.00710E-05	2.50770E-01	0.63000E-02	6.77000E-00	3.55932E-01
0.91001E-02	6.90002E-09	1.00010E-01	1.72051E-02	1.10000E-05	0.0
0.0	20	1.09790E-01	3.00900E-02	3.51910E-04	1.10010E-01
1.09009E-02	3.50520E-06	3.00070E-01	1.92051E-02	2.70903E-06	1.17515E-01
1.71909E-02	3.02290E-05	1.61709E-01	2.01222E-02	0.07070E-06	3.03111E-00
7.30120E-02	0.0	1.02250E-01	2.72100E-02	0.03700E-07	6.20000E-00
1.99330E-02	1.23050E-06	0.0	2.65105E-01	2.73005E-02	1.01000E-06
3.00000E-02	1.21705E-02	1.05293E-06	0.0	1.10300E-01	1.27305E-02
0.91000E-07	0.30257E-01	3.00507E-02	0.91000E-07	0.17700E-01	1.03500E-01
2.72109E-06	4.50933E-02	1.03500E-01	2.72109E-06	5.27007E-00	1.22015E-02
3.20001E-06	7.10057E-00	1.50000E-02	2.90795E-06	1.12107E-01	1.60000E-02
2.39730E-05	3.05070E-01	1.50000E-02	1.62303E-06	1.20000E-01	2.92005E-02
2.27200E-06	2.79391E-01	1.35910E-02	7.20130E-07	1.21001E-01	1.01021E-02
1.57000E-06	1.55230E-01	2.17500E-02	2.57125E-06	0.0	0.0
70	1	20	3	00	1
	2	30	2	30	2
	2	20	1	2	20
	1	20	1	2	30
00	7.92205E-01	0.05001E-02	0.75000E-00	1.10370E-01	0.0
0.05701E-10	0.75023E-00	1.10309E-01	0.0	0.50002E-10	3.00009E-00
7.11502E-02	0.0	7.05000E-11	3.00110E-00	7.11500E-02	0.0
7.05071E-11	0.0	0.0	1.79215E-02	0.0	20
1.70079E-02	0.0	1.15333E-02	0.0	20	1.90000E-02
2.30905E-02	9.50005E-09	1.07070E-00	0.90250E-03	0.39950E-00	3.07700E-03
1.00300E-07	9.50005E-00	1.17922E-02	0.99003E-00	3.71579E-03	0.29200E-10
7.30000E-00	2.20271E-02	0.0	20	1.20900E-01	1.60037E-02
1.20900E-01	1.60350E-02	0.99290E-00	1.37000E-02	1.20900E-01	1.79530E-02
1.10391E-00	1.90920E-07	9.99000E-00	1.30251E-02	3.65559E-00	0.90791E-02
0.0	20	2.30777E-02	0.0	2.10001E-02	0.0
0.0	20	1.72015E-02	0.0	2.73527E-02	0.0
0.0	20	7.00009E-02	0.0	3.00007E-02	0.0

Table 3. CONTINUED

2.00951E-04	2.02432E-04	1.67669E-04	1.06793E-04	1.70726E-04	1.27047E-04	CARD	89
1.00449E-04	1.01502E-04	1.02750E-04	0.37947E-04	0.20950E-04	1.03072E-04	CARD	89
1.69003E-07	2.10025E-07	1.31200E-07	2.09950E-07	1.23719E-07	7.17251E-07	CARD	90
5.70070E-04	2.07493E-05	1.36200E-04	1.95227E-04	1.07400E-07	3.04300E-07	CARD	91
6.04101E-11	6.04120E-07	0.19233E-07	1.07510E-04	1.07000E-04	1.35003E-07	CARD	92
9.10050E-08	6.30060E-07	1.72013E-04	7.71023E-04	7.00000E-04	1.00000E-04	CARD	93
2.04002E-07	6.04100E-07	0.57705E-04	0.10020E-04	0.0	1.00000E-04	CARD	94
2.36043E-07	2.21041E-04	1.06501E-04	0.70020E-04	1.20000E-04	2.17050E-04	CARD	95
2.00091E-04	1.37200E-04	1.25130E-04	0.03250E-04	1.20013E-04	1.65007E-04	CARD	96
1.31021E-04	0.69505E-04	0.37000E-02	7.16350E-10	0.00000E-11	1.65000E-07	CARD	97
1.00045E-09	1.21500E-04	2.30121E-04	1.10770E-04	7.20000E-07	0.30072E-04	CARD	98
2.72351E-05	1.26200E-04	7.07000E-04	1.17670E-07	7.00110E-07	0.95130E-11	CARD	99
0.00130E-30	4.30000E-07	1.70001E-04	1.16205E-04	1.60000E-07	1.00052E-07	CARD	100
6.77050E-02	6.07000E-04	1.04772E-04	0.23007E-04	1.10100E-04	3.23017E-07	CARD	101
7.02490E-09	1.03910E-07	0.10020E-04	0.0	1.00000E-04	0.04161E-07	CARD	102
2.20500E-04	0.07000E-07	0.00700E-04	1.32232E-04	1.72300E-04	2.03000E-04	CARD	103
1.04200E-07	1.00000E-04	1.00321E-04	1.20070E-04	1.00000E-04	1.27050E-04	CARD	104
9.13051E-04	0.37000E-02	0.17000E-10	0.10551E-11	1.60022E-07	1.01007E-04	CARD	105
1.10000E-04	1.00507E-04	1.00025E-04	1.33000E-07	4.70713E-04	2.95150E-05	CARD	106
1.36200E-04	0.57000E-04	1.25007E-07	1.93770E-07	3.03030E-11	0.70772E-04	CARD	107
0.50390E-07	1.25327E-04	1.22003E-04	1.70000E-07	1.00000E-07	7.00000E-07	CARD	108
1.05170E-08	2.16210E-04	2.00700E-04	0.92520E-04	3.00000E-07	7.13510E-09	CARD	109
1.00000E-07	5.10020E-04	0.0	1.10000E-04	2.00700E-04	2.10000E-04	CARD	110
7.20700E-07	0.04110E-04	1.00570E-04	1.00222E-04	2.95010E-04	0.00300E-04	CARD	111
1.50705E-08	3.07000E-04	1.22501E-04	1.51102E-04	1.10707E-04	0.66917E-04	CARD	112
0.37060E-02	0.56605E-10	0.25000E-11	1.55000E-07	1.35000E-04	1.00120E-04	CARD	113
1.10267E-09	1.20041E-10	7.12732E-07	7.12220E-04	1.07000E-04	1.30200E-04	CARD	114

1.00000E-07	1.22470E-10	0.27000E-10	0.30200E-11	1.20010E-10	0.57000E-07	CARD	1177
6.66113E-06	2.05232E-05	1.36200E-04	0.30100E-04	1.19332E-04	2.70702E-07	CARD	1178
2.91000E-12	6.66030E-04	0.43720E-07	1.71073E-10	1.25237E-06	1.06917E-07	CARD	1179
1.00000E-07	7.00172E-07	7.00032E-04	1.00700E-04	1.05233E-04	6.40103E-10	CARD	1180
2.00000E-07	5.02312E-10	1.10630E-07	0.10020E-04	0.0	1.00000E-04	CARD	1181
2.10210E-07	2.36162E-04	0.0	30	2.01720E-05		CARD	1182
0.0	0.0	1.00000E-04	0.0	30	0.77000E-02	CARD	1183
0.0	10P	1.36200E-04	0.0	10P	5.10020E-04	CARD	1184
0.0	1.00000E-04	0.0	2.36162E-04	0.0	30	CARD	1185
2.01720E-05	0.0	0.0	1.00000E-04	0.0	30	CARD	1186
0.37060E-02	0.0	10P	1.36200E-04	0.0	10P	CARD	1187
5.10020E-04	0.0	1.00000E-04	0.0	2.36162E-04	0.0	CARD	1188
0.0	30	2.01720E-05	0.0	0.0	1.00000E-04	CARD	1189
0.0	30	0.37060E-02	0.0	10P	1.36200E-04	CARD	1190
0.0	10P	5.10020E-04	0.0	1.00000E-04	0.0	CARD	1191
2.36162E-04	0.0	30	2.01720E-05	0.0	0.0	CARD	1192
1.00000E-04	0.0	30	0.37060E-02	0.0	10P	CARD	1193
1.36200E-04	0.0	10P	5.10020E-04	0.0	1.00000E-04	CARD	1194
0.0	2.36162E-04	0.0	30	2.01720E-05	0.0	CARD	1195
0.0	0.0	0.0	1.00000E-04	0.0	0.0	CARD	1196
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1197
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1198
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1199
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1200
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1201
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1202
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1203
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1204
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1205
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1206
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1207
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1208
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1209
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1210
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1211
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1212
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1213
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1214
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1215
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1216
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1217
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1218
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1219
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1220
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1221
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1222
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1223
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1224
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1225
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1226
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1227
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1228
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1229
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1230
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1231
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1232
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1233
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1234
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1235
0.0	0.0	0.0	0.0	0.0	0.0	CARD	1236

- NOTE
PAGES
DELETED -

Table 3. CONTINUED

SUMMARY OF FILE PROFILES		FILE NAME		L/O CODE		L/O CODE		TOTAL FILE SIZE		TOTAL # OF FILES		TOTAL # OF FILES	
FILE NAME	FILE SIZE	EXTENSION	FILE TYPE	FILE SIZE	FILE TYPE	FILE SIZE	FILE TYPE	FILE SIZE	FILE TYPE	FILE SIZE	FILE TYPE	FILE SIZE	FILE TYPE
DATA FILE	1000000	DATA	DATA	1000000	DATA	1000000	DATA	1000000	DATA	1000000	DATA	1000000	DATA
INDEX FILE	500000	INDEX	INDEX	500000	INDEX	500000	INDEX	500000	INDEX	500000	INDEX	500000	INDEX
CONTROL FILE	200000	CONTROL	CONTROL	200000	CONTROL	200000	CONTROL	200000	CONTROL	200000	CONTROL	200000	CONTROL
REPORT FILE	100000	REPORT	REPORT	100000	REPORT	100000	REPORT	100000	REPORT	100000	REPORT	100000	REPORT
LOG FILE	50000	LOG	LOG	50000	LOG	50000	LOG	50000	LOG	50000	LOG	50000	LOG
TEMP FILE	20000	TEMP	TEMP	20000	TEMP	20000	TEMP	20000	TEMP	20000	TEMP	20000	TEMP
OTHER FILE	10000	OTHER	OTHER	10000	OTHER	10000	OTHER	10000	OTHER	10000	OTHER	10000	OTHER
TOTAL	1800000			1800000		1800000		1800000		1800000		1800000	

FILE NAME	FILE SIZE	EXTENSION	FILE TYPE	FILE SIZE	FILE TYPE	FILE SIZE	FILE TYPE	FILE SIZE	FILE TYPE	FILE SIZE	FILE TYPE	FILE SIZE	FILE TYPE
DATA FILE	1000000	DATA	DATA	1000000	DATA	1000000	DATA	1000000	DATA	1000000	DATA	1000000	DATA
INDEX FILE	500000	INDEX	INDEX	500000	INDEX	500000	INDEX	500000	INDEX	500000	INDEX	500000	INDEX
CONTROL FILE	200000	CONTROL	CONTROL	200000	CONTROL	200000	CONTROL	200000	CONTROL	200000	CONTROL	200000	CONTROL
REPORT FILE	100000	REPORT	REPORT	100000	REPORT	100000	REPORT	100000	REPORT	100000	REPORT	100000	REPORT
LOG FILE	50000	LOG	LOG	50000	LOG	50000	LOG	50000	LOG	50000	LOG	50000	LOG
TEMP FILE	20000	TEMP	TEMP	20000	TEMP	20000	TEMP	20000	TEMP	20000	TEMP	20000	TEMP
OTHER FILE	10000	OTHER	OTHER	10000	OTHER	10000	OTHER	10000	OTHER	10000	OTHER	10000	OTHER
TOTAL	1800000			1800000		1800000		1800000		1800000		1800000	

FILE NAME	FILE SIZE	EXTENSION	FILE TYPE	FILE SIZE	FILE TYPE	FILE SIZE	FILE TYPE	FILE SIZE	FILE TYPE	FILE SIZE	FILE TYPE	FILE SIZE	FILE TYPE
DATA FILE	1000000	DATA	DATA	1000000	DATA	1000000	DATA	1000000	DATA	1000000	DATA	1000000	DATA
INDEX FILE	500000	INDEX	INDEX	500000	INDEX	500000	INDEX	500000	INDEX	500000	INDEX	500000	INDEX
CONTROL FILE	200000	CONTROL	CONTROL	200000	CONTROL	200000	CONTROL	200000	CONTROL	200000	CONTROL	200000	CONTROL
REPORT FILE	100000	REPORT	REPORT	100000	REPORT	100000	REPORT	100000	REPORT	100000	REPORT	100000	REPORT
LOG FILE	50000	LOG	LOG	50000	LOG	50000	LOG	50000	LOG	50000	LOG	50000	LOG
TEMP FILE	20000	TEMP	TEMP	20000	TEMP	20000	TEMP	20000	TEMP	20000	TEMP	20000	TEMP
OTHER FILE	10000	OTHER	OTHER	10000	OTHER	10000	OTHER	10000	OTHER	10000	OTHER	10000	OTHER
TOTAL	1800000			1800000		1800000		1800000		1800000		1800000	

Table 3. CONTINUED

SPECIAL SCRATCH DATASET REQUIREMENTS
MAXIMUM PHYSICAL RECORD IS 7200 WORDS

SIZE COMPILER ARRAYS, CONTROL 31 DATA 70003
FILE 24 DEFAULTS TO CORE - NO. RECS, REC. LNGTH, TOT. LNGTH, START LOC, CORE LEFT. 4 3400 10500 1 35000
FILE 27 DEFAULTS TO CORE - NO. RECS, REC. LNGTH, TOT. LNGTH, START LOC, CORE LEFT. 4 3400 10500 10500 40000
FILE 28 DEFAULTS TO CORE - NO. RECS, REC. LNGTH, TOT. LNGTH, START LOC, CORE LEFT. 4 3400 10500 20120 26353
DIRECT ACCESS FILE 40 REQUIRES 4 RECORDS 7367 WORDS IS LENGTH

NO PARAMETERS FOLLOW FOR 01 = 3520 AND 02 = 32000
02- 10 03- 10 04- 1 05- 0 06- 10 07- 1 08- 1 09- 5 10- 5 11- 7 12- 1 13- 5 14- 1 15- 10
016- 19 (NOTE THAT IF THE FILES ARE TO BE EXPANDED FROM EXISTING DEVICES, 016- 19)

REQUIRED DISK STORAGE SPACE FOR FILE (UNITS 24, 27, 28) IS 66000 BYTES.
FOR CONSTRAINTS (UNIT 40) IS 200000 BYTES.
FOR CONSTRAINTS (UNIT 23) IS 35000 BYTES.
REQUIRED TOTAL DISK STORAGE SPACE IS 6301400 BYTES.

FOR THE ASSIGNED DATA STORAGE, THE REQUIRED MEDIUM SIZE IS APPROXIMATELY 490K BYTES

MINIMUM STORAGE USED FOR MACROSCOPIC CROSS SECTION CALCULATION 10756 WORDS

THE BAKING AND BURNING DIFFUSION COEFFICIENTS ARE 0.20632E 00 0.07740E-01

FILE NAME DESCRIPTION - POINT IS LOCATED AT THE CENTER OF THE WELDER HEAD:

Table with 10 columns: DISTANCE TO POINT - DIMENSION 1 (LEFT TO RIGHT), DISTANCE TO POINT - DIMENSION 2 (TOP TO BOTTOM), and 8 numerical columns. Rows 1-13 show data for Dimension 1, and rows 14-26 show data for Dimension 2.

DESIRABLE INITIAL PARAMETERS FOR ITERATIVE PROCEDURE

REFERENCE POINT FOR INITIALIZATION WILL BE AT COLUMN = 26 ROW = 26 PLATE = 1 TUBE = 116
INITIAL OUTER ITERATION HIGHVALUE 0.064000 OPTIO = 95
INITIAL OVERRELAXATION COEFFICIENTS BAL. 1.530000 MIN. 1.252676 INNER ITERATIONS BAL. 0 0 0 OPTIO = 0
HIGH POINT BURN OPTIO = 1
OUTER ITERATION LIMIT TO BE USED 75 ESTIMATED 31

MINIMUM STORAGE USED FOR CALCULATING INITIAL PARAMETERS WAS 0439

INITIAL FLUX IS PRC(J,K)OPT(I)OPT(K)

TOTAL CORE REQUIRED FOR DATA STORAGE IS 64903 WORDS
BLANKED CPU AND CLOCK TIMES ARE 0.007 1.092

A FILE - SIGNALS PROFILE FOLLOWS
0 TUBES HZ, 0 TUBES HZ - CHECKOUT DATA ON TUBES
016-1 000000

Table with 10 columns: TYPE, YLOC, ICYD, OCYD, FLUX CHANGE, 40-40R, O'HEP-RU, SEP-10C, ACCURATION, PARAMETER, SOURCE, 0-00ED, 0-CALLC. Rows 1-11 show data for ICYD and OCYD, and rows 12-13 show data for 0-00ED and 0-CALLC.

Table with 10 columns: 0-00ED, 0-00ED, 0-00ED, 0-00ED, 0-00ED, 0-00ED, 0-00ED, 0-00ED, 0-00ED, 0-00ED. Rows 1-35 show data for various 0-00ED values.

Table 3. CONTINUED

0.85161E 13	1.06150E 14	1.02 83E 16	9.88709E 13	9.10063E 13	6.70077E 13	6.88F22E 17	6.39098E 13	3.52776E 13
2.03111E 13	2.27210E 13	1.02879E 13	1.06674E 13	1.17969E 13	6.88E55E 12	1.62828E 12	4.90113E 12	6.47003E 12
0.35763E 13	9.99598E 13	9.88986E 13	9.07794E 13	7.92825E 13	6.89108E 13	5.28892E 13	8.28469E 13	3.81878E 13
2.73560E 13	2.19120E 13	1.75617E 13	1.88866E 13	1.13060E 13	9.07325E 12	1.27295E 12	1.42169E 12	4.82762E 12
7.65797E 13	9.06589E 13	9.88983E 13	8.17226E 13	7.28186E 13	6.01882E 13	6.89625E 13	3.88065E 13	3.15561E 13
2.52206E 13	2.05189E 12	1.61112E 13	1.28817E 13	1.07216E 13	8.26801E 12	4.59889E 12	5.78111E 12	3.47789E 12
6.72606E 13	7.79803E 13	7.68831E 13	7.07216E 13	6.07839E 13	5.01588E 13	4.06897E 13	3.25873E 13	2.60078E 13
2.07255E 13	1.45172E 13	1.31783E 13	1.05188E 13	9.88298E 12	6.78928E 12	5.38225E 12	4.21899E 12	3.17088E 12
0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
3.30688E 13	2.18831E 12							4.44329E 13

THE MAXIMUM POWER DENSITY IS AT PLANE 1, ROW 16, AND COLUMN 1 AND IS 1.966760E 09 WATTS/CC.

THE MAXIMUM NEUTRON DENSITY IS AT PLANE 1, ROW 17, AND COLUMN 1 AND IS 5.677862E 09 NEUTRONS/CC.

THE MAXIMUM POWER DENSITY (WATTS/CC) IN EACH ZONE IS								
1.62532E 01	1.68687E 01	1.53862E 01	1.31875E 01	1.09401E 01	9.93568E 00	7.27898E 00	5.92792E 00	4.78823E 00
3.79781E 00	3.06681E 00	2.87988E 00	2.70665E 00	1.62596E 00	1.31807E 00	1.06823E 00	8.68169E 00	7.33208E 01
1.58873E 01	1.68307E 01	1.52297E 01	1.38816E 01	1.09137E 01	8.92898E 00	7.22915E 00	5.92792E 00	4.78823E 00
3.78992E 00	3.05657E 00	2.86993E 00	2.69507E 00	1.61812E 00	1.38836E 00	1.05895E 00	8.77873E 00	7.22912E 01
1.58542E 01	1.63819E 01	1.50788E 01	1.39569E 01	1.09756E 01	8.98606E 00	7.27822E 00	5.92892E 00	4.87755E 00
3.77806E 00	3.08809E 00	2.85118E 00	2.78218E 00	1.60783E 00	1.29899E 00	1.08259E 00	8.88268E 00	7.10122E 01
1.68816E 01	1.58893E 01	1.48833E 01	1.27883E 01	1.07768E 01	8.88158E 00	7.18822E 00	5.77888E 00	4.68888E 00
3.78768E 00	3.08892E 00	2.81851E 00	1.98827E 00	1.57859E 00	1.26832E 00	1.02808E 00	8.78199E 00	6.91713E 01
1.62878E 01	1.53875E 01	1.48861E 01	1.25351E 01	1.06131E 01	8.72852E 00	7.07788E 00	5.71592E 00	4.58888E 00
3.67821E 00	2.95882E 00	2.37829E 00	1.98868E 00	1.53355E 00	1.23353E 00	1.07852E 00	7.88888E 00	6.88122E 01
1.39528E 01	1.45973E 01	1.38816E 01	1.21868E 01	1.02573E 01	8.58828E 00	6.97898E 00	5.77733E 00	4.87288E 00
3.58229E 00	2.86981E 00	2.29838E 00	1.88889E 00	1.48881E 00	1.18888E 00	1.07888E 00	7.57888E 00	6.37888E 01
1.28831E 01	1.38892E 01	1.28838E 01	1.13827E 01	9.72751E 00	8.03788E 00	6.78888E 00	5.78888E 00	4.18888E 00
3.38728E 00	2.87323E 00	2.13888E 00	1.78838E 00	1.36888E 00	1.09232E 00	8.78888E 00	6.88888E 00	5.78888E 01
1.31583E 01	1.36182E 01	1.25892E 01	1.08888E 01	9.88888E 00	7.38888E 00	5.98888E 00	4.71312E 00	3.78888E 00
2.97328E 00	2.36387E 00	1.88888E 00	1.48888E 00	1.18888E 00	9.52131E 00	7.58132E 00	5.98532E 00	4.78888E 01
0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
0.0	0.0							

THE RELATIVE POWER DENSITY TRAVERSE LEFT-TO-RIGHT IS								
1.08888E 00	9.98828E 01	9.93885E 01	9.98888E 01	9.97776E 01	9.88888E 01	9.88158E 01	9.88888E 01	9.78738E 01
9.68188E 01	9.68218E 01	9.61822E 01	9.53888E 01	9.48888E 01	9.43572E 01	9.28888E 01	9.18888E 01	9.18252E 01
9.02838E 01	8.78117E 01	8.65786E 01	8.38888E 01	8.18775E 01	7.98888E 01	7.68738E 01	7.88888E 01	7.38888E 01
7.87818E 01	7.72268E 01	0.0	7.7	3.0	0.0	7.7	0.0	

THE RELATIVE POWER DENSITY TRAVERSE TOP-TO-BOTTOM IS								
0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
6.0	8.25330E 01	4.63888E 01	9.38888E 01	1.00000E 00	8.88888E 01	4.93775E 01	1.77278E 01	7.62388E 01
6.88851E 01	6.18888E 01	5.78888E 01	4.93888E 01	4.28182E 01	3.98188E 01	3.83888E 01	3.15533E 01	2.78288E 01
2.53252E 01	2.25288E 01	2.03788E 01	1.91888E 01	1.82822E 01	1.87677E 01	1.32721E 01	1.18813E 01	1.07388E 01
9.68387E 02	8.68816E 02	7.91736E 02	7.98888E 02	6.37563E 02	5.71221E 02	5.18888E 02	4.88888E 02	4.38888E 02
4.27388E 02	0.0	0.0	0.0	0.0	0.0	0.0		

POWER DENSITY IMPACT FILE PROBT (NEUTRON 1) HAS BEEN WRITTEN ON SBI MEMORY 18

BOOK USE OF CONTAINER ARRAYS, CONTROL 11, MAX DATA 87600

TOTAL CPU MINUTES USED 1.107 TOTAL CLOCK MINUTES USED 7.017 TOTAL I/O USED 28%

PROB# - KIPROBT BOOKLE - PRE-RELEASE VERSION 16 - AUGUST 16, 1979 - QUALITY ASSURANCE LEVEL 0

CASE TITLE - SAMPLE PROBLEM, TWO DIMENSIONAL SPHERICAL REACTOR HYDRAULICS

SIZE CONTAINER ARRAYS, CONTROL 4 DATA 1

TITLE OF THE LATEST VERSION CROSS SECTION FILE
 T100 SAME AS T105 PLUS W-237, L155 20-135

METHOD OF SOLUTION - EXPLICIT CHAIN

THE LONGEST EXPLICIT CHAIN IS 16

CONTINUOUS FUELING MODE

FILES READ BEFORE COMPUTING FUEL MATERIAL COMPOSITION FOR ZONE PLOTS	185
NUMBER OF CROSS SECTION FILES THROUGH THE REACTOR	8
NUMBER OF ZONES ALONG EACH BODY PATH	18
ZONE PLOT OUTPUT	1 2087 185 THROUGH ZONE 152

MAXIMUM ARRAY SIZE USED FOR INITIAL PROCESSING IS 2568

STORAGE REQUESTED FOR MAXIMUM DATA IS 2568

STORAGE SUPPLIED IS	10928
MAXIMUM STORAGE REQUESTED IS	62804
MINIMUM STORAGE REQUESTED IS	12136

MODES = 0 MODPRT = -1

NUMBER ACTUALLY USED WILL BE 62804

DATA-TO-LATEST VERSION NUMBER NOT AVAILABLE FOR LINEAR PLOT APPROXIMATION

— CONTINUOUS
 FUELING
 EXPOSURE
 CALCULATION —

Table 3. CONTINUED

EXPOSURE TIME STEP SIZE IS 2.726700E-06 DAYS
 EXPOSURE TIME STEP IS 1.000000E-07 DAYS (0.000000 OF SECONDS) THE NUMBER OF PASSES IS 2
 REFERENCE POINT 1.000000E-06 DAYS

RELEASE POINT 1.000000E-06 DAYS PER PASS
 MAXIMUM AVERAGE PCB% DENSITY 2.000000E-06 DAYS/CC "A" 100%

INITIAL DENSITY DATA WILL BE UNCORRECTED BY 1.000000E-06 PCB% PER PASS 1.000000E-06

DEPENDENCY POINT LEVEL HAS BEEN ESTABLISHED

FEED DENSITIES FOR ZONE PATH 1

TR-232	2.361920E-06	U-235	2.017150E-05	U-238	1.055100E-04	C	0.700000E-02
SE	1.361900E-06	O	5.103107E-06	RECYCL	0.000000E-00		

DISCHARGE DENSITIES FOR ZONE PATH 1 EXPOSURE TIME FOR EACH ZONE IN PATH 61.1111 DAYS

TR-232	2.950130E-06	PA-233	1.031113E-07	U-235	5.072020E-06	U-238	1.050000E-06
U-235	7.060920E-07	O-236	2.000460E-06	TR-239	0.020104E-11	TR-240	1.033000E-00
AB-243	5.261207E-09	U-238	1.165507E-06	TR-239	1.270002E-00	TR-240	0.000235E-00
PA-241	7.020500E-09	C	0.370500E-02	I-135	0.500000E-11	TR-135	0.700000E-11
PA-147	1.136027E-07	PA-148	1.701020E-10	PA-149	0.700372E-10	PA-149	1.000000E-10
SB-109	5.273033E-10	SB-143	7.101000E-07	PP1	0.510070E-04	PP2	3.000000E-04
SE	1.361900E-06	KB-82	1.102500E-07	KB-83	1.173070E-07	TR-103	2.700000E-07
BB-105	0.107730E-12	BB-109	7.003370E-05	BB-133	0.001303E-07	TR-133	1.000000E-07
CS-133	1.002290E-06	CS-136	1.026000E-07	CS-135	1.010307E-07	TR-135	0.700000E-07
BB-153	0.350051E-00	BB-150	2.013000E-04	TR-150	2.003750E-00	TR-150	1.000000E-00
SB-150	3.000000E-07	SB-151	7.210027E-00	SB-152	1.200030E-07	C	0.700000E-00
RECYCL	0.000000E-00	BP-237	3.020070E-07				

FEED DENSITIES FOR ZONE PATH 2

TR-232	2.361920E-06	U-235	2.017150E-05	U-238	1.055100E-04	C	0.700000E-02
SE	1.361900E-06	O	5.103107E-06	RECYCL	0.000000E-00		

DISCHARGE DENSITIES FOR ZONE PATH 2 EXPOSURE TIME FOR EACH ZONE IN PATH 61.1111 DAYS

TR-232	2.152000E-06	PA-233	1.012173E-07	U-235	5.060700E-06	U-238	1.031000E-06
U-235	0.200300E-07	O-236	2.000300E-06	TR-239	0.200000E-11	TR-240	1.000000E-00
AB-243	5.255000E-09	U-238	1.160000E-06	TR-239	1.303000E-00	TR-240	0.000235E-00
PA-241	7.100000E-09	C	0.370000E-02	I-135	0.003000E-11	TR-135	0.700000E-11
PA-147	1.100000E-07	PA-148	1.700000E-10	PA-149	0.700000E-10	PA-149	1.000000E-10
SB-109	5.300000E-10	SB-143	7.100000E-07	PP1	0.000000E-04	PP2	3.000000E-04
SE	1.361900E-06	KB-82	1.100000E-07	KB-83	1.100000E-07	TR-103	2.700000E-07
BB-105	0.100000E-12	BB-109	7.000000E-05	BB-133	0.000000E-07	TR-133	1.000000E-07
CS-133	1.000000E-06	CS-136	1.000000E-07	CS-135	1.000000E-07	TR-135	0.700000E-07
BB-153	0.350000E-00	BB-150	2.000000E-04	TR-150	2.000000E-00	TR-150	1.000000E-00
SB-150	3.000000E-07	SB-151	7.200000E-00	SB-152	1.200000E-07	C	0.700000E-00
RECYCL	0.000000E-00	BP-237	3.000000E-07				

FEED DENSITIES FOR ZONE PATH 3

TR-232	2.361920E-06	U-235	2.017150E-05	U-238	1.055100E-04	C	0.700000E-02
SE	1.361900E-06	O	5.103107E-06	RECYCL	0.000000E-00		

DISCHARGE DENSITIES FOR ZONE PATH 3 EXPOSURE TIME FOR EACH ZONE IN PATH 61.1111 DAYS

TR-232	2.150000E-06	PA-233	0.001200E-00	U-235	5.000000E-06	U-238	1.000000E-06
U-235	0.200000E-07	O-236	2.000000E-06	TR-239	0.200000E-11	TR-240	1.000000E-00
AB-243	5.100000E-09	U-238	1.100000E-06	TR-239	1.300000E-00	TR-240	0.000235E-00
PA-241	7.000000E-09	C	0.300000E-02	I-135	0.000000E-11	TR-135	0.000000E-11
PA-147	1.100000E-07	PA-148	1.600000E-10	PA-149	0.700000E-10	PA-149	1.000000E-10
SB-109	5.300000E-10	SB-143	7.000000E-07	PP1	0.000000E-04	PP2	3.000000E-04
SE	1.361900E-06	KB-82	1.100000E-07	KB-83	1.100000E-07	TR-103	2.700000E-07
BB-105	0.000000E-12	BB-109	7.000000E-05	BB-133	0.000000E-07	TR-133	1.000000E-07
CS-133	1.000000E-06	CS-136	1.000000E-07	CS-135	1.000000E-07	TR-135	0.700000E-07
BB-153	0.300000E-00	BB-150	2.000000E-04	TR-150	2.000000E-00	TR-150	1.000000E-00
SB-150	3.000000E-07	SB-151	7.000000E-00	SB-152	1.200000E-07	C	0.700000E-00
RECYCL	0.000000E-00	BP-237	3.000000E-07				

FEED DENSITIES FOR ZONE PATH 4

TR-232	2.361920E-06	U-235	2.017150E-05	U-238	1.055100E-04	C	0.700000E-02
SE	1.361900E-06	O	5.103107E-06	RECYCL	0.000000E-00		

Table 3. CONTINUED

DISCHARGE DENSITIES FOR ZONE PATH				61.1111 DAYS			
TR-232	2.162526E-06	PA-233	9.597865E-09	U-233	5.129058E-06	W-236	1.488877E-06
U-235	9.275054E-07	U-236	2.942588E-06	W-239	8.053862E-07	W-282	1.789668E-08
AR-243	8.072782E-09	U-238	1.185793E-06	W-239	1.553057E-09	W-280	1.038778E-08
W-241	7.485087E-09	C	0.379596E-02	I-135	6.150087E-11	W-134	8.778146E-11
W-167	1.155454E-07	PH-140	1.625551E-10	PH-140	8.767186E-10	W-188	1.988733E-10
SD-149	5.410263E-10	SD-143	1.247805E-07	FP1	8.167550E-08	PP2	1.881783E-08
BE	1.361999E-08	FR-92	1.091623E-07	FR-93	1.481775E-07	W-103	2.683687E-07
RR-105	1.952088E-12	AG-104	7.751228E-09	FR-131	4.843263E-07	W-131	1.374578E-07
CS-133	1.828999E-06	CS-138	1.788788E-07	CS-135	1.073008E-07	W-185	1.888418E-07
SD-153	9.089178E-08	W-158	2.781976E-08	FR-154	2.819388E-08	W-187	9.688388E-10
SD-150	3.739787E-07	SD-151	7.157483E-08	SP-152	1.268289E-07	C	4.188887E-08
BCVBL	9.999999E-10	SP-237	3.247615E-07				

FREE DENSITIES FOR ZONE PATH

TR-232	2.361620E-08	U-235	2.017198E-05	U-238	1.495188E-06	C	8.778586E-02
BE	1.361999E-08	O	4.185187E-08	BCVBL	9.999999E-10		

DISCHARGE DENSITIES FOR ZONE PATH

DISCHARGE DENSITIES FOR ZONE PATH				61.1111 DAYS			
TR-232	2.178525E-06	PA-233	9.039611E-09	U-233	5.169688E-06	W-236	1.871208E-06
U-235	1.821889E-06	U-236	2.761881E-06	W-239	8.588887E-11	W-282	1.789668E-08
AR-243	8.939289E-09	U-238	1.181036E-06	W-239	1.390832E-09	W-280	1.038778E-08
W-241	7.668777E-09	C	0.379596E-02	I-135	5.422270E-11	W-134	8.752929E-11
W-167	1.168758E-07	PH-140	1.645488E-10	PH-140	8.478726E-10	W-188	1.136788E-10
SD-149	5.408125E-10	SD-143	7.764188E-07	FP1	1.855912E-07	PP2	1.882132E-08
BE	1.361999E-08	FR-92	1.053781E-07	FR-93	1.455912E-07	W-103	2.759888E-07
RR-105	1.827287E-12	AG-104	1.036771E-09	FR-131	8.922868E-07	W-131	1.188888E-07
CS-133	1.789668E-06	CS-138	1.697688E-07	CS-135	1.985128E-07	W-185	1.888418E-07
SD-153	8.778128E-08	W-158	2.278538E-08	FR-154	2.738388E-08	W-187	9.787788E-10
SD-150	3.450688E-07	SD-151	7.046328E-08	SP-152	1.218188E-07	C	4.188887E-08
BCVBL	9.999999E-10	SP-237	1.248888E-07				

FREE DENSITIES FOR ZONE PATH

TR-232	2.361620E-08	U-235	2.017198E-05	U-238	1.495188E-06	C	8.778586E-02
BE	1.361999E-08	O	4.185187E-08	BCVBL	9.999999E-10		

DISCHARGE DENSITIES FOR ZONE PATH

DISCHARGE DENSITIES FOR ZONE PATH				61.1111 DAYS			
TR-232	2.181131E-06	PA-233	8.339268E-09	U-233	5.198593E-06	W-236	1.255107E-06
U-235	1.203327E-06	U-236	2.962887E-06	W-239	7.950516E-11	W-282	1.789668E-08
AR-243	3.988837E-09	U-238	1.285783E-06	W-239	1.435388E-09	W-280	1.112888E-08
W-241	7.982138E-09	C	0.379596E-02	I-135	5.588888E-11	W-134	8.588888E-11
W-167	1.989972E-07	PH-140	1.855858E-10	PH-140	8.613312E-10	W-188	1.657888E-10
SD-149	5.688178E-10	SD-143	7.852813E-07	FP1	7.623762E-08	PP2	1.788888E-08
BE	1.361999E-08	FR-92	1.083978E-07	FR-93	1.489588E-07	W-103	2.837768E-07
RR-105	3.682837E-12	AG-104	7.318228E-09	FR-131	8.055888E-07	W-131	1.288888E-07
CS-133	1.959688E-06	CS-138	1.451818E-07	CS-135	1.988888E-07	W-185	1.888418E-07
SD-153	8.888788E-08	W-158	2.892688E-08	FR-154	2.568888E-08	W-187	9.788888E-10
SD-150	3.581618E-07	SD-151	6.963288E-08	SP-152	1.178888E-07	C	4.188887E-08
BCVBL	9.999999E-10	SP-237	1.185788E-07				

FREE DENSITIES FOR ZONE PATH

TR-232	2.361620E-08	U-235	2.017198E-05	U-238	1.495188E-06	C	8.778586E-02
BE	1.361999E-08	O	4.185187E-08	BCVBL	9.999999E-10		

DISCHARGE DENSITIES FOR ZONE PATH

DISCHARGE DENSITIES FOR ZONE PATH				61.1111 DAYS			
TR-232	2.202619E-06	PA-233	7.322058E-09	U-233	5.071278E-06	W-236	1.178138E-06
U-235	1.878938E-06	U-236	2.958938E-06	W-239	8.058218E-11	W-282	1.838888E-08
AR-243	3.865752E-09	U-238	1.282178E-06	W-239	1.417258E-09	W-280	1.108888E-08
W-241	7.965671E-09	C	0.379596E-02	I-135	5.065358E-11	W-134	8.788888E-11
W-167	1.225168E-07	PH-140	1.385338E-10	PH-140	8.432688E-10	W-188	9.888888E-11
SD-149	5.697888E-10	SD-143	7.411888E-07	FP1	7.189788E-08	PP2	1.658888E-08
BE	1.361999E-08	FR-92	9.283888E-08	FR-93	1.328788E-07	W-103	2.898888E-07
RR-105	3.339888E-12	AG-104	7.073888E-09	FR-131	8.188788E-07	W-131	1.188888E-07
CS-133	1.303038E-06	CS-138	1.328888E-07	CS-135	1.968788E-07	W-185	1.788888E-07
SD-153	7.888888E-08	W-158	2.253888E-08	FR-154	2.328888E-08	W-187	9.272888E-10
SD-150	3.262188E-07	SD-151	6.684188E-08	SP-152	1.127188E-07	C	5.188887E-08
BCVBL	9.999999E-10	SP-237	2.887888E-07				

Table 3. CONTINUED

FEED DENSITIES FOR ZONE PATH

TR-232	2.36162E-04	7-235	2.41719E-05	8-239	1.44919E-06	C	9.77446E-02
RE	1.36199E-04	0	5.16379E-04	RECVL	9.44999E-13		

DISCHARGE DENSITIES FOR ZONE PATH

TR-232	2.22093E-04	TR-233	6.23573E-06	7-233	6.56067E-06	8-234	9.4977E-07
0-235	1.68130E-06	0-236	2.9039E-06	TR-239	3.35065E-11	TR-242	1.1719E-09
18-243	1.97917E-04	0-238	1.20409E-06	TR-274	1.33292E-09	TR-289	8.72610E-04
TR-281	6.16128E-04	C	6.37954E-02	1-134	6.24339E-11	TR-134	3.79138E-11
TR-147	1.26153E-07	TR-148	1.32796E-10	TR-149	6.68064E-10	TR-149	7.87279E-11
TR-149	5.12899E-19	TR-143	6.92025E-07	TR-1	6.776651E-04	TR-2	2.09011E-04
RE	1.36199E-04	TR-02	4.235791E-09	TR-03	1.209621E-07	TR-107	2.79162E-07
TR-105	2.70451E-12	TR-109	6.737913E-09	TR-131	6.670043E-07	TR-133	4.35249E-10
CS-133	1.26870E-06	CS-134	1.001103E-07	CS-135	1.020050E-07	TR-141	7.15670E-07
TR-153	7.226561E-04	TR-154	1.950029E-04	TR-154	1.452009E-04	TR-147	6.64517E-10
TR-150	3.62700E-17	TR-151	5.019732E-04	TR-152	1.151213E-07	C	5.168197E-04
RECVL	9.44999E-13	TR-237	2.100593E-07				

AVERAGE POWER 1.63773E 09 WATTS PER DAY
 AVERAGE AVERAGE POWER DENSITY 2.66406E 01 WATTS/CC PER DAY

FEED AND DISCHARGE RATES (KILOGRAMS PER DAY) BY ABSOLUTE NUCLEIDE

NO.	NAME	MOVING TOWNS		STATIONARY TOWNS	
		FEED	DISCHARGE	FEED	DISCHARGE
1	RE	1.66034E-01	1.96930E-01	0.0	0.0
2	C	2.71015E 02	2.71015E 02	6.61563E 02	6.61563E 02
3	TR-147	0.0	3.55092E-05	0.0	0.0
4	I-135	0.0	2.00055E-06	0.0	0.0
5	0	1.10030E 00	1.10030E 00	0.0	0.0
6	RECVL	0.0	0.0	0.0	0.0
7	COBALT	0.0	0.0	0.0	0.0
8	TR-135	0.0	1.60120E-06	0.0	0.0
9	CS-133	0.0	8.95097E-02	0.0	0.0
10	CS-134	0.0	4.00000E-03	0.0	0.0
11	CS-135	0.0	4.03820E-03	0.0	0.0
12	TR-147	0.0	8.60153E-07	0.0	0.0
13	TR-148	0.0	1.02070E-05	0.0	0.0
14	TR-149	0.0	4.01649E-06	0.0	0.0
15	TR-149	0.0	2.17610E-05	0.0	0.0
16	TR-151	0.0	2.70001E-04	0.0	0.0
17	TR-153	0.0	3.53259E-03	0.0	0.0
18	0-234	0.0	1.07930E-01	0.0	0.0
19	TR-242	0.0	1.05079E-03	0.0	0.0
20	TR-243	0.0	2.73000E-04	0.0	0.0
21	TR-2	0.0	1.05629E 00	0.0	0.0
22	TR-1	0.0	2.00452E-01	0.0	0.0
23	TR-232	1.87663E 01	1.36159E 01	0.0	0.0
24	0-233	0.0	3.19810E-01	0.0	0.0
25	0-234	0.0	8.89435E-02	0.0	0.0
26	0-235	1.27763E 00	6.4004E-02	0.0	0.0
27	TR-239	0.0	5.20176E-06	0.0	0.0
28	TR-149	0.0	4.43072E-06	0.0	0.0
29	TR-02	0.0	2.27957E-03	0.0	0.0
30	TR-03	0.0	3.17121E-03	0.0	0.0
31	TR-103	0.0	7.56026E-03	0.0	0.0
32	TR-105	0.0	1.00000E-07	0.0	0.0
33	TR-109	0.0	2.15164E-04	0.0	0.0
34	TR-131	0.0	1.72050E-02	0.0	0.0
35	TR-133	0.0	8.56700E-05	0.0	0.0
36	TR-143	0.0	2.70051E-02	0.0	0.0
37	TR-145	0.0	3.02660E-02	0.0	0.0
38	TR-150	0.0	1.03991E-02	0.0	0.0
39	TR-152	0.0	4.95727E-03	0.0	0.0
40	TR-154	0.0	1.00000E-02	0.0	0.0
41	TR-155	0.0	1.09563E-04	0.0	0.0
42	TR-233	0.0	5.07690E-13	0.0	0.0
43	0-230	9.61660E-02	7.70335E-02	0.0	0.0
44	TR-239	0.0	0.57297E-04	0.0	0.0
45	TR-240	0.0	6.63070E-04	0.0	0.0
46	TR-241	0.0	8.76906E-04	0.0	0.0
47	TR-237	0.0	1.97509E-02	0.0	0.0
	FISSILE	1.27763E 00	3.92110E-01	0.0	0.0

POWER (WATTS) FOR EACH ZONE PATH
 1) 2.87500E 09 2) 2.03913E 09 3) 2.03272E 09 4) 1.09640E 09 5) 1.01019E 09
 6) 2.20104E 09 7) 2.04276E 09 8) 1.04997E 09

TOTAL POWER (WATTS) FOR ZONE PATHS 1.63773E 09

ACTIVIDE FEED RATE (KILOGRAMS PER DAY) FOR EACH ZONE PATH
 1) 1.06320E 00 2) 1.00120E 00 3) 1.06026E 00 4) 1.07322E 00 5) 1.04633E 00
 6) 2.31207E 00 7) 2.27019E 00 8) 2.20033E 00

TOTAL ACTIVIDE FEED RATE (KILOGRAMS PER DAY) FOR ZONE PATHS 1.01305E 01

EXPOSURE (HOUR-DAYS PER KILOGRAM) FOR EACH ZONE PATH
 1) 1.19309E 02 2) 1.10315E 02 3) 1.00000E 02 4) 1.06500E 02 5) 1.03056E 02
 6) 9.46210E 01 7) 9.10725E 01 8) 6.66924E 01

TOTAL EXPOSURE (HOUR-DAYS PER KILOGRAM) FOR ZONE PATHS 1.01305E 02

Table 3. CONTINUED

INVENTORY AND REACTION RATES BY ABSOLUTE NUCLIDE

NO.	NAME	INVENTORY (KG)	ABSORPTION	FISSION	PRODUCTION	CAPTURE (%/s)
1	BE	1.61516E-02	7.80078E-05	0.0	0.0	6.75250E-05
2	C	8.05423E-05	8.37200E-02	0.0	0.0	4.29217E-02
3	BD-147	3.83654E-01	8.11806E-09	0.0	0.0	3.47727E-09
4	T-135	2.29279E-02	1.43790E-10	0.0	0.0	1.19120E-11
5	O	1.21412E-03	7.65610E-05	0.0	0.0	6.96230E-06
6	BDCVRL	0.0	7.40612E-08	0.0	0.0	7.40612E-08
7	COBARR	0.0	3.51439E-02	0.0	0.0	3.51439E-02
8	FE-135	3.45967E-03	2.26053E-02	0.0	0.0	2.26053E-02
9	CS-133	8.16705E-01	5.02562E-03	0.0	0.0	5.02562E-03
10	CS-134	5.12529E-06	8.88599E-06	0.0	0.0	8.88599E-06
11	CS-135	4.7120E-06	8.49270E-05	0.0	0.0	8.49270E-05
12	PD-147	6.00391E-06	5.44227E-03	0.0	0.0	5.44227E-03
13	PD-148M	8.65410E-02	2.36100E-03	0.0	0.0	2.36100E-03
14	PD-148	4.85460E-02	1.20200E-06	0.0	0.0	9.12020E-06
15	SR-149	4.82780E-02	7.25039E-03	0.0	0.0	7.25039E-03
16	SR-151	2.92209E-01	3.57007E-03	0.0	0.0	3.57007E-03
17	FE-153	2.73132E-06	1.49136E-03	0.0	0.0	1.49136E-03
18	U-232	1.78510E-02	4.29590E-03	4.80045E-05	1.07176E-08	8.25565E-03
19	PD-242	7.69275E-01	9.11269E-05	1.04625E-07	4.48202E-07	4.60167E-05
20	AR-243	1.71200E-01	1.00200E-05	4.33113E-08	1.43180E-07	2.99771E-05
21	PF2	8.57235E-02	3.21300E-03	0.0	0.0	3.21300E-03
22	PF1	1.49533E-02	1.30291E-03	0.0	0.0	1.30291E-03
23	FE-232	1.53591E-06	2.67409E-01	4.60509E-06	1.11490E-03	2.67053E-01
24	U-233	2.47195E-02	1.80492E-01	1.62567E-01	8.06417E-01	1.83005E-02
25	U-234	6.07750E-01	9.14537E-03	1.28430E-05	4.73592E-05	9.14537E-03
26	U-235	2.46721E-02	2.84675E-01	2.36970E-01	5.76787E-01	5.16892E-02
27	HF-239	6.27052E-02	1.26719E-05	7.44529E-08	2.14526E-07	1.25910E-05
28	PD-149	6.49250E-02	8.71600E-10	0.0	0.0	2.47707E-11
29	FE-02	1.76966E-06	2.95195E-06	0.0	0.0	2.95195E-06
30	FE-03	2.61900E-06	1.39300E-03	0.0	0.0	1.39300E-03
31	BE-103	7.97070E-06	5.93700E-03	0.0	0.0	5.93700E-03
32	BE-105	1.29500E-03	1.09600E-05	0.0	0.0	7.09600E-05
33	AC-109	1.85200E-01	4.70000E-04	0.0	0.0	9.70000E-05
34	FE-131	1.53260E-01	5.52400E-03	0.0	0.0	5.52400E-03
35	FE-132	4.71126E-01	2.56660E-06	0.0	0.0	2.56660E-06
36	BD-145	2.71401E-01	1.35010E-02	0.0	0.0	1.35010E-02
37	BD-145	2.62103E-01	1.80700E-03	0.0	0.0	3.80700E-03
38	SR-150	1.22439E-01	2.02100E-03	0.0	0.0	2.02100E-03
39	SR-152	4.20979E-06	2.63400E-03	0.0	0.0	2.63400E-03
40	SR-154	8.03000E-01	1.51607E-03	0.0	0.0	1.51607E-03
41	SR-155	0.45501E-02	1.57463E-03	0.0	0.0	1.57463E-03
42	PA-233	0.33290E-09	1.12151E-02	1.23923E-05	3.22095E-05	1.12027E-02
43	U-238	9.08676E-01	8.28462E-03	1.10305E-05	1.12416E-05	4.23307E-03
44	PD-240	1.16403E-06	0.00500E-03	2.47960E-03	7.17752E-02	1.50711E-03
45	PD-240	7.89425E-01	1.37307E-03	1.10307E-06	1.02630E-06	1.37333E-03
46	PD-241	5.35775E-01	1.24033E-03	4.23961E-08	2.70000E-03	3.25671E-06
47	HF-237	1.56900E-01	3.80605E-03	4.58000E-06	2.70500E-03	3.74691E-03
TOTALS		8.28771E-05	9.60700E-01	8.03500E-01	9.90000E-01	3.55091E-01
OTHER LOSS RATE			3.46125E-02			
TOTAL LOSS RATE			1.30000E-00			
SYSTEM LOSS RATE (W/SEC)			1.29250E-00			
RELATIVE FLOW LEVEL			1.00770E-00			

SUBMARY TABLES FOR REACTION RATES AT TIME 2.836720E-04 DAYS FOR CASE SAMPLE PROBLEMS, THE DIMENSIONAL TABLES AND DIFFERENTIAL EQUATIONS

AVERAGE REACTION LOSSES BY NUCLIDE CLASS AND ZONE CLASS - SYSTEM LOSS RATE 1.292500E-00 W/SEC

ZONE CLASS ID.	FISSION	FERTILE	C. REACTION	FISSION RATE	STRUCTURAL
1	0.0461107	0.2020234	0.3122281	0.1005723	0.0257078
5	0.0	0.0	0.0	0.0	0.0
2	0.0	0.0	0.0	0.0	0.0369000
3	0.0	0.0	0.0	0.0	0.0156536
4	0.0	0.0	0.0	0.0	0.0007661
SUB	0.0461107	0.2020234	0.3122281	0.1005723	0.0790511

ZONE CLASS ID.	ABSORPTION LOSS RATE	EFFECTIVE CONVERSION RATIO REACTION RATE	POWER (WATTS)
1	0.4070397	0.47000	1.637730E-09
5	0.0	0.0	0.0
2	0.0369000	0.0	0.0
3	0.0156536	0.0	0.0
4	0.0007661	0.0	0.0
OVERALL	0.4603810	0.47000	1.637730E-09
OTHER LOSSES	0.0396191		
TOTAL LOSSES	1.0000000		
EFFECTIVE CONVERSION RATIO FROM MASS BALANCE		0.50000	

Table 3. CONTINUED

RATES/CC SOURCE BY RESERVOIR													HEAT SOURCE			
RADIAL	0.0	0.0003	0.1006	0.2010	0.2730	0.3040	0.3390	0.3700	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000
AXIAL																
0.0	13.916	13.070	13.020	13.770	13.699	13.630	13.570	13.495	13.387	13.273	13.170	13.066	12.925			
0.0270	15.000	15.000	10.000	10.000	10.000	10.000	10.000	10.000	10.000	10.000	10.000	10.000	10.000			
0.0556	15.700	15.700	15.701	15.659	15.590	15.520	15.492	15.435	15.331	15.220	15.106	15.059	10.000			
0.0833	16.000	16.000	16.013	15.975	15.912	15.856	15.800	15.710	15.713	15.600	15.561	15.500	15.370			
0.1111	15.000	15.000	15.010	15.003	15.027	15.070	15.070	15.070	15.070	15.070	15.070	15.070	15.070			
0.1389	15.132	15.107	15.070	15.001	14.902	14.807	14.807	14.807	14.800	14.800	14.800	14.800	14.800			
0.1667	10.226	10.200	10.173	10.107	10.105	10.066	10.093	10.101	10.032	10.055	10.059	10.059	10.059			
0.1944	12.900	12.902	12.936	12.913	12.800	12.807	12.800	12.800	12.800	12.800	12.800	12.800	12.800			
0.2222	11.097	11.002	11.000	11.013	11.013	11.013	11.013	11.013	11.013	11.013	11.013	11.013	11.013			
0.2500	10.667	10.655	10.630	10.622	10.599	10.575	10.607	10.626	10.503	10.535	10.556	10.562	10.562			
0.2770	9.665	9.650	9.639	9.627	9.607	9.587	9.617	9.630	9.590	9.556	9.577	9.601	9.502			
0.3056	8.675	8.671	8.600	8.590	8.577	8.561	8.507	8.602	8.572	8.537	8.556	8.570	8.527			
0.3333	7.775	7.700	7.757	7.709	7.730	7.721	7.703	7.757	7.730	7.700	7.716	7.736	7.691			
0.3611	6.900	6.930	6.925	6.910	6.906	6.890	6.913	6.925	6.902	6.875	6.890	6.906	6.866			
0.3889	6.202	6.237	6.229	6.223	6.212	6.202	6.210	6.220	6.200	6.180	6.196	6.210	6.175			
0.4167	5.500	5.575	5.568	5.563	5.550	5.505	5.550	5.560	5.500	5.520	5.537	5.500	5.517			
0.4444	5.010	5.010	5.000	5.000	5.000	5.000	5.000	5.000	5.000	5.000	5.000	5.000	5.000			
0.4722	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000			
0.5000	4.030	4.031	4.026	4.022	4.015	4.000	4.030	4.020	4.000	4.000	4.000	4.000	4.000			
0.5270	3.617	3.610	3.600	3.600	3.599	3.593	3.600	3.602	3.590	3.575	3.579	3.583	3.562			
0.5556	3.251	3.200	3.200	3.200	3.200	3.200	3.200	3.200	3.200	3.200	3.200	3.200	3.200			
0.5833	2.910	2.910	2.912	2.903	2.903	2.899	2.902	2.903	2.893	2.891	2.892	2.893	2.866			
0.6111	2.620	2.622	2.616	2.610	2.610	2.605	2.609	2.609	2.600	2.598	2.599	2.599	2.570			
0.6389	2.350	2.356	2.353	2.350	2.305	2.300	2.303	2.303	2.300	2.290	2.290	2.290	2.269			
0.6667	2.122	2.120	2.117	2.110	2.109	2.105	2.107	2.107	2.090	2.080	2.080	2.080	2.070			
0.6944	1.900	1.907	1.903	1.901	1.896	1.892	1.890	1.893	1.893	1.895	1.897	1.896	1.862			
0.7222	1.710	1.716	1.713	1.711	1.707	1.703	1.700	1.703	1.696	1.697	1.696	1.695	1.673			
0.7500	1.500	1.500	1.502	1.500	1.500	1.500	1.500	1.500	1.500	1.500	1.500	1.500	1.500			
0.7770	1.392	1.391	1.390	1.390	1.390	1.390	1.390	1.390	1.390	1.390	1.390	1.390	1.390			
0.8056	1.253	1.251	1.200	1.207	1.203	1.200	1.200	1.200	1.200	1.200	1.200	1.200	1.200			
0.8333	1.120	1.127	1.120	1.122	1.119	1.116	1.116	1.116	1.100	1.100	1.100	1.100	1.090			
0.8611	1.010	1.010	1.012	1.010	1.007	1.000	1.003	1.002	1.000	1.000	1.000	1.000	1.000			
0.8889	0.910	0.910	0.912	0.910	0.907	0.900	0.900	0.900	0.900	0.900	0.900	0.900	0.900			
0.9167	0.820	0.820	0.820	0.820	0.820	0.820	0.820	0.820	0.820	0.820	0.820	0.820	0.820			
0.9444	0.762	0.760	0.760	0.760	0.757	0.750	0.751	0.750	0.750	0.750	0.750	0.750	0.750			
0.9722	0.727	0.725	0.723	0.722	0.719	0.716	0.716	0.716	0.716	0.716	0.716	0.716	0.716			
1.0000	0.720	0.710	0.717	0.715	0.712	0.710	0.709	0.709	0.709	0.709	0.709	0.709	0.709			

RATES/CC SOURCE BY RESERVOIR													HEAT SOURCE			
RADIAL	0.5600	0.5000	0.6105	0.6000	0.6795	0.7000	0.7325	0.7500	0.7000	0.7000	0.7000	0.7000	0.7000	0.7000	0.7000	0.7000
AXIAL																
0.0	12.700	12.605	12.506	12.301	12.120	11.922	11.701	11.405	11.212	10.976	10.751	10.552	10.405			
0.0270	13.000	13.000	13.030	13.015	13.010	13.000	13.000	13.000	13.000	13.000	13.000	13.000	13.000			
0.0556	10.700	10.607	10.510	10.200	10.107	10.001	10.000	10.000	10.000	10.000	10.000	10.000	10.000			
0.0833	15.230	15.153	15.021	10.799	10.600	10.403	10.170	10.000	10.000	10.000	10.000	10.000	10.000			
0.1111	15.150	15.100	15.000	10.779	10.653	10.512	10.211	10.020	10.000	10.000	10.000	10.000	10.000			
0.1389	10.551	10.529	10.461	10.200	10.155	10.002	10.000	10.000	10.000	10.000	10.000	10.000	10.000			
0.1667	13.752	13.700	13.700	13.500	13.430	13.307	13.001	12.979	12.903	12.870	12.830	12.810	12.810			
0.1944	12.610	12.633	12.600	12.025	12.305	12.327	12.002	12.000	11.903	11.800	11.707	11.600	10.700			
0.2222	11.005	11.026	11.000	11.000	11.010	11.010	11.010	11.010	11.010	11.010	11.010	11.010	11.010			
0.2500	10.039	10.000	10.000	10.010	10.000	10.000	10.000	10.000	10.000	10.000	10.000	10.000	10.000			
0.2770	9.070	9.003	9.000	9.000	9.000	9.000	9.000	9.000	9.000	9.000	9.000	9.000	9.000			
0.3056	8.070	8.005	8.001	8.000	8.000	8.000	8.000	8.000	8.000	8.000	8.000	8.000	8.000			
0.3333	7.000	7.000	7.000	7.000	7.000	7.000	7.000	7.000	7.000	7.000	7.000	7.000	7.000			
0.3611	6.000	6.000	6.000	6.000	6.000	6.000	6.000	6.000	6.000	6.000	6.000	6.000	6.000			
0.3889	6.130	6.152	6.107	6.000	6.000	6.000	6.000	6.000	6.000	6.000	6.000	6.000	6.000			
0.4167	5.000	5.000	5.000	5.000	5.000	5.000	5.000	5.000	5.000	5.000	5.000	5.000	5.000			
0.4444	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000			
0.4722	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000	4.000			
0.5000	3.000	3.000	3.000	3.000	3.000	3.000	3.000	3.000	3.000	3.000	3.000	3.000	3.000			
0.5270	2.500	2.500	2.500	2.500	2.500	2.500	2.500	2.500	2.500	2.500	2.500	2.500	2.500			
0.5556	3.170	3.170	3.170	3.170	3.170	3.170	3.170	3.170	3.170	3.170	3.170	3.170	3.170			
0.5833	2.000	2.000	2.000	2.000	2.000	2.000	2.000	2.000	2.000	2.000	2.000	2.000	2.000			
0.6111	2.550	2.550	2.500	2.500	2.500	2.500	2.500	2.500	2.500	2.500	2.500	2.500	2.500			
0.6389	2.200	2.200	2.200	2.200	2.200	2.200	2.200	2.200	2.200	2.200	2.200	2.200	2.200			
0.6667	2.050	2.050	2.050	2.050	2.050	2.050	2.050	2.050	2.050	2.050	2.050	2.050	2.050			
0.6944	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000			
0.7222	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000			
0.7500	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000			
0.7770	1.330	1.330	1.330	1.330	1.330	1.330	1.330	1.330	1.330	1.330	1.330	1.330	1.330			
0.8056	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000			
0.8333	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000			
0.8611	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700			
0.8889	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700			
0.9167	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700			
0.9444	0.720	0.710	0.710	0.700	0.690	0.680	0.670	0.660</								

Table 3. CONTINUED

0.3333	6.357	6.120	6.276	6.407
0.3611	5.664	6.000	6.571	5.842
0.3889	5.092	6.071	6.893	5.079
0.4167	4.522	6.324	6.821	4.593
0.4444	4.066	6.065	7.489	4.919
0.4722	3.601	6.835	6.504	3.567
0.5000	3.219	6.067	6.120	3.182
0.5278	2.967	6.720	6.791	2.827
0.5556	2.562	6.076	6.892	2.542
0.5833	2.208	6.170	6.209	2.265
0.6111	2.041	6.424	6.712	2.003
0.6389	1.921	6.729	6.758	1.785
0.6667	1.429	6.544	6.570	1.594
0.6944	1.050	6.378	6.801	1.322
0.7222	1.307	6.232	6.251	1.278
0.7500	1.162	6.100	6.117	1.133
0.7778	1.039	6.093	6.097	1.012
0.8056	0.920	6.077	6.089	0.902
0.8333	0.824	6.782	6.793	0.804
0.8611	0.738	6.697	6.706	0.715
0.8889	0.658	6.620	6.627	0.635
0.9167	0.580	6.553	6.557	0.563
0.9444	0.531	6.507	6.509	0.502
0.9722	0.485	6.459	6.456	0.456
1.0000	0.446	6.417	6.435	0.435

GUESS DEL T (°F) 6.271D-01 AT DENSITY 1.9851D 00 VOLUME 2.978D 00, MASS FLOW (KG/SEC) 6.377D 02 POWER 1.676D 09

MAXIMUM LOCALIZED BULK FLUID AND SURFACE TEMPERATURES (K) 1204.02 1209.34 APPARENT PRESSURE DROP (ATM) 0.6719

INITIALIZATION OF PROBLEM COMPLETE, START ITERATION CONVERGENCE DATA FOLLOWS

PROCESSOR TIME (SEC) AT START OF ITERATION 0.01 --COEFFICIENTS 1.3322 0.7090 1.0090 1.4532 MAX IT 170

ITERATION	MAXIMUM CHANGE (PSI)	BULK TEMP.	SURF TEMP.	PRESSURE	BETA (N)	PRESSURE DROP	DEL T BULK BALANCE	TR0 (S)				
1	-0.002901	0.000813	-0.004742	-0.001178	1.151E	0.6731	-0.000473	0.0004	0.021	0.1047	0.0438	0.3135
2	0.001677	0.006403	-0.004478	0.000560	1.151E	0.6718	0.000017	0.5083	0.9683	1.0288	0.8009	0.3084
3	0.001354	0.000890	0.001677	0.000262	1.3032	0.6722	-0.000077	0.9172	0.9829	2.1239	0.5412	1.1038
4	0.001263	0.000808	0.000985	0.000103	1.3932	0.6723	-0.000173	0.9336	0.9948	0.9765	0.6638	1.1038
5	0.001038	0.001976	0.001952	0.000068	1.3032	0.6720	-0.000186	0.8225	0.9932	2.2080	0.7616	1.1582
6	0.000911	0.001668	0.001646	-0.000029	1.3032	0.6724	-0.000200	0.8781	0.9877	1.0096	0.9280	1.1825
7	0.000821	0.001522	0.001501	-0.000025	1.3932	0.6727	-0.000199	0.9023	0.9572	0.9556	0.8923	0.9672
8	0.000756	0.001367	-0.000135	-0.000022	1.3032	0.6728	-0.000199	0.9212	0.9679	0.9557	0.9492	0.9591
9	0.000703	0.001231	0.001219	-0.000020	1.3032	0.6725	-0.000202	0.9292	0.9683	0.9652	0.9467	0.9683
10	0.000642	0.001112	0.001101	-0.000018	1.3032	0.6730	-0.000213	0.9185	0.9689	0.9712	0.9555	0.9680
11	0.000609	0.001009	0.001000	-0.000017	1.3032	0.6731	-0.000238	0.9493	0.9700	0.9773	0.9583	0.9719
12	0.000577	0.000914	0.000911	-0.000016	1.3032	0.6732	-0.000264	0.9464	0.9709	0.9815	0.9611	0.9789
13	0.000542	0.000839	0.000832	-0.000015	1.3032	0.6733	-0.000305	0.9404	0.9719	0.9858	0.9633	0.9778
14	0.000522	0.000769	0.000762	-0.000014	1.3032	0.6734	-0.000354	0.9454	0.9726	0.9898	0.9652	0.9796
15	0.000506	0.000706	0.000700	-0.000013	1.3932	0.6735	-0.000389	0.9606	0.9734	0.9907	0.9669	0.9811
16	0.000488	0.000646	0.000641	-0.000012	1.3032	0.6735	-0.000404	0.9654	0.9743	0.9906	0.9679	0.9821
17	0.000473	0.000587	0.000582	-0.000012	1.3032	0.6736	-0.000482	0.9697	0.9789	0.9906	0.9686	0.9826
18	0.000460	0.000543	0.000540	-0.000011	1.3032	0.6737	-0.000488	0.9723	0.9766	0.9910	0.9692	0.9830
19	0.000452	0.000507	0.000506	-0.000011	1.3032	0.6737	-0.000480	0.9821	0.9781	0.9907	0.9707	0.9833
20	0.000439	0.000477	0.000476	-0.000011	1.3032	0.6738	-0.000511	0.9733	0.9777	0.9910	0.9695	0.9836
21	0.000430	0.000452	0.000451	-0.000011	1.3032	0.6738	-0.000500	0.9785	0.9772	0.9913	0.9708	0.9838
22	0.000422	0.000437	0.000435	-0.000010	1.3032	0.6739	-0.000506	0.9822	0.9777	0.9916	0.9735	0.9839
23	0.000416	0.000423	0.000421	-0.000010	1.3932	0.6740	-0.000511	0.9811	0.9781	0.9916	0.9735	0.9840
24	0.000404	0.000404	0.000404	-0.000010	1.3032	0.6741	-0.000526	0.9904	0.9789	0.9916	0.9738	0.9839
25	0.000400	0.000400	0.000400	-0.000010	1.3032	0.6741	-0.000562	0.9853	0.9789	0.9915	0.9738	0.9839
26	0.000394	0.000400	0.000400	-0.000010	1.3032	0.6742	-0.000572	0.9951	0.9789	0.9919	0.9738	0.9837
27	0.000389	0.000404	0.000404	-0.000010	1.3032	0.6742	-0.000585	0.9876	0.9797	0.9919	0.9738	0.9838
28	0.000384	0.000404	0.000404	-0.000010	1.3032	0.6742	-0.000582	0.9980	0.9809	0.9919	0.9735	0.9831
29	0.000380	0.000404	0.000404	-0.000010	1.3032	0.6743	-0.000603	0.9896	0.9803	0.9915	0.9736	0.9827

EXTRAPOLATION OF SELECTED ITERATION DATA WITH HIGH VALUE OF 0.9248 FACI (BS) 0.81 53.2° 36.7° LEVEL 0

30	0.000375	0.000404	0.000404	-0.000010	1.3532	0.6750	-0.022090	1.570	0.999	2.6635	0.6138	1.0097
31	0.000370	0.000404	0.000404	-0.000010	1.3532	0.6755	-0.023956	0.6288	1.0513	0.9510	0.9527	1.1195
32	0.000365	0.000404	0.000404	-0.000010	1.3532	0.6758	-0.025510	0.5734	0.9902	0.9309	0.9216	0.9804
33	0.000360	0.000404	0.000404	-0.000010	1.3532	0.6758	-0.027015	0.6695	0.9719	0.9288	0.9183	0.9573
34	0.000357	0.000404	0.000404	-0.000010	1.3532	0.6753	-0.028287	0.8526	0.9768	0.9321	0.9189	0.9531
35	0.000357	0.000404	0.000404	-0.000010	1.3532	0.6752	-0.029282	0.9085	0.9788	0.9357	0.9198	0.9545
36	0.000351	0.000404	0.000404	-0.000010	1.3532	0.6751	-0.030281	0.9094	0.9794	0.9363	0.9199	0.9554
37	0.000345	0.000404	0.000404	-0.000010	1.3532	0.6751	-0.031286	0.9388	0.9788	0.9391	0.9173	0.9561
38	0.000340	0.000404	0.000404	-0.000010	1.3532	0.6751	-0.032288	0.9393	0.9770	0.9450	0.9164	0.9577
39	0.000335	0.000404	0.000404	-0.000010	1.3532	0.6750	-0.033289	0.9329	0.9789	0.9475	0.9168	0.9580
40	0.000330	0.000404	0.000404	-0.000010	1.3532	0.6750	-0.034285	0.9579	0.9682	0.9417	0.9191	0.9598
41	0.000325	0.000404	0.000404	-0.000010	1.3532	0.6750	-0.035287	0.9877	0.9663	0.9545	0.9195	0.9602
42	0.000320	0.000404	0.000404	-0.000010	1.3532	0.6750	-0.036287	0.9766	0.9639	0.9522	0.9217	0.9592
43	0.000315	0.000404	0.000404	-0.000010	1.3532	0.6750	-0.037287	0.9411	0.9614	0.9503	0.9260	0.9649
44	0.000310	0.000404	0.000404	-0.000010	1.3532	0.6751	-0.038283	0.9778	0.9583	0.9433	0.9289	0.9536
45	0.000307	0.000404	0.000404	-0.000010	1.3532	0.6751	-0.039286	0.9891	0.9583	0.9399	0.9325	0.9608
46	0.000304	0.000404	0.000404	-0.000010	1.3532	0.6751	-0.040287	0.9876	0.9583	0.9294	0.9351	0.9685
47	0.000301	0.000404	0.000404	-0.000010	1.3532	0.6752	-0.041288	0.9907	0.9583	0.9287	0.9375	0.9612
48	0.000298	0.000404	0.000404	-0.000010	1.3532	0.6752	-0.042288	0.9981	0.9583	0.9213	0.9397	0.9587
49	0.000295	0.000404	0.000404	-0.000010	1.3532	0.6753	-0.043289	0.9978	0.9583	0.9202	0.9423	0.9374
50	0.000292	0.000404	0.000404	-0.000010	1.3532	0.6753	-0.044289	1.0004	0.9583	0.9203	0.9428	0.9370
51	0.000289	0.000404	0.000404	-0.000010	1.3532	0.6753	-0.045289	0.9994	0.9583	0.9205	0.9426	0.9376
52	0.000286	0.000404	0.000404	-0.000010	1.4032	0.6754	-0.046289	1.0000	0.9583	0.9205	0.9425	0.9374
53	0.000283	0.000404	0.000404	-0.000010	1.4032	0.6754	-0.047289	1.0000	0.9583	0.9205	0.9425	0.9374
54	0.000280	0.000404	0.000404	-0.000010	1.4032	0.6755	-0.048289	1.0000	0.9583	0.9205	0.9425	0.9374
55	0.000277	0.000404	0.000404	-0.000010	1.4032	0.6755	-0.049289	1.0000	0.9583	0.9205	0.9425	0.9374
56	0.000274	0.000404	0.000404	-0.000010	1.4032	0.6755	-0.050289	1.0000	0.9583	0.9205	0.9425	0.9374
57	0.000271	0.000404	0.000404	-0.000010	1.4032	0.6755	-0.051289	1.0000	0.9583	0.9205	0.9425	0.9374
58	0.000268	0.000404	0.000404	-0.000010	1.4032	0.6755	-0.052289	1.0000	0.9583	0.9205	0.9425	0.9374
59	0.000265	0.000404	0.000404	-0.000010	1.4032	0.6755	-0.053289	1.0000	0.9583	0.9205	0.9425	0.9374
60	0.000262	0.000404	0.000404	-0.000010	1.4032	0.6755	-0.054289	1.0000	0.9583	0.9205	0.9425	0.9374

Table 3. CONTINUED

61	0.000211	-0.000211	-0.000211	0.000211	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
62	0.000216	-0.000216	-0.000216	0.000216	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
63	0.000220	-0.000220	-0.000220	0.000220	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
64	0.000222	-0.000222	-0.000222	0.000222	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
65	0.000222	-0.000222	-0.000222	0.000222	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
66	0.000216	-0.000216	-0.000216	0.000216	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
67	0.000202	-0.000202	-0.000202	0.000202	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
68	0.000184	-0.000184	-0.000184	0.000184	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
69	0.000193	-0.000193	-0.000193	0.000193	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
70	0.000189	-0.000189	-0.000189	0.000189	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
71	0.000184	-0.000184	-0.000184	0.000184	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
72	0.000177	-0.000177	-0.000177	0.000177	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
73	0.000171	-0.000171	-0.000171	0.000171	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
74	0.000163	-0.000163	-0.000163	0.000163	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
75	0.000154	-0.000154	-0.000154	0.000154	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
76	0.000148	-0.000148	-0.000148	0.000148	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
77	0.000140	-0.000140	-0.000140	0.000140	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
78	0.000133	-0.000133	-0.000133	0.000133	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
79	0.000125	-0.000125	-0.000125	0.000125	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
80	0.000118	-0.000118	-0.000118	0.000118	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
81	0.000111	-0.000111	-0.000111	0.000111	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
82	0.000104	-0.000104	-0.000104	0.000104	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350
83	0.000097	-0.000097	-0.000097	0.000097	1.3333	0.6756	-0.011700	1.0239	0.4440	0.4163	0.4532	0.4350

EXTRAPOLATION OF SELECTED ITERATE DATA WITH EIGENVALU 0.91955 FACTORS 15.5" 12.6" 05.03 LEVEL 0
 84 -0.600024 -0.700015 -0.000238 0.000238 1.3333 0.6760 -0.011710 0.2661 0.2700 0.4537 1.4680 0.6271

PROCESSOR TIME (SEC) 000 P8 ITERATIONS 56.24 --COEFFICIENTS 1.3510 C.8796 1.0070 1.0171
 ESTIMATED FRACTIONAL ABSOLUTE ERROR 3.99455-08 RELATIVE CHANGE IN THE PRESSURE DROP 0.00004

— THE ABOVE DISPLAYS THE
 ITERATIVE PROCESS TO
 A STATE OF ACCEPTABLE
 CONVERGENCE —

SAMPLE PROBLEM, TWO DIMENSIONAL PEBBLE BED THERMAL HYDRAULICS

THERMAL HYDRAULIC DATA ARRAYS SAVED FOR RECOVERY OR UNIT 31 ← SPECIAL ACTION

TEMPERATURES ARBITRARILY ADJUSTED TO ELIMINATE THE HEAT BALANCE ERROR

BED RADII AND HEIGHT (M)	0.1500	5.5000
THERMAL POWER (MW)	1656.01	
COOLANT MASS FLOW RATE (KG/S)	637.787	
INLET AVERAGE VELOCITY NUMBER	21296.	
INLET COOLANT TEMPERATURE (K)	623.0	
BEAR OUTLET COOLANT TEMPERATURE (K)	1123.0	
PEBBLE OUTLET COOLANT TEMPERATURE (K)	1187.0	AT RADIAL LOCATION (M) 0.0
MAX AND MIN PEBBLE SURFACE TEMPERATURES (K)	1191.5	692.9
INLET PRESSURE (ATM)	40.000	
OUTLET PRESSURE (ATM)	39.328	
PRESSURE DROP (ATM)	0.67600	
ERRORS IN FLOW AND HEAT BALANCE (PERCENT)	-0.060	-1.171
APPROXIMATE AXIAL PRESSURE CHANGE CROSS CORE AT M/3 AND 2R/3 (ATM), --NO GRAVITY	-0.67256	-0.67367

MAXIMUM RADIAL COMPONENT OF THE RELATIVE MASS FLOW RATE (ABSOLUTE) 0.00500

APPARENT EXTREME PRESSURE DROP (ATM) 0.67600

RADIAL	RELATIVE MASS FLOW RATE, G											
	0.0	0.0803	0.1606	0.2410	0.3213	0.4016	0.4819	0.5622	0.6425	0.7228	0.8031	0.8834
0.0	0.9788	0.9792	0.9796	0.9800	0.9812	0.9819	0.9825	0.9830	0.9834	0.9838	0.9842	0.9846
0.0278	0.9785	0.9789	0.9793	0.9804	0.9809	0.9816	0.9823	0.9831	0.9841	0.9851	0.9861	0.9871
0.0556	0.9783	0.9788	0.9793	0.9802	0.9808	0.9818	0.9820	0.9828	0.9839	0.9850	0.9862	0.9873
0.0833	0.9780	0.9785	0.9790	0.9799	0.9805	0.9811	0.9817	0.9824	0.9835	0.9846	0.9857	0.9868
0.1111	0.9776	0.9781	0.9787	0.9795	0.9801	0.9807	0.9812	0.9819	0.9830	0.9841	0.9851	0.9861
0.1389	0.9772	0.9777	0.9783	0.9791	0.9797	0.9803	0.9808	0.9814	0.9826	0.9836	0.9845	0.9854
0.1667	0.9768	0.9773	0.9779	0.9787	0.9793	0.9799	0.9803	0.9809	0.9819	0.9830	0.9840	0.9849
0.1944	0.9764	0.9769	0.9775	0.9783	0.9788	0.9794	0.9798	0.9803	0.9813	0.9825	0.9832	0.9841
0.2222	0.9759	0.9765	0.9770	0.9778	0.9784	0.9790	0.9793	0.9799	0.9809	0.9819	0.9827	0.9835
0.2500	0.9755	0.9760	0.9766	0.9774	0.9780	0.9785	0.9788	0.9793	0.9803	0.9814	0.9822	0.9829
0.2778	0.9751	0.9756	0.9762	0.9770	0.9776	0.9781	0.9783	0.9788	0.9798	0.9809	0.9817	0.9824
0.3056	0.9747	0.9752	0.9758	0.9766	0.9771	0.9777	0.9779	0.9784	0.9794	0.9805	0.9812	0.9819
0.3333	0.9743	0.9748	0.9754	0.9762	0.9767	0.9773	0.9775	0.9780	0.9790	0.9800	0.9809	0.9816
0.3611	0.9739	0.9744	0.9750	0.9758	0.9764	0.9769	0.9771	0.9776	0.9786	0.9796	0.9804	0.9812
0.3889	0.9735	0.9741	0.9747	0.9754	0.9760	0.9765	0.9767	0.9772	0.9782	0.9792	0.9800	0.9807
0.4167	0.9732	0.9737	0.9743	0.9751	0.9756	0.9762	0.9764	0.9769	0.9779	0.9789	0.9797	0.9804
0.4444	0.9729	0.9734	0.9740	0.9748	0.9753	0.9758	0.9761	0.9765	0.9775	0.9785	0.9793	0.9800
0.4722	0.9726	0.9731	0.9737	0.9745	0.9750	0.9755	0.9758	0.9762	0.9772	0.9782	0.9790	0.9797
0.5000	0.9723	0.9728	0.9734	0.9742	0.9747	0.9752	0.9755	0.9759	0.9769	0.9779	0.9787	0.9794
0.5278	0.9720	0.9725	0.9731	0.9739	0.9744	0.9749	0.9752	0.9756	0.9766	0.9776	0.9784	0.9791
0.5556	0.9717	0.9722	0.9728	0.9736	0.9741	0.9746	0.9749	0.9753	0.9763	0.9773	0.9781	0.9788
0.5833	0.9715	0.9720	0.9726	0.9734	0.9739	0.9744	0.9747	0.9751	0.9761	0.9771	0.9779	0.9786
0.6111	0.9713	0.9718	0.9724	0.9732	0.9737	0.9742	0.9745	0.9749	0.9759	0.9769	0.9777	0.9784
0.6389	0.9711	0.9716	0.9722	0.9730	0.9735	0.9740	0.9743	0.9747	0.9757	0.9767	0.9775	0.9782
0.6667	0.9709	0.9714	0.9720	0.9728	0.9733	0.9738	0.9741	0.9745	0.9755	0.9765	0.9773	0.9780
0.6944	0.9707	0.9712	0.9718	0.9726	0.9731	0.9736	0.9739	0.9743	0.9753	0.9763	0.9771	0.9778
0.7222	0.9705	0.9710	0.9716	0.9724	0.9729	0.9734	0.9737	0.9741	0.9751	0.9761	0.9769	0.9776

Table 3. CONTINUED

0.7500	0.9704	0.9709	0.9715	0.9723	0.9729	0.9733	0.9737	0.9743	0.9752	0.9762	0.9772	0.9782	0.9796
0.7778	0.9702	0.9708	0.9714	0.9722	0.9727	0.9732	0.9736	0.9741	0.9751	0.9761	0.9771	0.9781	0.9795
0.8056	0.9701	0.9706	0.9713	0.9721	0.9726	0.9731	0.9735	0.9741	0.9750	0.9760	0.9770	0.9780	0.9794
0.8333	0.9700	0.9705	0.9712	0.9720	0.9725	0.9729	0.9734	0.9740	0.9750	0.9760	0.9770	0.9780	0.9793
0.8611	0.9699	0.9705	0.9711	0.9719	0.9724	0.9728	0.9733	0.9739	0.9749	0.9759	0.9769	0.9779	0.9792
0.8889	0.9699	0.9704	0.9710	0.9718	0.9723	0.9727	0.9732	0.9738	0.9748	0.9758	0.9768	0.9778	0.9791
0.9167	0.9698	0.9703	0.9710	0.9718	0.9723	0.9727	0.9732	0.9738	0.9748	0.9758	0.9768	0.9778	0.9791
0.9444	0.9698	0.9703	0.9710	0.9717	0.9722	0.9727	0.9731	0.9737	0.9746	0.9756	0.9767	0.9777	0.9790
0.9722	0.9697	0.9703	0.9710	0.9717	0.9722	0.9726	0.9731	0.9737	0.9746	0.9756	0.9767	0.9777	0.9790
1.0000	0.9697	0.9702	0.9709	0.9717	0.9722	0.9726	0.9731	0.9737	0.9746	0.9756	0.9767	0.9777	0.9790

RELATIVE MASS FLOW RATE, C

RADIAL	0.5600	0.6900	0.6105	0.6690	0.6795	0.7060	0.7225	0.7500	0.7800	0.8105	0.8402	0.8747	0.9012
AXIAL													
0.0	0.9904	0.9919	0.9937	0.9957	0.9979	1.0000	1.0023	1.0046	1.0070	1.0092	1.0130	1.0152	1.0170
0.0278	0.9902	0.9915	0.9936	0.9957	0.9979	1.0000	1.0023	1.0047	1.0071	1.0104	1.0131	1.0154	1.0172
0.0556	0.9900	0.9918	0.9932	0.9953	0.9975	0.9996	1.0020	1.0044	1.0073	1.0108	1.0134	1.0159	1.0181
0.0833	0.9895	0.9909	0.9926	0.9947	0.9969	0.9990	1.0015	1.0040	1.0071	1.0105	1.0130	1.0157	1.0183
0.1111	0.9889	0.9902	0.9919	0.9940	0.9962	0.9984	1.0010	1.0036	1.0068	1.0105	1.0132	1.0161	1.0185
0.1389	0.9887	0.9899	0.9912	0.9933	0.9955	0.9977	1.0005	1.0031	1.0065	1.0105	1.0146	1.0181	1.0216
0.1667	0.9886	0.9898	0.9905	0.9927	0.9948	0.9971	1.0000	1.0027	1.0063	1.0107	1.0149	1.0187	1.0226
0.1944	0.9885	0.9897	0.9905	0.9927	0.9948	0.9971	1.0000	1.0029	1.0061	1.0107	1.0153	1.0192	1.0235
0.2222	0.9884	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0030	1.0061	1.0108	1.0156	1.0197	1.0243
0.2500	0.9883	0.9894	0.9901	0.9924	0.9946	0.9969	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.2778	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.3056	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.3333	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.3611	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.3889	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.4167	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.4444	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.4722	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.5000	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.5278	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.5556	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.5833	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.6111	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.6389	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.6667	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.6944	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.7222	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.7500	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.7778	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.8056	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.8333	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.8611	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.8889	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.9167	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.9444	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
0.9722	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256
1.0000	0.9883	0.9895	0.9902	0.9925	0.9947	0.9970	1.0000	1.0031	1.0062	1.0109	1.0158	1.0207	1.0256

RELATIVE MASS FLOW RATE, C

RADIAL	0.6277	0.9518	0.9759	1.0000
AXIAL				
0.0	1.0179	1.0170	1.0144	1.0127
0.0278	1.0181	1.0173	1.0146	1.0130
0.0556	1.0193	1.0183	1.0149	1.0129
0.0833	1.0209	1.0197	1.0157	1.0132
0.1111	1.0225	1.0218	1.0169	1.0141
0.1389	1.0241	1.0231	1.0180	1.0150
0.1667	1.0255	1.0247	1.0200	1.0169
0.1944	1.0268	1.0263	1.0216	1.0185
0.2222	1.0279	1.0277	1.0232	1.0201
0.2500	1.0290	1.0289	1.0246	1.0217
0.2778	1.0299	1.0301	1.0260	1.0232
0.3056	1.0306	1.0311	1.0273	1.0246
0.3333	1.0313	1.0320	1.0285	1.0260
0.3611	1.0319	1.0329	1.0296	1.0272
0.3889	1.0325	1.0336	1.0306	1.0283
0.4167	1.0329	1.0342	1.0315	1.0294
0.4444	1.0334	1.0347	1.0323	1.0300
0.4722	1.0337	1.0352	1.0331	1.0313
0.5000	1.0340	1.0357	1.0338	1.0321
0.5278	1.0343	1.0360	1.0348	1.0329
0.5556	1.0345	1.0364	1.0349	1.0336
0.5833	1.0348	1.0370	1.0354	1.0342
0.6111	1.0349	1.0369	1.0359	1.0350
0.6389	1.0351	1.0371	1.0363	1.0353
0.6667	1.0352	1.0373	1.0366	1.0356
0.6944	1.0353	1.0375	1.0370	1.0362
0.7222	1.0354	1.0376	1.0373	1.0364
0.7500	1.0355	1.0377	1.0375	1.0369
0.7778	1.0355	1.0378	1.0378	1.0373
0.8056	1.0356	1.0379	1.0380	1.0376
0.8333	1.0356	1.0380	1.0382	1.0378
0.8611	1.0356	1.0380	1.0383	1.0381
0.8889	1.0356	1.0380	1.0385	1.0383
0.9167	1.0356	1.0381	1.0386	1.0385
0.9444	1.0356	1.0381	1.0387	1.0386
0.9722	1.0356	1.0381	1.0388	1.0388
1.0000	1.0356	1.0381	1.0389	1.0389

Table 3. CONTINUED

AXIAL COMPONENT OF RELATIVE MASS FLOW RATE, GZ													
RADIAL	0.0	0.0003	0.1606	0.2010	0.2739	0.3060	0.3399	0.3787	0.4096	0.4407	0.4795	0.5066	0.5337
AXIAL													
0.0	0.9788	0.9792	0.9798	0.9807	0.9812	0.9819	0.9825	0.9834	0.9844	0.9855	0.9867	0.9878	0.9891
0.0270	0.9785	0.9789	0.9795	0.9804	0.9809	0.9816	0.9823	0.9831	0.9841	0.9853	0.9865	0.9876	0.9889
0.0556	0.9783	0.9788	0.9793	0.9802	0.9808	0.9814	0.9820	0.9828	0.9835	0.9846	0.9857	0.9867	0.9880
0.0833	0.9780	0.9785	0.9790	0.9799	0.9805	0.9811	0.9817	0.9824	0.9835	0.9846	0.9857	0.9867	0.9880
0.1111	0.9776	0.9781	0.9787	0.9795	0.9801	0.9807	0.9812	0.9819	0.9830	0.9841	0.9851	0.9861	0.9874
0.1389	0.9772	0.9777	0.9783	0.9791	0.9797	0.9803	0.9808	0.9814	0.9824	0.9834	0.9845	0.9854	0.9867
0.1667	0.9768	0.9773	0.9779	0.9787	0.9793	0.9799	0.9803	0.9808	0.9814	0.9823	0.9832	0.9841	0.9854
0.1944	0.9764	0.9769	0.9775	0.9783	0.9788	0.9794	0.9799	0.9803	0.9813	0.9825	0.9832	0.9841	0.9854
0.2222	0.9759	0.9765	0.9770	0.9778	0.9784	0.9790	0.9793	0.9798	0.9808	0.9819	0.9827	0.9835	0.9848
0.2500	0.9755	0.9760	0.9766	0.9774	0.9780	0.9785	0.9788	0.9792	0.9802	0.9814	0.9821	0.9829	0.9842
0.2777	0.9751	0.9756	0.9762	0.9770	0.9776	0.9781	0.9783	0.9788	0.9798	0.9810	0.9817	0.9824	0.9837
0.3056	0.9747	0.9752	0.9758	0.9766	0.9771	0.9777	0.9779	0.9784	0.9794	0.9805	0.9812	0.9820	0.9833
0.3333	0.9743	0.9748	0.9754	0.9762	0.9767	0.9773	0.9775	0.9780	0.9790	0.9801	0.9808	0.9816	0.9829
0.3611	0.9739	0.9744	0.9750	0.9758	0.9763	0.9769	0.9771	0.9776	0.9786	0.9797	0.9804	0.9812	0.9825
0.3889	0.9735	0.9740	0.9746	0.9754	0.9759	0.9765	0.9767	0.9772	0.9782	0.9793	0.9800	0.9808	0.9821
0.4167	0.9732	0.9737	0.9743	0.9751	0.9756	0.9762	0.9764	0.9769	0.9779	0.9790	0.9797	0.9805	0.9818
0.4444	0.9728	0.9733	0.9739	0.9747	0.9752	0.9758	0.9760	0.9765	0.9775	0.9786	0.9793	0.9801	0.9814
0.4722	0.9726	0.9731	0.9737	0.9745	0.9750	0.9755	0.9757	0.9762	0.9772	0.9783	0.9790	0.9798	0.9811
0.5000	0.9723	0.9728	0.9734	0.9742	0.9747	0.9752	0.9754	0.9759	0.9769	0.9780	0.9787	0.9795	0.9808
0.5278	0.9720	0.9725	0.9731	0.9739	0.9744	0.9749	0.9751	0.9756	0.9766	0.9777	0.9784	0.9792	0.9805
0.5556	0.9717	0.9722	0.9728	0.9736	0.9741	0.9746	0.9748	0.9753	0.9763	0.9774	0.9781	0.9789	0.9802
0.5833	0.9715	0.9720	0.9726	0.9734	0.9739	0.9744	0.9746	0.9751	0.9761	0.9772	0.9779	0.9787	0.9800
0.6111	0.9713	0.9718	0.9724	0.9732	0.9737	0.9742	0.9744	0.9749	0.9759	0.9770	0.9777	0.9785	0.9798
0.6389	0.9711	0.9716	0.9722	0.9730	0.9735	0.9740	0.9742	0.9747	0.9757	0.9768	0.9775	0.9783	0.9796
0.6667	0.9709	0.9714	0.9720	0.9728	0.9733	0.9738	0.9740	0.9745	0.9755	0.9766	0.9773	0.9781	0.9794
0.6944	0.9707	0.9712	0.9718	0.9726	0.9731	0.9736	0.9738	0.9743	0.9753	0.9764	0.9771	0.9779	0.9792
0.7222	0.9705	0.9710	0.9716	0.9724	0.9729	0.9734	0.9736	0.9741	0.9751	0.9762	0.9769	0.9777	0.9790
0.7500	0.9704	0.9709	0.9715	0.9723	0.9728	0.9733	0.9735	0.9740	0.9750	0.9761	0.9768	0.9776	0.9789
0.7778	0.9702	0.9707	0.9713	0.9721	0.9726	0.9731	0.9733	0.9738	0.9748	0.9759	0.9766	0.9774	0.9787
0.8056	0.9701	0.9706	0.9712	0.9720	0.9725	0.9730	0.9732	0.9737	0.9747	0.9758	0.9765	0.9773	0.9786
0.8333	0.9700	0.9705	0.9711	0.9719	0.9724	0.9729	0.9731	0.9736	0.9746	0.9757	0.9764	0.9772	0.9785
0.8611	0.9699	0.9704	0.9710	0.9718	0.9723	0.9728	0.9730	0.9735	0.9745	0.9756	0.9763	0.9771	0.9784
0.8889	0.9698	0.9703	0.9709	0.9717	0.9722	0.9727	0.9729	0.9734	0.9744	0.9755	0.9762	0.9770	0.9783
0.9167	0.9697	0.9702	0.9708	0.9716	0.9721	0.9726	0.9728	0.9733	0.9743	0.9754	0.9761	0.9769	0.9782
0.9444	0.9696	0.9701	0.9707	0.9715	0.9720	0.9725	0.9727	0.9732	0.9742	0.9753	0.9760	0.9768	0.9781
0.9722	0.9695	0.9700	0.9706	0.9714	0.9719	0.9724	0.9726	0.9731	0.9741	0.9752	0.9759	0.9767	0.9780
1.0000	0.9694	0.9700	0.9706	0.9714	0.9719	0.9724	0.9726	0.9731	0.9741	0.9752	0.9759	0.9767	0.9780

AXIAL COMPONENT OF RELATIVE MASS FLOW RATE, GZ													
RADIAL	0.5608	0.4805	0.6105	0.6490	0.6795	0.7060	0.7325	0.7590	0.7880	0.8194	0.8482	0.8767	0.9012
AXIAL													
0.0	0.9904	0.9919	0.9927	0.9957	0.9970	1.0000	1.0023	1.0046	1.0078	1.0102	1.0130	1.0152	1.0170
0.0270	0.9903	0.9918	0.9926	0.9957	0.9970	1.0000	1.0023	1.0046	1.0078	1.0102	1.0131	1.0154	1.0172
0.0556	0.9900	0.9916	0.9924	0.9953	0.9965	0.9996	1.0020	1.0044	1.0073	1.0104	1.0134	1.0159	1.0181
0.0833	0.9895	0.9908	0.9922	0.9947	0.9969	0.9990	1.0015	1.0040	1.0071	1.0104	1.0134	1.0161	1.0183
0.1111	0.9890	0.9901	0.9915	0.9940	0.9962	0.9984	1.0010	1.0035	1.0066	1.0100	1.0130	1.0158	1.0180
0.1389	0.9882	0.9894	0.9911	0.9933	0.9955	0.9977	1.0004	1.0031	1.0065	1.0100	1.0130	1.0158	1.0180
0.1667	0.9875	0.9887	0.9904	0.9927	0.9949	0.9971	1.0000	1.0027	1.0062	1.0100	1.0130	1.0158	1.0180
0.1944	0.9869	0.9881	0.9898	0.9921	0.9943	0.9966	0.9995	1.0023	1.0060	1.0100	1.0130	1.0158	1.0180
0.2222	0.9864	0.9875	0.9892	0.9915	0.9937	0.9961	0.9991	1.0020	1.0058	1.0100	1.0130	1.0158	1.0180
0.2500	0.9858	0.9870	0.9887	0.9910	0.9933	0.9957	0.9987	1.0018	1.0057	1.0100	1.0130	1.0158	1.0180
0.2778	0.9853	0.9865	0.9882	0.9906	0.9929	0.9953	0.9985	1.0015	1.0056	1.0100	1.0130	1.0158	1.0180
0.3056	0.9849	0.9861	0.9878	0.9902	0.9925	0.9950	0.9982	1.0013	1.0056	1.0100	1.0130	1.0158	1.0180
0.3333	0.9844	0.9856	0.9874	0.9898	0.9922	0.9946	0.9980	1.0012	1.0055	1.0100	1.0130	1.0158	1.0180
0.3611	0.9841	0.9853	0.9871	0.9895	0.9920	0.9945	0.9978	1.0011	1.0055	1.0100	1.0130	1.0158	1.0180
0.3889	0.9837	0.9850	0.9868	0.9892	0.9917	0.9943	0.9976	1.0010	1.0055	1.0100	1.0130	1.0158	1.0180
0.4167	0.9833	0.9847	0.9865	0.9889	0.9915	0.9942	0.9975	1.0009	1.0055	1.0100	1.0130	1.0158	1.0180
0.4444	0.9831	0.9844	0.9863	0.9888	0.9913	0.9940	0.9973	1.0008	1.0055	1.0100	1.0130	1.0158	1.0180
0.4722	0.9828	0.9842	0.9861	0.9886	0.9912	0.9939	0.9973	1.0008	1.0056	1.0100	1.0130	1.0158	1.0180
0.5000	0.9826	0.9839	0.9859	0.9884	0.9910	0.9938	0.9972	1.0008	1.0056	1.0100	1.0130	1.0158	1.0180
0.5278	0.9823	0.9837	0.9857	0.9882	0.9909	0.9937	0.9971	1.0008	1.0056	1.0100	1.0130	1.0158	1.0180
0.5556	0.9821	0.9836	0.9855	0.9881	0.9908	0.9936	0.9971	1.0008	1.0057	1.0100	1.0130	1.0158	1.0180
0.5833	0.9819	0.9834	0.9854	0.9879	0.9907	0.9935	0.9970	1.0008	1.0058	1.0100	1.0130	1.0158	1.0180
0.6111	0.9818	0.9832	0.9853	0.9878	0.9906	0.9935	0.9970	1.0008	1.0059	1.0100	1.0130	1.0158	1.0180
0.6389	0.9816	0.9831	0.9851	0.9877	0.9905	0.9935	0.9970	1.0008	1.0059	1.0100	1.0130	1.0158	1.0180
0.6667	0.9814	0.9830	0.9850	0.9876	0.9905	0.9934	0.9970	1.0009	1.0060	1.0121	1.0145	1.0169	1.0192
0.6944	0.9813	0.9829	0.9850	0.9875	0.9904	0.9934	0.9969	1.0009	1.0060	1.0121	1.0146	1.0170	1.0194
0.7222	0.9812	0.9828	0.9848	0.9875	0.9904	0.9934	0.9969	1.0009	1.0061	1.0122	1.0147	1.0171	1.0195
0.7500	0.9811	0.9827	0.9848	0.9874	0.9903	0.9934	0.9969	1.0009	1.0062	1.0122	1.0148	1.0172	1.0196
0.7778	0.9810	0.9826	0.9847	0.9873	0.9903	0.9934	0.9969	1.0010	1.0062	1.0124	1.0149	1.0173	1.0197
0.8056	0.9809	0.9825	0.9847	0.9873	0.9903	0.9933	0.9969	1.0010	1.0063	1.0125	1.0150	1.0174	1.0198
0.8333	0.9808	0.9824	0.9846	0.9872	0.9903	0.9933	0.9970	1.0010	1.0064	1.0125	1.0151	1.0175	1.0200
0.8611	0.9807	0.9824	0.9846	0.9872	0.9902	0.9933	0.9970	1.0011	1.0064	1.0126	1.0152	1.0176	1.0201
0.8889	0.9807	0.9823	0.9845	0.9872	0.9902	0.9933	0.9970	1.0011	1.0065	1.0126	1.0152	1.0176	1.0201
0.9167	0.9806	0.9823	0.9845	0.9871	0.9902	0.9933	0.9970	1.0011	1.0065	1.0127	1.0153	1.0177	1.0202
0.9444	0.9806	0.9822	0.9844	0.9871	0.9902	0.9933	0.9970	1.0011	1.0066	1.0127	1.0153	1.0177	1.0202
0.9722	0.9805	0.9822	0.9844	0.9871	0.9901	0.9933	0.9970	1.0012	1.0066	1.0128	1.0154	1.0178	1.0203
1.0000	0.9805	0.9822	0.9844	0.9871	0.9902	0.9933</							

Table 3. CONTINUED

COOLANT BULK TEMPERATURE, °F (K)													
RADIAL	0.5680	0.4800	0.6105	0.6890	0.6795	0.7060	0.7325	0.7790	0.7899	0.8164	0.9492	0.9707	0.9012
AXIAL													
0.0	623.0	623.0	623.0	623.0	623.0	623.0	623.0	623.0	623.0	623.0	623.0	623.0	623.0
0.0270	657.0	656.6	656.1	655.5	655.0	654.4	653.7	652.9	652.0	651.1	649.9	648.6	647.3
0.0556	693.3	692.5	691.6	690.4	689.2	688.1	686.7	685.0	683.1	681.1	678.5	676.1	673.7
0.0833	731.0	729.9	728.6	726.8	725.1	723.0	721.1	718.3	715.0	711.0	706.6	701.3	695.3
0.1111	768.4	767.6	765.9	763.5	761.5	759.2	756.4	753.0	748.9	744.0	738.1	731.1	723.1
0.1389	805.9	804.8	802.8	799.5	797.0	794.0	790.4	786.0	780.7	774.6	767.6	760.6	752.7
0.1667	841.0	839.4	837.2	833.0	831.0	827.0	822.0	816.0	809.0	801.0	792.0	783.0	774.0
0.1944	873.7	872.0	869.6	865.0	862.7	858.8	854.7	848.0	840.0	831.0	821.0	811.0	801.0
0.2222	903.7	902.0	899.8	895.2	891.9	887.3	882.2	874.0	865.0	855.0	844.0	833.0	822.0
0.2500	931.1	929.2	926.5	922.1	918.5	913.9	908.2	900.0	890.0	879.0	867.0	855.0	843.0
0.2778	955.8	953.9	951.0	946.0	942.7	937.0	930.9	922.0	911.0	899.0	886.0	873.0	860.0
0.3056	978.1	976.1	973.1	967.3	962.4	955.2	947.9	938.0	925.0	912.0	898.0	884.0	870.0
0.3333	998.2	996.1	993.0	986.0	980.0	971.0	961.0	949.0	935.0	921.0	906.0	891.0	876.0
0.3611	1016.2	1014.0	1010.8	1003.9	1000.5	990.0	978.0	964.0	949.0	933.0	917.0	901.0	885.0
0.3889	1032.4	1030.1	1026.9	1021.7	1017.3	1006.1	1000.3	987.0	971.0	954.0	937.0	920.0	903.0
0.4167	1048.4	1046.5	1043.1	1035.9	1031.4	1020.6	1014.7	1000.0	983.0	965.0	947.0	929.0	911.0
0.4444	1064.9	1062.5	1058.0	1050.7	1046.0	1035.4	1029.5	1014.0	996.0	977.0	958.0	939.0	920.0
0.4722	1071.6	1069.1	1064.5	1056.2	1051.5	1040.7	1034.8	1018.0	999.0	979.0	959.0	939.0	919.0
0.5000	1082.1	1079.5	1074.8	1065.5	1060.7	1049.8	1043.9	1026.0	1006.0	985.0	964.0	943.0	922.0
0.5278	1091.5	1088.8	1084.1	1074.7	1070.0	1059.1	1053.2	1035.0	1014.0	992.0	970.0	948.0	926.0
0.5556	1100.0	1097.2	1092.5	1083.0	1078.2	1067.3	1061.4	1043.0	1021.0	998.0	975.0	952.0	929.0
0.5833	1107.6	1104.9	1100.2	1090.7	1085.9	1075.0	1069.1	1050.0	1028.0	1005.0	982.0	958.0	934.0
0.6111	1114.5	1111.5	1107.0	1097.5	1092.7	1081.8	1075.9	1056.0	1033.0	1010.0	986.0	962.0	937.0
0.6389	1120.6	1117.6	1113.1	1103.6	1098.8	1087.9	1082.0	1062.0	1039.0	1015.0	991.0	967.0	942.0
0.6667	1126.2	1123.1	1118.6	1109.1	1104.3	1093.4	1087.5	1067.0	1044.0	1020.0	996.0	971.0	946.0
0.6944	1131.1	1128.0	1123.5	1114.0	1109.2	1098.3	1092.4	1072.0	1048.0	1024.0	1000.0	975.0	950.0
0.7222	1135.6	1132.5	1128.0	1118.5	1113.7	1102.8	1096.9	1076.0	1052.0	1028.0	1003.0	978.0	953.0
0.7500	1139.7	1136.5	1132.0	1122.5	1117.7	1106.8	1100.9	1080.0	1055.0	1031.0	1006.0	981.0	956.0
0.7778	1143.3	1140.1	1135.6	1126.1	1121.3	1110.4	1104.5	1083.0	1058.0	1033.0	1008.0	983.0	958.0
0.8056	1146.6	1143.3	1138.8	1129.3	1124.5	1113.6	1107.7	1086.0	1061.0	1036.0	1011.0	986.0	961.0
0.8333	1149.6	1146.2	1141.7	1132.2	1127.4	1116.5	1110.6	1089.0	1064.0	1039.0	1014.0	989.0	964.0
0.8611	1152.3	1148.9	1144.4	1134.9	1130.1	1119.2	1113.3	1092.0	1067.0	1042.0	1017.0	992.0	967.0
0.8889	1154.7	1151.3	1146.8	1137.3	1132.5	1121.6	1115.7	1094.0	1069.0	1044.0	1019.0	994.0	969.0
0.9167	1156.4	1153.4	1148.9	1139.4	1134.6	1123.7	1117.8	1096.0	1071.0	1046.0	1021.0	996.0	971.0
0.9444	1159.9	1155.4	1150.9	1141.4	1136.6	1125.7	1119.8	1098.0	1073.0	1048.0	1023.0	998.0	973.0
0.9722	1160.0	1157.2	1152.6	1143.1	1138.3	1127.4	1121.5	1100.0	1075.0	1050.0	1025.0	1000.0	975.0
1.0000	1162.4	1159.8	1155.1	1145.6	1140.8	1129.9	1124.0	1102.0	1077.0	1052.0	1027.0	1002.0	977.0

COOLANT BULK TEMPERATURE, °F (K)				
RADIAL	0.9277	0.9510	0.9759	1.0000
AXIAL				
0.0	623.0	623.0	623.0	623.0
0.0270	649.5	649.9	651.5	652.6
0.0556	677.3	678.2	681.2	682.5
0.0833	706.1	707.2	711.6	714.4
0.1111	735.4	736.5	741.9	746.2
0.1389	764.1	765.2	771.4	776.8
0.1667	791.7	792.6	799.4	805.0
0.1944	817.7	818.8	825.5	831.0
0.2222	841.4	842.1	849.8	855.4
0.2500	863.4	863.9	871.1	877.8
0.2778	884.0	883.6	890.7	897.0
0.3056	902.2	901.8	908.3	914.5
0.3333	918.6	917.5	924.0	930.1
0.3611	933.4	931.9	938.1	943.9
0.3889	946.6	944.0	950.6	956.3
0.4167	958.7	956.5	963.8	969.2
0.4444	969.2	967.0	974.8	980.3
0.4722	978.4	976.2	984.7	990.5
0.5000	987.4	985.6	993.7	999.2
0.5278	995.2	992.2	999.9	1006.0
0.5556	1002.1	999.0	1006.2	1012.1
0.5833	1008.4	1005.1	1011.9	1017.5
0.6111	1014.0	1010.6	1017.1	1022.6
0.6389	1019.1	1015.4	1021.7	1027.4
0.6667	1023.7	1020.1	1026.8	1032.5
0.6944	1027.9	1024.1	1030.5	1036.9
0.7222	1031.6	1027.9	1034.9	1039.1
0.7500	1035.0	1031.1	1037.9	1043.4
0.7778	1038.1	1034.1	1041.7	1047.8
0.8056	1040.9	1036.8	1045.1	1051.6
0.8333	1043.7	1039.3	1048.0	1055.7
0.8611	1045.8	1041.4	1051.8	1059.5
0.8889	1047.9	1043.2	1055.6	1063.1
0.9167	1049.8	1045.5	1059.4	1066.6
0.9444	1051.6	1047.2	1063.4	1070.0
0.9722	1053.2	1048.7	1067.1	1073.2
1.0000	1054.5	1050.0	1070.9	1076.3

PEBBLE AVERAGE SURFACE TEMPERATURE, °F (K)													
RADIAL	0.0	0.0003	0.1606	0.2410	0.2739	0.3068	0.3398	0.3727	0.4056	0.4407	0.4795	0.5066	0.5337
AXIAL													
0.0	719.3	719.0	718.5	718.2	717.6	717.1	716.7	716.1	715.3	714.8	713.7	712.9	711.9
0.0270	759.8	759.0	758.4	757.9	757.2	756.5	755.9	755.1	754.0	752.8	751.0	749.6	748.0
0.0556	800.0	803.5	802.0	802.1	801.2	800.0	799.7	798.8	797.4	795.8	794.0	792.0	791.7
0.0833	846.7	846.2	845.3	844.6	843.5	842.6	842.0	841.1	839.5	837.7	835.5	833.2	831.1
0.1111	886.4	885.7	884.8	883.9	882.8	881.7	881.2	880.0	878.6	876.6	874.0	871.0	868.0
0.1389	923.3	920.6	919.6	919.6	917.4	916.2	915.8	915.0	913.1	911.4	909.0	906.5	904.0
0.1667	951.8	951.1	950.0	949.0	947.7	946.5	946.2	945.0	943.0	941.1	938.0	935.0	932.1
0.1944	978.7	977.5	976.6	975.2	973.9	972.7	972.4	971.0	969.0	967.0	964.0	961.0	958.1
0.2222	1001.3	1000.5	999.4	998.2	996.8	995.4	995.4	994.0	992.0	990.0	987.0	984.0	981.0
0.2500	1021.7	1020.8	1019.7	1018.4	1017.1	1015.8	1015.6	1014.9	1012.7	1010.2	1007.0	1003.0	1000.0

Table 3. CONTINUED

0.2770	1075.6	1070.0	1037.6	1036.3	1030.9	1033.6	1032.5	1032.0	1070.0	1029.9	1028.0	1025.7	1022.7
0.3056	1075.0	1070.0	1033.7	1032.3	1030.9	1030.9	1030.5	1030.9	1005.4	1000.4	1002.0	1001.0	1078.0
0.3333	1070.1	1069.2	1060.0	1066.6	1064.2	1063.9	1063.7	1063.7	1062.7	1060.2	1060.7	1055.7	1052.0
0.3611	1067.0	1062.1	1060.9	1070.0	1070.1	1070.4	1074.6	1077.0	1073.0	1071.0	1069.7	1060.0	1064.3
0.3889	1064.6	1061.7	1062.0	1061.0	1060.6	1060.3	1060.0	1060.0	1061.7	1061.0	1062.0	1061.0	1076.0
0.4167	1102.1	1104.1	1102.9	1107.0	1100.0	1099.0	1099.0	1099.0	1097.9	1094.3	1092.0	1091.0	1094.0
0.4444	1110.0	1113.5	1112.2	1110.7	1109.3	1109.1	1107.7	1106.0	1106.0	1102.0	1100.0	1099.0	1094.0
0.4722	1121.0	1122.0	1120.7	1119.1	1117.7	1116.6	1115.1	1113.2	1113.0	1109.4	1109.0	1107.3	1100.2
0.5000	1130.4	1129.6	1129.3	1126.7	1125.3	1124.2	1123.7	1122.0	1122.0	1118.0	1116.0	1116.7	1111.7
0.5278	1137.5	1136.5	1134.2	1133.6	1132.2	1131.0	1130.5	1129.0	1129.0	1125.0	1123.0	1121.0	1114.3
0.5556	1103.7	1102.7	1101.0	1100.7	1100.4	1100.7	1100.7	1100.7	1100.7	1100.0	1100.0	1100.0	1100.0
0.5833	1140.1	1140.3	1140.0	1145.3	1140.9	1142.0	1142.2	1141.7	1141.0	1139.5	1139.7	1132.0	1128.0
0.6111	1130.0	1135.0	1132.1	1133.3	1130.9	1130.9	1130.7	1130.2	1130.2	1128.0	1128.0	1137.7	1130.7
0.6389	1154.0	1150.0	1150.6	1151.9	1153.6	1152.0	1151.0	1150.0	1150.0	1149.0	1149.0	1142.1	1139.0
0.6667	1163.1	1162.1	1160.0	1159.9	1157.7	1156.6	1155.0	1154.0	1152.0	1150.0	1149.0	1146.1	1143.1
0.6944	1164.9	1165.0	1164.5	1162.7	1161.0	1160.3	1159.6	1159.6	1159.6	1158.2	1157.7	1150.7	1146.7
0.7222	1170.3	1169.3	1167.9	1166.1	1164.0	1163.7	1162.0	1161.0	1161.0	1159.0	1158.0	1152.0	1149.0
0.7500	1172.0	1172.0	1171.0	1169.2	1167.9	1166.7	1165.0	1164.0	1164.0	1162.0	1161.0	1155.0	1152.0
0.7778	1170.1	1170.1	1171.7	1171.0	1170.7	1169.5	1168.7	1167.0	1167.0	1165.0	1164.0	1154.0	1155.0
0.8056	1170.7	1171.7	1170.3	1170.0	1172.2	1172.0	1171.0	1169.0	1169.0	1167.0	1166.0	1160.0	1157.0
0.8333	1106.9	1109.0	1108.5	1107.0	1105.6	1104.3	1103.0	1102.0	1102.0	1100.0	1100.0	1100.0	1100.0
0.8611	1102.0	1102.0	1100.6	1100.7	1101.5	1101.0	1100.0	1100.0	1100.0	1100.0	1100.0	1100.0	1100.0
0.8889	1100.0	1103.0	1102.5	1100.0	1100.0	1100.0	1100.0	1100.0	1100.0	1100.0	1100.0	1100.0	1100.0
0.9167	1106.6	1106.6	1106.2	1102.3	1101.1	1100.0	1100.0	1100.0	1100.0	1100.0	1100.0	1100.0	1100.0
0.9444	1100.3	1107.3	1105.0	1102.0	1101.6	1100.0	1100.0	1100.0	1100.0	1100.0	1100.0	1100.0	1100.0
0.9722	1100.0	1100.0	1107.5	1105.0	1100.3	1102.2	1102.0	1100.0	1100.0	1100.0	1100.0	1100.0	1100.0
1.0000	1101.5	1100.0	1100.0	1107.1	1105.9	1100.7	1103.7	1102.3	1100.0	1100.0	1100.0	1100.0	1100.0

PEOPLE AVERAGE SURFACE TEMPERATURE, °S (H)

RADIAL	0.5400	0.4800	0.6105	0.6090	0.6700	0.7060	0.7325	0.7500	0.7800	0.8100	0.9002	0.8707	0.9072
AXIAL	710.9	709.9	700.7	707.2	704.0	700.3	702.7	701.1	699.0	697.0	699.7	696.3	693.2
0.0270	707.9	706.5	700.0	702.6	700.7	700.6	720.3	723.0	711.0	720.0	725.0	723.5	721.7
0.0540	700.0	700.2	706.1	701.1	700.9	700.1	700.0	715.0	710.1	700.0	700.2	700.7	703.7
0.0810	031.0	029.2	026.9	023.0	020.6	017.5	013.0	009.0	004.0	000.0	000.0	000.0	000.0
0.1080	060.3	067.5	045.0	061.0	057.0	050.0	049.7	049.7	049.7	049.7	049.7	049.7	049.7
0.1350	003.1	001.0	000.0	000.0	001.1	007.5	002.1	027.0	025.0	000.0	000.0	000.0	000.0
0.1620	031.1	031.0	029.7	023.9	020.5	016.4	010.0	009.0	000.0	000.0	000.0	000.0	000.0
0.1890	050.0	051.3	050.6	040.4	040.0	042.1	035.7	031.2	025.0	015.3	007.0	001.0	002.0
0.2160	001.7	000.0	077.2	071.9	060.3	043.3	037.7	032.0	026.5	020.2	020.3	021.3	012.5
0.2430	000.7	000.0	007.1	001.7	007.0	003.0	026.0	022.1	016.0	010.0	006.2	030.7	020.0
0.2700	1019.3	1017.5	1010.6	1009.1	1005.2	1001.0	993.9	990.0	980.0	970.0	962.1	950.2	948.7
0.2970	1030.2	1033.3	1030.2	1020.6	1020.6	1016.1	1009.1	1002.9	996.7	991.2	981.1	967.9	958.1
0.3240	1009.2	1007.2	1000.1	1009.5	1010.3	1007.0	1002.6	1001.2	1000.7	1000.0	1000.0	990.0	970.0
0.3510	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.3780	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.4050	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.4320	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.4590	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.4860	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.5130	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.5400	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.5670	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.5940	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.6210	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.6480	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.6750	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.7020	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.7290	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.7560	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.7830	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.8100	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.8370	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.8640	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.8910	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.9180	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.9450	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
0.9720	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0
1.0000	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0	1000.0

PEOPLE AVERAGE SURFACE TEMPERATURE, °S (H)

RADIAL	0.9277	0.9510	0.9740	1.0000
AXIAL	692.9	690.2	690.6	701.7
0.0270	721.0	722.7	720.7	733.1
0.0540	752.1	753.9	761.6	767.3
0.0810	703.1	700.7	703.6	690.3
0.1080	013.2	010.2	023.7	031.1
0.1350	000.5	000.1	050.0	050.5
0.1620	000.0	000.7	070.0	082.6
0.1890	004.1	005.5	001.3	001.3
0.2160	000.0	000.0	013.2	021.2
0.2430	021.0	020.0	021.0	036.7
0.2700	034.0	030.0	022.6	053.2
0.2970	000.0	000.0	040.0	062.0
0.3240	000.0	057.0	065.0	072.0
0.3510	070.0	067.0	070.0	081.5
0.3780	000.0	070.0	083.0	089.6

Table 3. CONTINUED

0.0007	1030.3	1030.1	1032.0	1030.0
0.0006	1031.3	1033.1	1030.0	1031.1
0.7222	1000.1	1034.0	1037.0	1033.1
0.7500	1002.0	1030.2	1030.1	1001.2
0.7770	1000.0	1000.1	1001.1	1002.0
0.0050	1000.0	1002.5	1002.0	1000.0
0.0333	1000.0	1000.0	1000.0	1000.0
0.0611	1030.6	1000.1	1000.0	1000.1
0.0000	1032.2	1000.6	1000.2	1000.2
0.0167	1033.6	1000.1	1000.5	1000.3
0.0000	1034.0	1000.0	1000.6	1003.2
0.0722	1034.3	1001.7	1030.7	1001.1
1.0000	1035.5	1032.0	1031.6	1001.0

PEOPLE THERMAL CONDUCTIVITY DATA WILL BE SAVED ← SPECIAL ACTION

SAMPLE PROBLEM, TWO DIMENSIONAL PEOPLE AND THERMAL HYDRAULICS

— NOW A REPRESENTATIVE PEOPLE IS

ROOMS 150 ZONELOADS 0 THERMAL, LITIAL, BATHAL 37 38

TREATED FOR AVERAGE ZONE CONDITIONS —

SOME ARE SURFACE TEMPERATURES (DEGREES C) FOR MASS FLOW RATE (KG/SEC) 6.37700 02 SURFACE TEMPS (M-TS) 1450.

ROOM	(CONDUCTIVITY AND P(EXPOSURE)), PLIES	SURFACE	SOIL	HEAT CAPACITY TEMPERATURES, BT/BB (DEG/C)
1	0.0003 0.2550700 21	307.2	005.7	000.0 010.7 000.0 -67.3
2	0.3303 0.0000000 21	005.5	570.0	001.2 070.0 000.0 -107.0
3	0.2062 0.2000000 21	701.0	000.1	007.1 007.0 000.0 -110.1
4	0.2030 0.3301050 22	013.0	701.0	021.0 003.7 000.0 -100.0
5	0.2000 0.5070020 22	012.3	700.0	001.0 001.0 000.0 -09.1
6	0.2700 0.0000010 22	720.0	770.0	002.7 007.0 000.0 -72.2
7	0.2033 0.0277220 22	700.0	000.0	010.0 000.0 000.0 -57.1
8	0.2001 0.0533000 22	700.0	027.0	030.0 000.0 000.0 -05.2
9	0.2050 0.0730170 22	010.0	005.0	052.0 000.0 000.0 -30.0
10	0.2000 0.0000000 22	030.0	000.0	005.0 000.0 000.0 -20.0
11	0.2000 0.7030150 22	052.0	072.0	070.0 000.0 000.0 -23.0
12	0.2000 0.7107200 22	000.0	000.0	005.0 000.0 000.0 -10.5
13	0.2000 0.7230000 22	077.0	000.0	052.0 000.0 000.0 -10.0
14	0.2000 0.7300350 22	000.0	000.0	000.0 000.0 000.0 -12.0
15	0.2000 0.7307500 22	000.0	000.0	000.0 000.0 000.0 -0.7
16	0.2000 0.7000000 22	000.0	000.0	000.0 000.0 000.0 -7.0
17	0.2000 0.7000000 22	000.0	000.0	000.0 000.0 000.0 -6.0
18	0.2000 0.7000000 22	000.0	000.0	000.0 000.0 000.0 -5.0
19	0.2000 0.2000120 21	000.0	000.0	000.0 000.0 000.0 -65.2
20	0.2000 0.0700000 21	000.0	000.0	000.0 000.0 000.0 -100.2
21	0.2000 0.2000000 21	000.0	000.0	000.0 000.0 000.0 -110.0
22	0.2000 0.3277000 22	000.0	000.0	000.0 000.0 000.0 -100.2
23	0.2700 0.5170000 22	000.0	000.0	000.0 000.0 000.0 -09.0
24	0.2700 0.5500150 22	000.0	000.0	000.0 000.0 000.0 -72.2
25	0.2000 0.5000000 22	000.0	000.0	000.0 000.0 000.0 -57.1
26	0.2000 0.0533000 22	000.0	000.0	000.0 000.0 000.0 -05.2
27	0.2000 0.0730170 22	000.0	000.0	000.0 000.0 000.0 -30.0
28	0.2000 0.0000000 22	000.0	000.0	000.0 000.0 000.0 -20.0
29	0.2000 0.7030150 22	000.0	000.0	000.0 000.0 000.0 -23.0
30	0.2000 0.7107200 22	000.0	000.0	000.0 000.0 000.0 -10.5
31	0.2000 0.7230000 22	000.0	000.0	000.0 000.0 000.0 -10.0
32	0.2000 0.7300350 22	000.0	000.0	000.0 000.0 000.0 -12.0
33	0.2000 0.7307500 22	000.0	000.0	000.0 000.0 000.0 -0.7
34	0.2000 0.7000000 22	000.0	000.0	000.0 000.0 000.0 -7.0
35	0.2000 0.7000000 22	000.0	000.0	000.0 000.0 000.0 -6.0
36	0.2000 0.7000000 22	000.0	000.0	000.0 000.0 000.0 -5.0
37	0.2000 0.2000120 21	000.0	000.0	000.0 000.0 000.0 -65.2
38	0.2000 0.0700000 21	000.0	000.0	000.0 000.0 000.0 -100.2
39	0.2000 0.2000000 21	000.0	000.0	000.0 000.0 000.0 -110.0
40	0.2000 0.3277000 22	000.0	000.0	000.0 000.0 000.0 -100.2
41	0.2700 0.5170000 22	000.0	000.0	000.0 000.0 000.0 -09.0
42	0.2700 0.5500150 22	000.0	000.0	000.0 000.0 000.0 -72.2
43	0.2000 0.5000000 22	000.0	000.0	000.0 000.0 000.0 -57.1
44	0.2000 0.0533000 22	000.0	000.0	000.0 000.0 000.0 -05.2
45	0.2000 0.0730170 22	000.0	000.0	000.0 000.0 000.0 -30.0
46	0.2000 0.0000000 22	000.0	000.0	000.0 000.0 000.0 -20.0
47	0.2000 0.7030150 22	000.0	000.0	000.0 000.0 000.0 -23.0
48	0.2000 0.7107200 22	000.0	000.0	000.0 000.0 000.0 -10.5
49	0.2000 0.7230000 22	000.0	000.0	000.0 000.0 000.0 -10.0
50	0.2000 0.7300350 22	000.0	000.0	000.0 000.0 000.0 -12.0
51	0.2000 0.7307500 22	000.0	000.0	000.0 000.0 000.0 -0.7
52	0.2000 0.7000000 22	000.0	000.0	000.0 000.0 000.0 -7.0
53	0.2000 0.7000000 22	000.0	000.0	000.0 000.0 000.0 -6.0
54	0.2000 0.7000000 22	000.0	000.0	000.0 000.0 000.0 -5.0
55	0.2000 0.2000120 21	000.0	000.0	000.0 000.0 000.0 -65.2
56	0.2000 0.0700000 21	000.0	000.0	000.0 000.0 000.0 -100.2
57	0.2000 0.2000000 21	000.0	000.0	000.0 000.0 000.0 -110.0
58	0.2000 0.3277000 22	000.0	000.0	000.0 000.0 000.0 -100.2
59	0.2700 0.5170000 22	000.0	000.0	000.0 000.0 000.0 -09.0
60	0.2700 0.5500150 22	000.0	000.0	000.0 000.0 000.0 -72.2
61	0.2000 0.5000000 22	000.0	000.0	000.0 000.0 000.0 -57.1
62	0.2000 0.0533000 22	000.0	000.0	000.0 000.0 000.0 -05.2
63	0.2000 0.0730170 22	000.0	000.0	000.0 000.0 000.0 -30.0
64	0.2000 0.0000000 22	000.0	000.0	000.0 000.0 000.0 -20.0
65	0.2000 0.7030150 22	000.0	000.0	000.0 000.0 000.0 -23.0
66	0.2000 0.7107200 22	000.0	000.0	000.0 000.0 000.0 -10.5
67	0.2000 0.7230000 22	000.0	000.0	000.0 000.0 000.0 -10.0
68	0.2000 0.7300350 22	000.0	000.0	000.0 000.0 000.0 -12.0
69	0.2000 0.7307500 22	000.0	000.0	000.0 000.0 000.0 -0.7
70	0.2000 0.7000000 22	000.0	000.0	000.0 000.0 000.0 -7.0
71	0.2000 0.7000000 22	000.0	000.0	000.0 000.0 000.0 -6.0

Table 3. CONTINUED

72	0.2863	0.4718482	22	876.2	880.5	881.5	884.6	888.8	-5.2
73	0.3196	0.2173500	21	387.6	465.4	676.2	519.8	368.2	-45.7
74	0.3516	0.9386408	21	888.8	581.7	359.6	631.2	708.0	-13.0
75	0.3801	0.1703188	22	519.1	610.6	631.4	723.8	746.2	-107.2
76	0.2835	0.2705320	22	583.2	661.4	688.5	761.7	878.1	-100.7
77	0.2778	0.3824882	22	439.1	786.5	723.3	788.7	858.0	-85.9
78	0.2759	0.5898378	22	693.8	739.0	752.7	806.6	859.7	-70.8
79	0.2753	0.5707808	22	728.0	768.6	775.5	818.5	861.8	-55.8
80	0.2769	0.5851712	22	749.5	785.2	793.8	828.0	862.3	-48.7
81	0.2782	0.6188352	22	773.2	801.4	808.5	835.7	863.0	-35.8
82	0.2792	0.6306188	22	792.2	818.8	828.3	852.0	863.8	-28.2
83	0.2801	0.6832622	22	837.8	825.6	829.9	847.2	868.6	-22.5
84	0.2808	0.6538132	22	818.7	838.2	837.7	851.5	865.8	-17.9
85	0.2815	0.6896882	22	829.6	847.2	848.0	855.8	866.2	-18.3
86	0.2815	0.6552382	22	837.5	846.9	849.1	857.8	866.8	-11.5
87	0.2819	0.6888882	22	848.0	851.5	853.2	860.2	867.5	-9.2
88	0.2823	0.6847212	22	849.2	855.2	856.6	862.2	868.1	-7.8
89	0.2826	0.6881082	22	853.8	858.3	859.4	864.0	868.8	-5.2
90	0.2828	0.6986782	22	856.9	861.0	862.8	867.0	870.0	-5.1
91	0.5260	0.2815152	21	379.8	458.0	667.8	507.5	348.6	-51.3
92	0.3587	0.7828202	21	882.6	528.8	545.8	611.8	678.8	-85.8
93	0.3835	0.1536862	22	537.9	598.1	613.6	680.8	768.2	-100.8
94	0.2883	0.2880972	22	568.0	688.0	668.6	739.1	811.1	-95.8
95	0.2772	0.3286732	22	628.5	685.8	702.0	765.8	828.1	-82.7
96	0.2788	0.8228832	22	663.6	716.8	738.2	782.5	828.1	-68.2
97	0.2732	0.5892632	22	698.5	781.8	752.1	798.3	868.0	-55.1
98	0.2728	0.3835712	23	726.6	768.8	769.3	802.8	836.2	-43.6
99	0.2728	0.1858502	23	788.2	778.8	783.1	808.7	826.8	-38.5
100	0.2737	0.1895552	23	767.2	788.8	798.2	815.3	836.6	-27.8
101	0.2745	0.3881592	23	781.6	798.0	803.2	828.0	837.0	-21.8
102	0.2752	0.1891282	23	793.2	807.1	818.8	822.8	837.8	-17.8
103	0.2754	0.1898962	23	802.5	813.6	816.3	827.0	838.8	-13.9
104	0.2763	0.1185162	23	818.0	818.8	821.8	828.6	838.3	-11.1
105	0.2767	0.1181822	23	816.1	823.2	828.9	831.7	838.7	-8.9
106	0.2770	0.1188102	23	820.8	826.6	828.8	833.5	838.8	-7.1
107	0.2773	0.1117272	23	828.8	829.8	830.6	835.0	838.8	-5.7
108	0.2775	0.1118682	23	828.1	832.0	832.9	836.7	840.6	-8.8
109	0.5881	0.1817782	21	377.8	458.8	659.7	805.7	533.7	-86.6
110	0.3701	0.6725012	21	835.6	515.1	529.8	588.6	688.8	-76.3
111	0.3183	0.1327222	22	895.5	78.8	592.5	662.8	732.5	-90.8
112	0.2875	0.2828082	22	551.3	623.1	648.2	707.8	775.2	-88.1
113	0.2781	0.2688292	22	588.5	650.3	675.3	738.8	753.0	-77.0
114	0.2738	0.3317882	22	638.6	688.2	701.7	758.8	789.8	-68.8
115	0.2718	0.3880752	22	672.1	712.0	722.1	781.8	801.3	-51.9
116	0.2707	0.8881122	22	688.3	738.1	738.2	778.0	801.7	-81.6
117	0.2702	0.5826512	22	718.3	788.8	758.9	776.3	801.5	-33.8
118	0.2799	0.5729382	22	738.1	758.2	761.2	781.3	801.5	-26.2
119	0.2657	0.6818682	22	748.6	765.6	769.8	785.5	801.8	-20.8
120	0.2697	0.4885162	22	768.5	775.2	776.8	788.1	801.8	-16.5
121	0.2701	0.6878282	22	769.3	779.8	781.8	792.1	802.3	-13.1
122	0.2706	0.8828262	23	776.8	788.5	788.5	798.6	802.8	-10.5
123	0.2705	0.8828682	23	782.2	788.7	790.3	796.7	803.3	-8.2
124	0.2709	0.8828212	23	786.9	792.1	793.8	798.5	803.7	-6.6
125	0.2711	0.8838812	23	798.0	795.0	796.8	800.1	808.3	-5.3
126	0.2718	0.8833122	23	798.1	797.5	798.8	801.9	805.8	-4.5
127	0.5659	0.1879872	21	378.2	453.9	662.7	808.1	538.8	-85.7
128	0.3893	0.5388372	21	836.9	516.8	538.2	588.1	639.7	-69.8
129	0.3337	0.1812952	22	895.7	573.8	589.1	651.5	718.8	-81.0
130	0.3855	0.1888732	22	588.8	618.3	633.8	683.2	753.0	-77.8
131	0.2919	0.1921582	22	585.1	652.6	665.7	717.7	768.5	-67.7
132	0.2888	0.2288782	22	632.7	679.0	689.9	732.8	775.7	-56.3
133	0.2887	0.2588782	22	682.9	699.8	708.6	783.8	788.0	-85.3
134	0.2782	0.2833982	22	687.2	716.3	723.8	751.2	779.0	-36.3
135	0.2766	0.3858862	22	786.5	728.6	735.2	757.8	779.5	-28.8
136	0.2755	0.3238812	22	722.1	788.3	788.8	762.8	788.0	-23.0
137	0.2788	0.3883982	22	738.7	789.0	752.5	766.6	788.6	-18.3
138	0.2782	0.3888822	22	788.6	756.1	758.8	770.1	781.2	-18.6
139	0.2739	0.3879382	22	752.8	761.8	768.2	773.1	782.0	-11.6
140	0.2736	0.3788552	22	758.8	766.7	768.5	775.8	782.7	-8.2
141	0.2738	0.3888582	22	768.8	778.6	772.1	777.7	783.8	-7.8
142	0.2732	0.3888882	22	769.3	773.8	775.8	775.8	788.1	-5.8
143	0.2731	0.8888722	22	773.8	776.6	777.5	781.1	788.6	-8.6
144	0.2731	0.6188172	22	776.8	778.8	778.7	782.6	785.8	-3.8
145	0.0	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
146	0.0	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
147	0.0	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
148	0.0	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
149	0.0	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
150	0.0	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
151	0.0	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
152	0.0	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
153	0.0	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
154	0.0	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
155	0.0	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0

DISTRIBUTION FRACTIONS OF 188 HEAT TEMPERATURES IN TEMPERATURE FRACILES COPY NET RANGE (C) 390.0 917.9
 0.0 0.0 0.0 0.0 0.0 0.02778 0.02082 0.00649 0.01389 0.03388
 0.02883 0.02883 0.03872 0.08167 0.09722 0.15278 0.18617 0.18583 0.15972 0.13888

SOOT AVERAGE TEMP AND T002, TREN SUBJECT 793.82 798.31 0.0 0.0

MAX TEMPS, PEAK/NEAR BY SOOT, SOOTAGE 922.2 917.8 0.0 0.0 POWER (WAT) 1658.

AVERAGE AND PEAK TEMPERATURE SLOPE AT FIBRE HEAT/SHELL INTERFACE (DEG/C) -81.8 -118.1

CORRELATION FAILURE COUNT 1051 0

FILE -GUTHP- UNITEN, UNIT AND VERBICE 32 1

Table 3. CONTINUED

96	0.2485	0.414228E 22	663.6	700.0	731.7	788.0	844.4	-75.6
97	0.2474	0.513204E 22	699.5	701.0	753.2	820.9	866.7	-61.0
98	0.2470	0.652045E 22	726.4	700.0	770.3	807.8	848.8	-68.8
99	0.2469	0.871236E 22	749.2	776.0	783.9	813.6	847.4	-38.3
100	0.2475	0.696296E 22	767.2	788.0	794.8	819.2	847.8	-20.4
101	0.2484	0.699331E 22	793.6	799.0	803.6	822.7	847.1	-24.2
102	0.2485	0.707974E 22	797.2	807.1	810.0	825.7	846.7	-19.7
103	0.2489	0.715701E 22	802.7	813.6	816.6	829.4	846.4	-15.8
104	0.2497	0.104041E 23	813.1	819.0	821.3	832.8	845.8	-12.0
105	0.2493	0.104558E 23	816.1	823.2	827.1	837.7	845.8	-9.0
106	0.2495	0.104956E 23	820.9	826.4	829.1	840.2	845.8	-7.0
107	0.2497	0.105273E 23	826.9	829.5	832.7	843.6	845.7	-6.3
108	0.2499	0.105518E 23	829.1	832.0	835.0	847.3	845.6	-5.4
109	0.4894	0.193165E 21	377.0	440.9	460.6	498.0	492.7	-51.0
110	0.3334	0.679791E 21	435.6	435.1	431.0	498.7	463.2	-94.7
111	0.2801	0.130289E 22	435.5	474.0	494.5	477.0	789.8	-100.0
112	0.2599	0.204892E 22	551.3	427.1	492.1	717.1	791.6	-97.7
113	0.2517	0.270015E 22	599.5	660.2	677.0	787.5	897.2	-95.8
114	0.2474	0.329915E 22	639.4	699.3	707.1	787.8	811.7	-90.0
115	0.2460	0.380170E 22	672.1	712.0	713.2	767.3	810.0	-57.4
116	0.2450	0.427059E 22	694.3	719.1	719.1	776.0	809.3	-46.1
117	0.2444	0.471890E 22	719.3	748.7	751.6	778.0	807.7	-36.0
118	0.2441	0.516777E 22	736.1	756.2	761.0	788.1	806.8	-29.1
119	0.2439	0.567622E 22	749.6	765.6	770.0	797.7	805.4	-23.1
120	0.2438	0.610793E 22	760.5	773.2	776.7	799.0	805.0	-18.3
121	0.2437	0.728742E 22	769.3	774.6	782.2	797.5	808.0	-14.6
122	0.2437	0.778270E 22	774.4	784.4	786.8	795.7	808.8	-11.6
123	0.2440	0.902525E 22	782.2	788.7	790.5	797.6	808.0	-9.3
124	0.2439	0.102878E 23	786.9	797.1	793.5	795.2	809.0	-7.8
125	0.2442	0.103158E 23	790.9	798.0	796.1	800.7	805.3	-5.0
126	0.2443	0.103369E 23	794.1	797.6	798.5	802.8	806.7	-5.0
127	0.5079	0.149096E 21	379.2	451.0	463.6	493.1	508.0	-80.0
128	0.3594	0.535952E 21	436.9	436.0	437.7	493.6	472.7	-77.6
129	0.3010	0.102160E 22	495.7	472.0	490.8	660.0	729.8	-89.0
130	0.2759	0.150809E 22	539.8	474.3	474.0	701.8	767.8	-86.2
131	0.2634	0.192583E 22	595.1	482.4	467.2	728.8	782.7	-75.7
132	0.2576	0.227387E 22	632.7	478.0	491.1	734.9	784.7	-67.7
133	0.2539	0.255900E 22	662.9	499.9	509.6	749.2	786.8	-60.3
134	0.2516	0.279366E 22	687.2	516.3	528.2	755.0	785.7	-60.2
135	0.2501	0.299198E 22	706.5	529.6	535.8	760.8	788.0	-32.1
136	0.2491	0.316127E 22	722.1	540.3	545.3	768.9	788.7	-25.4
137	0.2483	0.330750E 22	738.5	549.0	552.9	769.6	788.0	-20.2
138	0.2478	0.343520E 22	748.5	556.1	559.2	770.6	788.0	-16.2
139	0.2475	0.358718E 22	752.8	561.4	568.4	776.3	788.2	-12.9
140	0.2472	0.364536E 22	759.8	564.7	568.7	776.6	788.2	-10.7
141	0.2470	0.373128E 22	764.0	570.4	572.2	779.6	788.9	-8.2
142	0.2469	0.380566E 22	769.3	573.9	575.2	780.2	788.2	-6.4
143	0.2469	0.387894E 22	771.0	576.0	577.0	781.8	788.5	-5.1
144	0.2467	0.397690E 22	776.0	578.9	579.0	783.0	788.3	-4.2
145	0.0	0.0	850.0	850.0	857.0	877.0	877.0	0.0
146	0.0	0.0	850.0	850.0	857.0	877.0	877.0	0.0
147	0.0	0.0	850.0	850.0	857.0	877.0	877.0	0.0
148	0.0	0.0	850.0	850.0	857.0	877.0	877.0	0.0
149	0.0	0.0	850.0	850.0	857.0	877.0	877.0	0.0
150	0.0	0.0	850.0	850.0	857.0	877.0	877.0	0.0
151	0.0	0.0	850.0	850.0	857.0	877.0	877.0	0.0
152	0.0	0.0	850.0	850.0	857.0	877.0	877.0	0.0
153	0.0	0.0	850.0	850.0	857.0	877.0	877.0	0.0
154	0.0	0.0	850.0	850.0	857.0	877.0	877.0	6.0
155	0.0	0.0	850.0	850.0	857.0	877.0	877.0	0.0

DISTRIBUTION FRACTIONS OF 100 WT% TEMPERATURES IN ZONE FRACTIONS OVER THE RANGE (°) 390.0 916.8
 0.0 0.0 0.0 0.0 0.0 0.32093 0.32093 0.01389 0.01389 0.01389 0.01389 0.01389 0.01389
 0.02083 0.02778 0.02083 0.04972 0.11111 0.13889 0.11111 0.14583 0.16667 0.14583

ZONE AVERAGE TEMP AND TMAX, TMIN 799.20 702.40 0.0 0.0

MAX TEMPS, PEAK/MPAN BY ZONE, SIZE/CM 923.2 918.8 0.0 0.0 0.0000 0.0000 789.2 0.0 POWER (W) 1654.

AVERAGE AND PEAK TEMPERATURE SLOPE AT PEARL REAC/SHELL INTERFACE (DEG/CM) -86.4 -170.9

CORRELATION PEARL COEFF 0.00 0

TEMPERATURES RECALCULATED FOR THE PEARL ZONE SURFACE TEMPERATURES (ASSUMED WORST CASE, DISPERSED INTERFACES) ← NOTE

ZONE (CONDUCTIVITY AND P (EXPOSURE)), PLOTS	STORAGE	SHELL	PEARL	COEFF	TEMPERATURES, DT/DP (DEG/CM)			
1	0.4983	0.256836E 21	826.8	509.8	521.2	477.8	477.8	-67.3
2	0.3822	0.103189E 22	496.9	493.1	413.6	695.6	778.8	-106.3
3	0.2997	0.208968E 22	508.1	463.0	485.7	744.7	848.7	-116.6
4	0.2871	0.324731E 22	611.9	716.2	736.8	817.6	897.2	-105.5
5	0.2934	0.494796E 22	649.3	757.0	776.2	808.0	888.0	-89.1
6	0.2825	0.515668E 22	738.1	780.3	802.2	857.9	891.7	-71.8
7	0.2887	0.467788E 22	771.0	815.1	824.1	865.5	892.4	-56.6
8	0.2861	0.592248E 22	900.7	838.1	888.8	879.3	893.7	-88.9
9	0.2878	0.613580E 22	928.7	852.0	860.0	887.4	894.0	-35.9
10	0.2885	0.630189E 22	888.1	867.0	872.8	888.8	894.4	-28.6
11	0.2895	0.648538E 22	859.8	878.1	882.5	890.1	894.7	-22.0
12	0.2903	0.668389E 22	872.5	887.3	890.9	894.0	894.8	-18.8
13	0.2910	0.689399E 22	882.9	898.0	897.7	895.7	895.7	-14.8
14	0.2916	0.702328E 22	891.3	901.0	903.3	892.5	895.9	-11.0
15	0.2915	0.702996E 23	898.2	904.0	907.9	897.0	896.0	-9.4
16	0.2920	0.703760E 23	907.5	911.2	911.7	897.7	896.0	-7.8
17	0.2928	0.703733E 23	918.5	913.7	918.9	898.9	896.8	-6.3
18	0.2927	0.704020E 23	912.4	916.9	919.0	892.7	896.5	-5.5
19	0.4978	0.287337E 21	435.3	798.8	516.8	567.7	619.6	-65.2
20	0.3839	0.477810E 21	481.7	481.1	489.2	688.5	770.0	-108.1
21	0.3007	0.197092E 22	559.9	457.6	480.0	748.4	846.4	-115.2
22	0.2869	0.319318E 22	626.9	710.7	731.0	811.8	890.7	-108.9

Table 3. CONTINUED

TEMPERATURES RECALCULATED FOR THE THERMAL CONDUCTIVITY POLYNOMIAL BY 0.4 ← NOTE

SOOR	(CONDUCTIVITY AND PLOT POSITIVE), FLUID	TEMP	SHELL	TEMP	TEMP	TEMP	TEMP	
1	0.2436	0.254038E 21	197.2	685.7	705.0	558.0	619.6	-78.9
2	0.2457	0.261165E 22	665.5	770.8	781.5	781.8	781.6	-110.1
3	0.2479	0.270689E 22	781.8	888.1	889.5	889.5	889.7	-120.4
4	0.2501	0.280638E 22	613.4	791.0	728.2	818.8	801.7	-110.8
5	0.2522	0.288257E 22	672.3	788.4	763.0	827.3	811.7	-98.0
6	0.2536	0.297216E 22	720.8	778.6	799.2	845.8	815.1	-89.0
7	0.2554	0.310877E 22	759.2	808.9	819.2	864.6	818.4	-83.1
8	0.2569	0.320000E 22	790.6	827.8	837.6	879.1	818.8	-80.2
9	0.2580	0.324092E 22	815.9	853.8	853.8	888.1	818.8	-79.0
10	0.2590	0.328169E 22	836.2	880.2	868.8	890.9	815.4	-77.0
11	0.2598	0.332040E 22	852.7	907.0	876.9	896.4	816.8	-75.5
12	0.2604	0.335701E 22	866.1	934.4	885.6	901.8	817.8	-70.5
13	0.2612	0.339239E 22	877.0	961.5	892.7	901.8	819.3	-68.5
14	0.2617	0.342710E 22	885.8	989.0	898.5	908.8	819.2	-67.2
15	0.2622	0.346132E 22	893.1	1017.7	903.3	917.6	820.0	-67.7
16	0.2626	0.349508E 22	899.0	1046.6	907.3	918.0	820.0	-67.7
17	0.2629	0.352839E 22	903.8	1075.7	910.6	918.0	821.6	-67.1
18	0.2634	0.356130E 22	907.5	1105.0	913.7	918.4	823.2	-66.2
19	0.2639	0.359382E 21	912.2	1134.5	916.8	922.0	823.7	-65.5
20	0.2643	0.362597E 21	916.4	1164.2	919.8	927.0	824.2	-64.8
21	0.2647	0.365777E 21	919.3	1194.1	922.7	932.2	824.7	-64.1
22	0.2651	0.368922E 21	921.9	1224.2	925.4	937.6	825.2	-63.4
23	0.2655	0.372033E 21	924.4	1254.5	928.0	943.2	825.7	-62.7
24	0.2659	0.375110E 21	926.7	1285.0	930.5	948.9	826.2	-62.0
25	0.2663	0.378163E 21	928.8	1315.7	932.9	954.6	826.7	-61.3
26	0.2667	0.381193E 21	930.8	1346.6	935.2	960.3	827.2	-60.6
27	0.2671	0.384200E 21	932.6	1377.7	937.4	966.0	827.7	-60.0
28	0.2675	0.387185E 21	934.3	1409.0	939.5	971.8	828.2	-59.3
29	0.2679	0.390148E 21	935.9	1440.5	941.5	977.6	828.7	-58.6
30	0.2683	0.393089E 21	937.4	1472.2	943.4	983.4	829.2	-57.9
31	0.2687	0.396008E 21	938.8	1504.1	945.2	989.1	829.7	-57.2
32	0.2691	0.398905E 21	940.1	1536.2	946.9	994.8	830.2	-56.5
33	0.2695	0.401780E 21	941.3	1568.5	948.5	1000.4	830.7	-55.8
34	0.2699	0.404633E 21	942.4	1601.0	949.9	1006.0	831.2	-55.1
35	0.2703	0.407464E 21	943.4	1633.7	951.2	1011.6	831.7	-54.4
36	0.2707	0.410273E 21	944.3	1666.6	952.4	1017.1	832.2	-53.7
37	0.2711	0.413060E 21	945.1	1699.7	953.5	1022.6	832.7	-53.0
38	0.2715	0.415825E 21	945.8	1733.0	954.5	1028.1	833.2	-52.3
39	0.2719	0.418568E 21	946.4	1766.5	955.4	1033.6	833.7	-51.6
40	0.2723	0.421289E 21	946.9	1800.2	956.2	1039.1	834.2	-50.9
41	0.2727	0.423988E 21	947.3	1834.1	956.9	1044.6	834.7	-50.2
42	0.2731	0.426665E 21	947.6	1868.2	957.5	1050.1	835.2	-49.5
43	0.2735	0.429320E 21	947.8	1902.5	958.0	1055.6	835.7	-48.8
44	0.2739	0.431953E 21	947.9	1937.0	958.4	1061.1	836.2	-48.1
45	0.2743	0.434564E 21	947.9	1971.7	958.7	1066.6	836.7	-47.4
46	0.2747	0.437153E 21	947.8	2006.6	958.9	1072.1	837.2	-46.7
47	0.2751	0.439720E 21	947.6	2041.7	959.0	1077.6	837.7	-46.0
48	0.2755	0.442265E 21	947.3	2077.0	959.0	1083.1	838.2	-45.3
49	0.2759	0.444788E 21	946.9	2112.5	958.9	1088.6	838.7	-44.6
50	0.2763	0.447289E 21	946.4	2148.2	958.7	1094.1	839.2	-43.9
51	0.2767	0.449768E 21	945.8	2184.1	958.4	1100.0	839.7	-43.2
52	0.2771	0.452225E 21	945.1	2220.2	958.0	1105.9	840.2	-42.5
53	0.2775	0.454660E 21	944.3	2256.5	957.5	1111.8	840.7	-41.8
54	0.2779	0.457073E 21	943.4	2293.0	956.9	1117.7	841.2	-41.1
55	0.2783	0.459464E 21	942.4	2329.7	956.2	1123.6	841.7	-40.4
56	0.2787	0.461833E 21	941.3	2366.6	955.4	1129.5	842.2	-39.7
57	0.2791	0.464180E 21	940.1	2403.7	954.5	1135.4	842.7	-39.0
58	0.2795	0.466505E 21	938.8	2441.0	953.5	1141.3	843.2	-38.3
59	0.2799	0.468808E 21	937.4	2478.5	952.4	1147.2	843.7	-37.6
60	0.2803	0.471089E 21	935.9	2516.2	951.2	1153.1	844.2	-36.9
61	0.2807	0.473348E 21	934.3	2554.1	949.9	1159.0	844.7	-36.2
62	0.2811	0.475585E 21	932.6	2592.2	948.5	1164.9	845.2	-35.5
63	0.2815	0.477800E 21	930.8	2630.5	947.0	1170.8	845.7	-34.8
64	0.2819	0.480093E 21	928.9	2669.0	945.4	1176.7	846.2	-34.1
65	0.2823	0.482364E 21	926.9	2707.7	943.7	1182.6	846.7	-33.4
66	0.2827	0.484613E 21	924.8	2746.6	941.9	1188.5	847.2	-32.7
67	0.2831	0.486840E 21	922.6	2785.7	940.0	1194.4	847.7	-32.0
68	0.2835	0.489045E 21	920.3	2825.0	937.9	1200.3	848.2	-31.3
69	0.2839	0.491228E 21	917.9	2864.5	935.7	1206.2	848.7	-30.6
70	0.2843	0.493389E 21	915.4	2904.2	933.4	1212.1	849.2	-29.9
71	0.2847	0.495528E 21	912.8	2944.1	931.0	1218.0	849.7	-29.2
72	0.2851	0.497645E 21	910.1	2984.2	928.5	1223.9	850.2	-28.5
73	0.2855	0.499740E 21	907.3	3024.5	925.9	1229.8	850.7	-27.8
74	0.2859	0.501813E 21	904.4	3065.0	923.2	1235.7	851.2	-27.1
75	0.2863	0.503864E 21	901.4	3105.7	920.4	1241.6	851.7	-26.4
76	0.2867	0.505893E 21	898.3	3146.6	917.5	1247.5	852.2	-25.7
77	0.2871	0.507900E 21	895.1	3187.7	914.5	1253.4	852.7	-25.0
78	0.2875	0.509885E 21	891.8	3229.0	911.4	1259.3	853.2	-24.3
79	0.2879	0.511848E 21	888.4	3270.5	908.2	1265.2	853.7	-23.6
80	0.2883	0.513789E 21	884.9	3312.2	904.9	1271.1	854.2	-22.9
81	0.2887	0.515708E 21	881.3	3354.1	901.5	1277.0	854.7	-22.2
82	0.2891	0.517605E 21	877.6	3396.2	898.0	1282.9	855.2	-21.5
83	0.2895	0.519480E 21	873.8	3438.5	894.4	1288.8	855.7	-20.8
84	0.2899	0.521333E 21	869.9	3481.0	890.7	1294.7	856.2	-20.1
85	0.2903	0.523164E 21	865.9	3523.7	886.9	1300.6	856.7	-19.4
86	0.2907	0.524973E 21	861.8	3566.6	883.0	1306.5	857.2	-18.7
87	0.2911	0.526760E 21	857.6	3609.7	879.0	1312.4	857.7	-18.0
88	0.2915	0.528525E 21	853.3	3653.0	874.9	1318.3	858.2	-17.3
89	0.2919	0.530268E 21	848.9	3696.5	870.7	1324.2	858.7	-16.6
90	0.2923	0.531989E 21	844.4	3740.2	866.4	1330.1	859.2	-15.9
91	0.2927	0.533688E 21	839.8	3784.1	862.0	1336.0	859.7	-15.2
92	0.2931	0.535365E 21	835.1	3828.2	857.5	1341.9	860.2	-14.5
93	0.2935	0.537020E 21	830.3	3872.5	852.9	1347.8	860.7	-13.8
94	0.2939	0.538653E 21	825.4	3917.0	848.2	1353.7	861.2	-13.1
95	0.2943	0.540264E 21	820.4	3961.7	843.4	1359.6	861.7	-12.4

Table 3. CONTINUED

23	0.2079	0.079419	22	692.9	749.2	768.0	837.7	891.0	-87.5
24	0.2079	0.080789	22	729.2	783.2	797.2	874.0	925.6	-71.8
25	0.2079	0.081316	22	766.0	808.0	819.9	893.3	943.0	-56.6
26	0.2079	0.081901	22	802.8	842.6	850.0	927.0	977.0	-48.0
27	0.2079	0.082539	22	839.6	879.6	885.0	960.7	1014.4	-35.0
28	0.2079	0.083234	22	876.4	916.4	920.0	993.6	1059.7	-20.4
29	0.2079	0.083989	22	913.2	953.2	955.0	1026.2	1104.2	-22.0
30	0.2079	0.084808	22	950.0	990.0	990.0	1058.0	1147.0	-19.3
31	0.2079	0.085695	22	986.8	1026.8	1025.0	1090.0	1189.0	-18.7
32	0.2079	0.086654	22	1023.6	1063.6	1060.0	1122.0	1230.0	-11.0
33	0.2079	0.087690	22	1060.4	1100.4	1095.0	1154.0	1270.0	-9.6
34	0.2079	0.088808	22	1097.2	1137.2	1130.0	1186.0	1310.0	-7.7
35	0.2079	0.089914	22	1134.0	1174.0	1165.0	1218.0	1350.0	-6.3
36	0.2079	0.091104	22	1170.8	1211.0	1200.0	1250.0	1390.0	-5.5
37	0.2079	0.092384	22	1207.6	1248.0	1235.0	1282.0	1430.0	-4.5
38	0.2079	0.093760	22	1244.4	1285.0	1270.0	1314.0	1470.0	-3.5
39	0.2079	0.095238	22	1281.2	1322.0	1305.0	1346.0	1510.0	-2.5
40	0.2079	0.096814	22	1318.0	1359.0	1340.0	1378.0	1550.0	-1.5
41	0.2079	0.098494	22	1354.8	1396.0	1375.0	1410.0	1590.0	-0.5
42	0.2079	0.100274	22	1391.6	1433.0	1410.0	1442.0	1630.0	0.5
43	0.2079	0.102160	22	1428.4	1470.0	1445.0	1474.0	1670.0	1.5
44	0.2079	0.104158	22	1465.2	1507.0	1480.0	1506.0	1710.0	2.5
45	0.2079	0.106274	22	1502.0	1544.0	1515.0	1538.0	1750.0	3.5
46	0.2079	0.108514	22	1538.8	1581.0	1550.0	1570.0	1790.0	4.5
47	0.2079	0.110884	22	1575.6	1618.0	1585.0	1602.0	1830.0	5.5
48	0.2079	0.113390	22	1612.4	1655.0	1620.0	1634.0	1870.0	6.5
49	0.2079	0.116038	22	1649.2	1692.0	1655.0	1666.0	1910.0	7.5
50	0.2079	0.118834	22	1686.0	1729.0	1690.0	1698.0	1950.0	8.5
51	0.2079	0.121784	22	1722.8	1766.0	1725.0	1730.0	1990.0	9.5
52	0.2079	0.124894	22	1759.6	1803.0	1760.0	1762.0	2030.0	10.5
53	0.2079	0.128170	22	1796.4	1840.0	1800.0	1794.0	2070.0	11.5
54	0.2079	0.131618	22	1833.2	1877.0	1840.0	1826.0	2110.0	12.5
55	0.2079	0.135244	22	1870.0	1914.0	1880.0	1858.0	2150.0	13.5
56	0.2079	0.139054	22	1906.8	1951.0	1920.0	1890.0	2190.0	14.5
57	0.2079	0.143054	22	1943.6	1988.0	1960.0	1922.0	2230.0	15.5
58	0.2079	0.147250	22	1980.4	2025.0	2000.0	1954.0	2270.0	16.5
59	0.2079	0.151658	22	2017.2	2062.0	2040.0	1986.0	2310.0	17.5
60	0.2079	0.156284	22	2054.0	2099.0	2080.0	2018.0	2350.0	18.5
61	0.2079	0.161134	22	2090.8	2136.0	2120.0	2050.0	2390.0	19.5
62	0.2079	0.166214	22	2127.6	2173.0	2160.0	2082.0	2430.0	20.5
63	0.2079	0.171530	22	2164.4	2210.0	2200.0	2114.0	2470.0	21.5
64	0.2079	0.177098	22	2201.2	2247.0	2240.0	2146.0	2510.0	22.5
65	0.2079	0.182934	22	2238.0	2284.0	2280.0	2178.0	2550.0	23.5
66	0.2079	0.189054	22	2274.8	2321.0	2320.0	2210.0	2590.0	24.5
67	0.2079	0.195474	22	2311.6	2358.0	2360.0	2242.0	2630.0	25.5
68	0.2079	0.202210	22	2348.4	2395.0	2400.0	2274.0	2670.0	26.5
69	0.2079	0.209278	22	2385.2	2432.0	2440.0	2306.0	2710.0	27.5
70	0.2079	0.216684	22	2422.0	2469.0	2480.0	2338.0	2750.0	28.5
71	0.2079	0.224434	22	2458.8	2506.0	2520.0	2370.0	2790.0	29.5
72	0.2079	0.232544	22	2495.6	2543.0	2560.0	2402.0	2830.0	30.5
73	0.2079	0.241020	22	2532.4	2580.0	2600.0	2434.0	2870.0	31.5
74	0.2079	0.249870	22	2569.2	2617.0	2640.0	2466.0	2910.0	32.5
75	0.2079	0.259100	22	2606.0	2654.0	2680.0	2498.0	2950.0	33.5
76	0.2079	0.268720	22	2642.8	2691.0	2720.0	2530.0	2990.0	34.5
77	0.2079	0.278740	22	2679.6	2728.0	2760.0	2562.0	3030.0	35.5
78	0.2079	0.289170	22	2716.4	2765.0	2800.0	2594.0	3070.0	36.5
79	0.2079	0.299920	22	2753.2	2802.0	2840.0	2626.0	3110.0	37.5
80	0.2079	0.311000	22	2790.0	2839.0	2880.0	2658.0	3150.0	38.5
81	0.2079	0.322420	22	2826.8	2876.0	2920.0	2690.0	3190.0	39.5
82	0.2079	0.334200	22	2863.6	2913.0	2960.0	2722.0	3230.0	40.5
83	0.2079	0.346350	22	2900.4	2950.0	3000.0	2754.0	3270.0	41.5
84	0.2079	0.358880	22	2937.2	2987.0	3040.0	2786.0	3310.0	42.5
85	0.2079	0.371800	22	2974.0	3024.0	3080.0	2818.0	3350.0	43.5
86	0.2079	0.385130	22	3010.8	3061.0	3120.0	2850.0	3390.0	44.5
87	0.2079	0.398880	22	3047.6	3098.0	3160.0	2882.0	3430.0	45.5
88	0.2079	0.413070	22	3084.4	3135.0	3200.0	2914.0	3470.0	46.5
89	0.2079	0.427720	22	3121.2	3172.0	3240.0	2946.0	3510.0	47.5
90	0.2079	0.442850	22	3158.0	3209.0	3280.0	2978.0	3550.0	48.5
91	0.2079	0.458480	22	3194.8	3246.0	3320.0	3010.0	3590.0	49.5
92	0.2079	0.474630	22	3231.6	3283.0	3360.0	3042.0	3630.0	50.5
93	0.2079	0.491320	22	3268.4	3320.0	3400.0	3074.0	3670.0	51.5
94	0.2079	0.508580	22	3305.2	3357.0	3440.0	3106.0	3710.0	52.5
95	0.2079	0.526440	22	3342.0	3394.0	3480.0	3138.0	3750.0	53.5
96	0.2079	0.544830	22	3378.8	3431.0	3520.0	3170.0	3790.0	54.5
97	0.2079	0.563780	22	3415.6	3468.0	3560.0	3202.0	3830.0	55.5
98	0.2079	0.583320	22	3452.4	3505.0	3600.0	3234.0	3870.0	56.5
99	0.2079	0.603480	22	3489.2	3542.0	3640.0	3266.0	3910.0	57.5
100	0.2079	0.624280	22	3526.0	3579.0	3680.0	3298.0	3950.0	58.5
101	0.2079	0.645750	22	3562.8	3616.0	3720.0	3330.0	3990.0	59.5
102	0.2079	0.667920	22	3599.6	3653.0	3760.0	3362.0	4030.0	60.5
103	0.2079	0.690830	22	3636.4	3690.0	3800.0	3394.0	4070.0	61.5
104	0.2079	0.714520	22	3673.2	3727.0	3840.0	3426.0	4110.0	62.5
105	0.2079	0.738940	22	3710.0	3764.0	3880.0	3458.0	4150.0	63.5
106	0.2079	0.764130	22	3746.8	3801.0	3920.0	3490.0	4190.0	64.5
107	0.2079	0.790140	22	3783.6	3838.0	3960.0	3522.0	4230.0	65.5
108	0.2079	0.816920	22	3820.4	3875.0	4000.0	3554.0	4270.0	66.5
109	0.2079	0.844500	22	3857.2	3912.0	4040.0	3586.0	4310.0	67.5
110	0.2079	0.872920	22	3894.0	3949.0	4080.0	3618.0	4350.0	68.5
111	0.2079	0.902230	22	3930.8	3986.0	4120.0	3650.0	4390.0	69.5
112	0.2079	0.932480	22	3967.6	4023.0	4160.0	3682.0	4430.0	70.5
113	0.2079	0.963720	22	4004.4	4060.0	4200.0	3714.0	4470.0	71.5
114	0.2079	0.996000	22	4041.2	4097.0	4240.0	3746.0	4510.0	72.5
115	0.2079	1.029380	22	4078.0	4134.0	4280.0	3778.0	4550.0	73.5
116	0.2079	1.063900	22	4114.8	4171.0	4320.0	3810.0	4590.0	74.5
117	0.2079	1.109600	22	4151.6	4208.0	4360.0	3842.0	4630.0	75.5
118	0.2079	1.156520	22	4188.4	4245.0	4400.0	3874.0	4670.0	76.5
119	0.2079	1.204700	22	4225.2	4282.0	4440.0	3906.0	4710.0	77.5
120	0.2079	1.254280	22	4262.0	4319.0	4480.0	3938.0	4750.0	78.5
121	0.2079	1.305300	22	4298.8	4356.0	4520.0	3970.0	4790.0	79.5

Table 3. CONTINUED

EXTRAPOLATION OF SELECTED ITERATE DATA WITH RICHARDSON'S CORRECTION FACTORS

37	-0.000006	-0.000100	-0.000100	-0.000001	1.3510	0.6722	-0.010024	1.1801	1.0021	0.0152	0.6257	0.0041
38	-0.000030	-0.000089	-0.000085	-0.000001	1.3510	0.6722	-0.010006	1.0717	0.9988	0.0273	1.1628	0.9110
39	-0.000009	-0.000078	-0.000078	-0.000001	1.3510	0.6723	-0.010033	1.0205	0.9924	0.0399	0.0561	0.0050
40	-0.000009	-0.000067	-0.000067	-0.000001	1.3510	0.6723	-0.010020	0.9857	0.9900	0.0135	0.0208	0.0004
41	-0.000009	-0.000057	-0.000057	-0.000000	1.3510	0.6723	-0.010030	0.9703	0.9877	0.0045	0.0065	0.0050
42	-0.000009	-0.000048	-0.000048	-0.000000	1.3510	0.6723	-0.010027	0.9622	0.9850	0.0046	0.0293	0.0021

PROCESSOR TIME (SEC) FOR 82 ITERATIONS 16.02 -- COEFFICIENTS 1.3510 0.6726 1.0010 1.0000
 ESTIMATED FRACTIONAL ABSOLUTE ERROR 1.93570E-03 FRACTIONAL CHANGE IN THE PRESSURE DROP 0.00007

SAMPLE PROBLEM, TWO DIMENSIONAL FRICTION AND THERMAL HYDRAULICS

TEMPERATURES ARBITRARILY ADJUSTED TO ELIMINATE THE HEAT BALANCE ERROR

ORF RADII AND HEIGHT (M)	0.1509	5.5000
THERMAL POWER (MW)	1856.01	
COOLANT MASS FLOW RATE (KG/S)	637.787	
INLET AVERAGE REYNOLDS NUMBER	21296.	
INLET COOLANT TEMPERATURE (K)	623.0	
HEAT EXCHANGER COOLANT TEMPERATURE (K)	1122.0	
HEAT EXCHANGER COOLANT TEMPERATURE (K)	1107.2	AT RADIAL LOCATION (M) 0.0
HEAT AND SIB FUEL SURFACE TEMPERATURES (K)	1191.7	492.9
INLET PRESSURE (ATM)	40.000	
OUTLET PRESSURE (ATM)	39.326	
PRESSURE DROP (ATM)	0.67230	
ERRORS IN FLOW AND HEAT BALANCE (PERCENT)	-0.000	-1.143
APPROXIMATE AXIAL PRESSURE CHANGE ACROSS CORE AT P/3 AND 2P/3 (ATM), --NO GRAVITY	-0.67369	-0.67369

MAXIMUM RADIAL COMPONENT OF THE RELATIVE MASS FLOW RATE (ABSOLUTE) 0.00603.

APPARENT EXTERNAL PRESSURE DROP (ATM) 0.67230

	RELATIVE MASS FLOW RATE, G												
RADIAL	0.0	0.0403	0.1606	0.2810	0.2739	0.2068	0.3398	0.3787	0.4096	0.4486	0.4795	0.5066	0.5337
0.0	0.9783	0.9787	0.9793	0.9802	0.9808	0.9814	0.9821	0.9830	0.9840	0.9852	0.9864	0.9875	0.9889
0.0278	0.9783	0.9787	0.9793	0.9802	0.9808	0.9814	0.9821	0.9830	0.9840	0.9852	0.9864	0.9875	0.9889
0.0556	0.9781	0.9785	0.9791	0.9800	0.9806	0.9812	0.9819	0.9827	0.9839	0.9850	0.9861	0.9872	0.9885
0.0833	0.9778	0.9783	0.9788	0.9797	0.9803	0.9810	0.9815	0.9823	0.9838	0.9849	0.9856	0.9866	0.9880
0.1111	0.9774	0.9779	0.9785	0.9793	0.9799	0.9806	0.9811	0.9818	0.9829	0.9839	0.9845	0.9850	0.9860
0.1389	0.9770	0.9775	0.9781	0.9789	0.9795	0.9802	0.9806	0.9813	0.9823	0.9835	0.9844	0.9853	0.9867
0.1667	0.9766	0.9771	0.9777	0.9785	0.9791	0.9797	0.9801	0.9807	0.9818	0.9829	0.9838	0.9846	0.9860
0.1944	0.9762	0.9767	0.9773	0.9781	0.9787	0.9793	0.9797	0.9803	0.9814	0.9825	0.9832	0.9840	0.9854
0.2222	0.9757	0.9763	0.9768	0.9776	0.9782	0.9788	0.9791	0.9797	0.9808	0.9819	0.9826	0.9834	0.9848
0.2500	0.9753	0.9758	0.9764	0.9772	0.9778	0.9784	0.9787	0.9793	0.9804	0.9815	0.9821	0.9829	0.9843
0.2778	0.9749	0.9754	0.9760	0.9768	0.9774	0.9780	0.9783	0.9789	0.9800	0.9811	0.9817	0.9824	0.9838
0.3056	0.9745	0.9750	0.9756	0.9764	0.9770	0.9776	0.9779	0.9785	0.9796	0.9807	0.9812	0.9819	0.9833
0.3333	0.9741	0.9746	0.9752	0.9760	0.9766	0.9772	0.9775	0.9781	0.9792	0.9803	0.9808	0.9815	0.9829
0.3611	0.9737	0.9742	0.9748	0.9756	0.9762	0.9768	0.9771	0.9777	0.9788	0.9799	0.9804	0.9811	0.9825
0.3889	0.9733	0.9738	0.9744	0.9752	0.9758	0.9764	0.9767	0.9773	0.9784	0.9795	0.9800	0.9807	0.9821
0.4167	0.9729	0.9734	0.9740	0.9748	0.9754	0.9760	0.9763	0.9769	0.9780	0.9791	0.9796	0.9803	0.9817
0.4444	0.9725	0.9730	0.9736	0.9744	0.9750	0.9756	0.9759	0.9765	0.9776	0.9787	0.9792	0.9799	0.9813
0.4722	0.9721	0.9726	0.9732	0.9740	0.9746	0.9752	0.9755	0.9761	0.9772	0.9783	0.9788	0.9795	0.9809
0.5000	0.9717	0.9722	0.9728	0.9736	0.9742	0.9748	0.9751	0.9757	0.9768	0.9779	0.9784	0.9791	0.9805
0.5278	0.9713	0.9718	0.9724	0.9732	0.9738	0.9744	0.9747	0.9753	0.9764	0.9775	0.9780	0.9787	0.9801
0.5556	0.9709	0.9714	0.9720	0.9728	0.9734	0.9740	0.9743	0.9749	0.9760	0.9771	0.9776	0.9783	0.9797
0.5833	0.9705	0.9710	0.9716	0.9724	0.9730	0.9736	0.9739	0.9745	0.9756	0.9767	0.9772	0.9779	0.9793
0.6111	0.9701	0.9706	0.9712	0.9720	0.9726	0.9732	0.9735	0.9741	0.9752	0.9763	0.9768	0.9775	0.9789
0.6389	0.9697	0.9702	0.9708	0.9716	0.9722	0.9728	0.9731	0.9737	0.9748	0.9759	0.9764	0.9771	0.9785
0.6667	0.9693	0.9698	0.9704	0.9712	0.9718	0.9724	0.9727	0.9733	0.9744	0.9755	0.9760	0.9767	0.9781
0.6944	0.9689	0.9694	0.9700	0.9708	0.9714	0.9720	0.9723	0.9729	0.9740	0.9751	0.9756	0.9763	0.9777
0.7222	0.9685	0.9690	0.9696	0.9704	0.9710	0.9716	0.9719	0.9725	0.9736	0.9747	0.9752	0.9759	0.9773
0.7500	0.9681	0.9686	0.9692	0.9700	0.9706	0.9712	0.9715	0.9721	0.9732	0.9743	0.9748	0.9755	0.9769
0.7778	0.9677	0.9682	0.9688	0.9696	0.9702	0.9708	0.9711	0.9717	0.9728	0.9739	0.9744	0.9751	0.9765
0.8056	0.9673	0.9678	0.9684	0.9692	0.9698	0.9704	0.9707	0.9713	0.9724	0.9735	0.9740	0.9747	0.9761
0.8333	0.9669	0.9674	0.9680	0.9688	0.9694	0.9700	0.9703	0.9709	0.9720	0.9731	0.9736	0.9743	0.9757
0.8611	0.9665	0.9670	0.9676	0.9684	0.9690	0.9696	0.9699	0.9705	0.9716	0.9727	0.9732	0.9739	0.9753
0.8889	0.9661	0.9666	0.9672	0.9680	0.9686	0.9692	0.9695	0.9701	0.9712	0.9723	0.9728	0.9735	0.9749
0.9167	0.9657	0.9662	0.9668	0.9676	0.9682	0.9688	0.9691	0.9697	0.9708	0.9719	0.9724	0.9731	0.9745
0.9444	0.9653	0.9658	0.9664	0.9672	0.9678	0.9684	0.9687	0.9693	0.9704	0.9715	0.9720	0.9727	0.9741

103	0.2705	0.751701R	22	816.0	826.7	829.0	880.0	850.7	-13.8
104	0.2709	0.757976R	22	823.2	831.8	837.9	882.0	851.0	-11.0
105	0.2713	0.762903R	22	829.0	835.0	837.6	884.4	851.3	-8.4
106	0.2716	0.767548R	23	833.7	839.2	840.6	885.0	851.5	-7.0
107	0.2719	0.771973R	23	837.5	842.0	843.1	887.0	851.0	-5.7
108	0.2722	0.776162R	23	840.7	844.5	845.5	889.2	851.1	-4.4
109	0.2724	0.780199R	21	843.1	846.5	847.8	891.5	850.4	-86.6
110	0.2726	0.784071R	21	845.0	849.0	850.5	894.9	850.4	-75.4
111	0.2728	0.787789R	22	846.3	851.0	852.0	898.5	850.0	-89.0
112	0.2729	0.791354R	22	847.0	851.4	852.0	902.2	850.0	-87.1
113	0.2730	0.794778R	22	847.5	851.7	852.0	906.0	850.0	-76.1
114	0.2731	0.798062R	22	848.0	851.9	852.0	909.9	850.0	-63.3
115	0.2732	0.801216R	22	848.5	852.0	852.0	914.0	850.0	-51.3
116	0.2733	0.804250R	22	849.0	852.0	852.0	918.2	850.0	-41.1
117	0.2734	0.807174R	22	849.5	852.0	852.0	922.5	850.0	-32.0
118	0.2735	0.810000R	22	849.5	852.0	852.0	926.9	850.0	-26.0
119	0.2736	0.812738R	22	849.5	852.0	852.0	931.4	850.0	-20.6
120	0.2737	0.815490R	22	849.5	852.0	852.0	936.0	850.0	-16.0

↑
SEVERAL
PAGES
DELETED

Table 3. CONTINUED

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---- FLOATING CONTROL VARIABLES ----
VOID FRACTION                                0.0
INLET TEMPERATURE (C)                       0.35000 03
INLET PRESSURE (ATM)                         0.00000 02
MASS FLOW RATE (KG/S)                        0.0
CHARACTERISTIC HYDRAULIC DIAMETER (CM)      0.00000 01
RECOVERABLE FLUX                             0.0
RECOVERABLE ENERGY FRACTION                 0.00000 00
SPECIFIED POWER LEVEL                         0.0
DIAMETER OF CELL FOR HEAT REMOVAL (CM)      0.0
FUEL RADIUS OF BOMB MATERIAL (CM)            0.25000 01
FUEL RADIUS OF SURROUND MATERIAL (CM)        0.25000 01
OUTLET TEMPERATURE (C)                      0.05000 02
FLOWSPEC MULTIPLIER                          0.0
THERMAL CONDUCTIVITY MULTIPLIER              0.0
CONVERGENCE CRITERIA                         0.0

MAXIMUM CPU TIME IN SECONDS                  0.15000 07

0.0      0.0      0.0      0.0      0.0
0.0      0.0      0.0      0.0      1.50000 01

MAXIMUM MEMORY REQUIREMENT -- 40959 WORDS, MEMORY AVAILABLE -- 160000 WORDS
POWER OF EXPOND - 0.16397 10 DOES NOT MATCH PREDICTED - 0.14000 10
TIME OF EXPOND - 0.20372 05 DOES NOT MATCH PREDICTED - 0.0

DATA UNIT NUMBERS, GEOMETRY, EXPOSURE, SCHE AND POWER POWER DENSITY 10 20 30 40
PROBLEM MESH (IN)      1      20      11      16      0.0      015.00      200.17      750.20
THE ENDS OF THE VARIABLY DIMENSIONED DATA BLOCKS      5015      6001      31020      03277

DATA ARRAY STORAGE REQUIREMENT      0.0271
LOGICAL VOID FRACTION, MAXIMUM AND MINIMUM 0.00000 0.00000 0.00000

MAXIMUM POWER DENSITY (W/CC) LOCATION - RADIUS / SPFH PFCR 707 (IN)
-----
10.061                                0.723 / 0.050

GOALS DEL P (ATM) 0.27110-01 AT DENSITY 1.98510 00 VOLUME 2.97500 00, MASS FLOW (KG/S) 0.27700 02 POWER 1.65400 00
MAXIMUM INITIALIZED MESH FLUX AND FUEL TEMPERATURES (K) 1200.02 1200.30 APPARENT PRESSURE 0.00000 00 (ATM) 0.6710

INITIALIZATION OF PROBLEM COMPLETE, START ITERATION ..... CONVERGENCE DATA FOLLOWS
PROCESSOR TIME (SEC) AT START OF ITERATION      0.02 --COEFFICIENTS 1.3032 0.2022 1.0030 1.0532 MAX IT 170

ITERATION, BALANCE CHANGE (PSI), BULK TEMP, SURF TEMP, PRESSURE, BETA IN, APPARENT DENS, DEL P, BALANCE, *NO (PSI)
1 -0.002688 0.000688 0.000117 0.001246 1.1516 0.7225 -0.000137 0.0000 0.0000 0.1322 0.0476 0.3382
2 -0.001639 1.070492 -0.001730 0.000551 1.1516 0.6723 -0.000067 0.0000 0.0000 0.1322 0.0476 0.3382
3 0.001235 0.001258 0.001720 0.000447 1.3032 0.6723 -0.000106 0.0000 0.0000 2.2048 0.7023 1.1053
4 0.001005 0.000972 0.001331 0.000320 1.3032 0.6723 -0.000106 0.0000 0.0000 0.0000 0.0000 0.0000
5 0.000967 0.002785 0.002720 0.000220 1.3032 0.6725 -0.0002213 0.0000 0.0000 0.0000 0.0000 0.0000
6 0.000611 0.001931 0.001400 0.000166 1.3032 0.6726 -0.000190 0.0000 0.0000 0.0000 0.0000 0.0000
7 0.000782 0.001670 0.001410 0.000113 1.3032 0.6727 -0.000200 0.0000 0.0000 0.0000 0.0000 0.0000
8 0.000770 0.001888 0.001430 0.000073 1.3032 0.6729 -0.000305 0.0000 0.0000 0.0000 0.0000 0.0000
9 0.000655 0.001309 0.001240 0.000053 1.3032 0.6729 -0.000330 0.0000 0.0000 0.0000 0.0000 0.0000
10 0.000600 0.001170 0.001163 0.000041 1.3032 0.6730 -0.000040 0.0000 0.0000 0.0000 0.0000 0.0000
11 0.000560 0.001100 0.001071 0.000031 1.3032 0.6730 -0.000013 0.0000 0.0000 0.0000 0.0000 0.0000
12 0.000560 0.001050 0.001010 0.000022 1.3032 0.6731 -0.000005 0.0000 0.0000 0.0000 0.0000 0.0000
13 0.000539 0.001006 0.000971 0.000019 1.3032 0.6732 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
14 0.000510 0.000960 0.000930 0.000010 1.3032 0.6733 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
15 0.000490 0.000917 0.000891 0.000009 1.3032 0.6733 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
16 0.000460 0.000875 0.000846 0.000008 1.3032 0.6733 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
17 0.000460 0.000850 0.000832 0.000007 1.3032 0.6733 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000

EXTRAPOLATION OF SELECTED ITERATE DATA WITH FITTING COEFFICIENTS OF 7TH ORDER
18 0.001995 0.004730 0.006760 0.007040 1.3532 0.6740 -0.016100 2.4571 1.1302 5.5075 1.2120 1.4650
19 0.001023 0.004200 0.006100 0.006072 1.3532 0.6740 -0.010000 0.0000 0.0000 0.0000 0.0000 0.0000
20 0.000943 0.003800 0.005710 0.005027 1.3532 0.6740 -0.008000 0.0000 0.0000 0.0000 0.0000 0.0000
21 0.000802 0.003417 0.005340 0.004023 1.3532 0.6740 -0.007110 0.0000 0.0000 0.0000 0.0000 0.0000
22 0.000660 0.003070 0.005010 0.003000 1.3532 0.6740 -0.006100 0.0000 0.0000 0.0000 0.0000 0.0000
23 0.000500 0.002777 0.004727 0.002000 1.3532 0.6740 -0.005100 0.0000 0.0000 0.0000 0.0000 0.0000
24 0.000350 0.002500 0.004460 0.001000 1.3532 0.6740 -0.004100 0.0000 0.0000 0.0000 0.0000 0.0000
25 0.000200 0.002250 0.004220 0.000000 1.3532 0.6740 -0.003100 0.0000 0.0000 0.0000 0.0000 0.0000
26 -0.000022 0.002000 0.004010 0.000000 1.3532 0.6739 -0.002100 0.0000 0.0000 0.0000 0.0000 0.0000
27 -0.000066 0.001800 0.003810 0.000000 1.3532 0.6739 -0.001200 0.0000 0.0000 0.0000 0.0000 0.0000
28 -0.000000 0.001650 0.003630 0.000000 1.3103 0.6738 -0.000200 0.0000 0.0000 0.0000 0.0000 0.0000
29 -0.000011 0.001500 0.003460 0.000000 1.3103 0.6738 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
30 -0.000001 0.001330 0.003310 0.000000 1.3103 0.6738 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
31 0.000000 0.001170 0.003170 0.000000 1.3103 0.6738 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
32 0.000000 0.001000 0.003050 0.000000 1.3103 0.6739 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
33 0.000000 0.000830 0.002950 0.000000 1.3103 0.6740 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
34 0.000000 0.000670 0.002870 0.000000 1.3103 0.6740 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
35 0.000000 0.000510 0.002800 0.000000 1.3103 0.6740 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
36 0.000000 0.000350 0.002700 0.000000 1.3103 0.6740 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
37 0.000000 0.000200 0.002600 0.000000 1.3103 0.6740 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
38 0.000000 0.000000 0.002500 0.000000 1.3103 0.6740 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
39 0.000000 0.000000 0.002400 0.000000 1.3103 0.6740 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
40 0.000000 0.000000 0.002300 0.000000 1.3103 0.6740 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
41 0.000000 0.000000 0.002200 0.000000 1.3103 0.6740 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
42 0.000000 0.000000 0.002100 0.000000 1.3103 0.6740 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
43 0.000000 0.000000 0.002000 0.000000 1.3103 0.6740 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
44 0.000000 0.000000 0.001900 0.000000 1.3103 0.6740 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000
45 0.000000 0.000000 0.001800 0.000000 1.3103 0.6740 -0.000000 0.0000 0.0000 0.0000 0.0000 0.0000

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Table 3. CONTINUED

46	0.000202	-0.001225	-0.001215	-0.000034	1.2264	0.6750	-0.005910	0.4787	0.4579	0.4230	0.9567	0.9403
47	0.000198	-0.001220	-0.001218	-0.000038	1.2264	0.6750	-0.006573	0.4793	0.4579	0.4095	0.9569	0.9366
48	0.000192	-0.001212	-0.001207	-0.000037	1.2264	0.6750	-0.007262	0.4797	0.4579	0.4073	0.9569	0.9323
49	0.000190	-0.001174	-0.001175	-0.000037	1.2264	0.6750	-0.007959	0.4798	0.4579	0.4063	0.9574	0.9286
50	0.000197	-0.001088	-0.001088	-0.000037	1.2264	0.6750	-0.008646	0.4812	0.4584	0.4045	0.9571	0.9260
51	0.000195	-0.001076	-0.001077	-0.000037	1.2264	0.6750	-0.009333	0.4817	0.4584	0.4033	0.9572	0.9248
52	0.000182	-0.001070	-0.001070	-0.000037	1.2264	0.6750	-0.010020	0.4827	0.4589	0.4013	0.9568	0.9240
53	0.000179	-0.001078	-0.001078	-0.000037	1.2264	0.6750	-0.010707	0.4838	0.4590	0.4006	0.9570	0.9233
54	0.000178	-0.001076	-0.001076	-0.000037	1.2264	0.6750	-0.011394	0.4848	0.4590	0.4006	0.9571	0.9255

EXTRAPOLATION OF SELECTED ITERATE DATA WITH EIGENVALUE 0.92378 FACTOR, 1E-74 6.0E 22.3E LEVEL 0

55	0.000537	0.000007	0.000794	0.000001	1.3028	0.6753	-0.010037	3.0285	0.7515	0.7481	0.8900	0.9467
56	0.000462	-0.001097	-0.001091	-0.000001	1.3028	0.6753	-0.010166	0.9603	0.9087	0.8582	0.9589	0.9012
57	0.000381	0.001093	0.001072	0.000001	1.3028	0.6753	-0.009888	0.7281	0.9809	0.8815	0.8924	0.9359
58	0.000348	-0.001394	-0.001385	0.000001	1.3028	0.6754	-0.009797	1.2381	0.9584	0.9024	0.8895	0.9544
59	0.000347	0.001827	0.001826	0.000001	1.3028	0.6754	-0.009617	0.7819	0.9667	0.8713	0.8054	0.9734
60	0.000343	-0.001782	-0.001774	0.000001	1.3028	0.6754	-0.009570	1.4222	0.9790	0.8614	0.9758	0.9415
61	0.000348	0.001891	0.001876	0.000001	1.3028	0.6754	-0.009577	0.6483	0.9872	0.8057	0.9386	0.9862
62	0.000348	-0.001852	-0.001848	0.000001	1.3028	0.6754	-0.009506	1.2671	0.9810	0.7826	0.9850	0.9560
63	0.000353	0.001312	0.001302	-0.000001	1.3028	0.6754	-0.009577	0.6484	0.9804	0.8073	0.9631	0.9888
64	0.000347	-0.001804	-0.001805	0.000001	1.3028	0.6754	-0.009570	1.0988	0.9019	0.9453	0.9715	0.9710
65	0.000345	0.000721	0.000715	0.000000	1.3028	0.6754	-0.009649	0.6487	0.9722	0.8962	0.9822	0.9163
66	0.000348	-0.000674	-0.000674	0.000000	1.3028	0.6754	-0.009724	0.9200	0.9311	0.9487	0.9821	0.9285
67	0.000345	0.000389	0.000384	0.000000	1.3028	0.6754	-0.009727	0.7174	0.9839	0.8884	0.8854	0.9704
68	0.000346	-0.000361	-0.000359	0.000000	1.3028	0.6754	-0.009768	0.9172	0.9822	0.9487	0.9832	0.9323
69	0.000342	0.000204	0.000202	0.000000	1.3028	0.6754	-0.009776	0.7164	0.9872	0.9024	0.9853	0.9343
70	0.000348	-0.000214	-0.000214	0.000000	1.3028	0.6754	-0.009787	0.9097	0.9872	0.9484	0.9839	0.9356
71	0.000348	0.000183	0.000182	0.000000	1.3028	0.6754	-0.009778	0.9097	0.9888	0.9112	0.9852	0.9383
72	0.000348	-0.000111	-0.000110	0.000000	1.3028	0.6754	-0.009782	0.9175	0.9887	0.9485	0.9855	0.9787
73	0.000348	0.000054	0.000054	0.000000	1.3028	0.6754	-0.009735	0.9480	0.9511	0.9481	0.9855	0.9489
74	0.000348	-0.000000	-0.000000	0.000000	1.3028	0.6754	-0.009735	0.9262	0.9511	0.9422	0.9856	0.9406
75	0.000346	0.000042	0.000042	0.000000	1.3028	0.6754	-0.009710	0.9875	0.9523	0.9214	0.9850	0.9417

EXTRAPOLATION OF SELECTED ITERATE DATA WITH EIGENVALUE 0.98077 FACTOR, 1E-77 7.4E 3.0 LEVEL 0

76	-0.000197	-0.000618	-0.000613	0.000000	1.3028	0.6754	-0.009720	1.4987	0.8348	1.0359	1.0140	0.7988
77	-0.000113	0.000477	0.000478	0.000000	1.3028	0.6754	-0.009692	0.4783	0.9677	0.9173	0.9864	0.7743
78	0.000045	-0.000335	-0.000333	0.000000	1.3028	0.6754	-0.009770	0.4728	0.9032	0.8847	0.7785	0.8422
79	-0.000052	0.000275	0.000273	0.000000	1.3028	0.6754	-0.009690	0.9568	0.9194	0.9136	0.9719	0.9854
80	0.000033	-0.000190	-0.000189	0.000000	1.3028	0.6754	-0.009686	0.6317	0.9709	0.8745	0.8602	0.9096
81	-0.000028	0.000160	0.000159	0.000000	1.3028	0.6754	-0.009686	0.8384	0.9887	0.9126	0.9817	0.9782
82	0.000018	-0.000092	-0.000091	0.000000	1.3028	0.6754	-0.009687	0.4324	0.9887	0.8671	0.8613	0.9163
83	-0.000018	0.000092	0.000091	0.000000	1.3028	0.6754	-0.009681	0.7948	0.9561	0.9082	0.9027	0.9182
84	0.000010	-0.000050	-0.000050	0.000000	1.3028	0.6754	-0.009682	0.7174	0.9511	0.8639	0.8628	0.9185
85	0.000008	0.000055	0.000055	0.000000	1.3028	0.6754	-0.009689	0.7726	0.9417	0.8647	0.8634	0.9195
86	0.000007	0.000030	0.000030	0.000000	1.3028	0.6754	-0.009681	0.9537	0.9617	0.8498	0.8633	0.9219

PROCESSOR TIME (SEC) FOR 86 ITERATIONS 6.96 --COEFFICIENTS 1.3028 0.2798 1.9999 1.5747
 ESTIMATED FRACTIONAL ABSOLUTE ERROR 3.19728E-08 RELATIVE CHANGE IN THE PRESSURE DROP 0.00000

SAMPLE PROBLEM, TWO DIMENSIONAL PARTLY BAD THERMAL HYDRAULICS
 TEMPERATURES ARBITRARILY ADJUSTED TO ELIMINATE THE HEAT BALANCE ERRORS

BED RADII AND HEIGHT (M) 0.1500 5.5000
 THERMAL POWER (MW) 1656.01
 COOLANT MASS FLOW RATE (KG/S) 637.787
 INLET AVERAGE REYNOLDS NUMBER 21294.
 INLET COOLANT TEMPERATURE (K) 223.0
 HEAT OUTLET COOLANT TEMPERATURE (K) 1123.0
 PEAK OUTLET COOLANT TEMPERATURE (K) 1187.5 AT RADIAL LOCATION (M) 0.0
 MAX AND MIN PEAK SURFACE TEMPERATURES (K) 1192.0 692.9
 INLET PRESSURE (ATM) 80.000
 OUTLET PRESSURE (ATM) 79.324
 PRESSURE DROP (ATM) 0.67545
 ERRORS IN FLOW AND HEAT BALANCE (PERCENT) 0.0 -0.968
 APPROXIMATE AXIAL PRESSURE CHANGE ACROSS CORE AT 0/3 AND 2R/3 (ATM), --5G GRAVITY -0.67797 -0.67826

RAIHER RADIAL COMPONENT OF THE RELATIVE MASS FLOW RATE (ABSOLUTE) 0.00508
 APPARENT EXTREME PRESSURE DROP (ATM) 0.47545

AXIAL COMPONENT OF RELATIVE MASS FLOW RATE, 02

RADIAL	0.0	0.0803	0.1606	0.2410	0.2734	0.3068	0.3398	0.3787	0.4096	0.4484	0.4795	0.5066	0.5337
AXIAL													
0.0	0.9781	0.9785	0.9791	0.9800	0.9806	0.9812	0.9819	0.9824	0.9830	0.9836	0.9843	0.9848	0.9857
0.0278	0.9781	0.9785	0.9791	0.9800	0.9806	0.9812	0.9819	0.9824	0.9830	0.9836	0.9843	0.9848	0.9857
0.0556	0.9779	0.9788	0.9789	0.9794	0.9800	0.9811	0.9817	0.9825	0.9834	0.9840	0.9849	0.9850	0.9868
0.0833	0.9776	0.9781	0.9787	0.9795	0.9801	0.9808	0.9818	0.9821	0.9832	0.9838	0.9845	0.9855	0.9874
0.1111	0.9772	0.9777	0.9783	0.9792	0.9798	0.9808	0.9818	0.9827	0.9839	0.9849	0.9859	0.9868	0.9887
0.1389	0.9769	0.9773	0.9779	0.9787	0.9794	0.9800	0.9806	0.9811	0.9822	0.9827	0.9833	0.9842	0.9866
0.1667	0.9768	0.9769	0.9775	0.9783	0.9789	0.9796	0.9800	0.9807	0.9816	0.9822	0.9826	0.9835	0.9859
0.1944	0.9759	0.9765	0.9770	0.9779	0.9785	0.9791	0.9794	0.9800	0.9811	0.9822	0.9831	0.9839	0.9853
0.2222	0.9755	0.9760	0.9766	0.9774	0.9780	0.9786	0.9789	0.9795	0.9806	0.9817	0.9825	0.9833	0.9847
0.2500	0.9751	0.9756	0.9762	0.9770	0.9776	0.9782	0.9785	0.9790	0.9801	0.9812	0.9820	0.9828	0.9842
0.2778	0.9746	0.9752	0.9758	0.9766	0.9772	0.9778	0.9780	0.9786	0.9796	0.9806	0.9815	0.9823	0.9837
0.3056	0.9742	0.9748	0.9754	0.9762	0.9768	0.9774	0.9776	0.9781	0.9791	0.9801	0.9810	0.9818	0.9832
0.3333	0.9738	0.9744	0.9750	0.9758	0.9764	0.9769	0.9772	0.9777	0.9787	0.9797	0.9806	0.9814	0.9828
0.3611	0.9735	0.9741	0.9746	0.9754	0.9760	0.9765	0.9768	0.9773	0.9783	0.9793	0.9802	0.9810	0.9824
0.3889	0.9731	0.9736	0.9742	0.9750	0.9756	0.9762	0.9764	0.9769	0.9779	0.9789	0.9798	0.9807	0.9821
0.4167	0.9728	0.9733	0.9739	0.9747	0.9753	0.9758	0.9761	0.9766	0.9776	0.9787	0.9795	0.9804	0.9818

Table 3. CONTINUED

0.4434	0.9724	0.9730	0.9736	0.9740	0.9746	0.9752	0.9758	0.9763	0.9773	0.9784	0.9792	0.9801	0.9815
0.4722	0.9721	0.9727	0.9733	0.9741	0.9747	0.9752	0.9755	0.9760	0.9770	0.9781	0.9789	0.9799	0.9812
0.5000	0.9719	0.9724	0.9730	0.9738	0.9744	0.9749	0.9752	0.9757	0.9767	0.9778	0.9787	0.9796	0.9810
0.5278	0.9716	0.9721	0.9727	0.9734	0.9741	0.9746	0.9749	0.9755	0.9764	0.9775	0.9784	0.9794	0.9807
0.5556	0.9713	0.9718	0.9725	0.9733	0.9740	0.9745	0.9747	0.9752	0.9762	0.9773	0.9782	0.9792	0.9805
0.5833	0.9711	0.9716	0.9722	0.9731	0.9736	0.9741	0.9745	0.9750	0.9760	0.9771	0.9780	0.9790	0.9803
0.6111	0.9709	0.9714	0.9720	0.9729	0.9734	0.9739	0.9742	0.9748	0.9758	0.9769	0.9778	0.9788	0.9801
0.6389	0.9706	0.9712	0.9718	0.9727	0.9732	0.9737	0.9740	0.9746	0.9756	0.9767	0.9777	0.9786	0.9800
0.6667	0.9705	0.9710	0.9716	0.9725	0.9730	0.9735	0.9739	0.9745	0.9755	0.9766	0.9775	0.9785	0.9799
0.6944	0.9702	0.9708	0.9714	0.9723	0.9728	0.9733	0.9737	0.9743	0.9753	0.9764	0.9774	0.9784	0.9798
0.7222	0.9701	0.9706	0.9712	0.9721	0.9726	0.9731	0.9735	0.9741	0.9751	0.9762	0.9773	0.9783	0.9796
0.7500	0.9700	0.9705	0.9711	0.9720	0.9725	0.9730	0.9734	0.9740	0.9750	0.9761	0.9771	0.9782	0.9795
0.7778	0.9698	0.9703	0.9710	0.9719	0.9724	0.9729	0.9733	0.9739	0.9749	0.9760	0.9770	0.9781	0.9795
0.8056	0.9697	0.9702	0.9709	0.9717	0.9722	0.9727	0.9732	0.9738	0.9748	0.9759	0.9770	0.9780	0.9794
0.8333	0.9696	0.9701	0.9707	0.9716	0.9721	0.9726	0.9731	0.9737	0.9747	0.9758	0.9769	0.9779	0.9793
0.8611	0.9695	0.9700	0.9707	0.9715	0.9720	0.9725	0.9730	0.9737	0.9747	0.9758	0.9769	0.9779	0.9793
0.8889	0.9694	0.9699	0.9706	0.9715	0.9720	0.9725	0.9730	0.9737	0.9747	0.9758	0.9769	0.9779	0.9793
0.9167	0.9693	0.9698	0.9705	0.9714	0.9719	0.9724	0.9729	0.9736	0.9746	0.9757	0.9768	0.9778	0.9792
0.9444	0.9693	0.9698	0.9705	0.9713	0.9718	0.9723	0.9728	0.9735	0.9745	0.9756	0.9767	0.9777	0.9791

105	0.2785	0.2791528	22	816.1	826.5	829.1	835.8	850.5	-75.8
106	0.2789	0.2845182	22	823.5	831.6	833.7	832.2	850.8	-11.0
105	0.2793	0.2804774	22	829.2	835.7	837.4	844.2	851.1	-8.8
106	0.2796	0.2860382	22	833.8	839.0	840.4	845.8	851.3	-7.0
107	0.2796	0.2872882	22	837.5	841.7	842.8	847.2	851.4	-5.7
108	0.2798	0.2896182	22	840.6	844.5	845.4	849.2	851.6	-4.9
109	0.5380	0.1819878	21	392.2	471.2	480.1	516.2	553.6	-66.6
110	0.3728	0.6760032	21	853.7	537.6	552.2	610.5	664.9	-75.7
111	0.3136	0.1325698	22	519.5	598.8	612.2	681.2	756.6	-89.7
112	0.2908	0.2811548	22	571.3	646.1	657.0	723.8	790.4	-87.0
113	0.2813	0.2658898	22	618.7	675.6	686.4	748.8	806.7	-76.1
114	0.2768	0.3286878	22	657.6	703.6	715.9	769.4	812.4	-63.3
115	0.2786	0.3286338	22	699.0	725.7	735.7	775.1	818.1	-51.3
116	0.2735	0.4306078	22	718.2	763.4	751.4	783.0	818.3	-61.1
117	0.2728	0.4823738	22	738.3	757.6	763.9	788.0	818.0	-32.8
118	0.2725	0.5398538	22	750.4	768.9	773.9	793.8	813.4	-36.0
119	0.2723	0.6106352	22	763.3	778.4	782.0	797.0	813.7	-20.4
120	0.2722	0.7232248	22	773.6	784.4	788.5	801.1	813.8	-16.4
121	0.2721	0.7301382	22	781.9	791.3	793.0	803.4	813.9	-13.0
122	0.2725	0.7356662	22	788.6	796.1	798.1	806.1	814.3	-10.4
123	0.2729	0.1049182	23	794.1	800.1	807.6	808.0	814.5	-8.2
124	0.2728	0.1052712	23	798.4	803.2	808.5	809.6	814.8	-6.4
125	0.2731	0.1055512	23	802.0	805.9	806.9	811.0	815.4	-5.1
126	0.2731	0.1057632	23	805.1	808.5	808.4	812.8	816.8	-4.1
127	0.5630	0.1881982	21	394.5	477.0	485.7	521.3	558.2	-65.9
128	0.4014	0.5331432	21	456.5	540.2	553.5	607.1	661.7	-69.8
129	0.3371	0.1007942	22	515.3	593.0	608.5	670.1	732.4	-80.0
130	0.3090	0.1474972	22	568.0	633.7	648.6	707.7	766.4	-76.9
131	0.2953	0.1882422	22	612.3	665.0	677.9	724.3	780.5	-66.9
132	0.2879	0.2220912	22	647.3	689.2	699.9	742.5	788.4	-55.4
133	0.2836	0.2497672	22	675.1	704.2	716.9	751.3	785.4	-48.4
134	0.2809	0.2725122	22	697.1	723.2	736.1	757.7	785.2	-35.4
135	0.2791	0.2913552	22	713.5	735.1	748.7	762.6	784.6	-28.6
136	0.2774	0.3070962	22	728.4	744.6	749.1	768.6	788.0	-22.8
137	0.2770	0.3203392	22	734.4	752.3	755.0	769.4	783.7	-18.1
138	0.2764	0.3315432	22	740.2	754.5	761.3	772.4	783.4	-14.5
139	0.2760	0.3410572	22	745.3	755.7	763.5	774.6	783.4	-11.5
140	0.2756	0.3594962	22	751.5	761.1	769.0	774.4	784.0	-9.2
141	0.2754	0.3598002	22	767.0	772.2	773.6	779.3	784.4	-7.3
142	0.2752	0.3679362	22	771.5	774.7	776.8	781.3	785.4	-5.8
143	0.2750	0.3751852	22	775.3	778.6	779.5	783.0	786.6	-4.6
144	0.2749	0.3832122	22	778.4	781.3	782.0	785.0	787.4	-3.8
145	0.0	0.0		850.0	350.0	304.0	304.0	304.0	0.0
146	0.0	0.0		850.0	350.0	304.0	304.0	304.0	0.0
147	0.0	0.0		850.0	350.0	304.0	304.0	304.0	0.0
148	0.0	0.0		850.0	350.0	304.0	304.0	304.0	0.0
149	0.0	0.0		850.0	350.0	304.0	304.0	304.0	0.0
150	0.0	0.0		850.0	350.0	304.0	304.0	304.0	0.0
151	0.0	0.0		850.0	350.0	304.0	304.0	304.0	0.0
152	0.0	0.0		850.0	350.0	304.0	304.0	304.0	0.0
153	0.0	0.0		850.0	350.0	304.0	304.0	304.0	0.0
154	0.0	0.0		850.0	350.0	304.0	304.0	304.0	0.0
155	0.0	0.0		850.0	350.0	304.0	304.0	304.0	0.0

↑ SEVERAL PAGES DELETED

DISTRIBUTION FRACTIONS OF 100 WTAT TEMPERATURES IN TUBETT FRACTIONS OVER THE RANGE (C) 350.0 922.0
 0.0 0.0 0.0 0.0 0.0 0.0 0.01389 0.01389 0.02278 0.00694 0.01389
 0.00694 0.03072 0.02003 0.04167 0.11111 0.11111 0.11806 0.15278 0.18056 0.14581

ZONE AVERAGE TEMP AND T002, TREN LOCUSSES 804.78 709.79 0.0 0.0

MAX TEMPS, PEAK/NEAR BY ZONE, SURFACES 927.2 922.0 0.0 0.0 (ZONE WEIGHTED) 740.1 0.0 0000 (WT) 1650.

AVERAGE AND PEAK TEMPERATURE SLOPE AT PIPBLE WTAT/SHELL INTERFACES (C/CM) -81.5 -116.0

CORRELATION FAILURE COUNT 0 0

TOTAL CPU TIME IS 0.071 MINUTES AND TOTAL CLOCK TIME IS 6.413 MINUTES FOR PIPBLE CODE EXECUTION

Table 3. CONTINUED

THERMAL HYDRAULIC DATA APPARS PROCEEDED FROM UNIT 31 ← SPECIAL ACTION

RAIUS INITIALIzed OVER FLOW AND PRESSURE TEMPERATURES (°F) 1101.12 1101.61 APPARENT PRESSURE DROP (ATM) 0.6760

INITIALIZATION OF PROGRAM COMPLETE, START ITERATION CONVERGENCE DATA FOLLOWS

PROCESSOR TIME (SEC) AT START OF ITERATION 0.29 --COEFFICIENTS 1.3510 0.6796 1.0000 1.0171 END IT 170

ITERATION	RAIUS CHANGE (PSI)	DIFF. TEMP. (°F)	DIFF. TEMP. (°C)	DIFF. TEMP. (°F)	DIFF. TEMP. (°C)	DIFF. TEMP. (°F)	DIFF. TEMP. (°C)	DIFF. TEMP. (°F)	DIFF. TEMP. (°C)	DIFF. TEMP. (°F)	DIFF. TEMP. (°C)	DIFF. TEMP. (°F)	DIFF. TEMP. (°C)
1	-0.000015	0.000000	0.000000	0.000000	1.1755	0.6760	-0.011700	0.6796	0.0000	0.0000	0.0000	0.0000	0.0000
2	-0.000013	0.000000	0.000000	0.000000	1.1744	0.6760	-0.011700	0.6796	0.0000	0.0000	0.0000	0.0000	0.0000
3	-0.000015	0.000000	0.000000	0.000000	1.1750	0.6760	-0.011700	0.6796	1.0000	1.1700	2.2000	0.9010	1.1971
4	-0.000015	0.000000	0.000000	0.000000	1.1750	0.6759	-0.011700	0.6796	1.0000	1.0000	0.9730	0.9357	1.2069
5	-0.000015	0.000000	0.000000	0.000000	1.1750	0.6759	-0.011700	0.6796	0.9000	0.9000	2.3776	0.9337	1.2023

PROCESSOR TIME (SEC) FOR 5 ITERATIONS 3.62 --COEFFICIENTS 1.3510 0.6796 1.0000 1.0171

ESTIMATED FRACTIONAL ABSOLUTE ERROR 6.5910E-04 RELATIVE CHANGE IN THE PRESSURE DROP -0.0002

SAMPLE PROBLEM, TWO DIMENSIONAL FLOW AND THERMAL HYDRAULICS

TEMPERATURES ARBITRARILY ADJUSTED TO ELIMINATE THE STAT. BALANCE ERROR

END RADIUS AND HEIGHT (IN) 4.1500 5.5000

THERMAL POWER (MW) 1656.01

COOLANT MASS FLOW RATE (KG/S) 637.787

INLET AVERAGE REYNOLDS NUMBER 21206.

INLET COOLANT TEMPERATURE (K) 623.0

HEAT OUTLET COOLANT TEMPERATURE (K) 712.0

PEAK OUTLET COOLANT TEMPERATURE (K) 118.0 AT RADIAL LOCATION (IN) 0.0

MAX AND MIN PEBBLE SURFACE TEMPERATURES (K) 1101.5 652.9

INLET PRESSURE (ATM) 00.000

OUTLET PRESSURE (ATM) 39.326

PRESSURE DROP (ATM) 0.67593

ERRORS IN FLOW AND HEAT BALANCE (PERCENT) -0.000 -1.171

APPROXIMATE AXIAL PRESSURE CHANGE ACROSS CORE AT 1/3 AND 2/3 (ATM), --NO GRAVITY -0.67356 -0.67370

RAIUS RANGAL COMPONENT OF THE RELATIVE MASS FLOW RATE (ABSOLUTE) 0.00400

APPARENT RETARD PRESSURE DROP (ATM) 0.67593

AXIAL COMPONENT OF RELATIVE MASS FLOW RATE, G2

RADIAL	0.0	0.0003	0.1606	0.2410	0.2739	0.3068	0.3398	0.3727	0.4056	0.4385	0.4714	0.5043	0.5372
AXIAL	0.0	0.0003	0.1606	0.2410	0.2739	0.3068	0.3398	0.3727	0.4056	0.4385	0.4714	0.5043	0.5372
0.0	0.9788	0.9789	0.9790	0.9803	0.9809	0.9816	0.9822	0.9831	0.9841	0.9853	0.9865	0.9876	0.9889
0.0270	0.9788	0.9789	0.9790	0.9803	0.9809	0.9816	0.9822	0.9831	0.9841	0.9853	0.9865	0.9876	0.9889
0.0556	0.9782	0.9787	0.9793	0.9801	0.9807	0.9814	0.9820	0.9828	0.9839	0.9850	0.9862	0.9872	0.9886
0.0833	0.9779	0.9786	0.9790	0.9799	0.9808	0.9817	0.9826	0.9835	0.9846	0.9857	0.9867	0.9877	0.9890
0.1111	0.9776	0.9781	0.9787	0.9795	0.9801	0.9807	0.9812	0.9819	0.9826	0.9834	0.9841	0.9848	0.9856
0.1389	0.9772	0.9777	0.9783	0.9791	0.9797	0.9803	0.9807	0.9814	0.9820	0.9828	0.9835	0.9842	0.9850
0.1667	0.9768	0.9773	0.9778	0.9786	0.9792	0.9798	0.9802	0.9809	0.9815	0.9822	0.9828	0.9834	0.9841
0.1944	0.9763	0.9769	0.9774	0.9782	0.9788	0.9794	0.9797	0.9803	0.9810	0.9817	0.9823	0.9829	0.9835
0.2222	0.9759	0.9764	0.9770	0.9778	0.9784	0.9790	0.9792	0.9797	0.9804	0.9810	0.9817	0.9823	0.9830
0.2500	0.9755	0.9760	0.9766	0.9774	0.9779	0.9785	0.9787	0.9792	0.9800	0.9806	0.9812	0.9819	0.9826
0.2778	0.9750	0.9756	0.9761	0.9769	0.9775	0.9781	0.9783	0.9788	0.9795	0.9801	0.9807	0.9814	0.9821
0.3056	0.9746	0.9752	0.9757	0.9765	0.9771	0.9776	0.9778	0.9783	0.9790	0.9796	0.9802	0.9809	0.9816
0.3333	0.9742	0.9748	0.9754	0.9761	0.9767	0.9772	0.9775	0.9779	0.9784	0.9790	0.9796	0.9802	0.9809
0.3611	0.9739	0.9745	0.9750	0.9758	0.9763	0.9768	0.9771	0.9775	0.9780	0.9786	0.9792	0.9798	0.9804
0.3889	0.9735	0.9740	0.9746	0.9754	0.9760	0.9765	0.9767	0.9772	0.9778	0.9784	0.9790	0.9796	0.9802
0.4167	0.9732	0.9737	0.9743	0.9751	0.9756	0.9761	0.9764	0.9768	0.9773	0.9779	0.9785	0.9791	0.9797
0.4444	0.9728	0.9734	0.9740	0.9748	0.9753	0.9758	0.9761	0.9765	0.9770	0.9776	0.9782	0.9788	0.9794
0.4722	0.9725	0.9731	0.9736	0.9745	0.9750	0.9755	0.9757	0.9762	0.9767	0.9773	0.9779	0.9785	0.9791
0.5000	0.9722	0.9728	0.9734	0.9742	0.9747	0.9752	0.9755	0.9760	0.9765	0.9771	0.9777	0.9783	0.9789
0.5278	0.9720	0.9725	0.9731	0.9739	0.9744	0.9749	0.9752	0.9757	0.9762	0.9767	0.9773	0.9779	0.9785
0.5556	0.9717	0.9722	0.9728	0.9736	0.9742	0.9746	0.9749	0.9754	0.9760	0.9765	0.9771	0.9777	0.9783
0.5833	0.9715	0.9720	0.9726	0.9734	0.9739	0.9744	0.9747	0.9752	0.9757	0.9762	0.9767	0.9773	0.9779
0.6111	0.9712	0.9717	0.9724	0.9732	0.9737	0.9742	0.9745	0.9750	0.9755	0.9760	0.9765	0.9771	0.9777
0.6389	0.9710	0.9715	0.9721	0.9729	0.9733	0.9738	0.9741	0.9746	0.9751	0.9756	0.9761	0.9767	0.9773
0.6667	0.9708	0.9713	0.9720	0.9728	0.9733	0.9738	0.9741	0.9746	0.9751	0.9756	0.9761	0.9767	0.9773
0.6944	0.9706	0.9712	0.9718	0.9726	0.9731	0.9736	0.9739	0.9744	0.9749	0.9754	0.9759	0.9765	0.9771
0.7222	0.9705	0.9710	0.9716	0.9725	0.9729	0.9734	0.9737	0.9742	0.9747	0.9752	0.9757	0.9763	0.9769
0.7500	0.9703	0.9709	0.9715	0.9723	0.9728	0.9733	0.9736	0.9741	0.9746	0.9751	0.9756	0.9762	0.9768
0.7778	0.9702	0.9707	0.9713	0.9722	0.9727	0.9731	0.9735	0.9740	0.9745	0.9750	0.9755	0.9761	0.9767
0.8056	0.9701	0.9706	0.9712	0.9721	0.9725	0.9730	0.9733	0.9738	0.9743	0.9748	0.9753	0.9759	0.9765
0.8333	0.9700	0.9705	0.9711	0.9720	0.9724	0.9729	0.9732	0.9737	0.9742	0.9747	0.9752	0.9758	0.9764
0.8611	0.9699	0.9704	0.9710	0.9719	0.9723	0.9728	0.9731	0.9736	0.9741	0.9746	0.9751	0.9757	0.9763
0.8889	0.9698	0.9703	0.9710	0.9718	0.9722	0.9727	0.9730	0.9735	0.9740	0.9745	0.9750	0.9756	0.9762
0.9167	0.9698	0.9703	0.9709	0.9718	0.9722	0.9727	0.9730	0.9735	0.9740	0.9745	0.9750	0.9756	0.9762
0.9444	0.9697	0.9702	0.9709	0.9717	0.9722	0.9726	0.9731	0.9735	0.9740	0.9745	0.9750	0.9756	0.9762

0.0000	1000.0	1000.0	1000.0	1000.0
0.0333	1000.0	1000.0	1000.0	1000.0
0.0667	1000.0	1000.0	1000.0	1000.0
0.1000	1000.0	1000.0	1000.0	1000.0
0.1333	1000.0	1000.0	1000.0	1000.0
0.1667	1000.0	1000.0	1000.0	1000.0
0.2000	1000.0	1000.0	1000.0	1000.0
0.2333	1000.0	1000.0	1000.0	1000.0
0.2667	1000.0	1000.0	1000.0	1000.0
0.3000	1000.0	1000.0	1000.0	1000.0

↑ SEVERAL PAGES DELETED

← SPECIAL ACTION

PEBBLE THERMAL CONDUCTIVITY DATA WILL BE RECOVERED

Table 3. CONTINUED

102	0.2787	0.120000E 24	876.4	822.7	847.5	866.1	870.1	-11.0
104	0.2790	0.160195E 22	923.4	852.8	830.1	882.4	881.2	-11.0
105	0.2793	0.165162E 22	929.7	859.1	837.8	888.8	888.4	-11.0
106	0.2796	0.170227E 23	931.9	879.4	840.7	888.2	889.7	-11.0
107	0.2796	0.123159E 23	937.7	882.1	843.2	887.6	882.0	-11.0
108	0.2798	0.123000E 23	943.8	888.7	845.6	888.0	882.4	-11.0
109	0.2798	0.181959E 21	952.1	889.4	877.5	887.8	882.0	-11.0
110	0.2726	0.677030E 21	871.1	871.9	850.5	879.0	880.8	-11.0
111	0.2732	0.131305E 22	518.4	891.1	812.5	897.8	887.4	-11.0
112	0.2784	0.202043E 22	578.1	881.7	850.4	877.1	881.4	-11.0
113	0.2612	0.26007E 22	817.4	877.1	892.1	880.7	880.8	-11.0
114	0.2749	0.327511E 22	854.6	885.1	881.4	881.0	881.0	-11.0
115	0.2787	0.30187E 22	888.2	872.1	877.0	880.8	880.8	-11.0
116	0.2736	0.432601E 22	711.5	888.5	852.5	888.0	887.1	-11.0
117	0.2730	0.003720E 22	733.4	888.4	868.7	889.9	888.0	-11.0
118	0.2726	0.519300E 22	750.8	888.4	878.7	888.4	888.4	-11.0
119	0.2726	0.607650E 22	761.3	888.4	882.6	888.0	888.0	-11.0
120	0.2721	0.713248E 22	771.5	888.1	889.1	887.7	888.0	-11.0
121	0.2723	0.720857E 22	781.9	888.0	888.3	888.0	888.0	-11.0
122	0.2727	0.117250E 23	786.7	888.4	888.6	888.6	888.6	-11.0
123	0.2726	0.19276E 23	788.2	888.7	882.1	888.7	888.7	-11.0
124	0.2729	0.119589E 23	789.7	888.7	887.0	888.7	888.7	-11.0
125	0.2731	0.119069E 23	822.1	888.8	887.3	888.5	888.5	-11.0
126	0.2733	0.120000E 23	825.1	888.8	889.7	888.7	888.7	-11.0
127	0.2637	0.104176E 21	398.2	878.7	883.5	888.0	888.0	-11.0
128	0.0816	0.536101E 21	855.7	878.2	872.5	888.0	888.0	-11.0
129	0.2368	0.101297E 22	815.1	887.6	889.1	888.0	888.0	-11.0
130	0.3000	0.100370E 22	567.5	887.1	850.1	888.0	888.0	-11.0
131	0.2952	0.109351E 22	611.1	888.5	879.8	888.0	888.0	-11.0
132	0.2879	0.273090E 22	686.2	890.7	881.4	888.0	888.0	-11.0
133	0.2836	0.250507E 22	678.2	890.6	880.1	888.0	888.0	-11.0
134	0.2810	0.273879E 22	658.4	888.2	881.1	888.0	888.0	-11.0
135	0.2792	0.291599E 22	718.0	888.4	881.5	888.0	888.0	-11.0
136	0.2780	0.307113E 22	729.0	888.3	889.7	888.0	888.0	-11.0
137	0.2771	0.320195E 22	739.2	882.9	884.4	888.0	888.0	-11.0
138	0.2765	0.331276E 22	749.2	888.0	881.8	888.0	888.0	-11.0
139	0.2761	0.340730E 22	755.4	888.0	882.2	888.0	888.0	-11.0
140	0.2758	0.360995E 22	761.6	888.5	888.1	888.0	888.0	-11.0
141	0.2755	0.390207E 22	767.1	882.7	888.1	888.0	888.0	-11.0
142	0.2753	0.367339E 22	771.7	888.1	887.2	888.0	888.0	-11.0
143	0.2752	0.376530E 22	775.5	888.0	889.9	888.0	888.0	-11.0
144	0.2750	0.381672E 22	778.4	888.4	882.3	888.0	888.0	-11.0
145	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
146	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
147	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
148	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
149	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
150	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
151	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
152	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
153	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
154	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0
155	0.0	0.0	850.0	850.0	850.0	850.0	850.0	0.0

SEVERAL PAGES DELETED

DISTRIBUTION FRACTIONS OF 100 HEAT TEMPERATURES IN TEMPT FRACILES CWT "HT PART" (°) 190.0 22.1
 0.0 0.0 0.0 0.0 0.0 0.01389 0.01300 0.02778 0.08494 0.11387
 0.00694 0.03072 0.02003 0.06367 0.10017 0.11111 0.11902 0.15270 0.18750 0.14501

LOAD AVERAGE TEMP AND TPO2, THEN SUB(COR) 905.10 409.15 0.0 0.0

HEAT TRNS, PEAK/READ BY SOLE, SUICBY 926.7 22.1 0.0 3.0 POWER D/CORPED 789.2 0.0 POWER (WAT) 1650.

AVERAGE AND PEAK TEMPERATURE SLOPE AT PYSNLS 984/SHP/L TRPPACK (DEG/C/M) -87.6 -116.6

CORRELATION FAILURE COUNT 458 0

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